

15

**EXTERNAL NITRIFICATION IN BIOLOGICAL  
NUTRIENT REMOVAL ACTIVATED SLUDGE  
SYSTEMS**

by

Rajan Moodley  
Bsc(Eng)(UCT)

Thesis submitted in partial fulfilment of the requirements  
for the degree of Master of Science in Engineering at the  
University of Cape Town.

Department of Civil Engineering  
University of Cape Town

September 1999

The copyright of this thesis vests in the author. No quotation from it or information derived from it is to be published without full acknowledgement of the source. The thesis is to be used for private study or non-commercial research purposes only.

Published by the University of Cape Town (UCT) in terms of the non-exclusive license granted to UCT by the author.

## ACKNOWLEDGMENTS

The writer wish to express his appreciation and gratitude to the following persons for their contribution to the research work contained in this report:

- Professor G A Ekama and Associate Professor M C Wentzel for their untiring and relentless guidance and support during the experimental investigation and writing up.
- Mr Taliep Lakay, Laboratory Manager, for his invaluable help in running and maintenance of analytical equipment in the laboratory and his immense insight in operating laboratory-scale activated sludge systems.
- Mr Percival Wilsnach, Laboratory Assistant, for his unfailing willingness to assist in tackling any problem encountered during the investigation.
- Charles Nicholas and Denis Botha, Technical Officers, for so ably constructing, maintaining and servicing equipment in the laboratory.
- Mr Peter Tapscott, formerly Scientific Officer at the Scientific Services Branch, Cape Metropolitan Council, for his very important contribution of filament identification during the investigation.
- Ms. Amina Rawat for her support and motivation during the investigation.

Acknowledgment is also due to the Water Research Commission Steering Committee under the chairmanship of Mr Greg Steenveld, for their guidance in this research and to the Water Research Commission, Water Sanitation Services SA (Pty) Ltd; a subsidiary of Lyonnaise Des Eaux : Center for International Water and Environmental Research and the National Research Foundation (formerly Foundation for Research Development) for financial support.

## TABLE OF CONTENTS

	<b>Page</b>
TITLE PAGE	
DECLARATION	
SYNOPSIS	i
ACKNOWLEDGMENTS	viii
TABLE OF CONTENTS	ix
LIST OF FIGURES	xii
LIST OF TABLES	xiv
LIST OF SYMBOLS	xv
<b>1 INTRODUCTION</b>	<b>1.1</b>
<b>2 LITERATURE REVIEW</b>	<b>2.1</b>
2.1 INTRODUCTION	2.1
2.2 NITRIFICATION	2.2
2.3 INTERNAL FIXED MEDIA SYSTEMS	2.3
2.4 EXTERNAL NITRIFYING TRICKLING FILTERS	2.5
2.5 THE DEPHANOX SYSTEM	2.5
2.6 THE PROPOSED EXTERNAL NITRIFICATION SYSTEM	2.7
2.7 OPPORTUNITIES FOR IMPLEMENTATION OF THE PROPOSED SYSTEM	2.7
2.8 PREVIOUS RESEARCH INTO EXTERNAL NITRIFICATION	2.10
2.9 RESEARCH OBJECTIVES	2.11
<b>3 EXPERIMENTAL INVESTIGATION</b>	<b>3.1</b>
3.1 EXPERIMENTAL SET-UP AND CONTROL	3.1
3.2 DATA ACQUISITION AND SYSTEM PERFORMANCE MONITORING	3.6
3.3 COD MASS BALANCE AND REMOVAL PERFORMANCE	3.11
3.4.1 The Effect of Different Configurations on COD Mass Balance	3.16

3.4	NITROGEN MASS BALANCE AND REMOVAL PERFORMANCE	3.17
3.4.1	Influent and Effluent Nitrogen Concentrations	3.17
3.4.2	Nitrogen Mass Balance	3.18
3.4.3	The Effect of Different Configurations on Nitrogen Mass Balance	3.21
3.4.4	Nitrification	3.22
3.4.5	Denitrification	3.24
3.5	BIOLOGICAL EXCESS PHOSPHORUS REMOVAL (BEPR) PERFORMANCE	3.29
3.5.1	P Removal and Effluent P Concentrations	3.29
3.5.2	P Balance over each Reactor and Settler	3.30
3.5.3	Comparison of Measured and Calculated P Removal	3.35
3.5.3.1	Determination of $f_{S,up}$	3.36
3.5.3.2	Dependency of $f_{XBG,P}$ on influent RBCOD concentration and $f_{S,up}$	3.42
3.6	FILAMENT IDENTIFICATION AND SLUDGE SETTLEABILITY	3.45
3.6.1	Filament Identification	3.45
3.6.2	Sludge Settleability	3.47
<b>4</b>	<b>CONCLUSIONS</b>	<b>4.1</b>
4.1	INTRODUCTION AND OBJECTIVES OF INVESTIGATION	4.1
4.2	SYSTEM COD AND N REMOVAL PERFORMANCE	4.3
4.3	NITRIFICATION AND DENITRIFICATION	4.5
4.4	BIOLOGICAL EXCESS PHOSPHOROUS REMOVAL	4.7
4.5	FILAMENT IDENTIFICATION AND SLUDGE SETTLEABILITY	4.8
4.6	DISCUSSION	4.9
<b>5</b>	<b>REFERENCES</b>	<b>R.1</b>
<b>6.</b>	<b>APPENDICES</b>	
6.1	Appendix A	
6.1.1	Daily Results of the External Nitrification BNRAS System.	A.1
6.1.2	Figures A1 to A28 : Graphs of Daily Results.	A.19

6.2	Appendix B	
6.2.1	Nitrogen Mass Balance.	B.1
6.2.2	COD Mass Balance.	B.4
6.3	Appendix C	
6.3.1	Average Sewage Batches Results of External Nitrification System.	C.1
6.3.2	Calculation of $f_{s,up}$ and $f_{x_{bg,p}}$ for External Nitrification System	C.3
6.4	Appendix D	
6.4.1	Daily Results of the UCT Control System	D.1
6.4.2	Figures D1 to D18 : Graphs of Daily Results	D.12
6.4	Appendix E	
6.4.1	Average Sewage Batch Results of UCT Control System	E.1
6.4.2	Calculation of $f_{s,up}$ and $f_{x_{bg,p}}$ for UCT Control System	E.1
6.4.3	Figures E1 to E14 Graphs of Average Results of UCT System	E.2
6.5	Appendix F	
6.5.1	Filament identified in external nitrification (EXT) and UCT control systems	F.1

## LIST OF FIGURES

FIGURE	DESCRIPTION	PAGE
2.1	The DEPHANOX biological nutrient removal system (after Bortone et al., 1996; Sorm et al., 1996)	2.6
2.2	Conventional integration of trickling filters with biological nutrient removal activated sludge removal systems.	2.9
2.3	Proposed integration of trickling filters with biological nutrient removal activated sludge systems : Nitrification is achieved externally on nitrifying trickling filters	2.9
3.1	Schematic layout of External Nitrification BNRAS system.	3.1
3.2	Details of fixed media stone column flow control and measurement.	3.3
3.3	Details of external suspended media nitrifier.	3.11
3.4	COD mass balance of external nitrification system for 37 sewage batches.	3.12
3.5	COD mass balance components of BNRAS system for 37 sewage batches.	3.13
3.6	Average sewage batch influent and effluent COD concentrations.	3.13
3.7	Average sewage batch influent and effluent nitrogen concentrations.	3.17
3.8	Nitrogen mass balance of BNRAS system for 37 sewage batches.	3.18
3.9	Nitrogen mass balance components for the 37 sewage batches.	3.19
3.10	Nitrification and Denitrification of BNRAS system for 37 sewage batches.	3.24
3.11	Average sewage batch influent and effluent P concentrations.	3.30
3.12	Components of P release and P uptake over all reactors and settlers in external nitrification system for the 37 sewage batches.	3.32
3.13	Average Anoxic/Aerobic P uptake for the 37 sewage batches.	3.33
3.14	Diagrammatic representation of the utilization of the Total influent COD in the model of Wentzel <i>et al.</i> (1990).	3.37
3.15a	P content of PAOs ( $f_{XBG,P}$ ) calculated for each sewage batch using the model of Wentzel <i>et al.</i> (1990).	3.39

3.15b	P content of PAOs ( $f_{\text{XBG,P}}$ ) calculated for each sewage batch fed to the system using the UCT model of Wentzel <i>et al.</i> (1990).	3.42
3.17	Comparison of P content of PAOs ( $f_{\text{XBG,P}}$ ) of UCT and external nitrification systems for sewage batches 2 to 19.	3.44
3.18	$f_{\text{XBG,P}}$ dependence on calculated $f_{\text{S,up}}$ fraction determined from the model of Wentzel <i>et al.</i> (1990).	3.45
3.19	Relationship between Diluted Sludge Volume Index (DSVI) and the main anoxic reactor nitrate concentration.	3.50
3.20	Relationship between Diluted Sludge Volume Index (DSVI) and the final effluent nitrate concentration.	3.51

## LIST OF TABLES

TABLE	DESCRIPTION	PAGE
2.1	Principal organism groups included in models for activated sludge systems, their functions and the zones in which these functions are performed.	2.2
3.1	External nitrification BNRAS system design and operating parameters.	3.2
3.2	Changes and Stoppages to the BNRAS system.	3.5
3.3	Sampling position and parameter measurement.	3.6
3.4	Summary of measured parameters with corresponding Figure numbers.	3.7
3.5	Components of COD mass balance and percentage COD removal.	3.14
3.6	Components of nitrogen mass balance and percentage N removal.	3.20
3.7	Nitrate and Nitrite mass balance across each each reactor and settler.	3.23
3.8	Calculated denitrification rates for sewage batches with $> 1 \text{ mg NO}_3\text{-N/l}$ in the main anoxic reactor.	3.27
3.9	Comparison of denitrification rates found in this investigation to those found in earlier investigations.	3.28
3.10	Average P release, uptake and net P removal for 37 sewage batches.	3.31
3.11a	Calculated $f_{\text{XBG,P}}$ and $f_{\text{S,up}}$ for the 37 sewage batches using model of Wentzel et al .(1990).	3.38
3.11b	Calculated $f_{\text{XBG,P}}$ for 37sewage batches with $f_{\text{S,up}} = 0.13$ in the model of Wentzel et al .(1990)	3.40
3.11c	Calculated $f_{\text{XBG,P}}$ and $f_{\text{S,up}}$ for the 21 sewage batches fed to the UCT system using model of Wentzel et al .(1990)	3.41
3.12	The percentage Dominance and Occurrence of filaments in the external nitrification and UCT systems.	3.46

## LIST OF SYMBOLS

SYMBOL	DESCRIPTION
$\mu_{nm}$	Maximum Specific growth rate of nitrifiers (/d)
AVSS	Active volatile suspended solids
BEPR	Biological excess phosphorous removal
$b_{HT}$	Specific Endogenous mass loss rate for heterotrophic organisms at T°C (/d)
$b_{nT}$	Specific Endogenous respiration rate for heterotrophic organisms at T°C (/d)
COD	Chemical oxygen demand
CTL	UCT control system
$D_{pl}$	Denitrification potential of main anoxic reactor
DSVI	Diluted sludge volume index
Ext(nit)	External nitrification BNRAS system
$f_{av,OHO}$	Active fraction of the sludge with respect to the OHOs
$f_{bs}$	Fraction RBCOD of the influent with respect to the biodegradable COD concentration
$f_{cv}$	COD to VSS ratio of the volatile sludge mass
$f_{S,up}$	Unbiodegradable particulate COD fraction in the influent
$f_{S,us}$	Unbiodegradable soluble COD fraction in the influent
$f_{XBG,P}$	Fraction of PAO biological active mass that is phosphorous
K	General parameter for denitrification rate (mgNO <sub>3</sub> /mgAVSS/d). Subscripts 1 and 2 refer respectively to the 1 <sup>st</sup> and 2 <sup>nd</sup> rates in the anoxic reactor
MUCT	Modified UCT system configuration
N	Nitrogen
N <sub>2</sub>	Nitrogen gas

NaHCO <sub>3</sub>	Sodium hydrogen carbonate
NH <sub>4</sub>	Saline ammonia
NO <sub>2</sub> <sup>-</sup>	Nitrite
NO <sub>3</sub> <sup>-</sup>	Nitrate
NO <sub>x</sub> <sup>-</sup>	Nitrite + Nitrate
OHO	Ordinary heterotrophic organism
OUR	Oxygen utilization rate (mgO/l/h)
P	Phosphorus
PAO	Poly-phosphate accumulating organism
RBCOD	Readily biodegradable COD
R <sub>s</sub>	Sludge age (days)
SBCOD	Slowly biodegradable COD
SCFA	Short chain fatty acids
S <sub>ii</sub>	Total COD concentration in the influent (mgCOD/l)
TKN	Total Kjeldahl Nitrogen
TP	Total Phosphorous
TSS	Total suspended solids
UCT	University of Cape Town
VFA	Volatile fatty acids
VSS	Volatile suspended solids
Y <sub>h</sub>	Heterotrophic organism yield coefficient = 0.45 mgVSS/mgCOD
Y <sub>n</sub>	Nitrifier organism yield coefficient = 0.10 mgVSS/mgN
WRC	Water Research Commission

*I dedicate the fruits of this work  
at THy lotus feet and those of my parents,  
without whom this would not have been possible.*

University of Cape Town

## SYNOPSIS

### INTRODUCTION

In conventional nitrification-denitrification biological excess phosphorous removal (NDBEPR) activated sludge systems, such as the UCT system for example, both nitrification and phosphorous uptake (P uptake) occur simultaneously in the, usually large, aerobic reactor. In the UCT system the nitrate load to the anoxic reactor is limited by the a-recycle (i.e. system constraint recycle from the aerobic to the anoxic reactor) and the internal aerobic nitrification performance. The latter process, is mediated by the nitrifiers having a slow growth rate of 0.45/d, governs the sludge age of the biological nutrient removal activated sludge (BNRAS) system and thus results in long (20 - 25 day) sludge ages and large aerobic mass fraction requirements to nitrify completely. However, if stable nitrification could be achieved outside the BNRAS external nitrification (EN) system then nitrification and the suspended solids sludge age become uncoupled allowing greater flexibility into the BNRAS system. EN has the benefits of (i) reducing the sludge age by at least half (i.e. to 8 - 10 days) (ii) reducing the aerobic volume requirements by at least a third or alternatively doubling the wastewater that can be treated (iii) allowing increase in either or both the anaerobic and anoxic reactor volumes which should improve BEPR (Wentzel *et al.*, 1990) and denitrification and thus N removal (WRC, 1984) respectively (iv) allowing a constant, higher load of nitrate to the anoxic reactor which is less constrained by the systems operating and design parameters (v) making the system more robust because the sensitive nitrifiers are not affected by perturbations in the BNRAS system since the very long sludge age EN biofilm/suspended nitrifying biomass is independent of the BNRAS systems sludge mass and sludge age (vi) improves the sludge settleability of the system due to the absence of the poor floc-forming nitrification biomass and the improved denitrification in the larger anoxic mass fraction.

### AIMS AND OBJECTIVES

Simultaneous external nitrification and anoxic phosphate uptake was studied in a BNR activated sludge systems with varying aerobic mass fractions. The aims of the experiments were to; (i) establish a stable population of slow-growing nitrifiers on a fixed media external nitrification system (later changed to a suspended medium due to *Psychoda* larvae infestation of the fixed

media stone column), (ii) double the volume of the wastewater treated to test one of the claimed benefits of the external nitrification system, (iii) promote conditions to achieve anoxic phosphate uptake, (iv) increase the aerobic mass fraction in an attempt to qualify its effect on anoxic P uptake, and (v) study the effect of increased aerobic mass fraction on the sludge settleability of the BNRAS system.

#### SYSTEM SET-UP AND MONITORING

The aims of the investigation were achieved by installing an internal settler and a fixed media (and later a suspended media) external nitrification system between the anaerobic and anoxic reactors of a BNRAS system. To establish and fully utilize the denitrification potential of the BNRAS anoxic reactor, nitrate was also dosed as a concentrated solution of 0.5 to 1.25 mg/l at 0.5 l/d directly to main anoxic reactor. A pre-anoxic reactor was also set-up ahead of the anaerobic reactor to ensure a near zero nitrate concentration entering the anaerobic reactor. This modified DEPHANOX system (after Bortone *et al.*, 1996) referred to as Configuration 1, has the benefits of (i) efficient utilization of organic substrate for both phosphorus and nitrogen removal, reducing the competition between ordinary heterotrophic organism (OHOs) denitrifiers and polyphosphate accumulating organisms (PAOs) (ii) not exposing the sensitive aerobic nitrifiers of the fixed/suspended media to either anaerobic or anoxic conditions as in conventional BNR activated sludge systems (iii) promoting the potential for anoxic P uptake because of the constant high load of nitrate and improved denitrification in the large anoxic reactor and (v) reducing the aerobic P uptake because of the reduced aerobic mass fraction.

During the first stage of the investigation external nitrification was achieved with the stone column fixed media system, which covered the period from day 1 to day 205. During this time a number of changes were made to Configuration 1, (a) which resulted in Configuration 2 (day 31 to day 154), (b) Configuration 3 (day 155 to day 205). From day 206 to day 373 the fixed media stone column was replaced with a suspended nitrification activated sludge system (Configuration 4) because of the poor nitrification performance due to *Psychoda* larvae infestation of the stone column. To monitor the performance and operation of these different system configurations samples were drawn virtually daily from each of the reactors, internal tank supernatant, the external nitrified outflow and the final effluent for TKN, FSA,  $\text{NO}_2/\text{NO}_3$ , COD

and P analysis throughout the 373 day investigation.

## RESULTS

### Mass balances

To establish the reliability of the experimental data, COD and N mass balances were performed on the BNRAS external nitrification system. In these balances, the mass entering the system is reconciled with the mass leaving the system and the reliability of the data is directly proportional to the mass balance deviation from 100%. The average COD and N mass balances were 80% and 91% respectively. Although considerably lower than 100%, these do not differ appreciable from COD and N balances observed in other investigations on BNR systems (Pilson *et al.*, 1995; Hu *et al.*, 1999).

### COD and N removal performance

The concentrated solution of nitrate dosed directly to the main anoxic reactor increased the influent TKN/COD ratio from around 0.08 to 0.14 mgN/mgCOD and produced a effluent total N concentration <20 mgN/l. The average percentage COD and N removals in the EN BNRAS system were 91% and 72% respectively. The main reason for the low N removal was poor nitrification in the fixed media stone column leading to high effluent TKN concentrations. The overall average 0.45<sub>µm</sub> membrane filtered effluent COD concentration from the BNRAS external nitrification system was 52 mgCOD/l, giving an unbiodegradable soluble fraction  $f_{s,us}$  of 0.075. The filtered effluent TKN concentration was not measured and thus the unbiodegradable soluble TKN fraction ( $f_{nu}$ ) was not determined, however, the overall unfiltered effluent TKN concentration was 18 mgN/l.

### Oxygen utilization rate and mixed liquor concentrations

The average oxygen utilization rate (OUR) for sewage batches 1 to 20 (days 1 to 154; Configurations 1 and 2) was 35 mgO/l aerobic reactor/h and 38 mgO/l aerobic reactor/h for sewage batches 21 to 37 (days 155 to 373; Configurations 3 and 4). This increased OUR was due to the increased aerobic mass fraction for Configuration 3 and 4 which supported nitrifiers in the aerobic reactor of the BNRAS system, and also because in Configuration 3 the fixed media stone column nitrified poorly, significant nitrification took place in the aerobic reactor. The

mean TSS and VSS concentrations in the BNRAS external nitrification system were 2628 mgTSS/l and 2163 mgVSS/l respectively, giving an average VSS/TSS ratio of 0.82.

### **External nitrifier performance**

In this investigation the primary aim was to establish a stable nitrifier population on a fixed media such that nitrification could be "restricted" to the fixed media system, thus enabling nitrification and the suspended solids sludge age to be uncoupled. However, due to the limitation imposed by the flow rate to the external nitrification system of about 76% of the flow leaving the anaerobic reactor, with 24% of the flow bypassing the external nitrification system, the maximum nitrification completion could be at best 76%, if the nitrifier outflow ammonia concentration was zero. Initially the fixed media stone column (SC) nitrifier produced a low effluent ammonia concentration of 3mgN/l which represented an 88% nitrification (Configuration 1) efficiency. However, due to *Psychoda* mothfly larvae infestation the nitrification efficiency fell below 50% and produced a wide and varied effluent SC ammonia concentration between 8 and 62mgN/l. In order to re-establish the external nitrification efficiency and prevent *Psychoda* infestation, a suspended medium external nitrifier replaced the fixed media SC to facilitate the nitrification process (Configuration 4). The suspended medium external nitrifier produced a low BNRAS effluent ammonia concentration of 9mgN/l.

### **BEPR and denitrification**

The effluent P concentration in the EN BNRAS system were kept above 5 mg/l by dosing P to the influent. This allowed the system P removal capacity of 10.4mgP/l influent or alternatively 0.015mgP/mgCOD to be measured. The average P release of 18 mg P/l influent took place in the anaerobic reactor and the P uptake was facilitated in both the aerobic and main anoxic reactors with 15.5 and 15.4mg /l influent respectively. The latter translates into 50% and 49% P uptake taking place in the aerobic and main anoxic reactors respectively. In this investigation, a too low nitrate load on the main anoxic reactor during sewage batches 7 to 23 (days 63 to 188) appeared to have a detrimental effect on the anoxic P uptake, and ultimately the P removal was reduced to 8.3 mgP/l. Increasing the aerobic mass fraction (Configurations 3 and 4) improved BEPR and surprisingly, also stabilized anoxic P uptake. This is in agreement with the literature: In an investigation to select DPAOs, Bortone *et al.* (1996) operated an anaerobic/anoxic

sequencing batch reactor (SBR). They found that this system did not stimulate BEPR. However, when a short aerobic period was included in the SBR cycle, stable BEPR with anoxic P uptake (and aerobic P uptake) was obtained. Thus it would appear that an aerobic period may be essential for stable anoxic P uptake. Recognizing that the anoxic P uptake DPAOs are facultative organisms, including an aerobic reactor would provide opportunity for aerobic metabolism by these organisms, in addition to the anoxic metabolism. Biochemically, aerobic metabolism provides a higher energy yield for the organism than anoxic metabolism, and this higher energy yield may provide the biological niche for DPAOs to stably exist in the system.

Because substantial anoxic P uptake (46%) was observed in the BNRAS external nitrification system, denitrification was therefore mediated by both the ordinary heterotrophic organisms (OHOs) and the polyphosphate accumulating organisms (PAOs). The relative contribution of the PAOs to the denitrification rate was assumed to be the percentage anoxic uptake times the nitrate equivalent of the readily biodegradable COD taken up by the PAOs in the anaerobic reactor (determined from the Wentzel et al., 1990 steady state BEPR model), viz: %Ax Pupt\*RBCOD taken up by PAOs/8.6 where 8.6 is the COD utilized per mg nitrate denitrified. With this approach it was found that the relative contribution of the PAOs to the denitrification rate is quite small - only 17% of the total rate because they utilize relatively little COD compared with the OHOs. The average OHO and PAO denitrification rates ( $K_2''_{\text{OHO}}$  and  $K_2''_{\text{PAO}}$ ) were found to be 0.1206 mgNO<sub>3</sub>-N/(mgOHOAVSS.d) and 0.0496 mgNO<sub>3</sub>-N/(mgPAOAVSS.d). If the observed nitrate removal in the anoxic reactor (overloaded with nitrate) were attributed to the OHOs then the uncorrected specific denitrification rate ( $K_2'$ ) is 0.1379 mgNO<sub>3</sub>-N/(mgOHOAVSS.d). This  $K_2'$  is rate has the same bases as the  $K_2'$  rates measured in earlier investigations by Clayton *et al.* (1989) and Sneyders *et al.* (1998) in which no anoxic P uptake was observed and Musvoto *et al.* (1992), Pilson *et al.* (1995) and Mellin *et al.* (1995) in which significant anoxic P uptake was observed.

To determine the unbiodegradable particulate fraction  $f_{s,\text{up}}$  of the influent sewage fed to the system, the appropriate  $f_{s,\text{up}}$  was selected so that the system VSS mass calculated with the BEPR model of Wentzel *et al.* (1990) was equal to that measured using the measured readily biodegradable (RB) COD concentration and the influent characteristics of the sewage ( $f_{s,\text{us}}$ ,  $S_{\text{ti}}$ )

and the system parameters as input. An average  $f_{s,up}$  value of 0.11 was found for the BNRAS external nitrification system. The active ordinary heterotrophic (OHO) and polyphosphate accumulating (PAO) organism fractions of the VSS which are required to define the OHO denitrification rate ( $K_2'$ ) and the P content of the PAOs ( $f_{XBG,P}$ ), are also obtained from the calculation procedure. The  $f_{XBG,P}$  fraction was obtained by adjusting the  $f_{XBG,P}$  value (mgP/mgPAOAVSS) in the model until the calculated P removal equaled the measured P removal. An average  $f_{XBG,P}$  value of 0.312 mgP/mgPAOAVSS was found for the EN BNRAS system. In comparing the  $f_{XBG,P}$  fraction obtained in this investigation with those obtained in earlier investigations it was confirmed that a lower  $f_{XBG,P}$  value is obtained when significant (> 40%) anoxic P uptake (as in this investigation) is observed than when aerobic P uptake is observed.

#### **Filament identification and sludge settleability**

The most frequently dominant Anoxic Aerobic (AA, low F/M) filament was *M. parvicella*, while type 1851 and type 0092 were also identified as secondary filaments. Type 021N also occurred but being a septic sewage filament (Jenkins *et al.*, 1984) this was probably due to aging sewage during storage. Apart from type 021N, these filaments are almost always observed in full scale NDBEPR systems (Blackbeard *et al.*, 1998).

The average  $NO_x$  concentrations leaving the anoxic reactor in the EN BNRAS system was 2.8 mg $NO_x$ -N/l. The stone column external nitrification system (Configuration 3) was replaced with the activated sludge system (Configuration 4) which led to a significant improved nitrification efficiency, the aerobic mass fraction was increased to 30% at the expense of the anoxic mass fraction (30%), the sludge age was increased from 8 to 10 days and a 1:1 mixed liquor a-recycle from the aerobic to the anoxic reactor was installed. All these changes led to increased nitrate load on the main anoxic reactor and a decreased denitrification potential leading to high nitrate and nitrite concentration in the outflow of the anoxic to the aerobic reactor. According to the hypothesis of Casey *et al.*, (1994) for proliferation of Nitrosomonas filaments, these high concentrations will impact sludge settleability evident in the latter stage of this investigation.

The mean DSVI in the EN BNRAS system was 94 ml/g (standard deviation 27). This DSVI is ideal (between 80 and 100 ml/g). The fluctuations in the DSVI from ~125 ml/g at the start of the investigation to 80 ml/g mid-way through the investigation and finally to ~150 ml/g at the end of the investigation is a direct result of change in the external nitrification system and the increase in the aerobic mass fraction and sludge age (Configuration 4). This period was also the time in which aerobic nitrification was significant which meant that the BNRAS external nitrification system now supported nitrifiers leading to higher effluent  $\text{NO}_x$  concentrations. This observation i.e. an increase in the  $\text{NO}_x$  concentration leaving the anoxic reactor with the increase in aerobic mass fraction and with the simultaneous increase in the DSVI, supports the hypothesis of Casey *et al.* (1994).

## CONCLUSIONS

Evaluation of the external nitrification biological nutrient removal activated sludge system (BNRASS) at laboratory-scale indicates that the scheme holds considerable potential for a step increase in system intensification through the reductions in sludge age and oxygen demand and significant improvement in sludge settleability. Because the BNRASS is not required to nitrify, its anoxic fraction can be considerably enlarged at the expense of the aerobic mass fraction creating conditions that (i) allow it to achieve high N removal with domestic wastewaters with high TKN/COD ratios and (ii) promote anoxic P uptake polyphosphate accumulating organisms (PAOs). The only negative factors are the slightly reduced BEPR (if anoxic P uptake is a requirement) and *Psychoda* larvae infestation of the fixed media external nitrification system at laboratory scale because of the ideal conditions conducive to rapid infestation.

# CHAPTER 1

## INTRODUCTION

The biological nutrient removal (BNR) activated sludge system (ASS) has become an established technology in wastewater treatment practice. This development has been facilitated by an improved understanding of the nitrification and denitrification (ND) and biological excess phosphorus removal (BEPR) processes. However, implementation of BNR has brought with it a new set of difficulties (Ekama and Wentzel, 1997), the main ones being (i) the long sludge age required for nitrification, (ii) filamentous organism bulking and (iii) the treatment /disposal of supernatants generated from the sludge and solids handling. This research project focuses on the long sludge age requirement for nitrification and investigates means by which nitrification can be successfully achieved external to the BNR activated sludge system to reduce the sludge age.

In the BNR activated sludge (BNRAS) system, the requirement to nitrify governs selection of the two linked parameters, sludge age and the aerated mass fraction. The need for nitrogen (N) and phosphorus (P) removal sets a requirement for a part of the sludge to be unaerated, for anaerobic<sup>1</sup> conditions to stimulate P removal and anoxic<sup>1</sup> conditions for N removal. In N and P removal plants, the unaerated sludge mass fraction usually needs to be high i.e. > 40%, causing the aerated mass fraction to be reduced, i.e. < 60 %. To compensate, to ensure near complete nitrification, long sludge ages have to be selected. For example, with a maximum specific growth rate of nitrifiers at 20° C ( $\mu_{nm20}$ ) of around 0.45/d, to guarantee nitrification at the minimum temperature of 14° C, the system sludge age must be around 20 to 25 days if 50 to 60 % of the sludge mass in the system is unaerated. Such long sludge ages result in large biological reactors per Ml wastewater (WW) treated. If nitrification can be made independent of the suspended solids sludge age, then the selection of the sludge age will no longer be governed by the requirement to nitrify, but rather by the N removal (denitrification) and P removal (BEPR) processes. For both these processes, a reduction in sludge age increases respectively the N and P removal per

---

<sup>1</sup>In this research, the term anaerobic is applied to a zone in which no nitrate/nitrite and dissolved oxygen (DO) is present or enters it, and anoxic to one where nitrate/nitrite is present or enters, but no DO is present or enters.

mass of organic load (WRC, 1984; Wentzel *et al.*, 1990), provided the sludge age remains longer than some lower limit to prevent “wash-out” of P removal and denitrifying organisms. Indications are that, if nitrification and the sludge age of the suspended solids can be uncoupled, then the sludge age can be reduced to less than half, from about 20-25 days to about 8-10 days. This will result in a reduction in the biological reactor volume requirement per Ml treated of about 1/3rd, or alternatively in an increase in the treatment capacity of some 50% (provided secondary settling tank area requirements are appropriately accommodated).

BNRAS systems have been found to promote the growth of a specific group of filamentous microorganisms, previously called low F/M (Jenkins *et al.*, 1984) but renamed anoxic/aerobic (AA) (Casey *et al.*, 1994) because of their frequent occurrence in biological N removal systems. These filamentous organisms cause sludges to settle poorly, resulting in an increase in the required surface area of secondary settling tanks. If the settleability of BNR sludges can be improved, then the flow through existing secondary settling tanks can be increased considerably, or, alternatively for a proposed system the secondary settling tank area can be considerably reduced, both options providing significant economic benefit. Casey *et al.* (1994) have identified two main causes for AA filament proliferation in BNRAS systems; (i) Aerated sludge mass fractions in the range 20 to 70 % and (ii) incomplete denitrification ( $\text{NO}_x > 1.0 \text{ mgN/l}$ ) in the anoxic reactor preceding the aerobic reactor. The uncoupling of nitrification and sludge age will introduce greater flexibility into the BNRASS configuration and should allow elimination of the two conditions identified above which promote AA filament growth.

One method to uncouple the suspended solids sludge age from the requirement to nitrify is to remove nitrification from the BNR activated sludge system to an external fixed media system for attached nitrifier growth. From the above, such an external nitrification system therefore holds promise of a significant system intensification by reducing the systems suspended solids sludge age and improving sludge settleability while retaining BNR. Because there are many wastewater treatment plants in South Africa where there are both old trickling filters and new BNRAS systems, there are many opportunities to implement the external nitrification scheme to realize the potential savings through increased wastewater treatment capacity of the scheme.

The primary objective of this investigation is to evaluate the external nitrification scheme at laboratory scale. In Chapter 2 a literature review is presented so that the objectives of this investigation is placed in context of the current research into external nitrification in BNR activated sludge systems. In Chapter 3 the experimental investigation is described in detail and in Chapter 4 the conclusions of the investigation are presented.

## CHAPTER 2

### LITERATURE REVIEW

#### 2.1 INTRODUCTION

The function of the single-sludge activated sludge systems has expanded from chemical oxygen demand (COD) removal to include, progressively, nitrification, denitrification and phosphorous removal, all biologically mediated in order to comply with more stringent effluent legislation. Not only have these expansions increased the complexity of the system configuration and its operation, but concomitantly the number of biological processes influencing the effluent quality and the number of compounds involved in these processes have increased.

The expansion in function of the activated-sludge system has been accomplished by manipulating the system configuration (through the incorporation of multiple in-series reactors, some aerated and others not, with various inter-reactor recycles) and the wastewater characteristics (through for example, primary sedimentation or acid fermentation of primary sludge). The objectives of these manipulations is to create environmental conditions in the activated sludge system that are conducive to the optimal growth and action of organisms that naturally perform the biological reactions necessary to treat the wastewater viz: aerobic zones for organic material breakdown and nitrification, anoxic zones for denitrification, and an anaerobic-aerobic sequence of zones, with the influent fed to the anaerobic zone, for BEPR. For the purpose of design, in the highly diverse mixed cultures that develop in these activated sludge systems, only the mass behaviour of the populations or groups of organisms is considered. The principal organism groups their functions, and the zones in which these functions are performed are summarized in Table 2.1.

From Table 2.1, for the design of nitrification-denitrification BEPR (NDBEPR) activated-sludge systems, three organism groups and their interactions must be taken into account (Wentzel *et al.*,

**Table 2.1** Principal organism groups included in models for activated sludge systems, their functions, and the zones in which these functions are performed.

Organism	Biological Process	Zone
1. Ordinary heterotrophs (OHOs)	COD removal (organic degradation; dissolved oxygen uptake)	Aerobic
	Ammonification (organic -N → NH <sub>4</sub> <sup>+</sup> )	Aerobic
	Denitrification (organic degradation; NO <sub>3</sub> <sup>-</sup> → NO <sub>2</sub> <sup>-</sup> → N <sub>2</sub> )	Anoxic
	Fermentation (F-RBCOD <sup>a</sup> → SCFA)	Anaerobic
2. Poly-P heterotrophs (PAOs)	P release (SCFA <sup>b</sup> uptake; PHA <sup>c</sup> storage)	Anaerobic
	P release (SCFA uptake; PHA storage)	Anoxic
	P uptake (PHA degradation; denitrification?)	Anoxic
	P uptake; P removal (PHA degradation; dissolved oxygen uptake)	Aerobic
3. Autotrophs (nitrifiers, ANOs)	Nitrification (NH <sub>4</sub> <sup>+</sup> → NO <sub>2</sub> <sup>-</sup> → NO <sub>3</sub> <sup>-</sup> ; dissolved oxygen uptake)	Aerobic

<sup>a</sup> Fermentable readily biodegradable COD

<sup>b</sup> Short-chain fatty acid.

<sup>c</sup> Polyhydroxyalkanoate.

1992): (1) heterotrophic organisms unable to accumulate polyphosphate (poly-P), termed ordinary heterotrophic organisms (OHOs); (2) heterotrophic organisms able to accumulate poly-P, generally called poly-P accumulating organisms (PAOs) (and variously phosphotrophs, bio-P organisms, or poly-P organisms); and (3) autotrophic organisms mediating nitrification, termed autotrophic nitrifier organisms (ANOs). The main focus of this review is on the autotrophic organism group which mediates nitrification.

## 2.2 NITRIFICATION

Nitrification is carried out by two different consecutive microbial processes, nitritification and nitrification. In nitritification, free and saline ammonia (FSA) is converted to nitrite due to its

oxidation by the ammonia oxidizing bacteria traditionally deemed to be *Nitrosomonas*. In nitrification, the nitrate oxidising bacteria, traditionally deemed to be *Nitrobacter*, but recently identified to be *Nitrosospira*, convert nitrite to nitrate. The ammonia and nitrite oxidizers are aerobic and autotrophic bacteria and are characterized by low specific growth rates. Thus the requirement to nitrify governs the sludge age of biological nutrient removal activated sludge systems (BNRAS). For maximum specific growth rate of nitrifiers of 0.45/d ( i.e.  $\mu_{nm}$  at 20°C ), to ensure nitrification the sludge age must be between 20 to 25 days with at least 40 to 50% of the sludge mass in the system aerated. The long sludge age leads to large volume reactors being required as well as the additional cost for the provision of oxygen to aerate these large reactors.

To uncouple the suspended solids sludge age from the requirement to nitrify, the activated sludge system can be modified in two ways, by including (i) internal and (ii) external fixed media for attached nitrifier growth. The nitrifiers grow on the fixed media establishing a population permanently resident in the nitrification system. These nitrifiers are not subjected to either the unaerated-aerated reactor interchanges or to the suspended solids sludge age with the result that the latter can be reduced to less than half, i.e from 20 to 25 days to 8 to 10 days, without losing nitrification .

### 2.3 INTERNAL FIXED MEDIA SYSTEMS

Randall *et al.* (1996) integrated into the aerobic zone of a single-sludge anoxic-aerobic treatment plant rope-like Ringlace fixed-film media which were installed in a volume of 475m<sup>3</sup> for a pilot investigation. The purpose of the integrated fixed-film media was to upgrade the short hydraulic retention time (HRT) basin (6 hrs nominal) for efficient, year round nitrogen removal without construction to increase the basin volume. The integrated Ringlace media increased the nitrification rate per unit volume to 225%, attaining a value of 1.75kg/d NH<sub>3</sub>-N nitrified per linear meter Ringlace media at 15°C. The media also increased denitrification in the aerobic media section to the extent that between 30 and 88% of the nitrates formed in this section were denitrified within it.

The results of Randall *et al.* (1996) showed that optimum nitrification and denitrification only

occurred in the fixed-film media when the supply of biodegradable COD to the fixed-film media section was sufficient to ensure biofilm growth, and when the ammonium-N supply was sufficient to maintain a substantial nitrifier population on the Ringlace media biofilm. This means that the successful denitrification/nitrification process efficiencies are dependent on the influent biodegradable COD and ammonia concentrations respectively. The results also showed that it is difficult to obtain optimum nitrification rates on Ringlace media when the sludge age of the suspended solids is too short and results in washout of nitrifiers from the fixed film Ringlace media. Randall *et al.* (1996) observed that the nitrification efficiency decreased at high ammonia concentrations (i.e. > 5mg/l) due to the simultaneously higher COD concentrations which stimulated heterotrophic bacterial growth that overgrew the nitrifiers and reduced their efficiency. This overgrowth of heterotrophic bacteria was possibly the reason for the high denitrification rates in the aerobic media section; possibly the biofilm was so thick and overgrown by heterotrophic bacteria that oxygen was utilized on the surface of the biofilm and could not penetrate deep into the biofilm, thus allowing the underlying biofilm to become anoxic and denitrify the nitrates generated in the aerobic media section. Supposedly, if this explains the occurrence of denitrification in the aerobic media section, it would imply that even though the nitrification efficiency quoted earlier (225%) was high, it does not mean that the nitrate produced was high (i.e. only 0.047 mgNO<sub>3</sub>-N/l per linear meter) since the nitrification efficiency was good only at low influent ammonia concentrations thus enabling the high denitrification efficiency.

From this research it would seem that internal fixed-film media would only be beneficial if: (1) the aerobic reactor is sufficiently large to accommodate the fixed-film media without hindering COD removal; (2) the influent biodegradable COD and ammonia concentrations are sufficiently high to promote denitrification and nitrification respectively, but, that the COD and ammonia concentration are not too high to cause a decrease in the nitrification efficiency. The effectiveness of the internal fixed media has not been as good as expected, the influent wastewater has to be carefully monitored; it yields a rather low cost/benefit ratio and the effect of the internal fixed media on BEPR has not been investigated. To resolve these difficulties, a BNRAS system in which nitrification is removed from the BNRAS system to an external fixed media system is proposed.

## 2.4 EXTERNAL NITRIFYING TRICKLING FILTERS

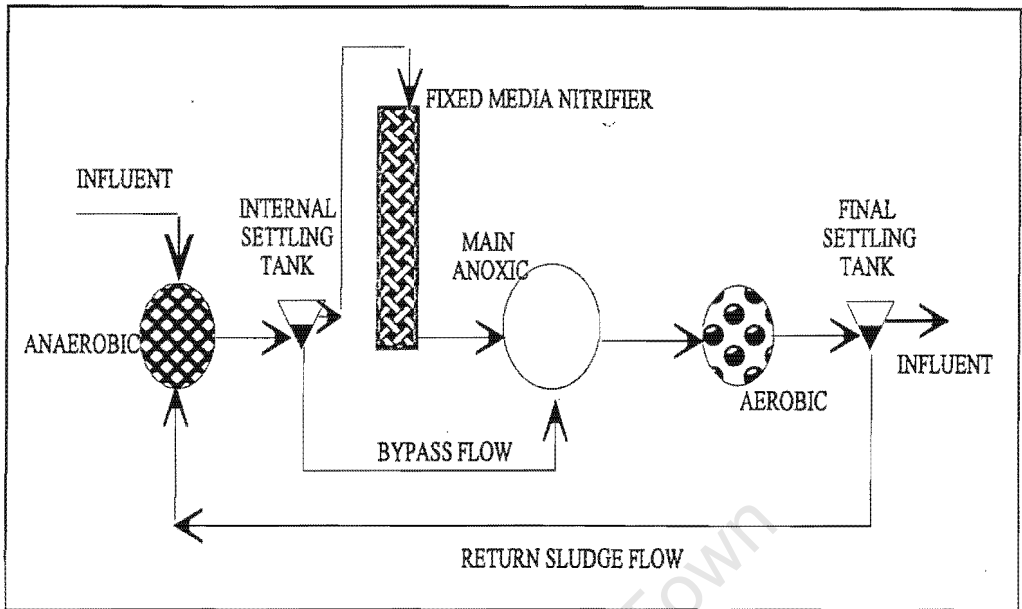
Trickling filters, in contrast with suspended activated sludge processes provide a support medium for biofilm growth. They are the most suitable external artificial environment for nitrification, since they allow the nitrifying bacteria to cultivate a 'permanent' population which remains in the filter for long periods of time i.e. long sludge age.

Tertiary nitrifying trickling filters which are employed for nitrification only and negligible organic material removal, are fairly common in USA (Lutz *et al.*, 1990). While certain problems with macro fauna (snails, worms, larvae, and flies), which reduce nitrification rates, have been encountered, high removals of ammonia have been economically achieved in tertiary nitrifying trickling filters (Parker *et al.*, 1989; 1995; 1996). Therefore, while some full scale trials would need to be done to determine how rock media trickling filters can be adapted to fulfill the external nitrification function, from USA experience this is not expected to be a major problem in implementing the external nitrification scheme.

## 2.5 THE DEPHANOX SYSTEM

The DEPHANOX system (Figure 2.1) is one in which nitrification takes place externally to the BNRAS system (Bortone *et al.*, 1996; Sorm *et al.*, 1996). In this system the influent wastewater is discharged to the anaerobic reactor to maximize BEPR. After the anaerobic reactor, the sludge mass is separated from the liquid in an internal settling tank and discharged to the anoxic reactor. The internal settling tank overflow, which has a high free and saline ammonia (FSA) concentration and low soluble COD concentration, is passed through a fixed medium reactor wherein nitrification takes place. The nitrified outflow from the fixed medium reactor is discharged to the anoxic reactor for denitrification. From the anoxic reactor, the mixed liquor passes to the last reactor which is aerobic. After the aerobic reactor, the activated sludge is separated from the treated wastewater in a final secondary settling tank. The final settling tank overflow is the final effluent and the settled sludge is returned to the anaerobic reactor.

**Figure 2.1** The DEPHANOX biological nutrient removal system (after Bortone *et al.*, 1996; Sorm *et al.*, 1996)



It appears that the DEPHANOX system was developed with the specific objective of stimulating denitrification by BEPR organisms, generally called denitrifying phosphate accumulating organisms (DPAOs). This has the advantage that the influent wastewater substrate sequestered by the PAOs in the anaerobic reactor (and therefore implicated in BEPR) also is used for denitrification (and therefore N removal). Some laboratory and pilot scale experimental work has been done on the DEPHANOX system by Bortone *et al.* (1996) and Sorm *et al.* (1996). They found considerable P uptake in the anoxic reactor, indicating that DPAOs did participate in the denitrification process. Also, improved sludge settleability (SVIs ~ 50 ml/g) have been consistently observed in the laboratory scale DEPHANOX system of Sorm *et al.* (1996). Thus, it would appear that the DEPHANOX system holds considerable promise, producing nutrient (N and P) removal and a sludge that settles well. However, the BNRAS system intensification benefit of the system does not appear to have been a consideration in the development of and investigation into this system. Therefore, while aspects of anoxic P uptake will be examined, the system intensification benefit of the external nitrification system is the main focus of this investigation.

## 2.6 THE PROPOSED EXTERNAL NITRIFICATION SYSTEM

In the proposed external nitrification system, based on the DEPHANOX system, but with some modifications (discussed in detail in Chapter 3, Section 3.1), nitrification takes place outside the suspended sludge BNRAS activated sludge system in a fixed media trickling filter (i.e. a stone column). This has the potential to reduce the sludge age of the BNRAS system significantly, from 20 - 25 days to 8-10 days. Further, removing nitrification from the aerobic reactor of the BNRAS system has a number of additional benefits:

1. Minimum aerobic mass fraction for nitrification is not required.
2. Aerobic reactor volume (and accordingly mass fraction) does not have to be maintained to accommodate internal fixed media.
3. Aeration for nitrification in the aerobic reactor is not required, only for COD utilization.

As a consequence of 1 and 2 above, the aerated mass fraction in the proposed system is no longer controlled by nitrification and therefore the unaerated mass fraction can be large (>60%). This would have two main benefits:

1. The anaerobic mass fraction can be increased, which should improve BEPR (Wentzel *et al.*, 1990).
2. The anoxic mass fraction can be increased, to improve denitrification and thus N removal (WRC, 1984) to the point where complete denitrification may be possible.

The possibility of complete denitrification at short sludge ages holds promise to ameliorate AA filament bulking (Casey *et al.*, 1994). As noted above this will be particularly beneficial as it will significantly increase the treatment capacity of an existing system, or reduce secondary settling tank surface area for a proposed system.

## 2.7 OPPORTUNITIES FOR IMPLEMENTATION OF THE PROPOSED SYSTEM

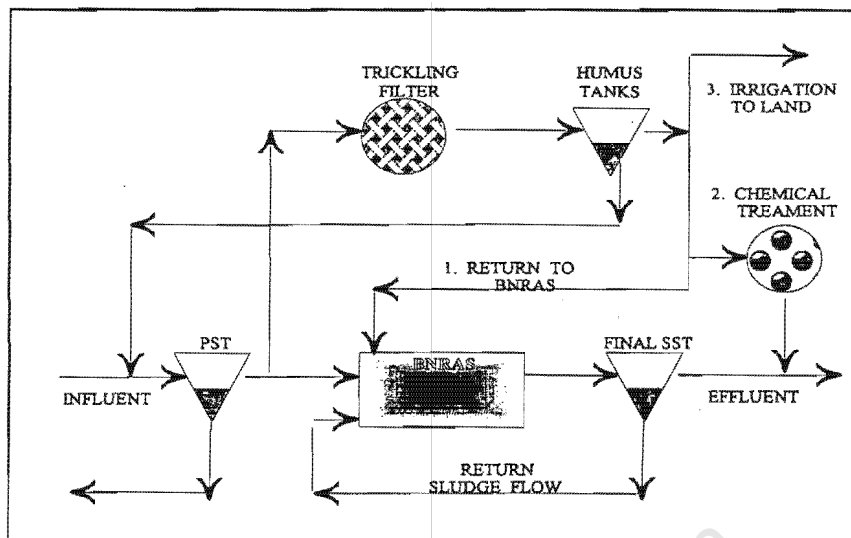
External nitrification could be achieved at wastewater treatment plants (WWTPs) where old trickling filter (TF) plants have been extended with a BNRAS system. There are many such WWTPs, particularly in South Africa. For example East Rand Water (ERWAT) treats in excess of 500MI/d, more than 50 % (270MI/d) of which in old trickling filter plants. Some 200 MI/d

is treated in 3 combined TF/BNRAS plants, of which 102 MI/d is treated in old TFs with chemical P removal, the balance in BNRAS systems. Also, 168MI/d is treated in TF only plants, which at some time in the future need to be extended. In the South Eastern Highveld region, some 10 TF/BNRAS plants treat more than 100MI/d, 25% of which is treated in old TFs. Then there are Krugersdorp, Daspoort (Guateng), Rooival (Guateng), Darvill (Kwazulu/Natal), and Athlone and Milnerton (W Cape) treating around 450 MI/d with TF treatment capacity in excess of 200MI/d. At these WWTPs where the special standard for phosphate needs to be met, to retain the benefit of the old TF, a proportion of the influent is passed through the TF and the effluents are (Figure 2.2):

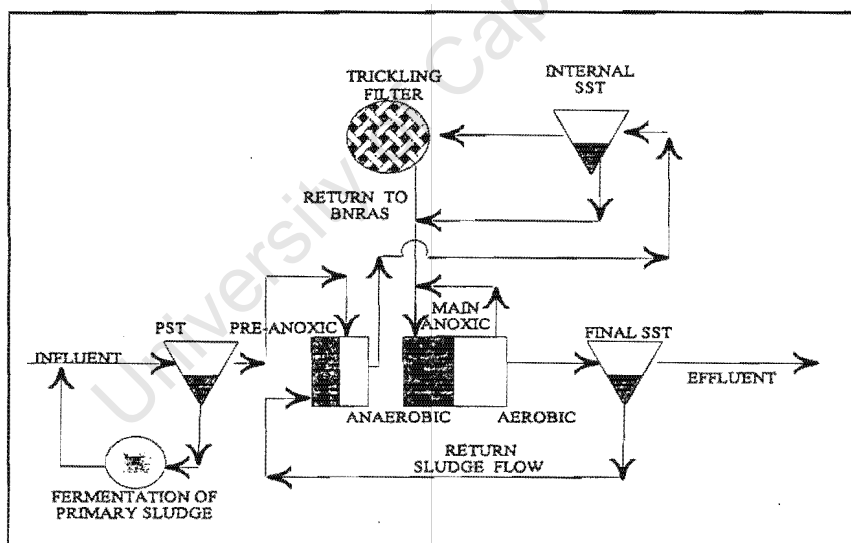
- 1 Discharged to the BNRAS system for biological N and P removal (e.g. van Hyssteen *et al.*, 1990). This in effect increases the TKN/COD and P/COD ratios of the WW discharged to the BNRAS system and increases the effluent nitrate and phosphate concentrations.
2. Chemically treated to precipitate the P before discharge as final effluent or to the BNRAS system. This is not only costly, but also reduces the alkalinity of the water and only reduces the effective P/COD ratio of the wastewater on the BNRAS system, the nitrogen returned is not reduced.
3. Irrigated on land at WWTP. This practice is being closely monitored by the Department of Water Affairs and Forestry in South Africa and is expected to be substantially disallowed because it leads to a significant loss of valuable surface water.

If, instead of the above three strategies, the nitrification process is removed from the BNRAS system and transferred to the TF, all the WW flow can be discharged to the BNRAS system (Figure 2.3): A side-stream of mixed liquor is taken from the end of the anaerobic zone and passed through the TF 'humus' tanks (upgraded to internal settling tanks ) to remove the activated sludge solids. The underflow sludge is discharged to the beginning of the anoxic zone and the overflow is passed onto the TF for nitrification. The nitrified TF effluent is then discharged to the anoxic zone for denitrification. In this way the TF assists the BNRASS in its area of weakness, i.e. nitrification, rather than taking away from it's strength, i.e. biological N and P removal with influent organics.

**Figure 2.2:** Conventional integration of trickling filters with biological nutrient removal activated sludge removal systems.



**Figure 2.3:** Proposed integration of trickling filters with biological removal activated sludge systems: nitrification is achieved externally on nitrifying trickling filters.



Furthermore, the oxygen demand in the aerobic reactor is markedly reduced because nitrification no longer takes place there. Indeed, not only is nitrification oxygen demand obtained 'free' outside the BNRAS system, but also the oxygen equivalent of the nitrate generated in the TF helps to reduce the carbonaceous oxygen demand in the BNRAS system, by about 1/3rd. In fact, with external nitrification, the reduction in oxygen demand in the BNRAS system is much greater than if 1/3rd of the wastewater is bypassed to the trickling filter as in existing TF/BNRAS

systems. Therefore, by changing the TF to a nitrifying system, the treatment capacity of the BNRAS plant is increased without having to increase the aeration capacity. If a TF plant is not available, it may be possible to construct an artificial external fixed media system, the cost of which may be offset by the increase in WW treatment capacity.

At short sludge ages and small aerobic mass fractions, nitrifiers would not ordinarily be supported in the BNRAS system. However, it will not be possible to completely exclude nitrifiers from the system because nitrifiers are likely to be seeded into the system from the TF effluent. Therefore, the potential for nitrification in the aerobic reactor will always exist in the system. The potential nitrate concentration in the aerobic reactor will be governed by the ammonia concentration that enters it. Provided the TF nitrifies well, this ammonia concentration will be mainly from the ammonia which bypasses the TF via the internal settling tank underflow, and therefore will be relatively low. If the TF does not nitrify well, the residual ammonia concentration from it is high, and then, if sufficient nitrifiers are present in the aerobic reactor, the nitrate concentration will be high, with the result that a significant nitrate concentration will be present in the final effluent and underflow from the final settling tank. To protect the BEPR against this potential nitrate ingress to the anaerobic reactor, a pre-anoxic reactor is placed in the underflow to denitrify the nitrate (Figure 2.3). If sufficient nitrifiers are not present in the aerobic reactor, then the ammonia concentration in the aerobic reactor will only be partially nitrified with the result that the return sludge nitrate concentration will be relatively low, but the effluent TKN concentration will be high, the concentration depending on the nitrification efficiency of the TF.

## 2.8 PREVIOUS RESEARCH INTO EXTERNAL NITRIFICATION

To examine the performance of an external nitrification BNRAS system Hu *et al.*, (1999) undertook a 250 day laboratory investigation with a 10 day sludge age, 48% anoxic and 19% aerobic mass fraction suspended solids system and found that :-

- (1) Good COD (~ 90%) and N (~90%) mass balances were obtained over the system;
- (2) Overall COD removal was excellent at 92% including an approximate 15% COD removal in the stone column nitrification system.
- (3) Including the nitrate dose to the main anoxic reactor, which increased the effective influent TKN/COD ratio to about 0.14mgN/mgCOD, the system produced an effluent

total N (TKN + NO<sub>x</sub>) concentration of <10 mgN/l. Nitrification was virtually complete in the stone column and the denitrification in the anoxic reactor was 58 mgN/l influent.

- (4) The P removal was 10.6mgP/l and considerable anoxic P uptake (>50% in the latter half of the investigation) took place in the main anoxic reactor. The BEPR was about 2/3rds of that expected from the aerobic P uptake BEPR model of Wentzel *et al.* (1990, 1992) and is probably a consequence of reduced energy capture by denitrifying PAOs (DPAOs) when nitrate serves as electron acceptor compared with oxygen (Payne, 1981; Murnleitner *et al.*, 1997).
- (5) The oxygen utilization rate (OUR) was very low - 29 mgO/(l.h) in the 19 % aerobic mass fraction. This is about 2.5 times lower than that in a conventional nitrification BNRAS system and arises because the nitrification OUR was obtained 'free' in the fixed media stone column system as well as the high denitrification which reduced the heterotrophic oxygen demand.
- (6) A very good settling sludge (DSVI ~ 60 ml/g) was consistently obtained in the BNRAS system. Filamentous organisms *Microthrix parvicella* and types 0092, 0041 and 0675, which are common in conventional BNRAS systems, were identified at low levels in the mixed liquor.

## 2.9 RESEARCH OBJECTIVES

The significant anoxic P uptake in the system and the reduction in BEPR this appeared to cause, led to an evaluation of the importance of the reduced aerobic mass fraction. Inclusion of anoxic P uptake PAOs in, and exclusion of aerobic P uptake PAOs from, the biocenosis of the BNRAS system mixed liquor are not essential for achieving external nitrification in the BNR scheme. In fact, inclusion and maximization of aerobic P uptake would appear desirable to maximize BEPR. In earlier investigations by Bortone *et al.* (1996), an anaerobic /anoxic sequencing batch reactor (SBR) was operated and they found that this system did not simulate BEPR unless a short aerobic period was included in the SBR. Thus, it would appear that in order to achieve stable (albeit reduced) anoxic phosphate uptake (and aerobic P uptake) an aerobic period may be essential for anoxic P uptake. However, conditions that promote aerobic P uptake BEPR are also conducive to nitrifier growth. Although exclusion of nitrifiers from the mixed liquor of the BNRAS system was originally considered essential, this is would not be necessary as long as virtual complete

external nitrification is obtained, to limit nitrification in the main aerobic reactor. In fact, complete exclusion of nitrifiers may not prove possible because, although conditions in the BNRAS system may not be conducive to their growth, nitrifiers are likely to be continually seeded into the system from the external nitrification system. Accepting nitrification in the BNRAS system, with complete nitrification in the external nitrification fixed/suspended media system, the nitrification in the BNRAS system will be limited by ammonia bypassing the trickling filters with the internal settling tank underflow to the anoxic reactor. However, should complete nitrification not be obtained in the external nitrification system, then the ammonia from the external nitrifier will be nitrified in the aerobic reactor of the BNRAS system. If the aerobic reactor nitrate concentration becomes too high due to poor nitrification in the external nitrification system, the pre-anoxic reactor will become overloaded with nitrate resulting in nitrate discharge into the anaerobic reactor and reduced BEPR. The occurrence of such a scenario can be minimized by the inclusion of an a-recycle from the aerobic to the main anoxic reactor of the BNRAS system, as employed in this investigation. On the other hand, if nitrification were not included in the BNRAS system, then the ammonia would leave via the effluent, which is a less desirable situation where a low ammonia (<1,0 mgN/l) concentration standard needs to be met.

Recognizing the advantages of including aerobic P uptake in the system (higher BEPR per influent RBCOD), the fact that including nitrification in the system is not entirely undesirable (provided the external nitrification system nitrifiers virtually completely) and acknowledging that an aerobic period is essential for BEPR and stable anoxic P uptake (Bortone *et al.*, 1996), it was decided to investigate the effect of increasing the aerobic mass fraction and stimulating aerobic P uptake in the external nitrification BNRAS system. Initially, the external nitrification BNRAS system with a fixed media stone column and small aerobic mass fraction was set up to establish a datum, and then the aerobic mass fraction was increased. In this manner, simultaneously, external nitrification and anoxic phosphate uptake was studied in the BNR activated sludge systems with varying aerobic mass fractions. The aims of the experiments were to:

- (i) firstly establish a stable population of slow-growing nitrifiers on a fixed media external nitrification system (later changed to a suspended medium due to *Psychoda* larvae infestation of the fixed media stone column),
- (ii) double the volume of the wastewater treated thereby testing one of the claimed benefits

of external nitrification system due to the shortened sludge age and improved sludge settleability,

- (iii) promote conditions to achieve aerobic phosphate uptake,
- (iv) increase the aerobic mass fraction in an attempt to qualify its effect on anoxic P uptake, and
- (v) study the effect of the increased aerobic mass fraction on the sludge settleability of the BNRAS system.

The BNRAS external nitrification experimental laboratory set up and control are discussed in detail in Chapter 3.

University of Cape Town

## CHAPTER 3

### EXPERIMENTAL INVESTIGATION

#### 3.1 EXPERIMENTAL SET-UP AND CONTROL

To achieve the aims of this investigation, i.e. external nitrification in a BNRAS system, either one or a combination of two techniques can be employed. Firstly, by installing a settler and a fixed media external nitrification system between the anaerobic and anoxic reactors, as shown in Figure 3.1, and or secondly by dosing nitrate directly to the anoxic reactor. To set up the laboratory system as close as possible to the envisioned application of the system, the first approach was adopted. However, in order to increase the nitrate load and ensure that the anoxic reactor was overloaded with nitrate, i.e. to maintain the nitrate load on the main anoxic reactor in excess of its denitrification potential thus allowing some nitrate to enter the aerobic reactor, nitrate was dosed directly into the main anoxic reactor as a concentrated solution of 0.5 to 1.25 mgN/ml.

With this in mind, the system shown in Figure 3.1 was set up, with the design parameters as given in Table 3.1. The system sludge age, temperature and unaerated mass fraction were initially 10 days, 20 °C, and 0.85 respectively. To avoid any interference of nitrate on the P release process in the anaerobic reactor, a 0.1 mass fraction pre-anoxic reactor was set up ahead of the anaerobic reactor to denitrify nitrate in the return sludge. This pre-anoxic reactor was necessary to ensure a near zero nitrate concentration in the flow entering the anaerobic reactor since (i) the main anoxic reactor was dosed nitrate such that its denitrification potential was exceeded allowing a low concentration ( $<5\text{mgNO}_3\text{-N/l}$ ) of nitrate in the outflow of this reactor and/or (ii) to denitrify nitrate generated from the residual ammonia from the internal settling tank underflow and/or the external nitrification system that may be nitrified in the aerobic reactor.

**Figure 3.1:** Schematic layout of External Nitrification BNRAS system

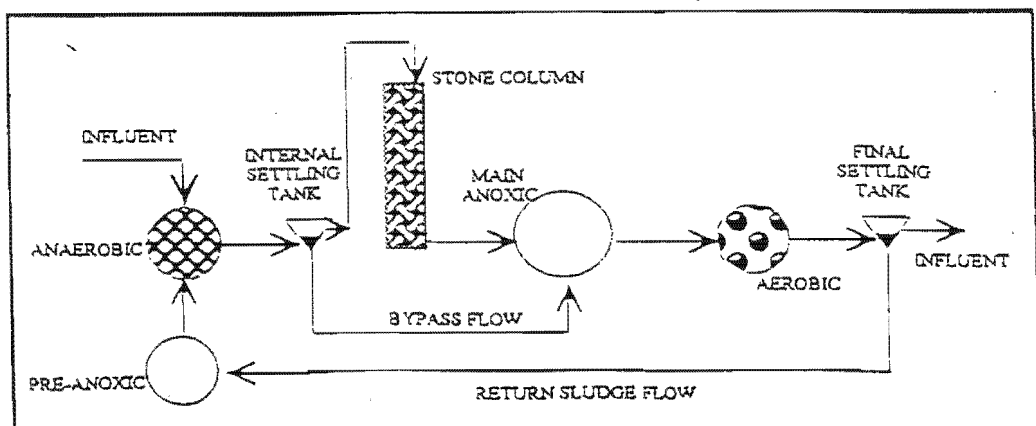


Table 3.1: External Nitrification BNRAS system design and operating parameters.

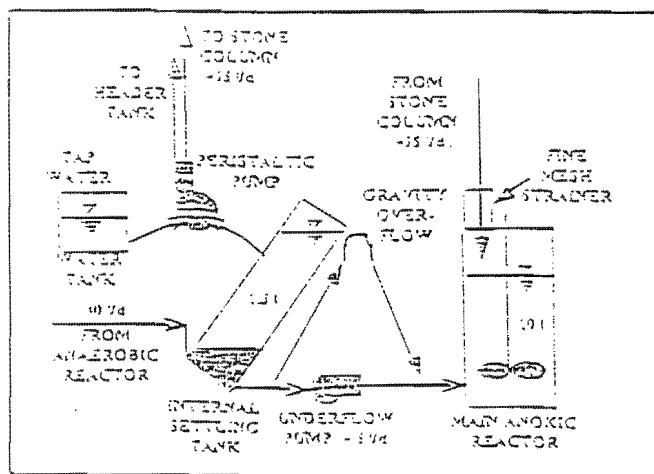
System Parameter	Configuration 1	Configuration 2	Configuration 3	Configuration 4
	Changed to ↗	Changed to ↗	Changed to ↗	
<b>Period:</b>	24/2-16/3	17/3-27/7	28/7-16/9	16/9-1/4/99
No of Days	30 (1-30)	124 (31-154)	51 (155-205)	164 (206-373)
Sewage Batch	1 to 3	4 to 20	22 to 25	26 to 37
<b>Operating:</b>				
Sludge age (days)	10	8	10	10
Waste (l/d)	2	2.5	2	2
Temperature (°C)	20	20	20	20
pH of anaerobic reactor	7.2-8.2	7.2-8.2	7.2-8.2	7.2-8.2
pH of aerobic reactor	7.2-8.2	7.2-8.2	7.2-8.2	7.2-8.
DO in aerobic reactor (mgO/l)	2.0 - 5.0	2.0 - 5.0	2.0 - 5.0	2.0 - 5.0
<b>Influent: Mitchell's Plain (raw) unsettled wastewater</b>				
Influent Feed (l/d)	20	40	30	30
COD (mgCOD/l)	709	677	646	716
RBCOD (mgCOD/l)	103	91	73	98
TKN/COD ratio	0.08 - 0.11	0.07 - 0.12	0.07 - 0.14	0.04 - 0.15
NO <sub>3</sub> dose/l Inf/ COD	0.03 - 0.04	0.01 - 0.03	0.02 - 0.03	0.02 (batch 28)
Total P (mg/l Influent)	18.2 - 26.1	15.6 - 32.6	19.4 - 28.9	20.1 - 29.5
Total P Removal(mgP/l)	9	8	13	12
TP Rem/ Inf COD	0.013	0.012	0.021	0.017
Ext Nitrification System	Stone Column	Stone Column	Stone Column	Suspended AS.
<b>Reactor Volumes Mass Fractions:</b>				
Total System Volume(l)	20	20	20	20
Anaerobic Vol (l)	5 ; 0.25	5 ; 0.25	5 ; 0.25	5 ; 0.25
Main Anoxic Vol (l)	10 ; 0.5	9 ; 0.45	6 ; 0.30	6 ; 0.30
Aerobic Vol (l)	3 ; 0.15	3 ; 0.15	6 ; 0.30	6 ; 0.30
Effective Pre Ano Vol	2 ; 0.10	3 ; 0.15	3 ; 0.15	3 ; 0.15
Unaerated	17 ; 0.85	17 ; 0.85	14 ; 0.70	14 ; 0.70
<b>Recycles flows and Ratios (l/d; ratio w.r.t to influent flow)</b>				
s- recycle (l/d)	10 ; 0.50	20 ; 0.50	15 ; 0.50	15 ; 0.50
a - recycle (l/d)	none ; 0.00	none ; 0.00	30 ; 1.00	30 ; 1.00
Flow to Ext Nitrifier	30 ; 1.50	50 ; 1.25	35 ; 1.17	32 ; 1.07
Bypass flow (l/d)	10 ; 0.50	10 ; 0.25	10 ; 0.33	13 ; 0.43

The activated sludge reactors and settling tanks were those usually used in laboratory investigations and were made from clear acrylic plastic as described in detail by Clayton *et al* (1989). The external nitrification system was a fixed medium reactor. It comprised a 100 mm diameter, 1.5 m tall clear acrylic plastic column filled with 9 - 13 mm granite stones, and will be

referred to as the stone column (SC). The base of the stone column was closed off and placed in a 200 mm diameter, 100 mm high plastic mini settling tank. Four 10 mm diameter holes were drilled 20 mm above the base of the stone column to allow the nitrified effluent to flow into the plastic mini settling tank as well as to allow for the inflow of air. A small fan was set at the top of the stone column and switched on for 15 seconds every 10 minutes to renew the air in the column since the column was too small to generate its own natural upflow of air. The nitrified effluent was passed through a 0.5 mm fine mesh strainer to remove solids, in particular mothfly larvae which appeared to adversely affect the laboratory scale stone column function and the activated sludge system (discussed in detail below).

The flow to the stone column was drawn from the internal settling tank supernatant with a peristaltic pump as shown in Figure 3.2 below. To provide control and monitoring of the flow to the column, a parallel channel in the peristaltic pump discharged tap water to a tank with a hydraulic head equal to that of the stone column. Of the 40 l/d passing through the internal settling tank (20 l/d influent plus a 1:1 underflow s recycle ratio) between 30 to 35 l/d was pumped to the stone column. The underflow sludge was pumped to the anoxic reactor at about 5 l/d. A gravity overflow from the settling tank to the anoxic reactor absorbed flow variations in the two pumps. The entire experimental was set up on a specially constructed frame at the base of which was a drip tray, to collect as much as possible sludge lost due to blockages or leaks and return these to the system so as to minimize sludge losses.

**Figure 3.2:** Detail of stone column flow control and measurement



During the first stage of the investigation external nitrification was achieved with the stone column fixed media system, which covered a period of 205 days. During this time a number of changes were made to the design and operating parameters which resulted in periods over which testing of the system was not carried out. The changes that were made are given in Table 3.2 and the design and operating parameters in Table 3.1.

During the first stage, comprising three configurations (see Table 3.1 for details), the system received 25 batches of sewage. These batches of raw sewage were collected approximately every two weeks, and after maceration, stored in stainless steel tanks in a cold room at 4°C, and served as feed until the next sewage batch was collected. To feed the laboratory system, a sample of sewage was drawn daily after thorough mixing and then diluted with tap water from a concentration of approximately 1200mg COD/l to a target influent concentration of 700 mg COD/l. The diluted influent was buffered by addition of sodium hydrogen carbonate ( $\text{NaHCO}_3$ ). About 7 mgP/l as potassium dihydrogen phosphate ( $\text{KH}_2\text{PO}_4$ ) was dosed to the influent to avoid P limitation and to ensure that the final effluent phosphorus concentration from the system remained above 5 mgP/l. After dilution and thorough mixing, a 250ml sample was drawn from the diluted influent. A measured volume of 20 l was then placed in the systems influent feed drums (20 l each), which were kept in a refrigerator at approximately 8°C. The influent flow to the system was pumped from the influent feed drums by a constant flow pump over a 24 hr period. Feeding the system daily in this way i.e. over a 24 hr period in daily batches, provided a check that the daily influent was fed to the system. At the end of the 24 hr period, whatever remaining wastewater (usually < 100 ml) was collected with the solids that may have settled out, and poured into the anaerobic reactor. The nitrate dosed to the main anoxic reactor was done using a constant flow pump delivering 500 ml/d. The dose concentration of the  $\text{NaNO}_3$  was made up daily and varied from 0.5 to 1.25  $\text{mgNO}_3\text{-N/ml}$  depending on the nitrate mass dose required daily.

The external nitrification BNRAS system, i.e. Configuration 1, was taken over from earlier investigations into external nitrification in biological nutrient removal activated sludge systems (Hu *et al.*, 1999). This system in the form of Configuration 1, was later changed to Configurations 2 and 3 in accordance with the design and operating conditions in Table 3.1. During the investigation, a conventional UCT system was operated and fed the same sewage (and

also numbered the same) as the external nitrification system with which to compare the nutrient removal. Details of this system, day to day results, and data evaluation are given in Appendices D and E.

**Table 3.2:** Changes and Stoppages to the system

Item	From day	To day	Reason
Nitrate dose	1	215	To supplement stone column (SC) nitrification and assess the denitrification potential of main anoxic reactor.
Influent	23	25	Increased influent flow from 20l/d to 40 l/d to observe an aim of this investigation.
Sludge age	23	25	Reduced from 10 days to 8 days in order to minimize the likelihood of internal nitrification
Sewage	110	119	Sewage batches 14 and 15 toxic. Nitrification very poor at this time.
Sewage	140	147	Sewage toxic
Stone Column (SC)	110	205	Larvae infestation ( <i>Psychoda</i> ), scoured biofilm during draining after periodic flooding to control <i>Psychoda</i> .
Influent	148	149	Decreased influent flow from 40 l/d to 30 l/d in order to reduce flow rate through the stone column.
Stone Column	155	168	Replaced existing SC (1.5m) with longer SC (2m) to increase retention time. Approx. 2 weeks for sludge growth.
a-recycle	185		Added 1:1 aerobic to main anoxic recycle to minimize nitrate recycled to anaerobic reactor
External Nitrifier	205		Changed external nitrification system from fixed media stone column to suspended nitrification activated sludge system
Settling	236	244	Poor settling sludge (not bulking) accumulated and filled up in final settler.
Samples	284	294	Samples were mistakenly discarded.
Blockages and settling	316	348	System beset with problems: frequent blockages and sludge loss, poor settling and sludge accumulation in final settler
End of Investigation		373	

### 3.2 DATA ACQUISITION AND SYSTEM PERFORMANCE MONITORING

To monitor the systems performance and operation, samples were drawn virtually daily from each of the reactors, the internal settling tank supernatant, the stone column nitrified outflow and the final effluent for analysis throughout the 373 day duration of the investigation. Generally, samples were not taken from the system (i) on the first day of a new sewage batch (because the system requires at least two days to adjust to the new sewage batch), and (ii) on days which the system did not operate properly, e.g. on days when one or more of the reactors, especially the pre-anoxic, got blocked causing sludge losses. In most cases the spilled sludge was collected and returned to the system. However, these spillages can be a major contribution to poor COD balances. Table 3.3 shows the parameters that were measured and the analytical methods that were applied. In addition to the above samples taken, the diluted sludge volume index (DSVI) was measured on sludge drawn from the aerobic reactor and the oxygen utilization rate (OUR) was monitored continuously online with the DO controller/OUR meter developed by Randall *et al.* (1991).

**Table 3.3:** Sampling position and parameter measurement

Test	COD <sup>1</sup>	TKN <sup>2</sup>	FSA <sup>3</sup>	NO <sub>3</sub> <sup>4</sup>	NO <sub>2</sub> <sup>4</sup>	Tot P <sup>5</sup>	OUR <sup>6</sup>	DSVI <sup>7</sup>	VSS/TSS <sup>8</sup>	pH <sup>9</sup>	RBCOD <sup>10</sup>
Pre Anoxic				¥	¥	¥			§		
Influent	∅	∅	∅			∅					¥
Anaerobic				¥	¥	¥			§	§	
S/Col Influent	∅	∅	∅	¥	¥	¥					
S/Col Effluent	∅	∅	∅	¥	¥	¥					
Anoxic				¥	¥	¥			§		
Aerobic	∅	∅		¥	¥	¥	§	§	§	§	
Final Effluent	∅	∅	∅	¥	¥	¥					¥

§ Measurement taken (filtering not applicable).

∅ Unfiltered Sample

¥ Filtered through Schleicher & Schüll 0.45µm glass fibre membrane.

<sup>1,2,3</sup> Method according to Standard Methods (1985)

<sup>4</sup> According to Technicon Auto Analyser Industrial Method No 33.69W

<sup>5</sup> Sulphuric acid/persulphate digestion at 100°C followed by molybdate-vanadate colour development for ortho-phosphate (Standard Methods, 1985- Method 424C III)

<sup>6</sup> With Yellow Springs DO probe and the automated method of Randall *et al.* (1991)

<sup>7</sup> According to Lee *et al.* (1983) or Ekama and Marias (1984).

<sup>8</sup> By separation with centrifugation, drying in a crucible at 105°C and incineration at 600°C.

<sup>9</sup> With Hanna Instruments pH meter No HI 9023.

<sup>10</sup> For RBCOD concentration, 1litre sample was subjected to 10ml of 0.25M Aluminium Sulphate flocculant concentration and allowed to settle for at least 10 min before filtration (Mamais *et al.*, 1993 ; Mbewe *et al.*, 1998)

The day to day results of the measured parameters are listed and are shown plotted in Figures A1 to A28 in Appendix A. A summary of these measured parameters with their corresponding

Figure numbers are shown in Table 3.4.

After 30 days of testing (day 30), having fed three batches of sewage and obtaining an average COD and N mass balance of 90 % and 99 % respectively, and an average P removal of 0.013 mgP/mgCOD, it was decided to commence with the first aim of this investigation, i.e. high influent flow treated per litre system volume.

**Table 3.4:** Summary of measured parameters with corresponding Figure numbers.

Test		Test	
COD	Figure A1 to Figure A2	Total P	Figure A15 to Figure A22
TKN	Figure A3 to Figure A4	Solids	Figure A23 to Figure A26
Ammonia	Figure A5 to Figure A6	mgO/d	Figure A27
Nitrate	Figure A7 to Figure A10	mgO/d	Figure A28

The first change made to the system was doubling of the influent feed from 20 l/d to 40 l/d. Consequently, the s-recycle doubled from 10 l/d to 20 l/d and the flow to the stone column from 30 l/d to 50 l/d. The main anoxic volume was reduced from 10 l to 9 l and the effective pre-anoxic volume was increased from 2 l to 3 l, thus changing their corresponding mass fractions. It was also decided to run this newly configured system, referred to as configuration 2, at an 8 day sludge age. A summary of the changes made to Configuration 1 can be found in Table 3.1.

Configuration 2 was run for a period of 124 days during which 17 batches of sewage were fed. Although having obtained an average COD and N mass balances of 79 % and 97 % respectively and a P removal of 0.012 mgP/mgCOD, the system required changes because it was failing in the fundamental aim i.e. external nitrification. The stone column nitrification efficiency (given by 1 minus the outflow FSA/inflow FSA concentration ratio) had dropped from a high average value of 88 % completion (Configuration 1) to a low average value of 44 % (Configuration 2), i.e. a 50 % reduction in nitrification efficiency. The poor performance was due to mainly three factors. The first factor, which also had a negative impact on the P removal, was due to bad (toxic)

sewage batches fed to the system viz, batches 10, 14, 15, 19 and 21 the results of which were discarded as not useful to this investigation. The second, a more direct effect, was due to fly larvae (*Psychoda*)<sup>2</sup> infestation of the stone column and subsequently the main anoxic and aerobic reactors. The larvae foraged the nitrifier biofilm off the stones and severely reduced the nitrification efficiency of the stone column. The effect of the larvae on the suspended sludge system was not clear but the denitrification efficiency and P uptake in the main anoxic reactor had declined.

In an effort to control the larvae infestation, periodic flooding of the stone column was carried out every 14 to 16 days (i.e. within a complete lifecycle from egg to emergence as an adult moth fly) in order to drown the adult flies and thus minimize the possibility of mating and laying of eggs and thereby hopefully achieving an improvement in nitrification efficiency. However, the periodic flooding resulted in a poorer nitrification performance due to the nitrifying biofilm being scoured off the stones during the draining periods and flowing out of the stone column after flooding. Poppelan (1998), states that at best this method is about 60 % effective in controlling *Psychoda* infestation. Although fine mesh sieves (0.5mm) were used at both the inlet and outlet of the stone column and periodic flooding of the stone column was carried out, the fly larvae infestation could not be effectively controlled.

---

<sup>2</sup>Trickling filters present an almost perfect habitat for many insect species, and have become a specialised niche for a number of them (Poppelan,1998). The four most commonly quoted nuisance species are *Sylvicola fenestralis*, *Metriocnemus hygropetricus*, *Lymnophyes minimus* and *Psychoda alternata*. Of these four species, *Psychoda* is of most interest as it is the only one which has so far been implicated as having potential effects on human health. *Psychoda* larvae are not truly aquatic, and should be described as hygropetric (alternate wet and dry cycles). This immediately explains why *Psychoda* has been so successful in colonizing trickling filters, where wet and dry periods alternate with regularity. The key to success for *Psychoda* is the presence of a thick biofilm, preferably algal or fungal, but also bacterial, on the filter media, which serves as both food and as protection against dehydration. Therefore, outbreaks of *Psychoda* are associated with heavily loaded or overloaded trickling filters. Psychodidae measure between 3 to 5 mm as adults. The adults are weak fliers, and do not migrate far from their place of origin. Adults are capable of mating and laying eggs when they emerge. However, this sort of behavior is usually seen only under stress (i.e. laboratory) conditions. The adult female lays between 50 to 140 eggs in a wet environment such as water, sludge or biofilm. The eggs hatch after one to two days. The larvae develop to the pupal phase in four stages, known as 'instars'. All four instars are feeding stages; the pupal stage is a non-feeding but still mobile resting stage. The duration of the four instar stages is temperature dependent, and, under optimum conditions, the first and second instars will be two days each, the third instar two or three days, and the fourth instar between five and eight days. The pupal stage is short but can vary from one to three days. The laboratory stone column is a better habitat for *Psychoda* infestation than real full scale TF because (i) temperature is constant and (ii) light penetrates into the entire media volume. The problem of *Psychoda* infestations scavenging the nitrifier biofilm causing a reduced nitrification efficiency is therefore not as serious a problem in full scale TFs as in laboratory ones.

The third factor influencing the performance of the stone column was the retention time. It was speculated that the high volume flow passing through the 1.5 m tall stone column was too short and did not allow for sufficient time for nitrification to reach completion.

To overcome these problems encountered with the stone column system, it was replaced with a taller, 80 mm diameter, 2 m tall stone column. This new stone column also had at its base a strainer to prevent excessive sludge leaving the stone column. An improved settling tray which prevented sludge loss from the stone from entering the main anoxic reactor and improved the air flow into the column. This taller stone column was selected to increase the retention time. Furthermore, to decrease the flow to the stone column, the influent flow was decreased to 30 l/d and as a result the s-recycle and the stone column flow were decreased to 15 l/d and 35 l/d respectively<sup>3</sup>. Up to this stage in the investigation the objective of the system was to obtain as much anoxic P uptake as possible while trying to keep the aerobic uptake and nitrification in the aerobic reactor as low as possible. Because of the difficulty of obtaining stable anoxic P uptake, the objective shifted such that the principal aim, i.e. external nitrification, could be achieved with aerobic P uptake. Other reasons for this shift in focus were (i) the poor phosphorus removal obtained with configuration 2 due to lower BEPR with anoxic P uptake compared to aerobic P uptake, and (ii) because anoxic P uptake is not a prerequisite for external nitrification. Therefore an external nitrification BNR system was set up to encourage aerobic P uptake BEPR, which from past experience is more stable and thus improves the overall BEPR performance of the system. Accordingly, the main anoxic reactor volume was decreased from 9 l to 6 l and the aerobic reactor volume increased from 3 l to 6 l. Also, the sludge age was increased to 10 days to stabilize the phosphate uptake and biological excess P removal (BEPR). This increased sludge age increased the likelihood of nitrification in the aerobic reactor, thus an a-recycle was introduced from the aerobic reactor to the main anoxic reactor to reduce the nitrate dosed to the anoxic reactor and hence the nitrate concentration in the aerobic reactor to thereby minimize nitrate recycled to the anaerobic reactor.

---

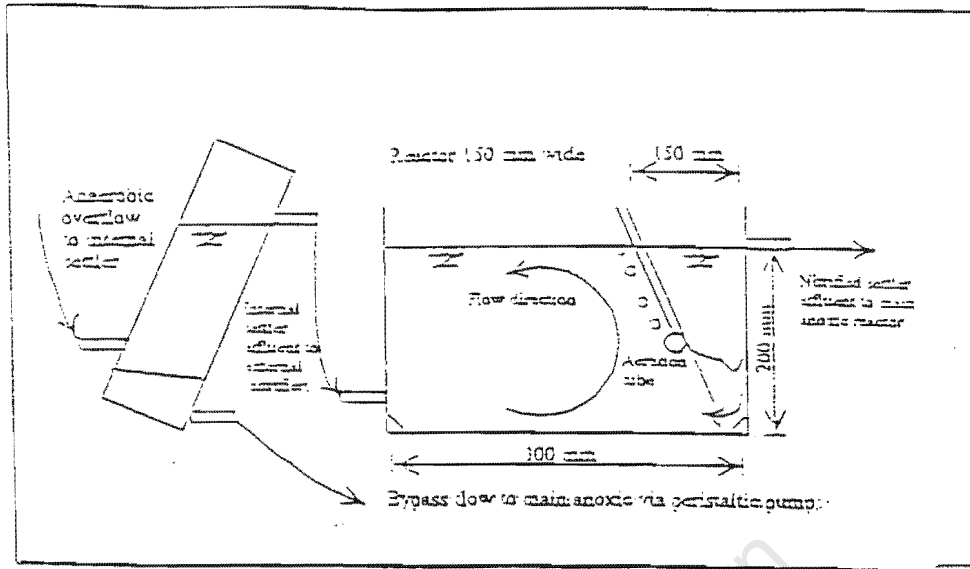
<sup>3</sup> It should be noted that the decrease in influent flow was necessitated by the poor stone column nitrification performance, and not for the suspended sludge system. Therefore, this reduction was not a failure of the increased treatment capacity objective of the external nitrification biological nutrient removal system.

The effect of all the changes made to Configuration 2 can be seen in Table 3.1. This modified system, called Configuration 3, was operated for a period of 51 days over which 5 sewage batches were fed to the system. An average COD and nitrogen mass balance of 94 % and 95 % respectively, and an average P removal of 0.021 mgP/mgCOD was attained over this period, which is significantly higher than earlier in the investigation and closer to that expected from aerobic P uptake BEPR performance (Ekama and Wentzel., 1999), even though the P uptake was still significant in the main anoxic reactor.

During the operation of Configuration 3, the stone column was still not performing as required. This was due to the same problem encountered as in Configuration 2 i.e. *Psychoda* larvae infestation and hydraulic overloading. In Configuration 3, the stone column nitrification efficiency had dropped by greater than 50 % of that of the previous stone column to a very low and unacceptable value of 17.5 %.

Having not achieved sufficiently high external nitrification efficiencies (>70 %) through the use of a fixed media stone column external nitrification system, it was decided to change the system to a suspended medium activated sludge external nitrification system. The suspended medium activated sludge external nitrification system comprised of a 20 cm long by 15 cm wide rectangular tank with a 5 l volume. The settling compartment was constructed within the tank by a sloping (30° to the vertical ) baffle plate (see Figure 3.3). A small gap between the baffle plate and the bottom corner of tank allowed the settled sludge to return to the reactor compartment. Aeration was supplied by a porous T-section tube attached on the reactor side of the baffle plate, which created a rotational flow pattern and provided mixing in the tank. The flow pattern (see Figure 3.3), being upwards at the aeration end and downwards at the settling compartment end assisted the return of sludge into the reactor. No sludge was intentionally wasted from the reactor; thus the sludge age was very long and was established by the sludge loss with the outflow from the settling compartment to the main anoxic reactor with a volume of 6 l, the nominal and 'actual' retention times in the reactor/settler at 30 l/d influent flow and 0.5 : 1 recycle ratio were 4.8h and 3.2h respectively. The details of the new design and operating parameters of Configuration 4 are given in Table 3.1. Unfiltered COD samples of the reactor inflow and outflow allowed determination of the COD reduction through the reactor.

Figure 3.3: Details of external suspended medium nitrifier.



An immediate improvement was noticed in the nitrification efficiency of the suspended medium external nitrification system and hence it was decided to keep this system for the remainder of the investigation (164 days and sewage batches 26 to 37). The nitrification efficiency had increased to 66 % while the average P removal dropped slightly to 0.017 mgP/mgCOD. The average COD and nitrogen mass balance for Configuration 4 were 81 % and 89 % respectively.

### 3.3 COD REMOVAL AND MASS BALANCE PERFORMANCE

To establish the accuracy of the experimental data, COD mass balances were performed on the system. For each of the sewage batches, the average values of the measured parameters (Table 3.5 and Appendix A) over the sewage batch were used to determine the COD balance. The COD balance was determined for each batch sewage batch because the influent TKN and RBCOD concentrations varied from sewage batch to sewage batch.

In the COD balance, the COD entering the system via the influent flow is compared to the COD leaving the system via the (i) the final effluent flow (ii) oxygen utilised (iii) sludge wasted (iv) nitrate and nitrite denitrified (v) COD utilized in the external nitrification (EN) system. The method for calculating the COD balance is given in Appendix B. The reliability of the experimental data is directly proportional to the mass balance deviation from 100 %. This implies that the closer the COD balance to 100 % the more reliable the data, in particular, the reliability

of the unbiodegradable particulate COD fraction,  $f_{S,up}$  and ordinary heterotrophic (OHO) and polyphosphate accumulating (PAO) organisms fractions of the VSS (i.e  $f_{av,OHO}$  and  $f_{av,PAO}$ ) estimates.

The averages of the measured parameters of the 37 sewage batches (5 sewage batches excluded due to toxic effects, giving 32 batches analyzed) are listed in Appendix C. Also given in Appendix C are the averages of all the measured parameters for the four system configurations time periods viz; Configuration 1, sewage batches 1 to 3; Configuration 2, sewage batches 4 to 20; Configuration 3, sewage batches 22 to 25; and Configuration 4, sewage batches 26-37). The results of the COD mass balance and its components are given in Table 3.5 and are shown plotted in Figures 3.4 and 3.5. In Figure 3.5 the six components making up the COD balance are shown as a stacked bar viz. effluent COD (Effluent, 10%), COD in waste sludge (Waste, 31%), COD removal in the external nitrification system (Extnit, 12%), COD (  $e^-$  ) passed on to oxygen (Oxygen, 13%), and nitrate (Mod Recov, 14%) as electron acceptors and the COD not recovered or unaccounted for in the COD balance (Unacc, 20%). The percentages given in brackets are the mean values for the investigation.

**Figure 3.4 :** COD mass balance of BNRAS system for 37 sewage batches.

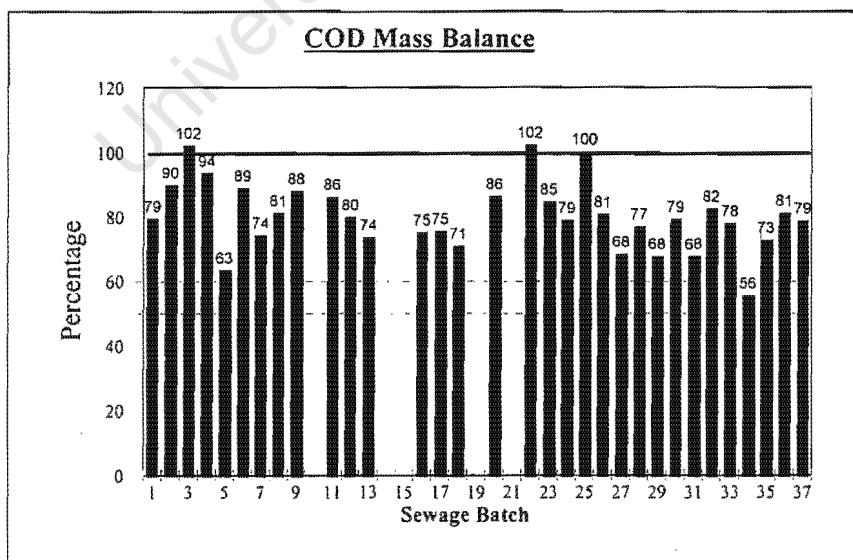


Figure 3.5 : COD mass balance components of BNRAS for 37 sewage batches.

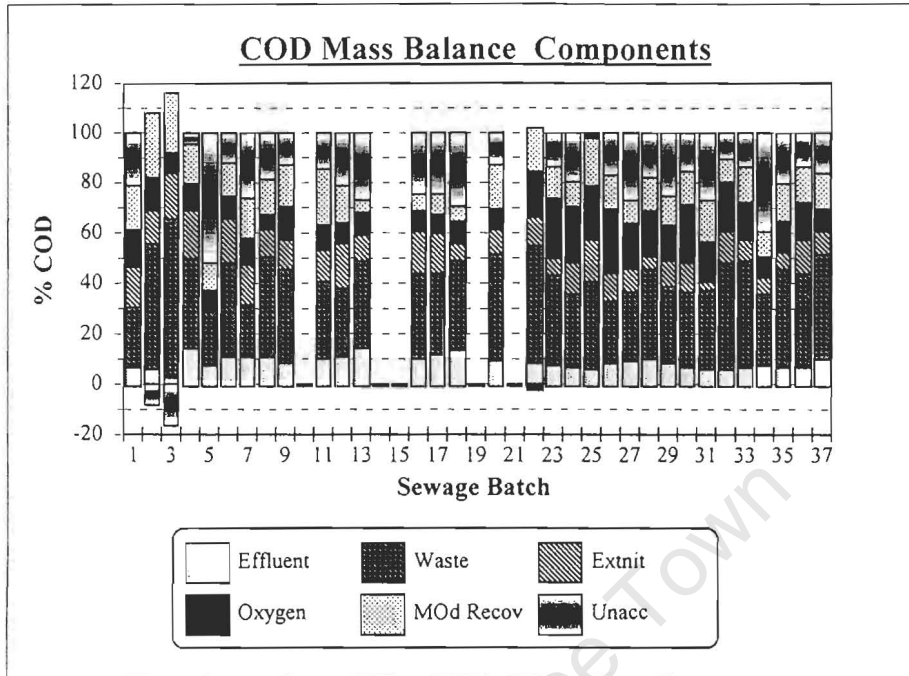
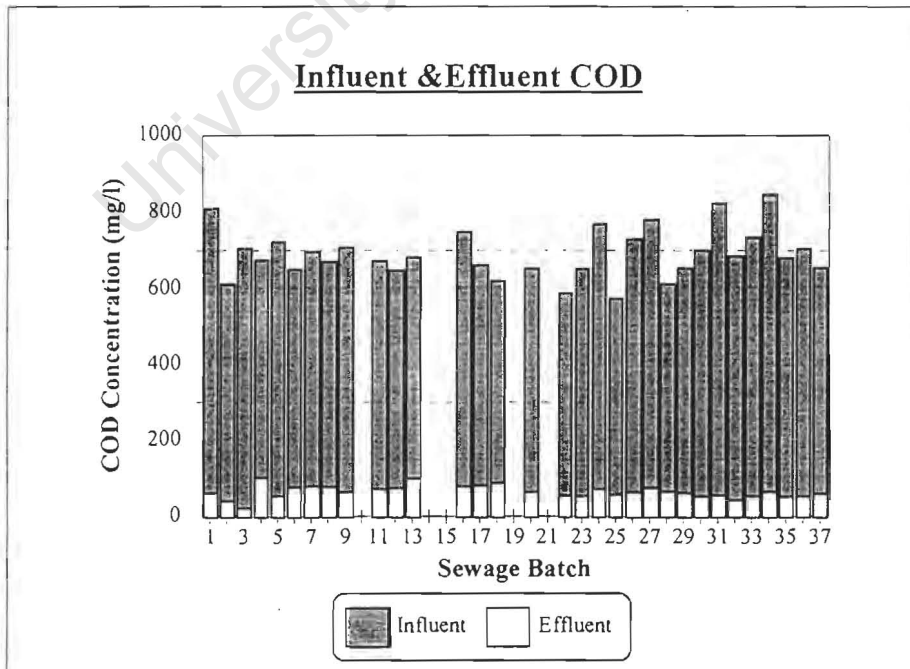


Figure 3.6 : Average sewage batch Influent and Effluent COD concentrations



**Table 3.5 :** Components of COD mass balance and % COD Removal

Average of Batch	Influent mgCOD	Effluent mgCOD	Waste mgCOD	Extnit mgCOD	Oxygen <sub>c</sub> mgO	Denit Recov mgO	COD Out mgCOD	COD Rem %	MBCOD %
1	16200	1212	3886	2535	2376	2859	12868	93	79
2	12236	810	4835	1670	633	3035	10983	93	90
3	14104	414	7155	2513	998	3321	14401	97	102
<b>Config 1</b>	<b>14810</b>	<b>812</b>	<b>5292</b>	<b>2239</b>	<b>1336</b>	<b>3072</b>	<b>12751</b>	<b>94</b>	<b>90</b>
4	26981	4033	9641	5178	2262	4146	25260	85	94
5	28861	2105	6298	4241	2320	3319	18284	93	63
6	26009	3021	9730	4523	2513	3323	23108	88	88
7	27838	3109	5779	4526	2956	4293	20662	89	74
8	26824	3065	10764	2902	1127	3889	21746	89	81
9	28288	2557	10608	3182	3774	4761	24882	91	87
11	26903	2840	8375	3481	2318	6158	23174	89	88
12	25861	2940	7190	4339	2270	3901	20640	89	80
13	27285	3942	9541	2760	2356	1458	20056	86	74
16	29920	3120	10125	5100	2480	1657	22482	90	75
17	26440	3200	8700	4100	1886	2073	19958	88	75
18	24800	3480	8750	1800	2028	1511	17569	86	71
20	19584	1897	8330	1958	1343	3367	16896	90	86
<b>Config 2</b>	<b>27168</b>	<b>3188</b>	<b>8792</b>	<b>3844</b>	<b>2303</b>	<b>3374</b>	<b>21485</b>	<b>89</b>	<b>79</b>
22	17640	1590	8220	2170	3159	2908	18047	91	102
23	19557	1572	6697	1011	4978	2280	16537	92	85
24	23079	2145	6475	2502	4604	2464	18190	91	79
25	17238	1704	6003	2887	3489	3187	17269	90	100
<b>Config 3</b>	<b>19379</b>	<b>1753</b>	<b>6849</b>	<b>2142</b>	<b>4057</b>	<b>2710</b>	<b>17511</b>	<b>91</b>	<b>91</b>
26	21858	1913	4429	2360	5958	2980	17640	91	81
27	23403	2227	5088	2180	4502	2005	16002	90	68
28	18360	1971	5173	940	3512	2053	14117	89	77
29	19619	1819	4715	1996	2672	2522	13255	91	68
30	21013	1573	5059	2283	4990	2714	16618	93	79
31	24713	1670	6193	777	2893	4186	16719	93	68
32	20580	1260	6980	2688	4165	1853	16946	94	82
33	22029	1603	7497	1847	3218	2995	17160	93	78
34	25394	1968	5758	1665	2202	2504	14096	92	56
35	20433	1544	6272	1380	2638	3035	14868	92	73
36	21128	1580	6113	2634	3986	2809	17124	93	81
37	19665	1815	6700	1888	2089	2972	15464	91	79
<b>Config 4</b>	<b>21516</b>	<b>1745</b>	<b>5831</b>	<b>1887</b>	<b>3652</b>	<b>2719</b>	<b>15834</b>	<b>92</b>	<b>74</b>
<b>Overall</b>	<b>22620</b>	<b>2178</b>	<b>7096</b>	<b>2688</b>	<b>2927</b>	<b>3270</b>	<b>18159</b>	<b>91</b>	<b>80</b>

In Figure 3.6 and Table 3.5 it can be seen that the average COD mass balance over the entire investigation period was 80 %. Although lower than 100 %, this value is significantly below the COD mass balances in other investigations with nutrient removal systems namely Pilson *et al* (1995) 84 % and 94 %, Sneyders *et al* (1998) 92 % and 92 % and Hu *et al* (1999) 91 %. The main reason why the COD balance is lower in this investigation than in other investigations is the sludge spillages that occurred in the system in particular during Configurations 2 and 4.

Looking at Figure 3.5 it can be seen that the largest contribution to the COD balance is made by the waste sludge (31%) leaving the system. This is followed by the oxygen utilised and denitrification both at 13 and 14 % respectively. This result is interesting in that it shows that nearly the same amount of COD was utilised with nitrate as electron acceptor as was utilised with oxygen as electron acceptor. However, this is in part due to the dosing of nitrate to the anoxic reactor which increased the TKN/COD ratio of the wastewater from around 0.09 to 0.14. The 12% COD utilized in the external nitrification system is surprisingly low in comparison to the 15 % (with no larvae infestation) observed by Hu et al., (1999). 10 % of the COD leaves the system via the final effluent, and 20 % is unaccounted for.

From Table 3.5, the system's COD removal efficiency was very good over the entire investigation period with an average COD removal of 91%. The influent COD concentration ranged between 575 and 846 with a mean of 691 mgCOD/l. The unfiltered effluent COD concentration ranged between 21 and 101 with a mean of 64 mgCOD/l. The filtered effluent COD concentration was measured by either filtering through a 0.45 $\mu$ m Schleicher & Schüll membrane filter or first flocculating the unfiltered effluent using 10ml/l effluent 0.25M aluminum sulphate solution and then filtering the effluent in the same manner as described above. The average floc-filtered effluent COD concentration ranged between 20 and 100 with a mean of 41 mgCOD/l. The 0.45 $\mu$ m membrane filtered effluent COD (non-flocculated) concentration ranged between 26 and 73 with a mean of 50 mgCOD/l. This value was accepted to correspond to the unbiodegradable soluble COD in the influent and gives an average unbiodegradable soluble COD fraction ( $f_{s,us}$ ) of 0.073. Figure 3.6 shows the systems mean unfiltered influent and effluent concentrations for the 37 sewage batches and shows that the COD removal performance of the system was not only good, but also stable throughout the investigation.

The low oxygen demand in the system is reflected in the low OUR in the aerobic reactor namely 36 mgO/(l.h) in ~20 % of the system volume. This is because the nitrification OUR no longer needs to be supplied in the suspended medium system and the nitrate produced "free" in the external nitrification system reduces the carbonaceous OUR. Nitrate dosing to the main anoxic reactor reduced the carbonaceous OUR further by 1.42 mgO/(l.h) per 1mgNO<sub>3</sub>-N/l influent dosed. The OUR in an equivalent internal nitrification BNRAS system with 20 % aerobic mass fraction, 90% COD balance, 10 day sludge age, complete nitrification, 90 % nitrate denitrification leading to a 50 % recovery in nitrification OUR is about 2 times higher at ~ 75 mgO/(l.h). Thus, not

nitrifying in the BNRAS system but rather utilising an external nitrifier to generate nitrate, clearly leads to a significant decrease in the OUR in the BNRAS system.

### 3.3.1 The Effect of Different Configurations on COD Balance and Removal

For each Configuration i.e. 1, 2, 3, and 4, the average COD mass balance and removal performance shown in Table 3.5 were calculated from the sewage batch means fed to system during each configuration. The initial BNRAS system (configuration 1) had a reasonable COD mass balance of 90 % and a COD removal of 94 %. As can be seen in Table 3.5 and Figure 3.5, sewage batches 2 and 3 are characteristic of a high COD concentration in the waste flow which accounts for the good COD mass balance and COD removal in Configuration 1. These results are similar to the results of Hu *et al.* (1999), who conducted investigations into external nitrification in BNRAS systems with small aerobic mass fractions i.e. Configuration 1. Hu *et al.* (1999) obtained a COD balance of 89% and a COD removal of 92% in the BNRAS system shown in Figure 3.1 and design and operating parameters listed in Table 3.1, Configuration 1.

With a significant number of changes as well as the ongoing problems with *Psychoda* infestations causing poor nitrification and sludge spillages, the Configuration 2 yielded an 80 % COD mass balance. Examining the UCT system results (Appendices D and E), it can be seen in Figure E2 that initially a good COD mass balance was obtained in the UCT system but as the investigation progressed poorer COD mass balances were obtained due to frequent sludge spillages. The average COD mass balance for the UCT system was also 80%. Thus the poor performance of the external nitrification system at this stage in the investigation was not due to the system characteristics but due to general system operational problems perhaps caused by the influent wastewater characteristics.

The Configuration 3 showed some improvement with the COD balance increasing to an average of 91 % mainly due to less frequent sludge spillages. However, while the system showed improvement in the COD balance, the system was still experiencing the same problem as Configuration 2 i.e. low external nitrification, but due to the larger aerobic mass fraction Configuration 3 had high internal nitrification (in the main aerobic reactor). However, the impact of this on the BEPR was not too large due to the 1:1 a-recycle ratio from the aerobic to the anoxic reactor and the reduced nitrate dose to the anoxic reactor.

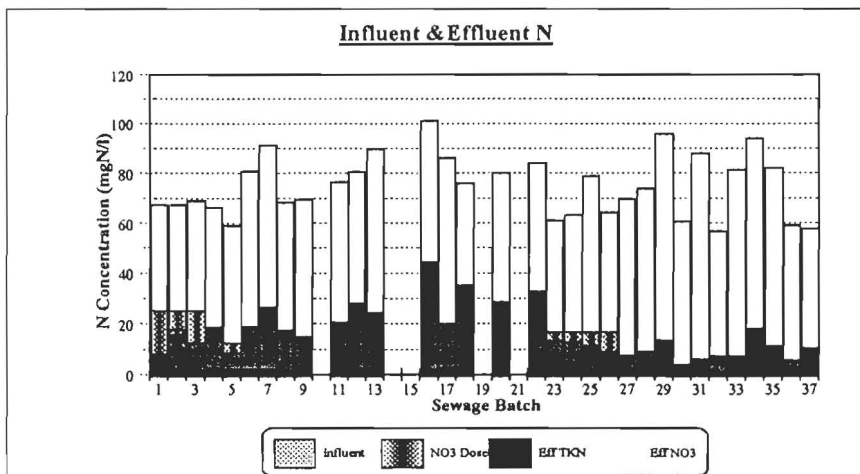
Configuration 4 showed a marked decrease in COD balance to 80%, again the result of frequent (2/3 per week) sludge spillages. However, the internal nitrification (in the main aerobic reactor) was reduced due to the replacement of the stone column external nitrification system with a suspended medium activated sludge system with resultant improved external nitrification performance.

### 3.4 NITROGEN REMOVAL AND MASS BALANCE PERFORMANCE

#### 3.4.1 Influent and Effluent Nitrogen Concentrations

For the 37 sewage batches, the nitrogen components in the influent and effluent flows are shown in Figure 3.7 below. It can be seen that the influent TKN concentration varied between 56 and 101 mgN/l and the dosed nitrate concentration between 0 and 25 mg NO<sub>3</sub>-N/l influent. This yielded a range of influent TKN/COD ratios between 0.06 to 0.17 mgN/mgCOD for this investigation. This influent TKN/COD range is wide and embraces most raw and settled wastewaters and demonstrates that the system is robust and well suited to unfavorable influent TKN/COD ratios while still ensuring (i) good BEPR and (ii) a low effluent N concentration. Indeed, the system requires high influent TKN/COD ratios to ensure a sufficiently high nitrate load on the main anoxic reactor to stimulate anoxic P uptake (see Section 3.5 below). From Figure 3.7 it can be seen that the N removal performance varied substantially over the investigation period. The effluent nitrogen concentration (TKN + NO<sub>2</sub> + NO<sub>3</sub>) varied between 8 and 47 mgN/l with an average of 23 mg/l. This translates to a N removal performance which varied between 36 and 89 % and an average of 72%. The low 36% removal occurred in sewage batch 16 and is result of the lag in the recovery of the system to the toxic sewage feed in batches 14 and 15. The overall low N removal performance was due to the generally poor external nitrification performance, discussed in Section 3.4.3 below.

**Figure 3.7:** Average sewage batch influent and effluent nitrogen concentrations.



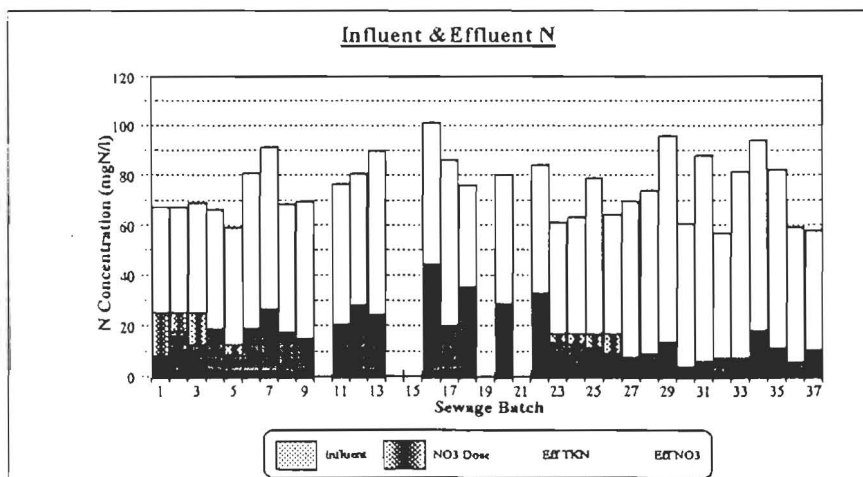
Configuration 4 showed a marked decrease in COD balance to 80%, again the result of frequent (2/3 per week) sludge spillages. However, the internal nitrification (in the main aerobic reactor) was reduced due to the replacement of the stone column external nitrification system with a suspended medium activated sludge system with resultant improved external nitrification performance.

### 3.4 NITROGEN REMOVAL AND MASS BALANCE PERFORMANCE

#### 3.4.1 Influent and Effluent Nitrogen Concentrations

For the 37 sewage batches, the nitrogen components in the influent and effluent flows are shown in Figure 3.7 below. It can be seen that the influent TKN concentration varied between 56 and 101 mgN/l and the dosed nitrate concentration between 0 and 25 mg NO<sub>3</sub>-N/l influent. This yielded a range of influent TKN/COD ratios between 0.06 to 0.17 mgN/mgCOD for this investigation. This influent TKN/COD range is wide and embraces most raw and settled wastewaters and demonstrates that the system is robust and well suited to unfavorable influent TKN/COD ratios while still ensuring (i) good BEPR and (ii) a low effluent N concentration. Indeed, the system requires high influent TKN/COD ratios to ensure a sufficiently high nitrate load on the main anoxic reactor to stimulate anoxic P uptake (see Section 3.5 below). From Figure 3.7 it can be seen that the N removal performance varied substantially over the investigation period. The effluent nitrogen concentration (TKN + NO<sub>2</sub> + NO<sub>3</sub>) varied between 8 and 47 mgN/l with an average of 23 mg/l. This translates to a N removal performance which varied between 36 and 89 % and an average of 72%. The low 36% removal occurred in sewage batch 16 and is result of the lag in the recovery of the system to the toxic sewage feed in batches 14 and 15. The overall low N removal performance was due to the generally poor external nitrification performance, discussed in Section 3.4.3 below.

**Figure 3.7:** Average sewage batch influent and effluent nitrogen concentrations.



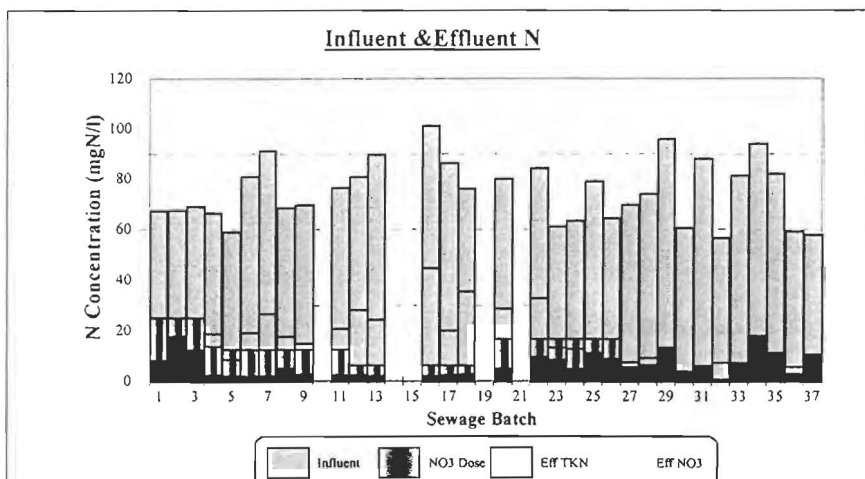
Configuration 4 showed a marked decrease in COD balance to 80%, again the result of frequent (2/3 per week) sludge spillages. However, the internal nitrification (in the main aerobic reactor) was reduced due to the replacement of the stone column external nitrification system with a suspended medium activated sludge system with resultant improved external nitrification performance.

### 3.4 NITROGEN REMOVAL AND MASS BALANCE PERFORMANCE

#### 3.4.1 Influent and Effluent Nitrogen Concentrations

For the 37 sewage batches, the nitrogen components in the influent and effluent flows are shown in Figure 3.7 below. It can be seen that the influent TKN concentration varied between 56 and 101 mgN/l and the dosed nitrate concentration between 0 and 25 mg NO<sub>3</sub>-N/l influent. This yielded a range of influent TKN/COD ratios between 0.06 to 0.17 mgN/mgCOD for this investigation. This influent TKN/COD range is wide and embraces most raw and settled wastewaters and demonstrates that the system is robust and well suited to unfavorable influent TKN/COD ratios while still ensuring (i) good BEPR and (ii) a low effluent N concentration. Indeed, the system requires high influent TKN/COD ratios to ensure a sufficiently high nitrate load on the main anoxic reactor to stimulate anoxic P uptake (see Section 3.5 below). From Figure 3.7 it can be seen that the N removal performance varied substantially over the investigation period. The effluent nitrogen concentration (TKN + NO<sub>2</sub> + NO<sub>3</sub>) varied between 8 and 47 mgN/l with an average of 23 mg/l. This translates to a N removal performance which varied between 36 and 89 % and an average of 72%. The low 36% removal occurred in sewage batch 16 and is result of the lag in the recovery of the system to the toxic sewage feed in batches 14 and 15. The overall low N removal performance was due to the generally poor external nitrification performance, discussed in Section 3.4.3 below.

**Figure 3.7:** Average sewage batch influent and effluent nitrogen concentrations.

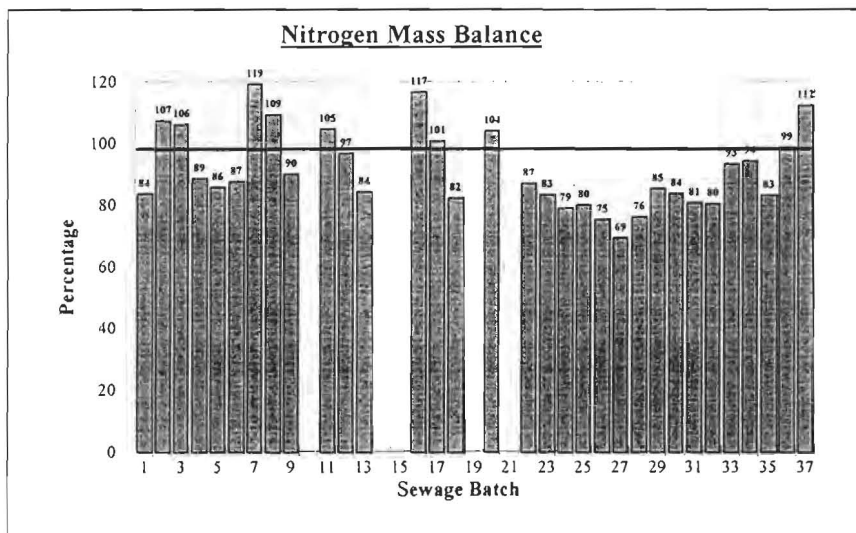


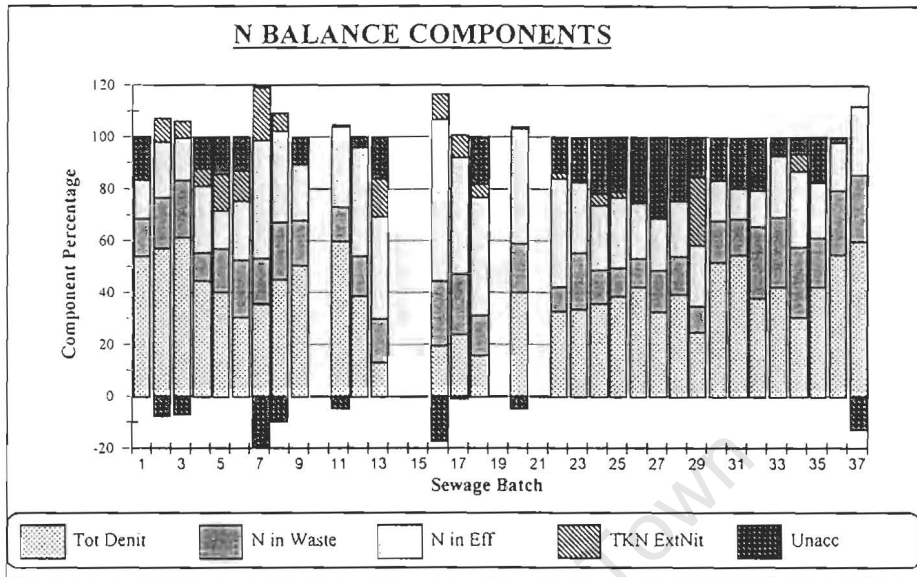
### 3.4.2 Nitrogen Mass Balance

Similarly to the COD mass balance, Nitrogen mass balances (for details see Appendix B) were performed on the system for the 32 sewage batches analyzed. Again, the averages of the measured parameters of each of the sewage batches as well as the averages for the 4 different system configurations calculated as averages of the sewage batches are listed in Appendix C.

In the Nitrogen balance, the Nitrogen entering the system via the influent flow and nitrate dose is reconciled with the Nitrogen leaving the system via the (i) the final TKN and  $\text{NO}_x$  ( $\text{NO}_2 + \text{NO}_3$ ) in the effluent flow (ii) N in the sludge wasted (iii) nitrate and nitrite denitrified and (iv) N removed in the external nitrification system. The N mass balance was calculated by separate determination of the net production or reduction of nitrate and nitrite in each reactor and each settling tank by means of a reactor nitrite and nitrate mass balance. This was done by subtracting the mass of nitrate or nitrite entering the reactor from that leaving the reactor, so that a negative value indicates a net reduction (i.e. denitrification) and a positive value indicates net production (i.e. nitrification). Details of the mass balance calculation procedure are given in Appendix B. The reliability of the experimental data is directly proportional to the mass balance deviation from 100%. This implies that the closer the N balance to 100 % the more reliable the data. The results of the Nitrogen mass balance and its components are given in Table 3.6 and are shown plotted in Figures 3.8 and 3.9 respectively.

**Figure 3.8:** Nitrogen mass balance for BNRAS system for 37 sewage batches



**Figure 3.9:** Nitrogen mass balance components of BNRAS for 37 sewage batches

In Figure 3.8 (and Table 3.6) it can be seen that the average N mass balance over the entire investigation period was 91 %. Although lower than 100 %, this value is similar to N mass balances in other investigations with nutrient removal systems namely Pilson *et al.* (1995) 99 % and 94 %, Sneyders *et al.* (1998) 88 % and 90 % and Hu *et al.* (1999) 86 %.

From Figure 3.9 it can be seen that in the investigation overall, the largest contribution the N balance is made by the nitrate and nitrite denitrified in the main and pre-anoxic reactors of 38%. The reason for such a high denitrification N removal is the large main anoxic reactor volume and the dosing of nitrate during the investigation in order to realize this reactors full denitrification potential. The next largest contribution to the N balance is the N that leaves the system via the final effluent (30%) of which 25 % is TKN and 5% nitrate. The high N in the effluent is as a result of the poor nitrification performance of the stone column external nitrification system because of the 25% TKN, 80% is FSA (20% of influent N) and 20% Organic N (5% of influent). Unlike in the COD balance where the largest fraction of COD leaves the system in the wasted sludge, the nitrogen in the wasted sludge only accounts for 18% of the N leaving the system. Of this, 15% is TKN and 3% nitrate. Finally, 5% of the influent N was removed in the external nitrification system leaving 9% unaccounted for.

Table 3.6: Components of Nitrogen mass balance

Average of Batch	Total Denitrification mgN/d	N in Waste mgN/d	N in Effluent mgN/d	TKN ExtNit mgN/d	Total TKN Out mgN/d	Inf TKN mgN/d	Nitrate dose mgN/d	MB %	N Removal %
1	1000	279	262	0	1541	1345	500	84	91
2	1061	361	397	162	1982	1349	500	107	97
3	1161	408	312	111	1992	1378	500	106	95
<b>Config 1</b>	<b>1074</b>	<b>349</b>	<b>324</b>	<b>91</b>	<b>1838</b>	<b>1357</b>	<b>500</b>	<b>99</b>	<b>95</b>
4	1450	341	833	214	2837	2704	500	89	72
5	1160	478	425	385	2448	2356	500	86	85
6	1162	821	838	448	3268	3237	500	87	76
7	1501	734	1865	835	4935	3646	500	119	49
8	1360	642	1050	182	3233	2461	500	109	66
9	1665	572	714	0	2951	2781	500	90	78
11	2153	458	1108	0	3720	3058	500	105	67
12	1364	533	1465	0	3362	3231	250	97	55
13	510	644	1538	536	3228	3584	250	84	59
16	579	746	1844	265	3435	2697	250	117	34
17	725	714	1358	234	3031	2759	250	101	53
18	528	518	1499	158	2704	3043	250	82	53
20	1177	557	1280	0	3015	2402	500	104	52
<b>Config 2</b>	<b>1180</b>	<b>600</b>	<b>1212</b>	<b>271</b>	<b>3263</b>	<b>2959</b>	<b>400</b>	<b>97</b>	<b>61</b>
22	1017	275	1260	75	2628	2528	500	87	61
23	797	502	641	0	1940	1834	500	83	78
24	862	325	604	97	1888	1898	500	79	76
25	111	325	778	70	2287	2367	500	80	81
<b>Config 3</b>	<b>947</b>	<b>357</b>	<b>821</b>	<b>61</b>	<b>2185</b>	<b>2157</b>	<b>500</b>	<b>82</b>	<b>57</b>
26	1042	266	518	0	1825	1929	500	75	86
27	701	335	410	0	1446	2091	-	69	89
28	882	882	323	482	1686	2221	-	76	88
29	718	303	677	754	2452	2876	-	85	91
30	949	297	272	0	1518	1817	-	84	92
31	1464	362	300	0	2126	2640	-	81	96
32	648	478	239	0	1365	1699	-	80	87
33	1047	665	651	0	2273	2438	-	93	86
34	875	763	838	180	2657	2851	-	94	89
35	1061	467	514	0	2042	2462	-	83	93
36	982	439	327	0	1748	1772	-	99	86
37	1039	450	453	0	1942	1729	-	112	86
<b>Config 4</b>	<b>951</b>	<b>429</b>	<b>466</b>	<b>78</b>	<b>1923</b>	<b>2208</b>	<b>42</b>	<b>86</b>	<b>88</b>
<b>Overall</b>	<b>1055</b>	<b>481</b>	<b>802</b>	<b>147</b>	<b>2484</b>	<b>2257</b>	<b>443</b>	<b>91</b>	<b>75</b>

### 3.4.3 The Effect of Different Configurations on Nitrogen Balance

Configuration 1 had an excellent average nitrogen mass balance of 99 %. With the significant number of changes as well as a number of ongoing problems, Configuration 2 yielded a 97 % N mass balance. This high value is unusual as the second configuration was beset with sludge spillages, as well as *Psychoda* infestation, which generally had a significant adverse affect on the COD mass balance of the system. It also should be noted that Configuration 2 was the period in which the greatest percentage of nitrogen could not be accounted for, as shown in Figure 3.9. The negative values plotted for the unaccounted nitrogen implies a N mass balance of greater than 100%, which increased the average value of the nitrogen mass balance over this period. From Figure E5<sup>4</sup>, it can be seen that a good N mass balance was also obtained in the UCT system at this stage in the investigation i.e. days 4 to 161. It can also be seen in Figure E5 that sewage batches 14,15,16 and 19 had extremely high N mass balances due to the poor influent wastewater characteristics and were omitted in the average N mass balance calculation. The average N mass balance for the UCT system was 99%.

Configuration 3 showed a decline in the nitrogen balance to an average of 82 %. This decrease in the nitrogen mass balance was due to the system still experiencing sludge spillage problems and low external nitrification. The reasons for the poor external nitrification performance were the persistent *Psychoda* infestation in the stone column and the high flow rate through the stone column placing the nitrification process under considerable strain leading to significantly reduced nitrification efficiency in the stone column, which in turn reduced the denitrification in the main anoxic reactor. The problem of poor external nitrification was overcome by increasing the nitrate dose from 8.3 mgNO<sub>3</sub>-N/l to 16.6 mgNO<sub>3</sub>-N/l influent to the anoxic reactor.

The *Psychoda* infestation and the frequent sludge spillages did not allow the system to reach steady state with respect to nitrification and denitrification and this is evident in Figure 3.10, where it can be seen that from sewage batches 13 to 25 the nitrification and consequently denitrification were the poorest recorded in the investigation. With the change from a fixed

---

<sup>4</sup> During the same time as this investigation, a control conventional UCT system was operated in parallel receiving the same sewage batches (and numbered identically) as the external nitrification system of this investigation. The results of the external nitrification system are compared with this UCT system. The day to day data of this UCT system are given in Appendix D and the systems operating and design parameters and data evaluation in Appendix E.

media external nitrification system to a suspended external activated sludge nitrification system the problem of *Psychoda* infestation was overcome and Configuration 4 (sewage batches 26 to 37) showed an increase in the nitrogen mass balance to 86%. This system also showed a significant improvement in external nitrification and improved internal denitrification (Fig 3.10).

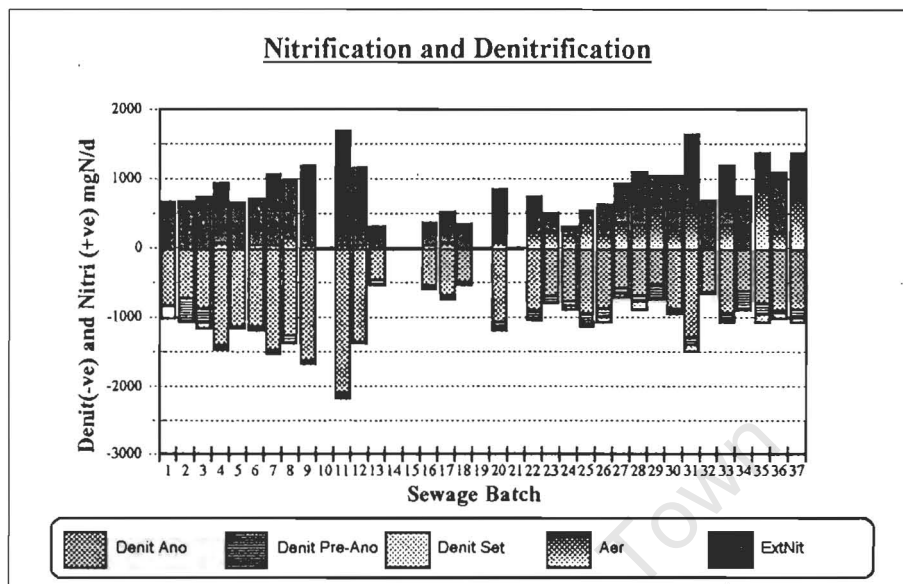
#### 3.4.4 Nitrification

In this system, nitrification was achieved externally in the external fixed media/suspended nitrification system. The BNRAS effluent free and saline ammonia (FSA) was thus controlled by (i) the flow to the external nitrifier and (ii) the efficiency of the external nitrification system. This can be seen in Table 3.7 and Figure 3.10, which gives the nitrate + nitrite ( $\text{NO}_x$ ) mass balance results over the aerobic, main and pre-anoxic reactors as well as the external nitrification system. In the investigation overall, 73% of the nitrate generated was produced by the external nitrification system while 27% was produced by nitrification of the residual ammonia in the aerobic reactor. Pumping an average of only 76% of the anaerobic overflow to the external nitrification system meant that at best nitrification could be 76% complete if the external nitrification systems FSA concentration was zero. On the measured results, the average nitrification efficiency was 51% i.e. the 73% nitrate generated in the external nitrification system was as a result of a nitrification efficiency of only 51% by the external nitrification system. An average N mass of 147 mgN/d (4.9 mgN/l at 30 l/d influent flow) was removed in the external nitrifier for 'biofilm' growth. However, this average value may not be representative of the N requirement for biofilm growth since it includes Configuration 2 where the average N removed is 261 mg/d and coincides with the period when the larvae infestation was at its worst. The N removal in the external nitrifier of Configurations 1, 3 and 4 were 91, 61 and 78 mgN/d respectively. From this it can be deduced that a far lower N requirement is needed for biofilm growth and maintenance than the 147 mgN/l average value, because in only 17 of the 32 sewage batches was a N removal observed across the external nitrifier.

**Table 3.7:** Nitrate and Nitrite mass balances across each reactor and settler.

Average of Sewage Batch	Nitrification (mgNO <sub>3</sub> -N)/d		Denitrification (mgNO <sub>3</sub> -N)/d			
	Main Aerobic	Ext Nitrifier	Main Anoxic	Pre-Anoxic	Anaerobic	Final Settler
1		667	-838	-153	-9	
2		673	-726	-316	-19	
3		738	-869	-212	-21	-60
<b>Config 1</b>	<b>0</b>	<b>693</b>	<b>-811</b>	<b>-227</b>	<b>-16</b>	<b>-20</b>
4	73	860	-1401	-39		
5		652	-1124	-37		
6	61	651	1128	-34		
7	60	1004	-1463	-26		-12
8	184	803	-1259	-97		-4
9	52	1133	-1615	-50		
11	44	1650	-2089	-43		-21
12	44	1119	-1351	-8		-5
13	24	283	-470	-39		
16	59	309	-539	-24		-16
17	69	452	-868	-31		-8
18	34	309	-493	-35		
20	91	748	-1076	-65		
<b>Config 2</b>	<b>66</b>	<b>767</b>	<b>-1135</b>	<b>-39</b>		<b>-7</b>
22	222	515	-900	-114	-3	
23	268	232	-687	-110		
24	195	116	-773	-71		-18
25	413	124	-940	-166		-8
<b>Config 3</b>	<b>275</b>	<b>247</b>	<b>-825</b>	<b>-115</b>	<b>-3</b>	<b>-9</b>
26	211	414	-883	-115		-44
27	396	534	-579	-80		-42
28	356	744	-688	-88		-105
29	570	479	-521	-196		
30	274	767	-872	-58		-19
31	550	1090	-1293	-99		-72
32	16	670	-628	-6		-14
33	366	825	-936	-111		
34		749	627	-248		
35	901	472	-788	-166		-107
36	262	833	-896	-42		-44
37	790	586	-889	-122		-28
<b>Config 4</b>	<b>443</b>	<b>680</b>	<b>-800</b>	<b>-111</b>		<b>40</b>
<b>Overall</b>	<b>244</b>	<b>663</b>	<b>-938</b>	<b>-94</b>	<b>-3</b>	<b>22</b>

**Figure 3.10 :** Nitrification and Denitrification in the BNRAS system (nitrification is plotted as +ve and denitrification as -ve)



### 3.4.5 Denitrification

The calculation of the denitrification potential for the completely mixed anoxic reactor is not possible unless the anoxic reactor receives a nitrate load greater than its denitrification potential i.e. only when the anoxic reactor is overloaded and nitrate and/or nitrite ( i.e.  $>1\text{mgNO}_3\text{-N/l}$ ) flows out of the anoxic reactor. Under this circumstance, the denitrification performance is equal to its denitrification potential i.e. the maximum nitrate/nitrite load that can be denitrified. If the anoxic reactor is under-loaded (i.e.  $<1\text{mgNO}_3\text{-N/l}$ ), then negligible quantities of  $\text{NO}_3$  will leave this reactor and although the denitrification performance can be calculated, this would be less than the denitrification potential. The  $\text{NO}_3$  concentrations exiting the anoxic reactors of the external nitrification system and UCT control systems were at times greater than  $1\text{mgNO}_3\text{-N/l}$  and therefore allowed the denitrification potential and hence the specific denitrification rate,  $K_2'$ , to be calculated. In this investigation the nitrate reduction rate and the nitrate denitrification rate are considered to be equal because nitrite was not observed at significantly high concentrations as to effect major differences in the two above mentioned rates. The difference between nitrate reduction rate and nitrate denitrification rate is that in the former, the product is nitrite i.e. ionic and with the latter the product is  $\text{N}_2$  i.e. gaseous. Nitrate reduction is therefore regarded as the rate of disappearance of nitrate from the mixed liquor while accepting only two electrons to form nitrite. Nitrate denitrification is the rate of nitrate disappearance from the mixed liquor whilst accepting five electrons to form  $\text{N}_2$  gas.

Stern and Marais (1974) found that when the nitrate versus time slopes [ $\text{mgNO}_3\text{-N}/(\text{l.d})$ ] were divided by the VSS concentration to obtain specific denitrification rates [ $\text{mgNO}_3\text{-N}/(\text{mgVSS.d})$ ], a decrease in the rate was observed as sludge age increased. When however, the slopes were divided by the Active VSS concentration, they were found to be independent of sludge age (i.e.  $\text{mgNO}_3\text{-N}/(\text{mgAVSS.d})$ ). They concluded that this was because the Active VSS relates the biological rate of denitrification to the particular component of the VSS mass that is responsible for this rate. This approach has been found to work reasonably well for N removal plants, because from a modeling perspective, the active mass (AVSS) comprises only one heterotrophic organism group i.e. “ordinary” heterotrophic organisms (OHOs) (Ekama and Wentzel, 1999). However, for N and P removal plants, the active heterotrophic organism mass comprises two distinct active heterotrophic organism groups namely, (1) the OHOs mentioned above and (2) the polyphosphate accumulating organisms (PAOs) which effect the biological excess P removal.

In earlier research on biological N and P removal systems, the PAO group was observed not to contribute significantly to denitrification and most of the P uptake was confined to the aerobic reactor (Wentzel *et al.*, 1990; Ekama and Wentzel, 1999). However, over the past 5 years significant P uptake has been observed indicating that under these conditions the PAOs may be contributing to the denitrification in the anoxic reactor (Kerrn-Jesspersen and Henze, 1993; Kuba *et al.*, 1993). Also significant P uptake has been observed in external nitrification systems by Sorm *et al.* (1996) and Hu *et al.* (1999). Sorm *et al.* (1996) found from anoxic batch tests of an external nitrification BNRAS system that P uptake with simultaneous denitrification occurred and they concluded that the observed  $\text{NO}_3\text{-N}$  reduction could also include a contribution by the OHO denitrifiers. However, they observed that the phosphate uptake ceased when  $\text{NO}_3\text{-N}$  was reduced to zero in the mixed liquor. This behaviour is expected because when nitrate is no longer available as an electron acceptor utilization of internally stored PHB by the PAOs can no longer continue, resulting in a cessation of P uptake by them.

For this investigation it was decided that, because the PAOs do participate in the denitrification process when anoxic P uptake takes place, the OHO and PAO contribution to the denitrification in the anoxic reactor should be separated in the same manner so that, the appropriate nitrate removal rates due to the OHO mass could be specified in terms of only the OHO mass i.e. due cognizance must be taken of the contribution of the PAOs to the nitrate removal rate. To do this, the measured nitrate removal rate (i.e. denitrification potential) was adjusted by an amount which

was speculated to be the contribution by the denitrifying PAOs. The adjustment was made by reducing the measured nitrate removal rate by the product of the observed anoxic P uptake (expressed as a percentage of the total P uptake) and the nitrate equivalent of the COD sequestered<sup>5</sup> by the PAOs. This manipulation of the nitrate removal rate assumes that; (1) the stoichiometry and metabolic processes of the PAOs are the same under both aerobic and anoxic conditions and (2) the percentage anoxic P uptake is directly proportional to the denitrification performance of the PAOs i.e. all the PAOs responsible for anoxic P uptake are also responsible for the contribution made to the nitrate removal. This adjustment was necessary in order to compare previously observed denitrification rates (i.e.  $K_2'$ ) in NDBEPR systems in which the P uptake took place under aerobic conditions only (i.e.  $K_2'$  rate due to OHOs only). The adjusted denitrification rate ( $K_2''$ ) can therefore be specified in terms of only the active ordinary heterotrophic mass [i.e.  $\text{mgNO}_3\text{-N}/(\text{mgOHOAVSS}\cdot\text{d})$ ]. The denitrification rate ( $K_2'$ ) without adjustment was also calculated to be able to compare the  $K_2'$  rates with those reported by Ekama and Wentzel (1999), who did not make this adjustment to the nitrate removal rate. The nitrate removal rate, adjusted for PAO activity or not, is divided by the mass of VSS ( $\text{mgVSS}$ ) in the system divided by the influent flow ( $Q_i$ , l/d) i.e.  $\text{mgVSS}/\text{l}$  influent and the OHO active fraction of the VSS mass  $f_{\text{av,OHO}}$  where the  $f_{\text{av,OHO}}$  is calculated from the BEPR model of Wentzel *et al.*, (1990) viz:-

$$K_2' \text{ or } K_2'' = \frac{D_p - f_{\text{PAOs}} * (\% \text{AnoP}_{\text{up}} * S_{\text{seq}} / 8.6)}{(X_v \cdot f_{\text{av,OHO}} \cdot f_{x1})} \quad \text{mgNO}_3\text{-N}/(\text{mgAVSS}\cdot\text{l inf}) \quad (3.1)$$

where: $D_p$	=	Denitrification potential (measured) $\text{mgN}/\text{l}$ influent
$f_{\text{PAOs}}$	=	1 when denitrification by PAOs is considered ( $K_2''$ ) and
$f_{\text{PAOs}}$	=	0 when denitrification by PAOs is ignored ( $K_2'$ )
$\% \text{AnoP}_{\text{up}}$	=	Percentage Anoxic P uptake
$S_{\text{seq}}$	=	COD sequestered by PAOs $\text{mgCOD}/\text{l}$ influent
$X_v$	=	VSS mass in system per l influent
$f_{\text{av,OHO}}$	=	OHO fraction of VSS mass (see Section 3.5.3.1 below for calculation method)
$f_{x1}$	=	Anoxic sludge mass fraction

<sup>5</sup> The COD sequestered by the poly-P organisms is calculated using the model of Wentzel *et al.*, (1990)

$$8.6^6 = \text{mgCOD utilized per mgNO}_3\text{-N denitrified.}$$

$$= (1-f_{cv} Y_H)/2.86 \text{ where}$$

$$2.86 = \text{oxygen equivalent of nitrate as electron acceptor}$$

Using Equation (3.1) and substituting the appropriate sewage batch average values of the measured parameters, the denitrification rates were calculated for the sewage batches in which the nitrate concentrations leaving the main anoxic reactor were greater than 1mgNO<sub>3</sub>-N/l. The denitrification rates are shown listed in Table 3.8 below.

**Table 3.8** Calculated denitrification rates for sewage batches with > 1mgNO<sub>3</sub>-N/l in the main anoxic reactor outflow.

Sewage Batch	Dp mgNO <sub>3</sub> -N/l	%Ano P up	Seq mgCOD/l	Dp mgNO <sub>3</sub> -N/l	f <sub>xi</sub>	X <sub>aoHO</sub> mgAVSS/l	K <sub>2</sub> <sup>o</sup> mgNO <sub>3</sub> -N/mgOHOAVSS	K <sub>2</sub> <sup>o</sup> HO 0.0987	X <sub>PAO</sub> mgAVSS/l	K <sub>2</sub> <sup>o</sup> PAO 0.0465
1	42	0.64	64	37	0.50	751	0.1115	0.0987	207	0.0465
2	36	0.65	59	32	0.50	475	0.1528	0.1339	191	0.0471
3	43	0.78	56	38	0.50	612	0.1419	0.1252	181	0.0563
8	31	0.50	78	27	0.45	553	0.1265	0.1083	212	0.0475
11	52	0.31	84	49	0.45	583	0.1992	0.1877	230	0.0291
12	34	0.62	69	29	0.45	520	0.1445	0.1233	187	0.0587
13	12	0.35	83	8	0.45	537	0.0486	0.0347	226	0.0331
18	12	0.31	60	10	0.45	595	0.0460	0.0379	193	0.0252
20	36	0.43	77	32	0.30	536	0.2230	0.1989	248	0.0522
22	30	0.35	38	28	0.30	358	0.2793	0.2647	123	0.0427
23	23	0.20	65	21	0.30	589	0.1296	0.1212	208	0.0238
25	31	0.60	52	28	0.30	466	0.2240	0.1983	166	0.0720
26	29	0.46	60	26	0.30	744	0.1318	0.1173	193	0.0557
27	19	0.29	56	17	0.30	810	0.0795	0.0717	179	0.0350
28	23	0.37	43	21	0.30	657	0.1163	0.1069	139	0.0446
29	17	0.50	78	13	0.30	636	0.0911	0.0675	249	0.0603
31	43	0.46	104	38	0.30	885	0.1623	0.1414	333	0.0555
33	31	0.49	84	26	0.30	732	0.1421	0.1203	270	0.0591
34	21	0.62	91	14	0.30	868	0.0803	0.0550	292	0.0753
35	26	0.57	81	21	0.30	691	0.1267	0.1006	261	0.0691
<b>Average 1</b>	<b>41</b>	<b>0.69</b>	<b>60</b>	<b>36</b>	<b>0.50</b>	<b>613</b>	<b>0.1354</b>	<b>0.1193</b>	<b>193</b>	<b>0.0499</b>
Averages above are for sewage batches 1 to 3 i.e. Configuration 1										
<b>Average 2</b>	<b>28</b>	<b>0.45</b>	<b>64</b>	<b>25</b>	<b>0.45</b>	<b>544.81</b>	<b>0.1130</b>	<b>0.0984</b>	<b>178</b>	<b>0.0387</b>
Averages above are for sewage batches 4 to 19 i.e. Configuration 2										
<b>Average 3</b>	<b>27</b>	<b>0.43</b>	<b>64</b>	<b>24</b>	<b>0.30</b>	<b>536.89</b>	<b>0.2110</b>	<b>0.1947</b>	<b>205</b>	<b>0.0461</b>
Averages above are for sewage batches 22 to 25 i.e. Configuration 3										
<b>Average 4</b>	<b>27</b>	<b>0.43</b>	<b>76</b>	<b>22</b>	<b>0.30</b>	<b>729.55</b>	<b>0.1163</b>	<b>0.0976</b>	<b>245</b>	<b>0.0568</b>
Averages above are for sewage batches 26 to 37 i.e. Configuration 4										
<b>Average 5</b>	<b>29</b>	<b>0.46</b>	<b>68</b>	<b>25</b>	<b>0.38</b>	<b>611.85</b>	<b>0.1379</b>	<b>0.1207</b>	<b>208</b>	<b>0.0494</b>
Averages above are for sewage batches 1 to 37 i.e. average over entire investigation.										

<sup>6</sup>It is recognized that the bioenergetics of aerobic metabolism is not the same as anoxic metabolism because under aerobic conditions the organisms obtain 3 moles ATP per e<sup>-</sup> equivalent whereas under anoxic conditions they obtain only 2 ATP per e<sup>-</sup> equivalent (Payne, 1981). This changes the Y<sub>H</sub> coefficient from a theoretical 0.42 mgVSS/mgCOD for aerobic conditions to 0.35 mgVSS/mgCOD for anoxic conditions i.e. 83% of the aerobic value. Accepting the Y<sub>H</sub> = 0.45 mgVSS/mgCOD, the COD/VSS ratio (f<sub>cv</sub>) as 1.48 mgCOD/mgVSS and the same reduction in yield makes the COD utilized per mgNO<sub>3</sub>-N denitrified 6.4 under anoxic conditions compared to 8.6 mgCOD/mg NO<sub>3</sub>-N under aerobic conditions.

**Table 3.9** Comparison of anoxic denitrification rates  $K_2'$  at 20°C obtained by Clayton *et al.* (1989), Musvoto *et al.* (1992), Pilson *et al.* (1995) and Sneyders *et al.* (1998) with those obtained in this investigation.

System	Nitrate Denitrification Rate $K_2'$			$f_{S,up}$	Active ( $f_{av,OHO}$ )
	Mean	Max	Min		
Clayton (1989)	0.255	-	-	0.150	0.210
Musvoto (1992)	0.335	0.517	0.193	0.287	0.130
Pilson (1995)	0.181	0.300	0.111	0.111	0.327
Mellin (1995)	0.254	0.410	0.150	0.140	2.880
Sneyders CTL (1998)	0.071	0.088	0.050	0.062	0.435
Without adjustment ( $K_2'$ )	0.138	0.274	0.046	0.115	0.497
With adjustment ( $K_2''$ )	0.121	0.265	0.035	0.115	0.497

Table 3.9 shows a comparison between the denitrification rates ( $K_2'$ ) observed in this investigation with those obtained by other researches also using NDBEPR laboratory scale activated sludge systems. In Table 3.9, the denitrification rate *without* adjustment is directly comparable to the rates obtained in earlier investigations because the calculation method is the same. It can be seen that the denitrification rates ( $K_2'$ ) obtained in this study are above those obtained by Sneyders *et al.* (1998) and below those obtained by Clayton *et al.* (1989), Musvoto *et al.* (1992), Pilson *et al.* (1995) and Mellin *et al.*, (1995). This is the consequence of the high active fraction of the OHOs ( $f_{av,OHO}$ ) which is used to calculate the denitrification rate, which in turn is a consequence of the very low  $f_{S,up}$  value.

In comparing the  $K_2'$  rates obtained in the different investigations, Mellin *et al.*, (1995) showed that the rates were directly proportional to the unbiodegradable particulate COD fraction ( $f_{S,up}$ ) and inversely related to the active OHO fraction of the VSS ( $f_{av,OHO}$ ). The higher the calculated  $f_{S,up}$ , the lower the  $f_{av,OHO}$  and the higher the  $K_2'$ . The  $K_2'$  rates of this investigation also fit this pattern (Table 3.9) in that the  $f_{S,up}$  is low, and hence the  $f_{av,OHO}$  is high and the  $K_2'$  rate is low. Comparing the unadjusted ( $K_2'$ ) and adjusted ( $K_2''$ ) rates, which gives an indication of the contribution of the PAOs to the denitrification rate, it can be seen that  $K_2''$  is not much lower than  $K_2'$  which indicates that the contribution of PAOs to the denitrification is not very large because the proportion of biodegradable organics utilized by them in the anoxic reactor is small compared with that utilized by the OHOs.

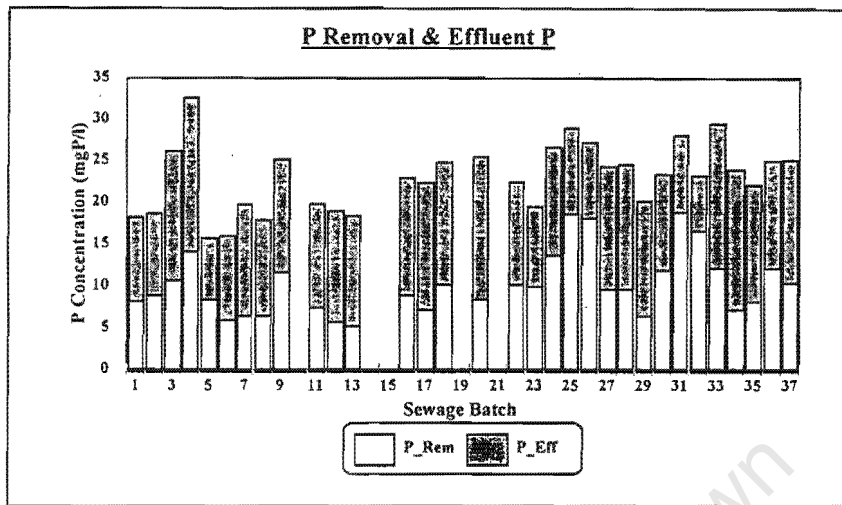
### 3.5 BIOLOGICAL EXCESS PHOSPHORUS REMOVAL (BEPR) PERFORMANCE

#### 3.5.1 P Removal and Effluent P Concentrations

Another objective of this investigation was to assess the biological excess phosphorus removal (BEPR) performance of the external nitrification BNRAS system. The last column in Table 3.10 lists, for each sewage batch, the P removal of the system and is shown plotted together with the effluent P concentration in Figure 3.11, where the total height of the stacked bar represents the influent P concentration. In comparing the P removal for the two modes of P uptake i.e. aerobic or anoxic, the average P removal was 9.33, 13.28 and 11.94 mgP/l for the first, third and fourth configurations respectively, in which anoxic P uptake was dominant. The configuration 2 in which aerobic P uptake was dominant showed a lower average P removal of 8.28 mgP/l. However, it should be noted that the lower aerobic P removal period was the same period in which the external nitrification and internal denitrification were poor (see Section 3.4.3, Figure 3.10) leading to high nitrate recycle to the anaerobic reactor. From earlier investigations on BEPR in conventional BNRAS systems (see Ekama and Wentzel, 1997 for details), it was noted that when the main anoxic reactor was underloaded with nitrate, then P uptake tended to be confined/dominant in the aerobic reactor, whereas if the nitrate load exceeded the denitrification potential so that nitrate was present in the anoxic reactor outflow, significant anoxic P uptake was observed. Accordingly, nitrate was dosed directly into the main anoxic reactor from sewage batch 1 to 26 and remained between 0.5 to 1.25 mgNO<sub>3</sub>-N/ml taking due cognizance to avoid nitrate overload of this reactor and hence a high nitrate recycle to the anaerobic reactor reducing the P release and hence the P removal in the BNRAS system.

The overall average P removal of the system was 10.4 mgP/l influent for the average influent COD concentration of 691 mgCOD/l. Although not very high, this value compares closely to other investigations with nutrient removal systems, namely Musvoto *et al.* (1992) 12.2 and 11.3 mgP/l for 1000 mgCOD/l influent (with significant anoxic P uptake), Pilson *et al.* (1995) 12.0 and 10.7 mg P/l for 1000 mg COD/l (with significant anoxic P uptake), Mellin *et al.* (1998) 11.4 mgP/l and 727 mdCOD/l (with significant anoxic P uptake), Sneyders *et al.* (1997) 13.1 and 16.8 mgP/l for 660 and 807 mgCOD/l (with no anoxic P uptake) all in conventional UCT type systems and ( and Hu *et al.* (1999) 8.8 mgP/l for 717 mgCOD/l in an external nitrification BNR system (with significant anoxic P uptake).

Figure 3.11: Average Effluent P concentration and system P removal for the 32 sewage



batches.

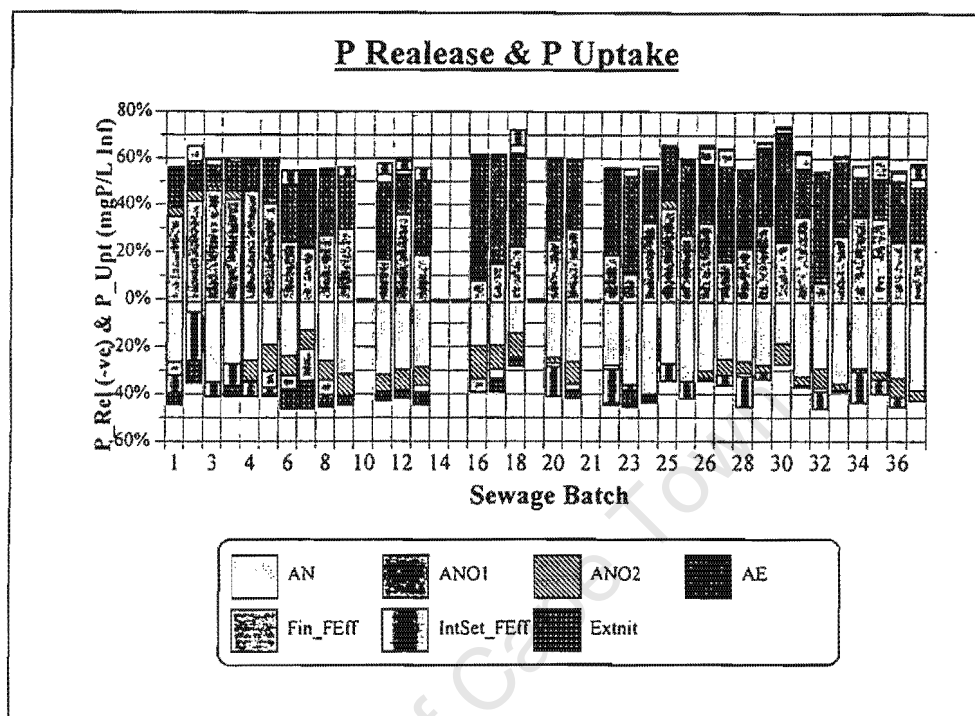
### 6.5.2 P Balance over each Reactor and Settler

From the averages of the influent, effluent and reactor concentrations for the 32 sewage batches the net P release or P uptake was calculated by conducting a TP balance (mass P in - mass P out) over each reactor and settler in the BNRAS system. A net positive TP balance indicates P uptake and a negative TP balance indicates P release. The net effect, i.e. uptake or release, for each of the reactors, the internal and final settlers and the external nitrification system for the 32 sewage batches are listed in Table 3.10 and are shown plotted in Figure 3.12. The total height of the stacked bar, either positive or negative shows the net P uptake or P release respectively of the BNRAS external nitrification system. From Figure 3.12 it can be seen that the most P release was obtained in the anaerobic (AN) reactor with an average value of 74% of the total P release of the system. This is followed by an average P release of 12% in the pre-anoxic reactor, 8% and 6% in the internal settler and external nitrification system respectively. The 8% average P release in the internal settler is probably due to leakage of some RBCOD out of the anaerobic reactor and stimulating P release in the sludge bed that forms at the bottom of the internal settling tank.

**Table 3.10:** Average P release or uptake for each reactor and settler as well as net P removal for the 32 sewage batches.

Average of Batch	AN mg P/l	Main ANO mg P/l	Pre_ANO mg P/l	AE mg P/l	Fin_FitEff mg P/l	IntSet_FilEff mg P/l	Extnit mg P/l	P_Rem mg P/l
1	-14.57	19.78	1.97	9.02	-3.01	-4.16	-2.43	8.21
2	-1.37	10.65	1.09	3.05	1.57	-5.13	-2.25	9.11
3	-18.68	24.97	0.95	4.65	1.55	-2.76	0.00	10.68
<b>Config 1</b>	<b>-11.54</b>	<b>18.47</b>	<b>1.33</b>	<b>5.57</b>	<b>0.04</b>	<b>-4.02</b>	<b>-1.56</b>	<b>9.33</b>
4	-19.57	35.56	-6.66	8.71	-0.45	-3.60	1.63	14.32
5	-8.18	17.72	-4.86	8.01	-2.97	-1.16	-0.11	8.52
6	-9.60	9.88	-3.27	9.82	-2.45	2.32	-2.91	6.11
7	-4.74	7.99	-2.93	12.01	-4.91	-0.13	-3.77	6.54
8	-12.81	13.77	-4.00	13.69	-3.16	-0.71	-1.35	6.50
9	-25.03	24.42	-7.40	17.91	0.00	2.41	-2.44	11.82
11	-13.00	7.32	-3.07	13.17	1.72	1.64	-1.29	7.52
12	-8.37	10.35	-2.45	4.91	0.62	0.83	-0.86	5.72
13	-9.73	6.70	-2.67	10.76	-1.03	1.72	-1.65	5.42
16	-7.40	3.36	-5.34	19.89	-1.81	0.26	0.00	8.95
17	-5.41	4.46	-2.79	12.71	-1.14	-0.31	-1.12	7.30
18	-3.10	4.97	-2.24	8.78	0.86	1.21	-0.72	10.33
20	-12.15	12.89	-1.15	14.08	-0.77	-5.74	2.81	8.52
<b>Config 2</b>	<b>-10.70</b>	<b>12.26</b>	<b>-3.76</b>	<b>11.88</b>	<b>-1.19</b>	<b>-0.10</b>	<b>-0.91</b>	<b>8.28</b>
22	-21.01	15.04	0.09	27.38	-1.29	-10.91	-0.20	10.33
23	-23.14	7.04	0.06	27.11	1.50	-1.48	-3.89	10.12
24	-35.48	29.49	0.68	19.38	0.98	-0.60	-2.29	13.87
25	-18.39	26.73	2.38	10.89	0.18	-4.76	4.58	18.81
<b>Config 3</b>	<b>-24.50</b>	<b>19.57</b>	<b>0.80</b>	<b>21.19</b>	<b>0.34</b>	<b>-4.44</b>	<b>0.45</b>	<b>13.28</b>
26	-17.02	18.75	-1.80	14.26	4.34	-0.42	3.22	18.25
27	-9.25	6.10	-2.54	15.29	2.48	-1.40	-0.21	9.88
28	-13.28	11.49	-2.44	16.60	-0.77	-6.24	1.79	9.85
29	-8.56	9.87	-0.94	10.35	0.58	-0.67	-2.02	6.64
30	-7.13	9.69	-3.02	18.07	0.75	0.08	-0.99	12.03
31	-25.07	27.49	-2.63	15.78	5.26	-0.53	-2.24	18.93
32	-36.06	9.66	-10.42	58.10	-1.66	-8.30	-5.51	16.78
33	-36.27	28.29	-2.80	32.28	1.99	-0.55	-6.56	12.23
34	-9.498	11.64	-0.49	5.53	1.48	-4.06	-0.39	7.38
35	-17.80	20.39	-1.84	9.68	5.53	-3.04	-4.62	8.30
36	-29.23	21.93	-7.24	23.29	3.46	-3.32	-3.93	12.36
37	-34.96	23.05	-3.45	20.68	3.95	4.98	-5.79	10.59
<b>Config 4</b>	<b>-20.34</b>	<b>16.53</b>	<b>-3.30</b>	<b>19.99</b>	<b>2.28</b>	<b>-1.96</b>	<b>-2.27</b>	<b>11.94</b>
<b>Overall</b>	<b>-16.12</b>	<b>15.36</b>	<b>-2.54</b>	<b>15.49</b>	<b>0.42</b>	<b>-1.70</b>	<b>-1.42</b>	<b>10.37</b>

**Figure 3.12:** Components of average P release (-ve) or P uptake (+ve) for the 32 sewage batches

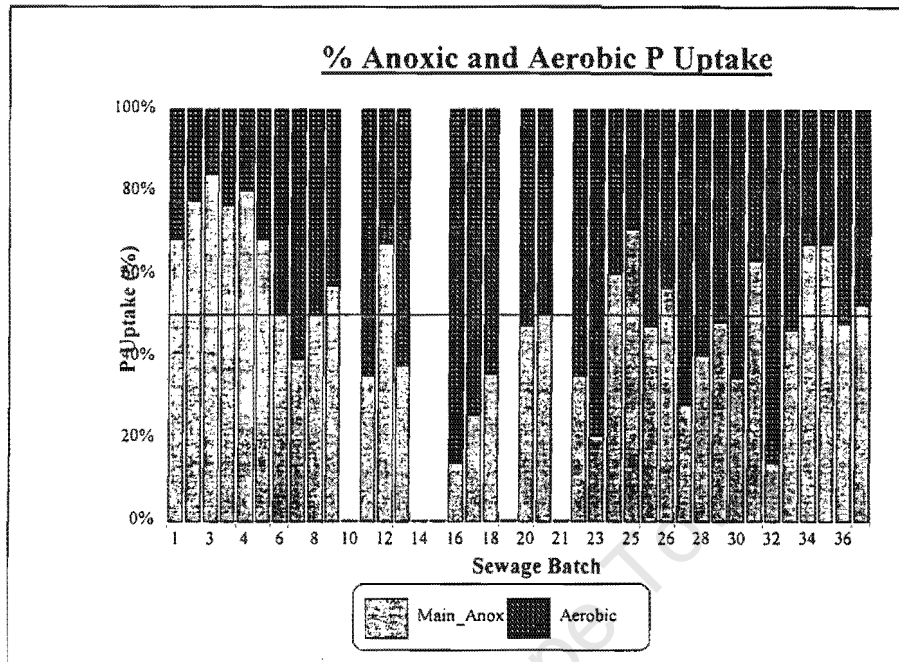


This P release in the internal settling tank is not undesirable but is actually beneficial to the BNRAS system in that it increases the P release of the system without increasing the anaerobic fraction of the system<sup>7</sup>. However, it should be noted that there were instances where P uptake was observed in both the internal settler and the external nitrification system, but not necessarily occurring simultaneously.

Figure 3.13. shows the anoxic/aerobic percentage P uptake relative for the 32 sewage batches. Although the anoxic P uptake reached around 60 % towards the end of the investigation (batches 25-37, Figure 3.13), the P removal had not yet stabilized and fluctuated between 6.7 to 18.9 mgP/l. From Figure 3.13 it can be noted that anoxic P uptake was 50% or greater in 18 of the 32 sewage batches i.e. during the investigation for 56% of the time P uptake in the anoxic reactor dominated. With regard to P uptake (Figure 3.13), initially (i.e. batches 1 to 5) this was achieved in the main anoxic reactor with an average P uptake of 22 mgP/l over this period.

<sup>7</sup>Indeed in the DEPHANOX II (Bortone *et al.*, 1997) system the first reactor is a combined anaerobic reactor -settling tank to (i) increase the anaerobic mass fraction per unit volume and (ii) reduce the cost of the internal settling tank in the system.

**Figure 3.13:** Average Anoxic/Aerobic P Uptake for the 32 sewage batches



In sewage batch 6, the P uptake was equal in the main anoxic and aerobic reactors with a value of 9.8 mgP/l. From batches 7 to 23, P uptake was predominantly achieved in the aerobic reactor with an average of 15.2 mgP/l. In batches 23 to 37, P uptake the main anoxic reactor was once again dominant in with an average value of 24 mgP/l. This variation in the P uptake process is dependent on the changes made to the system at batches 4, 22 and 26, i.e. at the time when the systems configuration was changed from Configuration 1 to Configuration 2, Configuration 2 to Configuration 3 and finally from Configuration 3 to Configuration 4. The most significant changes made to the systems were (i) doubling the influent flow, reducing the anoxic reactor volume by 1 l and reducing the sludge age from 10 days to 8 days in Configuration 2 (i.e sewage batches 4 to 20) and (ii) reducing the influent flow by 10 l/d, reducing the anoxic reactor by a further 2 l and concomitantly increasing the aerobic reactor by 2 l and increasing the sludge age from 8 days to 10 days in Configuration 3 ( i.e. sewage batches 22 to 25) and (iii) replacing the stone column with an activated sludge external nitrification system in Configuration 4 (sewage batches 26 to 37). From the changes made, the one which seemed to most influence the reactor in which P uptake took place was the nitrate load on the anoxic reactor. From sewage batches 1 to 5 and 24 to 37, anoxic P uptake was dominant whereas for sewage batches 6 to 23, aerobic

P uptake was dominant. During sewage batches 6 to 23 the nitrate load on the anoxic reactor tended to be low due to poor nitrification in the stone column external nitrification (see Section 3.4.3 above). However, other factors such as the anoxic and aerobic mass fractions may also have influenced the percentage anoxic uptake but it is suspected that these are small compared with the anoxic reactor nitrate load. It would therefore appear that to maximize anoxic P uptake, it is necessary to have a nitrate load on the anoxic reactor that exceeds this reactor's denitrification potential. This requires the system to have (i) excellent nitrification performance in the external nitrification system and (ii) a high influent TKN/COD ratio.

Up to sewage batch 22 the focus of the investigation was to maximize anoxic P uptake in the large anoxic mass fraction and minimize aerobic uptake in the small aerobic mass fraction BNRAS system. Knowledge of the kinetics and ideal environmental conditions for maximum anoxic P uptake is still limited. Bortone *et al.* (1997) noted that only when an aerobic zone was included in an anaerobic/anoxic sequencing batch reactor (SBR), did the system stimulate anoxic P uptake BEPR. Thus, it would appear that in order to achieve stable anoxic P uptake, an aerobic period may be essential. However, the ratio of aerobic/anoxic mass fractions was not known for optimum anoxic P uptake. In an attempt to qualify the effect of the aerobic mass fraction on anoxic P uptake, the aerobic mass fraction of Configuration 2 was increased to form Configuration 3 (see Table 3.1). Thus the focus from sewage batch 22 shifted from trying to maximize anoxic P uptake because of its (i) instability as a biological process and (ii) lower BEPR than aerobic P uptake (according to Ekama and Wentzel, 1999 and this investigation), to exploiting aerobic P uptake BEPR in the external nitrification system and studying the effects of the increased aerobic mass fraction on the BEPR of the system. However, it was realized that the conditions that promote aerobic P uptake BEPR, and hence more stable and greater BEPR in the system, would also encourage internal nitrification, which, if the external nitrification system did not achieve efficient nitrification (> 80%), would lead to high nitrate recycle to the anaerobic reactor and consequently reduced BEPR. Thus Configuration 2 was changed to form Configuration 3 by making the main anoxic and aerobic reactors with equal volumes and thus equal mass fractions. Interestingly, anoxic P uptake still dominated the total P uptake process. As a result of the poor nitrification efficiency in the external nitrification system (see Section 3.4.4) the nitrate recycled to the anaerobic reactor in Configuration 3 due to internal nitrification

(in the main aerobic reactor) decreased the BEPR to 8.8 mgP/l. From sewage batch 26, the fixed media stone column was abandoned and replaced with a suspended medium external nitrification system for Configuration 4. This change to the external nitrification system showed an improvement in external nitrification and a decline in internal nitrification and hence the nitrate recycled to the anaerobic reactor decreased, improving the BEPR of Configuration 4 to 12.4 mg/l with 60% and 34% P uptake in the main anoxic and aerobic reactors respectively.

### 3.5.3 Comparison of Measured and Calculated P removal

The BEPR performance in the BNRAS system was assessed by comparing the observed P removal with that theoretically calculated by the steady state BEPR model of Wentzel *et al.* (1990) which forms a sub-set of the UCTPHO (Wentzel *et al.*, 1992) and IAWQ ASM N<sup>2</sup>2 (Henze *et al.*, 1995). In order to calculate the predicted BEPR from the steady state BEPR model, the VSS constituent fractions need to be determined, including the two active heterotrophic organism fractions of the VSS to be determined (i.e. PAOs,  $f_{av,PAO}$  and OHOs,  $f_{av,OHO}$ ). To determine the PAO and OHO fractions, the proportion of the readily biodegradable (RB) COD that the PAOs obtain in the anaerobic reactor ( $S_{seq}$ ) needs to be determined. To do this, the volatile fatty acids (VFA) concentration in the influent needs to be known and also the proportion of the influent RBCOD converted to VFA in the anaerobic reactor by the ordinary heterotrophic organisms (OHOs). The PAOs obtain that part of the influent biodegradable COD which is VFA and the part of the RBCOD converted to VFA in the anaerobic reactor, while the OHOs obtain the balance of the biodegradable COD i.e. that part of the RBCOD not converted to VFA in the anaerobic reactor and all of the SBCOD, except for the approximately 13% of the COD that is utilized in the external nitrification system for sludge production (measured average COD reduction in external nitrification System). The difficulty in determining the substrate that the PAO and OHO active fractions obtain is further compounded by the fact that the unbiodegradable particulate COD fraction of the influent ( $f_{s,up}$ ) which also becomes part of the VSS in the system is unknown and determines the proportion of the total influent COD which is biodegradable. As a result, the determination of  $f_{s,up}$  and the PAO and OHO active fractions is done simultaneously using the measured MLVSS concentrations as benchmarks (for additional details see Mellin *et al.*, 1998, Pilson *et al.*, 1995 or Ekama and Wentzel, 1999).

### 3.5.3.1 Determination of $f_{S,up}$

The approach that is used to calculate  $f_{S,up}$ ,  $f_{av,OHO}$  and  $f_{av,PAO}$  follows the BEPR steady state model of Wentzel *et al.* (1990) shown schematically in Figure 3.14. The model is structured such that the heterotrophic organism mass is divided into two groups; the OHOs and the PAOs, the difference being their stoichiometric and kinetic constants, the main ones being the P content and endogenous respiration rate. With the influent unbiodegradable soluble COD fraction  $f_{S,us}$  known from the filtered effluent COD concentration ( $f_{S,us} = \text{filtered effluent COD}/\text{total influent COD}$ ), it involves an iterative process where an estimate of the unbiodegradable particulate fraction ( $f_{S,up}$ ) is made, from which the influent biodegradable COD is calculated by difference. The split of the biodegradable COD between the PAOs and OHOs is calculated iteratively from the measured influent RBCOD concentration and the known system design parameters that govern RBCOD conversion, i.e. anaerobic mass fraction and sludge age as demonstrated by Wentzel *et al.* (1990). With the proportions of the biodegradable COD obtained by the PAOs and OHOs known, the mass of the active and endogenous VSS generated by these two organism groups are calculated. Also, from the initial estimate of  $f_{S,up}$ , the inert VSS is calculated. By adding the 5 calculated constituent components of the VSS mass (shown in Figure 3.14), the total VSS mass of the system is known. The correct estimate of the  $f_{S,up}$  is that value which gives the calculated VSS mass equal to the measured VSS mass taking due account of the COD reduction in the external nitrification system. The OHO and PAO active VSS fractions  $f_{av,OHO}$  and  $f_{av,PAO}$  respectively are then determined from the ratio of the masses of OHO and PAO VSS to the total VSS. This calculation procedure assumes a 100% COD balance. An error in the COD balance may be the result of too low VSS mass in the system due to (i) steady state conditions not existing or (ii) sludge losses from spillages. The latter happened several times in this investigation, but its effect was reduced because as much as possible of the spilled sludge was returned to the system from the specially designed sludge spillage drip tray below the system. Low VSS mass in the system leads to low  $f_{S,up}$  fractions and high  $f_{av,OHO}$  and  $f_{av,PAO}$  fractions. This is the main reason for the large variation in  $f_{S,up}$  fractions and denitrification rates  $K_2'$  in NDBEPR systems (see Table 3.9 and Ekama and Wentzel, 1999).

Once the sludge VSS has been fractionated by reconciling the calculated and measured VSS masses, the P content of the PAOs ( $f_{XBG,P}$ ) is estimated so that the calculated sum of the P contents of the 5 constituent fractions of the VSS yield the measured P removal. The correct value of  $f_{XBG,P}$  is that value for which the calculated P removal is the same as the measured P

removal. The results of the spreadsheet calculations for the 32 analyzed sewage batches fed to the external nitrification system are shown in Appendix C. In the steady state model of Wentzel *et al.* (1990), which is based on aerobic P uptake, the fraction of the PAO P content ( $f_{XBG,P}$ ) is 0.38 mgP/mgPAOVASS. The calculated  $f_{XBG,P}$  fraction for each sewage batch is listed in Table 3.11a and shown plotted in Figure 3.15a. The same procedure was applied to the conventional UCT system results, details of which are given in Appendix E (see Table 3.11b).

**Figure 3.14:** Diagrammatic representation of utilisation of the Total influent COD in the model of Wentzel *et al.* (1990).

Total COD - known					
Total biodegradable COD - Unknown?			Total unbiodegradable COD - Unknown?		
Measured from influent - known		Unknown?		Unknown?	Measured from effluent - known
RBCOD		SBCOD		UPCOD ( $f_{S,ub}$ ) <sup>1</sup>	USCOD ( $f_{S,us}$ )
Unknown?		Unknown?		Unknown?	Determined from filtered effluent COD concentration
COD obtained by PAOs		COD obtained by OHOs			<sup>1</sup> Varied until calculated VSS = measured VSS masses.  <sup>2</sup> Varied until calculated BEPR = measured BEPR.
Active polyP VSS mass	Endogenous polyP VSS mass	Active ordinary heterotroph VSS mass	Endogenous ordinary heterotroph mass	Inert VSS mass	
1	2	3	4	5	
Components contributing to Total Total VSS mass (must equal measured value)					
$f_{XBG,P}$ <sup>2</sup>	0.03	0.03	0.03	0.03	
P content of VSS constituents					
$\Delta P_{GB}$	$\Delta P_{GE}$	$\Delta P_{HB}$	$\Delta P_{HE}$	$\Delta P_I$	
Total P removal (must equal measured value)					

Table 3.11a: Calculated  $f_{S,up}$  and  $f_{XBG,P}$  fractions using Wentzel *et al.* (1990) BEPR model.

Sewage Batch	$S_{bsi}$ <sup>2</sup>	$f_{S,us}$	$f_{XBG,P}$	$f_{S,up}$	MXv(calc) mgVSS/d	$\Delta P$ (calc) mgP/l inf	MXv(meas) mgVSS/d	$\Delta P$ (meas) mgP/l inf	$f_{av,OHO}$	$f_{av,PAO}$
1 <sup>1</sup>	92	0.07	0.233	-2.134	26769.3	8.209	21536.7	8.212	0.56	0.15
2	103	0.07	0.283	0.142	28403.4	9.114	28415.0	9.112	0.33	0.13
3 <sup>1</sup>	92	0.03	0.385	0.079	28240.4	10.643	28280.0	10.676	0.43	0.13
<b>Config 1</b>	<b>96</b>	<b>0.06</b>	<b>0.300</b>	<b>0.111</b>	<b>27813.4</b>	<b>9.34</b>	<b>26077.2</b>	<b>9.33</b>	<b>0.44</b>	<b>0.14</b>
4	89	0.09	0.491	0.021	39633.5	14.301	39622.0	14.315	0.53	0.19
5	41	0.05	0.451	-2.135	41381.8	8.512	37192.2	8.524	0.66	0.08
6	37	0.11	0.173	0.183	50964.7	6.122	51021.7	6.113	0.38	0.06
7	57	0.05	0.119	0.181	56391.9	6.531	56310.8	6.544	0.37	0.08
8	102	0.09	0.107	0.063	47977.8	6.500	47970.0	6.501	0.46	0.18
9	143	0.03	0.201	0.147	60555.9	11.770	60524.4	11.824	0.33	0.19
11	110	0.05	0.154	-2.135	42199.9	7.525	41580.0	7.519	0.55	0.22
12 <sup>1</sup>	92	0.07	0.118	0.019	39093.3	5.712	39162.9	5.717	0.53	0.19
13	109	0.08	0.058	0.076	49697.9	5.414	49665.0	5.424	0.43	0.18
16	73	0.06	0.248	0.104	51522.9	8.928	51571.7	8.954	0.44	0.12
17 <sup>1</sup>	92	0.09	0.146	0.122	49202.2	7.271	49243.3	7.301	0.39	0.15
18	78	0.10	0.384	0.020	46934.4	10.332	46896.7	10.332	0.51	0.16
20	102	0.09	0.184	0.128	47302.0	8.504	47235.8	8.524	0.34	0.16
<b>Config 2</b>	<b>85</b>	<b>0.07</b>	<b>0.221</b>	<b>0.094</b>	<b>47963.0</b>	<b>8.25</b>	<b>47563.4</b>	<b>8.26</b>	<b>0.44</b>	<b>0.15</b>
22	63	0.05	0.408	0.354	56868.7	10.341	56888.3	10.332	0.19	0.06
23	86	0.06	0.288	0.118	47899.5	10.096	47825.6	10.122	0.39	0.13
24	124	0.07	0.326	-2.134	43248.7	13.884	39520.6	13.869	0.51	0.22
25	71	0.08	0.925 <sup>3</sup>	0.090	34992.8	18.829	34989.2	18.810	0.40	0.14
<b>Config 3</b>	<b>86</b>	<b>0.07</b>	<b>0.341</b>	<b>0.187</b>	<b>45752.4</b>	<b>13.28</b>	<b>44805.9</b>	<b>13.28</b>	<b>0.37</b>	<b>0.14</b>
26	82	0.08	0.772	-2.134	39420.2	18.237	26970.2	18.249	0.57	0.15
27	70	0.07	0.348	-2.134	41839.4	9.854	30554.3	9.876	0.58	0.13
28	58	0.07	0.494	-2.134	33786.1	9.868	26766.7	9.852	0.58	0.12
29	100	0.05	0.150	-2.134	36465.0	6.614	27683.3	6.638	0.52	0.21
30	84	0.06	0.412	-2.134	38025.4	12.014	25868.3	12.034	0.55	0.17
31	123	0.03	0.448	-2.134	50289.1	18.944	38921.7	18.935	0.53	0.20
32	131	0.04	0.414	0.062	43801.6	16.789	43798.3	16.783	0.39	0.22
33	104	0.08	0.330	-2.134	41396.2	12.267	21330.0	12.234	0.53	0.20
34	115	0.07	0.118	-2.134	48175.8	7.380	29638.9	7.377	0.54	0.18
35	101	0.05	0.198	-2.134	39298.7	8.306	38949.2	8.299	0.53	0.20
36	102	0.10	0.332	0.094	46642.3	12.354	46655.0	12.357	0.39	0.16
37	124	0.10	0.248	0.044	39852.4	10.577	39904.0	10.592	0.42	0.23
<b>Config 4</b>	<b>98</b>	<b>0.07</b>	<b>0.348</b>	<b>0.067</b>	<b>41675.5</b>	<b>12.39</b>	<b>34625.0</b>	<b>12.4</b>	<b>0.49</b>	<b>0.18</b>
<b>Overall</b>	<b>92</b>	<b>0.07</b>	<b>0.291</b>	<b>0.115</b>	<b>43384.4</b>	<b>10.37</b>	<b>39904.0</b>	<b>10.37</b>	<b>0.46</b>	<b>0.16</b>

<sup>1</sup> The influent RBCOD concentration used for these sewage batches were not measured, the average of 92 mgCOD/l was used for the  $f_{XBG,P}$  calculation.

<sup>2</sup> Determined from the difference of the floc filtered influent and effluent COD concentrations.

<sup>3</sup> Not included in average.

Figure 3.15a: Polyphosphate accumulating organism (PAO) P content ( $f_{XBG,P}$  mgP/mgPAOAVSS).

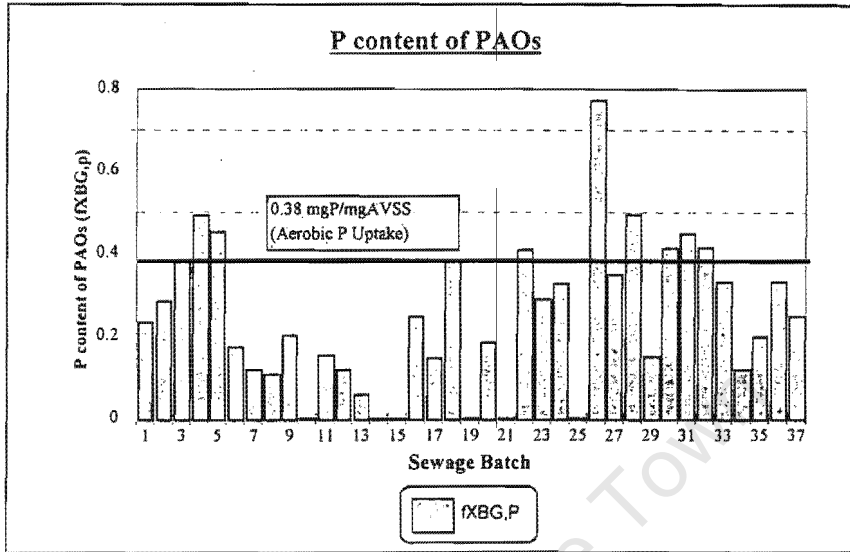
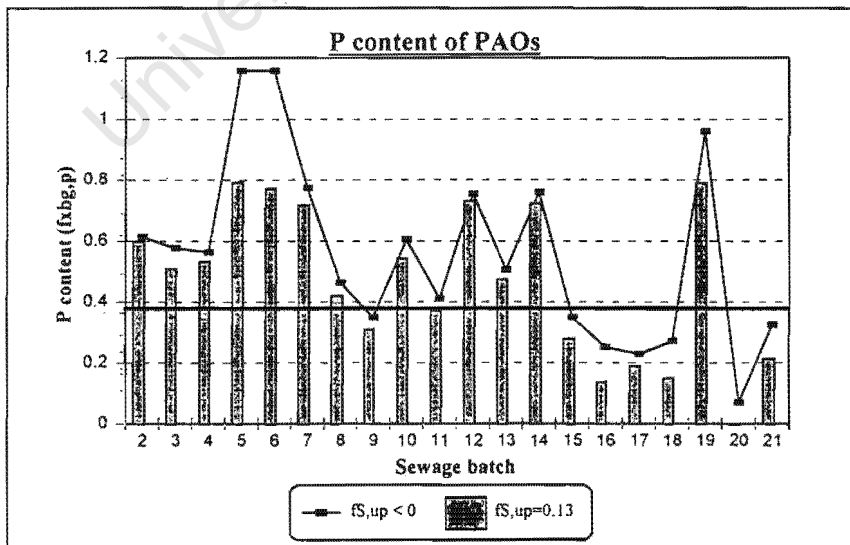


Figure 3.15b: Polyphosphate accumulating organism (PAO) P content ( $f_{XBG,P}$  mgP/mgPAOAVSS) in UCT system for sewage batches 2 to 21.



**Table 3.11b:** Calculated  $f_{X_{BG,P}}$  fractions for fixed  $f_{S,up}$  of 13% in Wentzel *et al.* (1990) BEPR model.

Sewage Batch	$S_{bsi}$ <sup>2</sup>	$f_{S,us}$	$f_{X_{BG,P}}$	$f_{S,up}$	MXv(calc)	$\Delta P$ (calc)	$\Delta P$ (meas)	$f_{av,OHO}$	$f_{av,PAO}$
					mgVSS/d	mgP/l inf	mgP/l inf		
1 <sup>1</sup>	92	0.07	0.175	0.13	35371.44	8.20	8.212	0.36	0.11
2	103	0.07	0.287	0.13	27805.01	9.11	9.112	0.35	0.14
3 <sup>1</sup>	92	0.03	0.369	0.13	30996.79	10.67	10.676	0.37	0.11
<b>Config 1</b>	<b>96</b>	<b>0.06</b>	<b>0.277</b>	<b>0.13</b>	<b>26077.22</b>	<b>9.32</b>	<b>9.33</b>	<b>0.36</b>	<b>0.12</b>
4	89	0.09	0.475	0.13	47666.45	14.30	14.315	0.37	0.15
5	41	0.05	0.361	0.13	53169.81	8.52	8.524	0.44	0.06
6	37	0.11	0.243	0.13	44200.26	6.11	6.113	0.42	0.07
7	57	0.05	0.151	0.13	52134.03	6.55	6.544	0.42	0.09
8	102	0.09	0.091	0.13	52435.89	6.48	6.501	0.37	0.16
9	143	0.03	0.203	0.13	58721.34	11.80	11.824	0.37	0.20
11	110	0.05	0.121	0.13	53300.00	7.51	7.519	0.37	0.17
12 <sup>1</sup>	92	0.07	0.085	0.13	47605.18	5.70	5.717	0.38	0.15
13	109	0.08	0.041	0.13	54432.83	5.41	5.424	0.37	0.16
16	73	0.06	0.235	0.13	54525.14	8.96	8.954	0.41	0.11
17 <sup>1</sup>	92	0.09	0.151	0.13	48565.87	7.28	7.301	0.37	0.15
18	78	0.10	0.351	0.13	58389.34	10.34	10.332	0.35	0.13
20	102	0.09	0.189	0.13	46099.64	8.50	8.524	0.33	0.16
<b>Config 2</b>	<b>85</b>	<b>0.07</b>	<b>0.209</b>	<b>0.13</b>	<b>52020.51</b>	<b>8.25</b>	<b>8.26</b>	<b>0.38</b>	<b>0.13</b>
22	63	0.05	0.495	0.13	40500.54	10.34	10.332	0.37	0.10
23	86	0.06	0.285	0.13	48607.33	10.413	10.122	0.35	0.13
24	124	0.07	0.299	0.13	54991.83	13.84	13.869	0.33	0.17
25	71	0.08	0.955	0.13	37182.82	18.81	18.810	0.35	0.13
<b>Config 3</b>	<b>86</b>	<b>0.07</b>	<b>0.359</b>	<b>0.13</b>	<b>45320.63</b>	<b>13.28</b>	<b>13.28</b>	<b>0.35</b>	<b>0.13</b>
26	82	0.08	0.748	0.13	49850.12	18.25	18.249	0.36	0.11
27	70	0.07	0.286	0.13	54453.91	9.87	9.876	0.37	0.10
28	58	0.07	0.431	0.13	44558.11	9.85	9.852	0.38	0.09
29	100	0.05	0.111	0.13	47168.56	6.66	6.638	0.34	0.15
30	84	0.06	0.371	0.13	49383.06	12.04	12.034	0.36	0.13
31	123	0.03	0.413	0.13	65084.42	18.91	18.935	0.35	0.15
32	131	0.04	0.405	0.13	49396.97	16.78	16.783	0.32	0.19
33	104	0.08	0.297	0.13	52924.08	12.22	12.234	0.34	0.15
34	115	0.07	0.071	0.13	62179.61	7.38	7.377	0.35	0.14
35	101	0.05	0.155	0.13	51204.70	8.29	8.299	0.34	0.15
36	102	0.10	0.337	0.13	47694.24	12.36	12.357	0.33	0.16
37	124	0.10	0.231	0.13	46916.92	10.6	10.592	0.31	0.19
<b>Config 4</b>	<b>98</b>	<b>0.07</b>	<b>0.360</b>	<b>0.13</b>	<b>50773.11</b>	<b>12.40</b>	<b>12.4</b>	<b>0.35</b>	<b>0.14</b>
<b>Overall</b>	<b>92</b>	<b>0.07</b>	<b>0.294</b>	<b>0.13</b>	<b>48956.76</b>	<b>10.37</b>	<b>10.37</b>	<b>0.36</b>	<b>0.14</b>

<sup>1</sup> The influent RBCOD concentration used for these sewage batches were not measured, the average of 92 mgCOD/l was used for the  $f_{X_{BG,P}}$  calculation.

<sup>2</sup> Determined from the difference of the floc filtered influent and effluent COD concentrations.

**Table 3.11c:** Calculated  $f_{S,up}$  and  $f_{XBG,P}$  fractions for sewage batches 2 to 21 of the UCT system using Wentzel *et al.* (1990) model.

Sewage Batch	$S_{bsi}^2$	$f_{S,us}$	$f_{XBG,P}^3$	$f_{S,up}$	MXv(calc)	$\Delta P$ (calc)	MXv(meas)	$\Delta P$ (meas)	$f_{av,OHO}$	$f_{av,PAO}$
					mgVSS/d	mgP/l inf	mgVSS/d	mgP/l inf		
2 <sup>1</sup>	103	0.08	0.612	0.068	33083.5	18.82	33070.7	18.85	0.43	0.14
3	92	0.04	0.563	0.0 <sup>4</sup>	32945.4	16.58	30212.4	16.58	0.58	0.13
4 <sup>1</sup>	89	0.05	0.563	0.030	27702.2	17.45	27735.5	17.45	0.56	0.13
5	40	0.05	1.297	0.053	28044.7	17.65	28003.3	17.67	0.57	0.06
6	37	0.05	7.075	0.031	27799.4	5.2	27744.0	17.19	0.65	
7	57	0.03	0.775	0.043	28636.0	14.9	28656.3	14.88	0.58	0.07
8	102	0.05	0.405	0.0 <sup>4</sup>	26452.6	16.37	25082.7	16.37	0.60	0.16
9	143	0.03	0.340	0.0 <sup>4</sup>	29532.9	17.00	26746.7	16.96	0.57	0.20
10	92	0.05	0.595	0.0 <sup>4</sup>	25911.3	15.72	24712.3	15.73	0.63	0.12
11	110	0.07	0.405	0.0 <sup>4</sup>	24525.6	14.55	24041.8	14.55	0.59	0.17
12 <sup>1</sup>	92	0.04	0.7555	0.044	26.862.9	19.49	26835.7	19.51	0.54	0.12
13	109	0.06	0.502	0.0 <sup>4</sup>	24774.0	17.62	23654.3	17.60	0.58	0.18
14	92	0.05	0.756	0.0 <sup>4</sup>	25023.3	20.58	23800.0	20.57	0.61	0.14
15	92	0.09	0.334	0.0 <sup>4</sup>	26381.7	11.53	24491.3	11.55	0.62	0.13
16	73	0.08	0.235	0.0 <sup>4</sup>	24545.3	7.33	23358.0	7.34	0.65	0.09
17 <sup>1</sup>	92	0.08	0.214	0.0 <sup>4</sup>	26550.6	12.55	21964.0	12.53	0.53	0.25
18	78	0.06	0.220	0.0 <sup>4</sup>	30474.7	8.22	23003.4	8.21	0.58	0.13
19	92	0.10	0.960	0.212	23727.9	17.69	23698.0	17.72	0.25	0.13
20	102	0.06	0.048	0.0 <sup>4</sup>	38004.7	4.96	26350.0	4.97	0.55	0.17
21	92	0.08	0.301	0.0 <sup>4</sup>	28616.8	9.71	18657.5	9.71	0.57	0.14
<b>Average</b>	<b>92</b>	<b>0.08</b>	<b>0.495</b>	<b>0.069</b>	<b>29403.3</b>	<b>15.01</b>	<b>26027.0</b>	<b>15.00</b>	<b>0.56</b>	<b>0.14</b>

<sup>1</sup> The influent RBCOD concentration used for these sewage batches were not measured, the average of 92 mgCOD/l was used for the  $f_{XBG,P}$  calculation.

<sup>2</sup> Determined from the difference of the flocculated influent and effluent COD concentrations.

<sup>3</sup> The  $f_{XBG,P}$  fraction of the UCT system was only determined while the system was monitored i.e. up to and including sewage batch 21.

<sup>4</sup> The  $f_{S,up}$  value to match the measured VSS mass is negative due to sludge spillages and low COD mass balances - see Appendix E. A minimum  $f_{S,up}$  value of 0.0 was accepted.

### 3.5.3.2 Dependency of $f_{\text{XBG,P}}$ fraction on influent RBCOD concentration and $f_{\text{S,up}}$

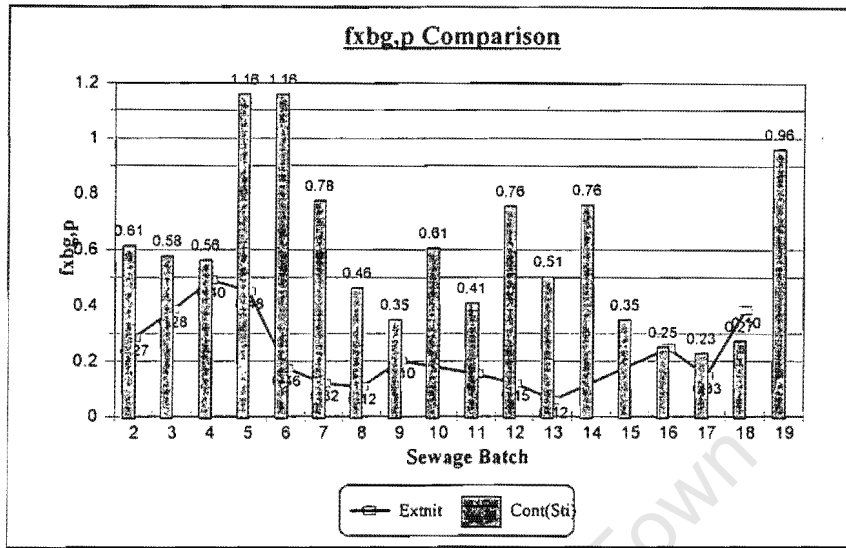
In Figure 3.15a and Table 3.11a it can be seen that the  $f_{\text{XBG,P}}$  fraction varies considerably between 0.057 and 0.991 mgP/mgPAOAVSS. The cause of the large variation in the  $f_{\text{XBG,P}}$  fraction is due to the large variation in the influent RBCOD of the wastewater since the determination of the  $f_{\text{XBG,P}}$  fraction is almost directly proportional to the influent RBCOD concentration (overall average of the influent RBCOD in this investigation was 92 with a standard deviation of 25 mgCOD/l). This is expected since the model of Wentzel *et al.* (1990) uses the influent RBCOD concentration to calculate the COD sequestered by the PAOs which in turn determines the PAO mass which is responsible for the largest proportion of the P removal ( $\sim 2/3^{\text{rds}}$ ). Fig 3.15b shows the  $f_{\text{XBG,P}}$  fraction determined with the same method for the period which the parallel UCT system was monitored (i.e. up to sewage batch 19) using the model of Wentzel *et al.* (1990).

Although from the steady state model, a direct relationship between RBCOD concentration and PAO mass and P removal is expected with a constant P content of PAOs ( $f_{\text{XBG,P}}$ ). This is because the effect (i.e either a high or low  $f_{\text{XBG,P}}$  fraction) of a change in influent RBCOD concentration does not manifest immediately but gradually as the PAO mass (and hence P removal) adjusts up or down in response to the influent RBCOD concentration change to establish a new steady state. This adjustment can take one or more sludge ages depending on the magnitude of the influent RBCOD concentration change. Because the BEPR model assumes steady state conditions a decrease (increase) in influent RBCOD concentration will result in an increase (decrease) in  $f_{\text{XBG,P}}$  because now a lower (higher) theoretical PAO mass has to account for a higher (lower) P removal from the higher (lower) influent RBCOD concentration from the previous sewage batch.

Despite the significant variation in  $f_{\text{XBG,P}}$  for reasons given above, from Figs 3.15a and 3.17, it can be seen that the overall  $f_{\text{XBG,P}}$  value for the UCT system (0.495) is greater than for the external nitrification system (0.291 mgP/mgPAOAVSS).

While generally the  $f_{\text{XBG,P}}$  value in the UCT system may be higher than in the external nitrification system because the COD balance ( and measured VSS mass) was lower than the external nitrification system, the magnitude of the difference in  $f_{\text{XBG,P}}$  cannot be accounted for by only the difference in COD balance.

**Figure 3.17:** Comparison of P content of PAOs of BNRAS external nitrification and UCT control system

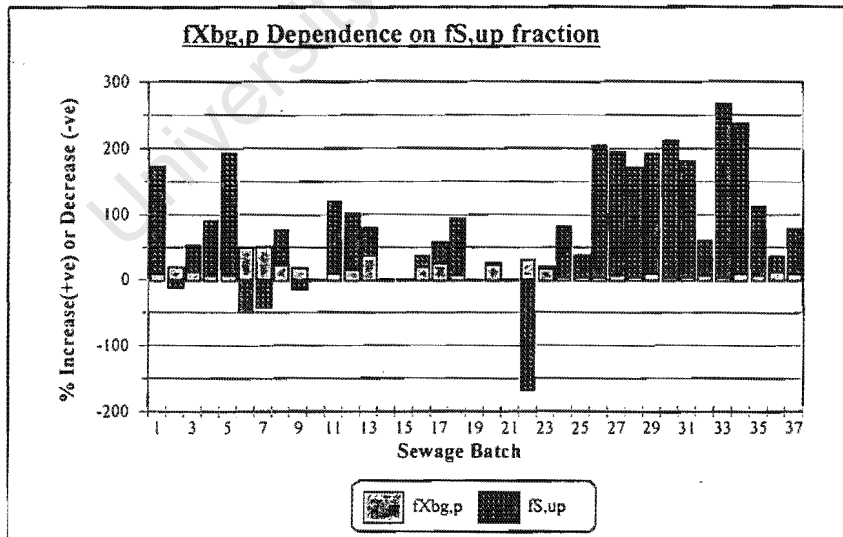


It can therefore be concluded that even at 100% COD balance in both systems, the  $f_{\text{XBG,P}}$  value is lower in the external nitrification system than the UCT system. This is in conformity with observations in earlier investigations (Ekama and Wentzel, 1999)- systems that exhibit significant anoxic P uptake ( $> 40\%$ ) show lower BEPR (at about  $2/3^{\text{rds}}$ ) than systems exhibiting aerobic P uptake BEPR. In this investigation the UCT system exhibited 100% aerobic P uptake BEPR (see mass balance for the UCT system in Appendix E), while in the external nitrification system, the P uptake took place in both the main anoxic (56%) and aerobic (42%) reactors respectively. The lower BEPR with anoxic P uptake can be explained biochemically. Aerobic metabolism provides a higher yield (3 ATPs per  $e^-$  pair transferred) for the PAOs and hence higher P removal than anoxic metabolism (2 ATPs per  $e^-$  pair transferred).

For the same wastewater source, one expects a relatively constant  $f_{\text{S,up}}$  fraction. For N removal systems fed the Mitchells Plein wastewater this is the case- Ubisi *et al.* (1997), Mbewe *et al.* (1995), Warburton *et al.* (1991) and Mellin *et al.* (1998) all found  $f_{\text{S,up}}$  values around 0.10 to 0.13. However, this is not the case for NDBEPR systems - Clayton *et al.* (1989), Musvoto *et al.* (1992), Kaschula *et al.* (1993), Pilson *et al.* (1995), Sneyders *et al.* (1997) and Mellin *et al.* (1998) found widely varying  $f_{\text{S,up}}$  values from 0.04 to 0.35 mgCOD/mgCOD for the Mitchells Plein wastewater as is evident in this investigation. These widely varying  $f_{\text{S,up}}$  values lead to widely varying OHO active fractions and  $K_2'$  denitrification rates (Ekama and Marais, 1999). In order to establish the

sensitivity of the  $f_{X_{BG,P}}$  fraction to the calculated  $f_{S,up}$  fraction, a constant  $f_{S,up}$  value of 0.13 was accepted for all 32 sewage batches analyzed, substituted for the  $f_{S,up}$  fraction in the Wentzel *et al.* (1990) model and the  $f_{X_{BG,P}}$  fraction was recalculated for the external nitrification system and UCT control system. This approach ignores the measured VSS as the benchmark for the  $f_{S,up}$  value (see Table 3.11b). The calculated  $f_{X_{BG,P}}$  for constant and calculated  $f_{S,up}$  are compared graphically for the external nitrification system in Fig3.18 showing the percentage change of both the  $f_{X_{BG,P}}$  and  $f_{S,up}$  fractions. From Figures 3.18 and 3.15b it can be seen that a large change in the  $f_{S,up}$  fraction from the initial value to 0.13 is not accompanied by a large change in the  $f_{X_{BG,P}}$  fraction, showing that the  $f_{X_{BG,P}}$  fraction is insensitive to the  $f_{S,up}$  fraction. The insensitivity of the  $f_{X_{BG,P}}$  fraction to the  $f_{S,up}$  fraction is not unexpected because the BEPR, P removal and  $f_{X_{BG,P}}$  are theoretically linked at steady state to the influent RBCOD concentration i.e. this concentration was not changed with varying  $f_{S,up}$ . The relative difference in  $f_{X_{BG,P}}$  between the UCT control and external nitrification system, both fed the same wastewater for 21 sewage batches, is therefore not a consequence of the  $f_{S,up}$  variation, but rather a consequence of system behaviour.

**Figure 3.18:**  $f_{X_{BG,P}}$  fraction dependence on  $f_{S,up}$  fraction for the external nitrification system.



### 3.6 FILAMENT IDENTIFICATION AND SLUDGE SETTLEABILITY

#### 3.6.1 Filament Identification

Approximately every four weeks samples of mixed liquor were taken from the aerobic reactors of the external nitrification and UCT control systems for microscopic analysis and filamentous organism identification (see Appendix F for details). This was done to compare the filaments occurring in the laboratory scale systems in this investigation and to ascertain whether or not the same type and relative abundance of filaments are similar to that found in full scale plants. During the investigation, the filament identifications were done 13 times (i.e. from day 1 to day 373, over 37 sewage batches) on both systems. However, as mentioned above the UCT system was tested and monitored for all the system compounds only for a part of this time i.e. days 4 to 167 spanning sewage batches 2 to 21 inclusive. For the 13 identifications on each system, the % frequency of dominance and occurrence were calculated as the number of times a particular filament was dominant (most abundant filament) and occurred (observed). The results are summarized in Table 3.12. Comparing the filaments identified in the external nitrification and UCT control systems (see Appendix F) with those identified by Blackbeard *et al.* (1988) in full scale nutrient removal plants in South Africa, it appears that the frequent occurrence of *M. parvicella*, type 0092 and type 1851 at both laboratory and full scale provides sufficient evidence that the filament types of the external nitrification and UCT systems are similar to full scale plants and are all of the low F/M (after Jenkins *et al.*, 1984) or Anoxic-Aerobic (AA after Casey *et al.*, 1994) types.

From Table 3.12, the most frequently dominant filament in both the external nitrification (EN) and UCT system was *M. parvicella* (69 and 85% respectively). From the survey of nutrient removal plants in South Africa by Blackbeard *et al.* (1988), *M. parvicella* occurred in 76% of plants and was dominant in 33%. The next most frequently dominant filaments in the EN system was type 1851 being the dominant filament in the system 25% of the sampling time; type 1851 was never observed (0%) to be the dominant filament in the UCT system.

Low F/M (AA) filaments that were observed to be present (occurrence) in the sludge most frequently

**Table 3.12:** The Dominance and Occurrence of filamentous organisms in the external nitrification and UCT systems

Filament Type	Dominance (%)		Occurrence (%)	
	Ext	UCT	Ext	UCT
<i>M. Parvicella</i>	69	85	81	92
Type 1851	25	0	44	31
Type 021N	6	8	25	8
Type 0092	0	0	13	15
Type 1701	0	8	6	15
<i>S. Natans</i>	6	0	6	0
<i>H. hydrosis</i>	0	8	6	23
<i>Thiothrix</i>	0	0	0	8
<i>Nocardia</i> sp	0	0	0	8

in the EN and UCT systems were *M. parvicella*, which occurred in 81% and 92% of samples, type 1851 in 44% and 30% and type 0092 in 13% and 15 % respectively. Thus the most important filaments in the EN and UCT systems were the low F/M (AA) types.

*H. hydrosis* occurred in 23% of the samples analyzed for the UCT system. Jenkins *et al.* (1984) associates this filament with Low Dissolved Oxygen (DO), low F/M and Nutrient deficiency. The measured concentrations of nutrients (N & P) in the influent fed to the UCT system were sufficient

(i.e  $N > 50 \text{ mgN/l}$  and  $P > 17 \text{ mgP/l}$ ) and therefore nutrient deficiency was unlikely to have occurred. Further, the DO in the aerobic reactor was maintained between 2 and 5 mgO/l and hence categorization as a low DO filament by Jenkins *et al.* (1984) is inappropriate. *H. hydrosis* can therefore reasonably be categorized as low F/M (Jenkins *et al.*, 1984). Casey *et al.* (1993) did not include *H. hydrosis* as an AA filament and from the filament survey of South African plants; *H. hydrosis* occurred in 21% of plants but was dominant in only 6%.

Type 021N was dominant in 6% and 8% of samples and occurred in 25% and 8% of samples

from the EN and UCT systems respectively and *Thiothrix* was never dominant in either system but occurred in 8% of samples from the UCT system. Type 021N and *Thiothrix* are sulphur accumulating organisms and are seldomly observed in full scale nutrient removal plants and are observed more frequently in lab scale systems. Type 021N is often associated with septic wastewaters in South Africa and its presence in the biocenosis is probably due to the storage period of the influent being too long i.e. up to two weeks albeit at 4°C. As mentioned above nutrient deficiency was unlikely and type 021N is not classified as an AA filament by Casey *et al.* (1993), which suggests that the occurrence of this filament in both systems (i.e dominant in both the EN and UCT systems during the same sewage batch) was either a consequence of the conditions under which the influent was stored or under which the systems were operated (i.e. cleaning of pipes and reactors etc.), but the former being the most likely reason. Although this filament type is not listed frequently occurring in South African full scale plants (Blackbeard *et al.*, 1988) it has been reported frequently in laboratory systems prior to this investigation (Musvoto *et al.*, 1992; Kaschula *et al.*, 1993; Casey *et al.*, Pilson *et al.*, 1995; Sneyders *et al.*, 1998).

### 3.6.2 Sludge Settleability

The expansion of the single-sludge activated sludge systems from chemical oxygen demand (COD) removal to include, progressively, nitrification, denitrification, and phosphorous removal, all biologically has brought with it a new set of difficulties. As mentioned earlier one of these difficulties is the occurrence of filamentous bulking. These filaments (named AA filaments by Casey *et al.*, 1994) produce a poor settling sludge which severely limits the treatment capacity of nutrient removal plants through decreased efficiency in the separation of solids from the liquid phase in the secondary settling tank.

From earlier research Casey *et al.* (1994) proposed an hypothesis for the proliferation of anoxic-aerobic (AA) filamentous organisms in nitrification-denitrification (ND) and nitrification-denitrification biological excess phosphorus removal (NDBEPR) systems. Their hypothesis is as follows:

“The majority of heterotrophic organisms can be classified by their morphological

characteristics as either filamentous or floc-forming organisms. The floc-forming organisms are aerobic-facultative; under aerobic conditions they utilize oxygen and under anoxic conditions they denitrify  $\text{NO}_3^-$  or  $\text{NO}_2^-$  to  $\text{N}_2$  via the gaseous denitrification intermediates  $\text{NO}$  and  $\text{N}_2\text{O}$ . The filamentous organisms are also aerobic-facultative but are nitrate reducers only; under anoxic conditions they reduce  $\text{NO}_3^-$  to  $\text{NO}_2^-$  only.

“When sludge is exposed to alternating anoxic-aerobic conditions ( $\text{NO}_3^-$  and/or  $\text{NO}_2^-$  present throughout anoxic period), nitrate and nitrite is denitrified during the anoxic period to nitrogen gas with some nitric oxide ( $\text{NO}$ ) also being produced. When a floc-forming with intracellular  $\text{NO}$  is subjected to aerobic conditions, the  $\text{NO}$  inhibits the utilization of oxygen. Also, while  $\text{NO}$  is present under aerobic conditions, the floc-formers continue to respire with  $\text{NO}_3^-$  or  $\text{NO}_2^-$  due to the intracellular inhibition by  $\text{NO}$  of the enzymes mediating the transfer of electrons to oxygen. Under anoxic conditions, the filamentous organisms do not produce  $\text{NO}$  as an intermediate and hence do not accumulate  $\text{NO}$  intracellularly. Consequently, these organisms are not inhibited in their utilization of oxygen (and hence substrate) under subsequent aerobic conditions.

“With intracellular  $\text{NO}$  present, and inhibition induced, floc-formers are placed at a disadvantage with respect to the filaments in competition for substrate under aerobic conditions. Consequently, the filamentous organisms utilize a greater proportion of the substrate under aerobic conditions than they would if the floc-formers were not inhibited. With floc-forming organisms inhibited, the filamentous organisms increase their relative mass in the sludge with each exposure to aerobic conditions, leading to the condition referred to as a bulking sludge.”

While it is difficult to measure the gaseous intermediates of denitrification (e.g.  $\text{NO}$ ), the ionic reactants nitrate and nitrite can be measured and indirectly it is the nitrate and nitrite concentrations in the anoxic reactor preceding an aerobic reactor which provides the best indication of the extent of denitrification and consequently the extent to which the oxygen uptake by floc-formers is inhibited on their passing from anoxic to aerobic conditions.

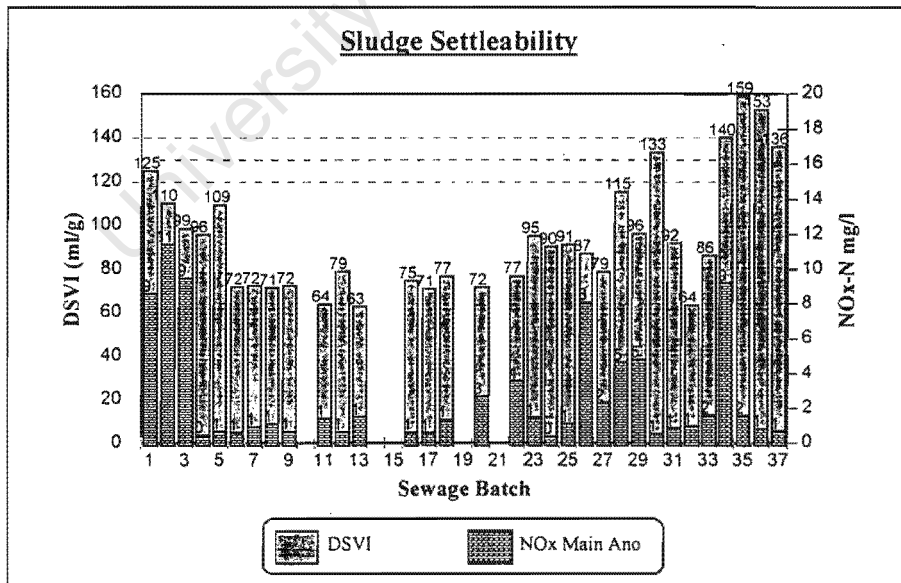
From the results of this investigation, the nitrate plus nitrite concentrations ( $\text{mgNO}_x\text{-N/l}$ ) leaving the main anoxic reactor of the external nitrification and UCT control system were found to be 2.77  $\text{NO}_x\text{-N/l}$  and 1.27  $\text{NO}_x\text{-N/l}$  respectively. The high  $\text{NO}_x$  concentration leaving the main anoxic reactor of the external nitrification system was intentional and maintained by the dosing of nitrate directly to this reactor in order to establish the denitrification potential of the reactor. Although  $>1$   $\text{mgNO}_x\text{-N/l}$  left the anoxic reactors of both the external nitrification and UCT systems, a reasonably good settling sludge was observed in both systems.

The mean diluted sludge volume index (DSVI) and the  $\text{NO}_x$  concentrations leaving the main anoxic reactor measured during the 37 sewage batches are shown plotted in Figure 3.19. From sewage batch 1, the system had a reasonably good settling sludge (DSVI  $\sim 125$  ml/g). The DSVI progressively improved from sewage batch 6 to 27 at which time it averaged around 70 ml/g. From sewage batch 28 to the end of the investigation the DSVI steadily increased from 80 ml/g to 150 ml/g. The increase in the DSVI, although still below a bulking sludge (i.e. 150 ml/g), is a direct result of change in the external nitrification system and the increase in the aerobic mass fraction and sludge age. The stone column external nitrification system was replaced with the activated sludge system which led to a significant improved nitrification efficiency, the aerobic mass fraction was increased to 30% (observed by Casey *et al.*, 1994 to be the aerobic mass fraction at which AA filament proliferation is at a maximum) at the expense of the anoxic mass fraction (30%), the sludge age was increased from 8 to 10 days and a 1:1 mixed liquor a-recycle from the aerobic to the anoxic reactor was installed. All these changes led to increased nitrate load on the main anoxic reactor and a decreased denitrification potential leading to high nitrate and nitrite concentration in the outflow of the anoxic to the aerobic reactor (see Fig.3.19). This is evident in Appendix C which shows that this period in investigation was the time during which the  $\text{NO}_x$  concentration was generally  $> 1.0$  mgN/l. This observation i.e. an increase in the  $\text{NO}_x$  concentration leaving the anoxic reactor with the increase in aerobic mass fraction and with the simultaneous increase in the DSVI, supports the hypothesis of Casey *et al.* (1994). This period was also the time in which aerobic nitrification was significant which meant that the BNRAS external nitrification system now supported nitrifiers leading to higher effluent  $\text{NO}_x$  concentrations. This is evident in Figure 3.20 which shows the relationship between the DSVI and the effluent  $\text{NO}_x$  concentration: it can be seen that the DSVI follows the increase in effluent

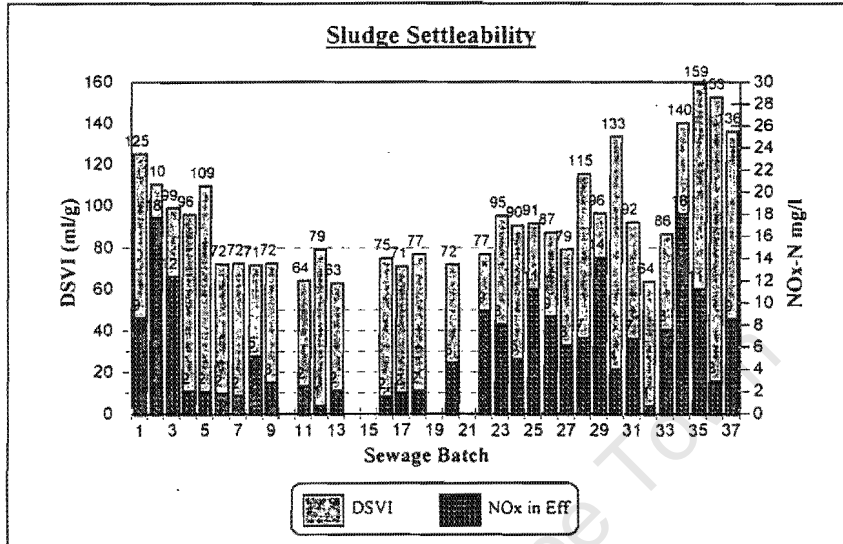
$\text{NO}_x$  concentration. The overall average DSVI of the investigation was 94ml/g and falls in the range of an ideal settling sludge i.e. 80 to 100ml/g.

Generally throughout the investigation the sludge settled very rapidly in the settler and did not form significant sludge beds in either the internal or final settling tanks. A problem with the sludge, especially the day or two after a new sewage batch was fed, was that it did not clarify well and left a fine turbidity in the effluent. This investigation confirmed that the external nitrification BNRAS system consistently produced a good settling sludge. Indeed the system improved the sludge settleability as the investigation progressed and the improved settling characteristics and smaller settling tank requirements which allowed an increase in the treatment capacity of the system, as demonstrated from sewage 4 to 20 of this investigation into the BNRAS external nitrification system.

**Figure 3.19:** Relationship of the Diluted Sludge Volume Index (DSVI) and Anoxic nitrate and nitrite concentration of sewage batches 1 to 37



**Figure 3.20:** Relationship of Dilutes Sludge Volume Index (DSVI) and effluent nitrate and nitrite concentration for sewage batches 1 to 37.



## CHAPTER 4

### CONCLUSIONS AND DISCUSSION

#### 4.1 INTRODUCTION AND OBJECTIVES OF INVESTIGATION

The expansion of the activated sludge system to progressively include nitrification denitrification has brought with it a new set of difficulties (Ekama and Wentzel, 1999;1999b), the main ones being the long sludge age required for nitrification, filamentous organism bulking and the treatment /disposal of supernatants generated from the sludge and solids handling. The focus of this investigation was on nitrification and in particular external nitrification.

In the BNR activated sludge (BNRAS) system, the requirement to nitrify governs selection of the two linked parameters, sludge age and the aerated mass fraction. The need for nitrogen (N) and phosphorus (P) removal sets a requirement for a part of the sludge to be unaerated, for anaerobic conditions to stimulate P removal and anoxic conditions for N removal. In N and P removal plants, the unaerated sludge mass fraction usually needs to be high i.e. > 40%, causing the aerated mass fraction to be reduced, i.e. <60 %. To compensate, to ensure near complete nitrification, long sludge ages have to be selected i.e. 20 to 25 days. Such long sludge ages result in large biological reactors per Ml wastewater (WW) treated. If nitrification can be made independent of the suspended solids sludge age, then the selection of the sludge age will no longer be governed by the requirement to nitrify, but rather by the N removal (denitrification) and P removal (BEPR) processes. For both these processes, a reduction in sludge age increases respectively the N and P removal per mass of organic load (WRC, 1994; Wentzel *et al.*, 1990), provided the sludge age remains longer than some lower limit to prevent “wash-out” of P removal and denitrifying organisms. Indications are that, if nitrification and the sludge age of the suspended solids can be uncoupled, then the sludge age can be reduced to less than half, from about 20-25 days to about 8-10 days. This will result in a reduction in the biological reactor volume requirement per Ml treated of about 1/3rd, or alternatively in an increase in the treatment capacity of some 50% (provided secondary settling tank area requirements are appropriately accommodated).

With the above discussion as motivation for BNRAS system intensification, the external

nitrification system was investigated with the specific objectives being to:

- 1) Establish a stable population of slow-growing nitrifiers on a fixed media external nitrification system.
- 2) Double the volume of the wastewater treated thereby testing one of the benefits of external nitrification because of the now shortened sludge age.
- 3) Promote conditions to achieve anoxic phosphate uptake
- 4) Increase the aerobic mass fraction in an attempt to qualify the effect of the aerobic mass fraction on anoxic P uptake.
- 5) Study the effect of increased aerobic mass fraction on the sludge settleability of the BNRAS system.

To achieve the aims of this investigation, i.e. external nitrification in a BNRAS system, either one or a combination of two ways can be employed. Firstly, by installing a settler and a fixed media external nitrification system between the anaerobic and anoxic reactors, and/or secondly by dosing nitrate directly to the anoxic reactor. To set up the laboratory system as close as possible to the envisioned application of the system, the first approach was adopted. However, in order to increase the nitrate load and ensure that the anoxic reactor was overloaded with nitrate was dosed directly into the main anoxic reactor as a concentrated solution of 0.5 to 1.25 mgN/ml, i.e. to maintain the nitrate load on the main anoxic reactor slightly in excess of its denitrification potential thus allowing some nitrate to enter the aerobic reactor. The system sludge age, temperature and unaerated mass fraction were initially 10 days, 20 °C, and 0.85 respectively. To avoid any interference of nitrate on the P release process in the anaerobic reactor, a 0.1 mass fraction pre-anoxic reactor was set up ahead of the anaerobic reactor to denitrify nitrate in the return sludge. This pre-anoxic reactor was necessary to ensure a near zero nitrate concentration in the flow entering the anaerobic reactor.

During the investigation, which took place over a 373 day continuous period during which time 37 sewage batches were fed, 4 different configurations were tested viz:

- 1) From day 1 to 30 (sewage batches 1 to 3) Configuration 1 as defined above.
- 2) From day 31 to 154 (sewage batches 4 to 20) Configuration 2 in which the influent flow

was doubled from 20 l/d to 40 l/d and sludge age reduced from 10 to 8 days.

- 3) From day 155 to 205 (sewage batches 21 to 25) Configuration 3 in which the influent was decreased to 30 l/d, the aerobic mass fraction increased to 30% at the expense of the anoxic reactor (30%), replaced existing stone column (1.5m) replaced with a longer stone column (2m) to increase retention time, an a-recycle of 1:1 from aerobic to anoxic reactor added and the sludge age increased from 8 to 10 days.
- 4) From day 206 to 373 (sewage batches 26 to 37) Configuration 4 in which the fixed media stone column external nitrifier was replaced with a suspended nitrification activated sludge system.

The evaluation and results of this investigation, which took place over a 373 day period are summarized below in Sections 4.2 to 4.5 and followed by a discussion in Section 4.6:

#### 4.2 SYSTEM COD AND N REMOVAL PERFORMANCE

1. Over the 373 day investigation during which 37 sewage batches were fed to the system the average COD balance in the external nitrification (EN) biological nutrient removal activated sludge (BNRAS) system was 80%, and the average N balance 91%. Although considerably lower than 100%, these are not considerably lower than the COD and N balances observed in other investigations on nutrient removal systems. The low COD balances were mainly the consequence of sludge losses due to mixed liquor spillages, resulting in low VSS masses in the system. The low COD masses in the system affects the unbiodegradable particulate COD fraction determination and specific denitrification rate, making these lower (see 9 and 12 below)
2. The concentrated solution of nitrate dosed (0.5 to 1.25mgNO<sub>3</sub>-N/ml) directly at 0.5 l/d to the main anoxic reactor increased the influent TKN/COD ratio from around 0.08 to 0.14 mgN/mgCOD. The system produced an average effluent total N concentration <20 mgN/l.
3. The average percentage COD removal in the EN BNRAS system was 91%. Of the 100%

of the influent COD, 10% passed out of the system via the effluent, 31% via the waste sludge, 12% in the external nitrifier, 14% via nitrate denitrified and 13% via oxygen utilized, with 20 % unaccounted for.

4. The average percentage N removal in the EN BNRAS system was 72%. Of the 100% influent TKN, 5% and 25% passed out of the system via the effluent as nitrate and TKN respectively, 18% via the waste sludge, 5% in the external nitrifier and 38% via denitrification, with 9% unaccounted for. The main reason for such low N removal is poor nitrification in the fixed media stone column leading to high effluent TKN concentrations (see 11 below).
5. The overall average 0.45  $\mu\text{m}$  membrane filtered effluent COD concentration from the EN BNRAS system was 52 mgCOD/l, giving an influent unbiodegradable soluble fraction  $f_{s,us}$  of 0.075.
6. The filtered effluent TKN concentration was not measured and thus the unbiodegradable soluble TKN fraction ( $f_{nu}$ ) was not determined. However, the overall average unfiltered effluent TKN concentration was 18 mgN/l (see 4 above and 9 below)
7. The average oxygen utilization rate (OUR) for sewage batches 1 to 20 was 35 mgO/l aerobic reactor/h and 38 mgO/l aerobic reactor/h for sewage batches 21 to 37. This increased OUR was due to the increased aerobic mass fraction for Configuration 3 and 4 which supported nitrifiers in the BNRAS system, and because in Configuration 3 the fixed media stone column nitrified poorly, significant nitrification took place in the aerobic reactor. This oxygen demand is significantly below (~50%) that in a conventional BNR system because (i) most of the nitrification oxygen demand is obtained “free” in the external nitrification system and (ii) the nitrate so generated reduces the carbonaceous oxygen demand.
8. The average TSS and VSS concentrations in the EN BNRAS were system 2628 mgTSS/l and 2163 mgVSS/l respectively, giving an average VSS/TSS ratio of 0.82.

9. To determine the unbiodegradable particulate fraction  $f_{s,up}$  of the influent sewage fed to the system, the appropriate  $f_{s,up}$  was selected so that the system VSS mass calculated with the BEPR model of Wentzel *et al.* (1990) was equal to that measured using the measured readily biodegradable (RB) COD concentration and the influent characteristics of the sewage ( $f_{s,us}$ ,  $S_{ii}$ ) and the system parameters as input. An average  $f_{s,up}$  value of 0.11 was found for the EN BNRAS system. The active ordinary heterotrophic (OHO) and polyphosphate accumulating (PAO) organism fractions of the VSS which are required to define the OHO denitrification rate ( $K_2'$ ) and the P content of the PAOs ( $f_{XBG,P}$ ), were also obtained from the calculation procedure (see 12 and 16 below).

#### 4.3 NITRIFICATION AND DENITRIFICATION

10. In this investigation the primary aim was to establish a stable nitrifier population on a fixed media such that nitrification could be "restricted" to the fixed media system thus enabling nitrification and the suspended solids sludge age to be uncoupled. However, due to the limitation imposed by the flow rate to the external nitrification system (in this investigation about 76%, with 24% of the flow bypassing the external nitrification system as internal settling tank underflow) the maximum nitrification completion was 76%, if the external nitrification system outflow ammonia concentration was zero.
11. Initially the fixed media stone column (SC) nitrifier produced a low effluent ammonia concentration of 3mgN/l which represented an 88% nitrification efficiency in the external nitrification system. However, due to *Psychoda* mothfly larvae infestation the nitrification efficiency fell below 50% and produced a wide and varied effluent ammonia concentration, between 8 and 62mgN/l. In order to re-establish the external nitrification efficiency and prevent *Psychoda* infestation, a suspended medium external nitrifier replaced the fixed media SC to facilitate the nitrification process. The suspended medium external nitrifier produced a low effluent ammonia concentration of 9mgN/l and produced an average nitrification efficiency of 72%. It was also noticed that the period while the continually aerated suspended medium nitrifier was employed, was the only

period in which measurable ( $\geq 0.01$  mgNO<sub>2</sub>-N/l) nitrite concentrations were recorded in the outflow of the external nitrification system..

12. In the EN BNRAS system an average of 29mgN/l nitrate was denitrified in the main anoxic reactor and usually there was nitrate running out of the anoxic reactor so the denitrification rates could be calculated from this reactor's nitrate removal.
  
13. Because substantial anoxic P uptake (56%) was observed in the EN BNRAS system, denitrification was therefore mediated by both the ordinary heterotrophic organisms (OHOs) and the polyphosphate accumulating organisms (PAOs). The relative contribution of the PAOs to the denitrification rate was assumed to be the percentage anoxic uptake times the nitrate equivalent of the readily biodegradable COD taken up by the PAOs in the anaerobic reactor (determined from the Wentzel et al., 1990 steady state BEPR model -see 9 above), viz:  $\%A_x P_{upt} * RBCOD$  taken up by PAOs/8.6 where 8.6 is the COD utilized per mg nitrate denitrified. With this approach it was found that the relative contribution of the PAOs to the denitrification rate is quite small - only 17% of the total rate, because they utilize relatively little COD compared with the OHOs. The average OHO and PAO denitrification rates ( $K_2''_{OHO}$  and  $K_2''_{PAO}$ ) were found to be 0.1206 mgNO<sub>3</sub>-N/(mgOHOAVSS.d) and 0.0496 mgNO<sub>3</sub>-N/(mgPAOAVSS.d). If the observed nitrate removal in the anoxic reactor (overloaded with nitrate ) were attributed to the OHOs then the uncorrected specific denitrification rate ( $K_2'$ ) is 0.1379 mgNO<sub>3</sub>-N/(mgOHOAVSS.d). This  $K_2'$  rate has the same bases as the  $K_2'$  rates measured in earlier investigations by Clayton *et al.* (1989) and Sneyders *et al.* (1998) in which no anoxic P uptake was observed and found the  $K_2'$  denitrification rate to be 0.255 and 0.0711 mgNO<sub>3</sub>-N/(mgOHOAVSS.d) respectively. In investigations by Musvoto *et al.* (1992), Pilson *et al.* (1995) and Mellin *et al.* (1995) significant anoxic P uptake was observed and they found the  $K_2'$  denitrification rate to be 0.335, 0.181 and 0.254 mgNO<sub>3</sub>-N/(mgOHOAVSS.d) respectively.

#### 4.4 BIOLOGICAL EXCESS PHOSPHOROUS REMOVAL

14. The effluent P concentration in the EN BNRAS system were kept above 5 mg/l by dosing P to the influent. This allowed the system average P removal capacity of 10.4 mgP/l influent or alternatively 0.015 mgP/mg influent COD to be measured.
15. An average P release of 31 mg P/l took place in the anaerobic reactor and the P uptake took place in both the aerobic and main anoxic reactors with averages 13 and 21 mgP/l respectively. The latter translates into 43% and 56% P uptake taking place in the aerobic and main anoxic reactors respectively. In this investigation, a too low nitrate load on the main anoxic reactor during sewage batches 7 to 23 appeared to have a detrimental effect on the anoxic P uptake. The low nitrate load on the anoxic reactor was caused by a low nitrification efficiency in the external nitrification system (Configurations 2 and 3) which, with the larger aerobic mass fraction, resulted in the support of nitrifiers in the activated sludge system and significant internal nitrification. This in turn led to a high nitrate recycle to the anaerobic reactor (to much for the pre-anoxic to denitrify), and ultimately the P removal was reduced to 8.1 mgP/l.
16. From the model of Wentzel *et al.* (1990) the P content of the PAOs ( $f_{\text{XBG,P}}$ ) was determined by adjusting the  $f_{\text{XBG,P}}$  value (mgP/mgPAOAVSS) in the model until the calculated P removal equaled the measured P removal. An average  $f_{\text{XBG,P}}$  value of 0.312 mgP/mgPAOAVSS was found for the EN BNRAS system. In earlier investigations by Clayton *et al.* (1989) and Sneyders *et al.* (1998) in which no anoxic P uptake was observed, the  $f_{\text{XBG,P}}$  fraction was found to be 0.388 and 0.471 mgP/mgPAOAVSS respectively. In investigations by Musvoto *et al.* (1992), Pilson *et al.* (1995) and Mellin *et al.* (1995) in which significant anoxic P uptake was observed, the  $f_{\text{XBG,P}}$  fraction was found to be 0.144, 0.136 and 0.280 mgP/mgPAOAVSS respectively. Comparing the  $f_{\text{XBG,P}}$  fraction obtained in this investigation with those obtained in earlier investigations we see that the  $f_{\text{XBG,P}}$  is lower when anoxic P uptake is observed than when aerobic P uptake is observed.

#### 4.5 FILAMENT IDENTIFICATION AND SLUDGE SETTLEABILITY

The AA filament bulking hypothesis of Casey *et al.* (1994) describes how a bulking sludge is the result of the nitrate and nitrite concentration ( $\text{NO}_x$ ) leakage from the anoxic reactor to the aerobic reactor. If these concentrations are high ( $>1 \text{ mgN/l}$ ) in conjunction with low aerobic mass fraction ( $<0.70$ ), then a bulking sludge with  $\text{DSVI} > 150 \text{ ml/g}$  would prevail. The filament analyses were carried out on the EN BNRAS system approximately every 4 weeks during the 373 day investigation.

17. The most frequently dominant Anoxic Aerobic (AA, low F/M) filament was *M. parvicella*, while type 1851 and type 0092 were also identified as secondary filaments. Type 021N also occurred but being a septic sewage filament (Jenkins *et al.*, 1984) this was probably due to aging sewage during storage. Apart from type 021N, these filaments are almost always observed in full scale NDBEPR systems (Blackbeard *et al.*, 1998)
18. The average  $\text{NO}_x$  concentrations leaving the anoxic reactor in the EN BNRAS system was  $2.8 \text{ mgNO}_x\text{-N/l}$ . The stone column external nitrification system (Configuration 3) was replaced with the activated sludge system (Configuration 4) which led to a significantly improved nitrification efficiency, the aerobic mass fraction was increased to 30% at the expense of the anoxic mass fraction (30%), the sludge age was increased from 8 to 10 days and a 1:1 mixed liquor a-recycle from the aerobic to the anoxic reactor was installed. All these changes led to increased nitrate load on the main anoxic reactor and a decreased denitrification potential leading to high nitrate and nitrite concentration in the outflow of the anoxic to the aerobic reactor.
19. The mean  $\text{DSVI}$  in the EN BNRAS system was  $94 \text{ ml/g}$  (standard deviation 27). This  $\text{DSVI}$  is ideal (between 80 and  $100 \text{ ml/g}$ ). The fluctuations in the  $\text{DSVI}$  from  $\sim 125 \text{ ml/g}$  at the start of the investigation to  $80 \text{ ml/g}$  mi-way through the investigation and finally to  $\sim 150 \text{ ml/g}$  at the end of the investigation is a direct result of change in the external nitrification system and the increase in the aerobic mass fraction and sludge age. This period was also the time in which internal aerobic nitrification was significant which

meant that the BNRAS system now supported nitrifiers leading to higher effluent  $\text{NO}_x$  concentrations (see 18 above). This observation i.e. an increase in the  $\text{NO}_x$  concentration leaving the anoxic reactor with the increase in aerobic mass fraction and with the simultaneous increase in the DSVI, supports the hypothesis of Casey *et al.* (1994).

#### 4.6 DISCUSSION

The external nitrification biological nutrient removal activated sludge system (BNRASS) allows a step increase in system intensification. Evaluation of the system at laboratory-scale indicates that the scheme holds considerable potential for BNR through the reductions in sludge age and oxygen demand and significant improvement in sludge settleability. Because the BNRASS is not required to nitrify, its anoxic fraction can be considerably enlarged at the expense of the aerobic mass fraction creating conditions that (i) allow it to achieve high N removal with domestic wastewaters with high TKN/COD ratios and (ii) promote anoxic P uptake polyphosphate accumulating organisms (PAOs) to develop in the BNRASS.

The behaviour observed in the laboratory-scale external nitrification BNRASS indicates significant (>56%) anoxic P uptake and reduced aerobic P uptake. To stimulate anoxic BEPR behaviour, it appears that (i) a high nitrate load and large anoxic mass fraction are required to ensure that the denitrifying PAOs (DPAOs) are not restricted in their P uptake and denitrification process (ii) a small aerobic mass fraction is required to limit aerobic PAO activity. The first requirement needs a high influent TKN/COD ratio. If this is too low (<0.14 mgN/mgCOD for the system design parameters) then insufficient nitrate is generated in the fixed media system for the denitrification potential of the anoxic reactor. From this investigation, too low a nitrate load on the anoxic reactors appears detrimental to the development of anoxic P uptake. A possible solution is to increase the TKN/COD ratio of the wastewater by including enhanced primary sedimentation. In fact, enhanced primary sedimentation may prove essential for this scheme, to facilitate acid fermentation of the primary sludge to generate additional volatile fatty acids (VFA) and readily biodegradable (RB)COD. These additional VFA and RBCOD are required to counter the observation that, in agreement with previous observations on conventional activated sludge systems (Ekama and Wentzel, 1997), the anoxic P uptake was reduced compared to aerobic P

uptake, resulting in a similarly reduced BEPR per mass organic load. Including primary sedimentation and acid fermentation of the primary sludge will reduce the overall COD load on the system (and hence reduce the system volume and oxygen demand), and increase the TKN/COD ratio and VFA/RBCOD concentration, which would stimulate more DPAO growth in the system at the expense of the OHOs.

As an alternative to increasing the TKN/COD ratio of the wastewater, it is possible to reduce the anoxic mass fraction and correspondingly increase the aerobic mass fraction. Increasing the aerobic mass fraction will favour aerobic P uptake BEPR behaviour. In evaluating the performance of the external nitrification system with small aerobic mass fractions (Hu *et al.*, 1999), it appeared that anoxic P uptake caused BEPR to be reduced compared to aerobic P uptake. Also, denitrification in the large anoxic reactor was complete, with an "excess" denitrification potential for the influent wastewater TKN (nitrate had to be dosed to the anoxic reactor to fully utilize the denitrification potential); from a denitrification point of view the anoxic reactor was in effect oversized. Further, in attempting to develop anoxic P uptake enhanced cultures (Hu *et al.*, in prep), it was not found possible to develop a stable culture, and the anoxic P uptake process was considered unreliable and unstable for reliable implementation at full scale.

This leads to a re-evaluation of the importance of the reduced aerobic mass fraction. Inclusion of anoxic P uptake PAOs in, and exclusion of aerobic P uptake PAOs from, the biocenosis of the BNRASS mixed liquor are not essential for achieving BNR in the external nitrification scheme. In fact, inclusion and maximization of aerobic P uptake would appear desirable to maximize BEPR. However, conditions that promote aerobic P uptake BEPR, are also conducive to nitrifier growth and hence internal nitrification. Although exclusion of nitrifiers from the mixed liquor of the BNRASS was considered essential, this is not necessary as long as virtual complete nitrification in the external fixed/suspended media nitrification system is obtained to limit nitrification in the main aerobic reactor. In fact, complete exclusion of nitrifiers may not prove possible because although conditions in the BNRASS may not be conducive to their growth, they are likely to be seeded into the system from the external nitrification system. Accepting nitrification in the BNRASS and complete external nitrification, the nitrification in the BNRASS

will be limited by the ammonia bypassing the external nitrification system with the internal settling tank underflow. Nitrate, if any, produced in the aerobic reactor is prevented from entering the anaerobic reactor with the underflow recycle by denitrification in the pre-anoxic reactor. However, should complete nitrification not be obtained in the external nitrification system, then the residual ammonia will be nitrified in the aerobic reactor of the BNRASS. If the aerobic reactor nitrate concentration is too high, the pre-anoxic will become overloaded with nitrate, resulting in nitrate discharge to the anaerobic reactor and a reduction in BEPR. However, if nitrification were not included in the BNR activated sludge system, the ammonia would leave the system via the effluent, which is a less desirable situation.

Recognizing the advantages of including aerobic uptake in the system, and in fact that including nitrification in the system is not entirely undesirable, the emphasis on large anoxic mass fractions to maximize anoxic P uptake process in the system has changed to the possibility of increasing the aerobic reactor mass fraction, to stimulate aerobic P uptake. Initial research on this aspect appears promising, in that increasing the aerobic mass fraction appears to improve BEPR and surprisingly, also stabilize anoxic P uptake. This is in agreement with the literature: In an investigation to select DPAOs, Bortone *et al.* (1996) operated an anaerobic/anoxic sequencing batch reactor (SBR). They found that this system did not stimulate BEPR. However, when a short aerobic period was included in the SBR cycle, stable BEPR with anoxic P uptake (and aerobic P uptake) was obtained. Thus it would appear that an aerobic period may be essential for stable anoxic P uptake. Recognizing that the anoxic P uptake DPAOs are facultative organisms, including an aerobic reactor would provide opportunity for aerobic metabolism by these organisms, in addition to the anoxic metabolism. Biochemically, aerobic metabolism provides a higher energy yield for the organism than anoxic metabolism, and this higher energy yield may provide the biological niche for DPAOs to stably exist in the system.

## REFERENCES

- Blackbeard J.R., Ekama G.A., Marais G.v.R. (1986). A survey of filamentous bulking and foaming in activated sludge plants in South Africa. *Water Pollut. Control*, **85**(1), 90-100.
- Blackbeard J.R., Gabb D.M.D., Ekama G.A and Marais G.v.R. (1988). Identification of filamentous organisms in nutrient removal activated sludge plants in South Africa. *Water SA*, **14**(1), 29-34.
- Bortone G., Saltarelli R., Alonso V., Sorm R., Wanner J. and Tilche A. (1996) Biological anoxic phosphorus removal -The DEPHANOX process. *Water Sci. Technol.*, **34**(1-2), 119-128.
- Bortone G., Sorm R., Wanner J. and Tilche A. (1997) Improvement of anoxic phosphate uptake with the DEPHANOX process. *Procs. 2<sup>nd</sup> ACE CR International Conference*, Jilhlava, Czech Rep., 1-18
- Buchan L. (1983) The possible biological mechanism of phosphorus removal. *Water Sci. Technol.*, **15**(Cape Town), 87-103.
- Casey T.G., Wentzel M.C., Ekama G.A., Loewenthal R.E. and Marais G.v.R (1994). An hypothesis for the cause and control of anoxic-aerobic (AA) filament bulking in nutrient removal activated sludge systems. *Water Sci. Technol.*, **29**(7), 203-212.
- Clayton J.A., Ekama G.A., Wentzel M.C. and Marais G.v.R. (1991). Denitrification kinetics in biological nitrogen and phosphorus removal systems treating municipal wastewaters. *Water Sci. Technol.*, **23**(4/6-2), 1025-1035.
- Cloete .E. and Steyn P.L. (1988). The role of *Acinetobacter* as a phosphorus removing agent in activated sludge. *Water Research*, **22**(8), 971-976.
- Dold P.L., Fleit E. and Han J. (1991). Hydrolysis of  $\alpha$ (1-4) glucan bonds in activated sludge mixed bacterial communities. *Environ. Tech.*, **12**, 871-879.
- Ekama G.A., Wentzel M.C., Casey T.G. and Marais G.v.R. (1996). Filamentous organism bulking in nutrient removal activated sludge systems. Paper 6: Review, evaluation and consolidation of results. *Water SA*, **22**(2), 147-152.
- Ekama G.A., Wentzel M.C. (1997a). Difficulties and Developments in biological nutrient removal technology and modelling. *Procs. 3rd AWWA/IAWQ BNR Conference*, 30 Nov- 3 Dec, Brisbane, Aus.
- Ekama G.A. and Wentzel M.C. (1997b). Denitrification kinetics in biological N&P removal activated sludge systems treating municipal wastewaters. *Procs. 3rd AWWA/IAWQ BNR Conference*, 30 Nov- 3 Dec, Brisbane, Aus.
- Hu Z., Wentzel M.C., Ekama., (1999). External Nitrification in biological nutrient removal activated sludge systems. (*Submitted to Water SA*).

- Jenkins D., Richard M.G. and Daigger G.T. (1984). Manual on the causes and control of activated sludge bulking and foaming. Published by Water Research Commission, P O Box 824, Pretoria, 0001, RSA
- Kaschula W.A., Ekama G.A., Wentzel M.C., Palmer S., and Birch R.R. (1993). The effect of alternative detergent builders on the nutrient removal activated sludge sewage treatment process. Research Report W78, Dept. Of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W. Cape, South Africa.
- Kern-Jespersen J.P. and Henze M. (1993). Biological phosphorus uptake under anoxic and oxic conditions. *Water Research*, **27**(4), 617-624.
- Kuba T., Smoulders G.J.F., van Loosdrecht M.C.M. and Heinen J.J. (1993). Biological phosphorous removal from wastewater by anaerobic-anoxic sequencing batch reactor. *Water Sci. Technol.*, **27**(5/6), 241-252.
- Kuba T., van Loosdrecht M.C.M., Brandse F.A. and Heinen J.J. (1997). Occurrence of denitrifying phosphorous removing bacteria in modified UCT-type wastewater treatment plants. *Water Research*, **31**(4), 777-786.
- Mbewe A., Wentzel M.C., Lakay M.T and Ekama G.A. (1995). Characterization of the carbonaceous materials in municipal wastewaters. Research Report W84, Dept. Of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W. Cape, South Africa.
- Murnleitner E., Kuba T., Van Loosdrecht M.C.M. and Heijnen J.J. (1997). An integrated metabolic model for the aerobic and denitrifying biological phosphorus removal process. *BioTech & BioEng.*, **54**(5), 434-450.
- Musvoto E.V., Casey T., Ekama G.A., Wentzel M.C. and Marais G.v.R. (1992). The effect of a large anoxic mass fraction and concentrations of nitrate and nitrite in the primary anoxic zones on low F/M filament bulking in nutrient removal activated sludge systems. Research Report W77, Dept. Of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W. Cape, South Africa.
- Parker D.S. and Richards T. (1986). Nitrification in trickling filters. *Journal WPCF*, **58**(9), 896-902.
- Parker D.S., Lutz M., Dahl R. and Bernkopf S. (1989). Enhancing reaction rates in nitrification trickling filters through biofilm control. *Journal WPCF*, **61**(5), 618-631.
- Parker D.S., Lutz M., Andersson B. and Aspegren H. (1995) Effect of operating variables on nitrification rates in trickling filters. *Water Environment Research*, **67**(7), 1111-1118.
- Parker D.S., Jacobs T., Bower E., Stowe D.W. and Farmer G. (1996). Maximizing trickling filter nitrification rates through biofilm control: Research review and full scale application. *Procs 3<sup>rd</sup> IAWQ Specialized Conferrence on Biofilm Systems*, Copenhagen, Aug 1996.

- Payne W.J. (1981) *Denitrification*, John Wiley and Sons, New York.
- Pilson R.A., Ekama., Wentzel M.C. and Casey T.G. (1995). The effect of temperature on denitrification kinetics and biological excess phosphorous removal in biological nutrient removal systems in temperature climates (12 °C - 20 °C). Research Report W86, Dept. of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W.Cape, South Africa.
- Poppelen P. ( June 1998). Control of Psychoda. WQI Casebook, 49-53.
- Randall C.W. and Sen D. (1996). Full-scale evaluation of an integrated fixed-film activated sludge (IFAS) process for enhanced nitrogen removal. *Water Sci. Technol.*, 33(12), 155-162.
- Sneyders M.J., Wentzel M.C. and Ekama G.A. (1998). The effect of dosing unstabilized landfill leachate to a nutrient removal activated sludge system. Research Report W95, Dept. of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W.Cape, South Africa.
- Stern L.B and Marais G.v.R. (1974). Sewage as the electron donor in biological denitrification. Research Report W7, Dept. of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W.Cape, South Africa.
- Ubisi M.F., Wentzel M.C., Lakay M.T and Ekama G.A. (1997). Organic and inorganic components of activated sludge mixed liquor. Research Report W94, Dept. Of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W. Cape, South Africa.
- van Hyssteen J.A., Barnard J.L. and Hendriksz J. (1990). The Olifantsfontein nutrient removal plant. *Water Sci. Technol.*, 22(7/8), 1-8.
- Wachtmeister A., Kuba T., Van Loosdrecht M.C.M. and Heijnen J.J. (1997). A sludge characterization assay for aerobic and denitrifying biological phosphorus removing sludge. *Wat. Res.* 31(3), 471-478.
- Warburton C.A., Lakay M.T., Casey T.G., Ekama G.A., Wentzel M.C. and Marais G.v.R. (1991). The effect of sludge age and aerobic mass fraction on low F/M filament bulking in intermittent aeration nitrogen removal systems. Research Report W65, Dept. Of Civil Eng., Univ. of Cape Town, Rondebosch, 7700, W. Cape, South Africa.
- Wentzel M.C., Ekama G.A., Dold P.L. and Marais G.v.R. (1985). Kinetics of biological excess phosphorus release. *Water Sci. Technol.*, 17(11/12), 57-71.
- Wentzel M.C., Ekama G.A., Dold P.L. and Marais G.v.R. (1990). Biological excess phosphorus removal – Steady state process design. *Water SA*, 16(1), 29-48.
- Wentzel M.C. and Ekama G.A. (1997). Principals in the design of single-sludge activated -sludge systems for biological removal of carbon, nitrogen, and phosphorus. *Water Environment*

*Research*, **69**(7), 1222-1231.

Wentzel M.C. and Ekama G.A.(1999). Denitrification kinetics in biological N and P removal activated sludge systems treating municipal wastewaters. *Water Sci. Technol.*, **39**(6), 69-77.

WRC (1984). Theory, design and operation of nutrient removal activated sludge processes. Published by the Water Research Commission, PO Box 824, Pretoria 0001, South Africa. ISBN 0908356137

University of Cape Town

# **APPENDICES**

## **APPENDIX A**

Daily Results of the External Nitrification BNRAS System.  
Figures A1 to A28 : Graphs of Daily Results.

## **APPENDIX B**

Nitrogen Mass Balance.  
COD Mass Balance.

## **APPENDIX C**

Average Sewage Batch Results of External Nitrification System.  
 $f_{S,up}$  and  $f_{XBG,P}$  Calculations for each Sewage Batch.

## **APPENDIX D**

Design and Operating Parameters of the UCT Control System.  
Daily Results of UCT Control System (monitored and measured by  
Mr. T Lakay.  
Figures D1 to D18 : Graphs of Daily Results.

## **APPENDIX E**

Average Sewage Batch Results of UCT Control System.  
Figures E1 to E14 : Graphs of Average Sewage Batch Results.

## **APPENDIX F**

Filament Identification in the External Nitrification and UCT Systems.

## **APPENDIX A**

- Daily Results of the External Nitrification BNRAS System.
- Figures A1 to A28 : Graphs of Daily Results.

University of Cape Town



Daily Tests on Modified Diaphragm (MVRAS) External Nitrogen System

Day No	1998	Sys In/ mCODM	Chlorination Oxygen Demand					RBCOD Floc			Free & Soluble Ammonia				Total Kjeldahl Nitrogen					
			Reactor 3 mCODM	Fn_UER mCODM	EqN4_FEB mCODM	INSE4_FEB mCODM	Fn_FEB mCODM	Floc In/ mCODM	Floc EB/ mCODM	RBCOD mCODM	Influent mgN/l	EqN4_UER mgN/l	INSE4_UER mgN/l	Influent mgN/l	Reactor 3 mgN/l	Fn_UER mgN/l	EqN4_UER mgN/l	INSE4_UER mgN/l		
120	23-Jun	Tuesday	760	3500	78	94	198	148	32	96	81	67	60	66	106	258	74	63	80	
121	24-Jun	Wednesday																		
122	25-Jun	Thursday	736	4650	78	84	184	86	36	30	66	45	51	67	97	337	60	61	78	
123	26-Jun	Friday																		
124	27-Jun	Saturday																		
125	28-Jun	Sunday																		
End of Batch 6			748	4780	78	89	191	117	44	73	74	56	58	67	101	398	67	62	79	
126	29-Jun	Monday	708	3940	64	84	140	62			64	43	39	57	88	283	48	42	78	
127	30-Jun	Tuesday																		
128	01-Jul	Wednesday	584	3320	76	56	136	148	40	100	69	38	46	60	101	351	44	51	63	
129	02-Jul	Thursday	652	3020	86	96	180	178	38	140	76	38	46	57	106	350	43	51	63	
130	03-Jul	Friday																		
131	04-Jul	Saturday																		
132	05-Jul	Sunday																		
133	06-Jul	Monday	700	3640	94	86	194	62			41	24	23	33	50	147	23	30	39	
134	07-Jul	Tuesday																		
End of Batch 7			661	3480	83	80	163	62	163	39	62	36	39	52	86	283	40	43	61	
135	08-Jul	Wednesday																		
136	09-Jul	Thursday	608	3840	96	140	164	134	58	78	80	36	34	46	70	129	38	43	49	
137	10-Jul	Friday									69	31	44	78	259	34	35	45		
138	11-Jul	Saturday	632	3140	78	94	142	64			56	22	15	45	80	111	34	39	50	
139	12-Jul	Sunday																		
140	13-Jul	Monday																		
141	14-Jul	Tuesday																		
142	15-Jul	Wednesday																		
143	16-Jul	Thursday																		
144	17-Jul	Friday																		
145	18-Jul	Saturday																		
146	19-Jul	Sunday																		
147	20-Jul	Monday																		
End of Batch 8			620	3900	87	117	153	64	156	38	78	61	30	35	45	76	223	35	38	48
148	21-Jul	Tuesday																		
149	22-Jul	Wednesday																		
End of Batch 9																				
150	23-Jul	Thursday	734	3431	73	90	159	57			64	34	41	53	70	262	39	46	64	
151	24-Jul	Friday	616	2938	57	71	120	139	39	100	59	35	41	48	88	330	39	44	61	
152	25-Jul	Saturday																		
153	26-Jul	Sunday																		
154	27-Jul	Monday	698	3427	59	88	153	133	29	104	60	38	38	51	82	251	36	42	56	
End of Batch 20			653	3332	63	83	144	57	136	34	102	61	56	40	80	291	38	44	60	
155	28-Jul	Tuesday																		
156	29-Jul	Wednesday																		
157	30-Jul	Thursday																		
158	31-Jul	Friday																		
159	01-Aug	Saturday																		
160	02-Aug	Sunday																		
161	03-Aug	Monday																		
162	04-Aug	Tuesday																		
163	05-Aug	Wednesday																		
164	06-Aug	Thursday																		
165	07-Aug	Friday																		
166	08-Aug	Saturday																		
167	09-Aug	Sunday																		
168	10-Aug	Monday																		
169	11-Aug	Tuesday	564	4860	70	72	176	50			67	36	29	36	81	116	34	36	47	
170	12-Aug	Wednesday	612	4160	56	102	122	154	28	126	71	28	30	38	67	141	31	32	56	
171	13-Aug	Thursday																		
172	14-Aug	Friday																		
173	15-Aug	Saturday																		
174	16-Aug	Sunday																		
175	17-Aug	Monday																		
End of Batch			598	4110	53	87	149	30	154	38	63	69	27	30	37	84	129	33	34	51
176	18-Aug	Tuesday	608	3500	68	100	116	38			44	9	20	27	59	208	10	25	31	
177	19-Aug	Wednesday	680	3180	69	80	116	194	42	152	37	6	22	23	64	221	7	27	33	
178	20-Aug	Thursday	624	2460	40	78	118	48			39	11	16	28	57	245	16	27	34	
179	21-Aug	Friday																		
180	22-Aug	Saturday	687	3698	59	85	122	53			39	11	18	28	57	245	16	27	34	
181	23-Aug	Sunday																		
182	24-Aug	Monday	642	3536	30	61	85	28			41	7	20	24	65	253	12	27	34	
183	25-Aug	Tuesday	671	3719	57	114	134				41	14	22	29	64	266	18	31	33	
184	26-Aug	Wednesday																		
185	27-Aug	Thursday																		
186	28-Aug	Friday																		
187	29-Aug	Saturday																		
188	30-Aug	Sunday																		
End of Batch 23			652	3349	52	86	115	42	123	37	86	40	9	19	27	61	240	13	27	33
189	31-Aug	Monday	691	3478	77	89	128	53			43	10	22	30	63	214	14	28	34	
190	01-Sep	Tuesday	703	2897	71	89	146	158	35	124	31	18	26	30	52	167	11	32	35	
191	02-Sep	Wednesday	711	2723	69	72	134	49			40	9	24	30	64	157	14	30	36	
192	03-Sep	Thursday	691	2784	87	87	205	67			43	12	27	32	63	139	16	33	38	
193	04-Sep	Friday																		
194	05-Sep	Saturday																		
195	06-Sep	Sunday	1071	4015	53	51	128	39			46	15	30	35	75	235	18	35	46	
196	07-Sep	Monday																		
End of Batch			769	3237	72	77	148	52	158	35	124	41	11	26	31	65	182	15	31	38
197	08-Sep	Tuesday																		
198	09-Sep	Wednesday																		
199	10-Sep	Thursday	539	2920	69	37	142	75	45	30	55	11								

Daily Tests on Modified Dephox BNRAS External Nitrification System

Day No	1998	Carbonaceous Oxygen Demand						RBCOD Flow			Free & Soluble Ammonia				Total Kjeldahl Nitrogen					
		Sys. Inlet mgCOD/L	Reactor 1 mgCOD/L	Fin. UZF mgCOD/L	Ext'n. PE mgCOD/L	Ins't. PE mgCOD/L	Fin. PE mgCOD/L	Flow Inlet mgCOD/L	Flow Eff. mgCOD/L	RBCOD mgCOD/L	Influent mgN/L	Fin. UZF mgN/L	xNbr. UZF mgN/L	Ins't. UZF mgN/L	Influent mgN/L	Reactor 1 mgN/L	Fin. UZF mgN/L	xNbr. UZF mgN/L	Ins't. UZF mgN/L	
253	05-Nov	728.24	2632	65.28	110.16	187.68	108.12	40.8	67.32	70	10.92	22.19	59.54	140	142.8	13.72	33	76.02		
254	06-Nov	718.08	2611.2	67.32	124.44	238.68	73.44	38.76	34.68	66.92	10.5	14	56.33	87.08	128.8	14.28	22.68	63.14		
257	07-Nov	734.4	2468.4	65.28	110.16	163.2	171.36	34.68	136.68	66.08	6.16	7.98	30.94	82.12	131.6	9.38	11.76	36.54		
258	08-Nov																			
259	09-Nov																			
260	10-Nov	522.24	2142	73.44	110.16	191.76	171.36	36.72	134.64	63	1.89	6.3	47.11	105.84	138.6	6.16	9.38	60.2		
261	11-Nov	530.4	2162.4	44.88	110.16	126.48	138.72	30.6	108.12	65.66	3.22	6.44	40.32	89.46	130.2	6.44	11.03	49.98		
262	12-Nov	807.84	2284.8	57.12	122.4	183.6	136.68	38.76	97.92	58.94	1.4	8.12	37.66	81.06	167.3	2.43	13.79	56.42		
263	13-Nov	538.56	2182.8	51	102	134.64	146.88	28.56	118.32	61.46	5.74	11.34	36.19	82.6	130.2	7	16.59	51.8		
End of Batch 29		653.9657	2357.457	60.61714	112.7829	175.1486	ERR	135.2229	35.55429	99.44887	44.58	5.49	10.91	42.73	95.88	138.5	8.49	17.75	56.3	
264	14-Nov																			
265	15-Nov																			
266	16-Nov	718.08	2632	65.28	130.56	187.68	63.24			43.64	2.8	4.34	25.2	75.04	175	5.6	7.84	17.23		
267	17-Nov	807.84	2632	53.04	89.76	143.2	130.56	30.6	99.96	34.72	1.4	4.9	23.87	59.64	138.6	3.36	5.32	29.12		
268	18-Nov	640.56	2305.2	38.76	65.28	150.96	20.4			37.38	1.4	3.78	23.94	56.28	135.6	3.36	5.6	28.89		
269	19-Nov	522.24	2632	53.08	39.16	161.16	124.44	36.72	87.72	32.76	3.85	4.2	24.78	59.92	126	6.86	6.23	30.24		
270	20-Nov	840.48	2244	51	75.48	173.4	124.44	30.6	93.84	38.64	3.92	5.88	27.65	60.06	147	5.46	7.14	31.36		
271	21-Nov	742.56	2386.8	48.96	89.76	183.6	42.54			42	2.1	3.92	28.7	36.28	138.6	4.62	5.74	31.08		
272	22-Nov																			
273	23-Nov																			
274	24-Nov																			
275	25-Nov	667.92	2691.92	48.376	99.176	151.8	30.36			48.44	1.96	6.44	28.56	61.6	141.4	5.8	6.44	34.16		
276	26-Nov	663.872	2631.44	58.696	170.016	178.112				40.6	1.4	6.3	23.06	55.72	149.8	3.6	10.64	30.24		
End of Batch 30		789.44	2529.42	52.42	97.40	168.74	39.21	118.64	35.11	83.54	46.82	2.35	4.97	25.97	60.57	144.03	5.86	6.87	38.42	
277	27-Nov																			
278	28-Nov																			
279	29-Nov																			
280	30-Nov																			
281	01-Dec																			
282	02-Dec	821.744	2793.12	46.532	109.296	133.584	26.312			31.92	2.1	5.46	32.48	66.78	173	5.04	11.2	44.24		
283	03-Dec	821.792	3400.32	64.768	129.536	153.824				159.896	36.432	123.464	36.56	1.82	8.26	41.3	109.2	170.8	1.47	29.54
284	04-Dec																			
285	05-Dec																			
286	06-Dec																			
End of Batch 31		821.768	3096.72	55.66	119.416	143.704	26.312	159.896	36.432	123.464	54.74	1.96	6.86	36.89	87.99	172.9	3.255	7.35	16.99	
287	07-Dec																			
288	08-Dec																			
289	09-Dec																			
290	10-Dec																			
291	11-Dec																			
292	12-Dec																			
293	13-Dec																			
294	14-Dec																			
295	15-Dec	576	3320	48	64	144	130	24	126	35.56	2.1	6.09	24.78	53.72	196	5.18	7.98	30.52		
296	16-Dec	584	3320	34	60	132	132	12	140	35.56	4.9	3.6	23.8	36	280	9.1	20.16	30.66		
297	17-Dec	792	3300	42	66	182	182	38	144	33.2	2.24	6.23	24.78	58.8	196	5.81	7.98	30.52		
298	18-Dec	792	3820	44	84	132	152	40	112	53.16	4.48	5.6	26.46	36	280	9.1	20.16	29.4		
299	19-Dec																			
300	20-Dec																			
301	21-Dec																			
302	22-Dec																			
End of Batch 32		684	3490	42	68.5	152.5	ERR	159	28.5	130.5	44.87	3.43	5.88	24.955	54.63	238	7.2975	14.07	38.275	
303	23-Dec																			
304	24-Dec	764	3660	54	100	160	170	46	124	56.84	11.76	23.28	36.68	86.8	350.2	12.88	28.14	43.26		
305	25-Dec	768	4560	48	92	172	44			59.64	11.76	17.22	38.36	61.04	145.6	15.12	23.66	40.46		
306	26-Dec	732	4640	40	92	168	140	44	96	57.12	7.56	17.22	34.72	60.76	284	11.62	17.08	41.16		
307	27-Dec																			
308	28-Dec	800	4520	64	96	168	136	56	100	58.8	8.82	12.88	37.94	69.44	330.4	12.74	19.18	42.14		
309	29-Dec	704	2640	84	124	164	68			59.92	5.74	11.76	30.8	80.08	348.6	11.48	20.02	48.16		
310	30-Dec	688	2960	60	124	164	144	32	112	50.96	4.62	6.3	31.64	78.96	315	7.7	17.64	49		
311	31-Dec																			
312	01-Jan																			
313	02-Jan																			
314	03-Jan																			
315	04-Jan	664	3060	24	80	116	104	18	86	79.52	3.92	10.5	38.71	131.88	295.4	6.02	14	48.44		
End of Batch 33		734.2857	3748.571	53.42857	101.1429	158.8571	56	142.8	39.2	103.4	60.4	7.74	15.4	35.55	81.28	325.6	11.88	19.96	44.64	
316	05-Jan	924	3240	52	108	120	86	34	52	58.38	3.5	8.4	33.46	83.44	200.2	6.02	9.52	48.44		
317	06-Jan																			
318	07-Jan																			
319	08-Jan																			
320	09-Jan																			
321	10-Jan																			
322	11-Jan																			
323	12-Jan																			
324	13-Jan	756	2720	72	118	202	64			67.76	6.23	16.38	44.1	91	210	9.59	20.23	53.44		
325	14-Jan	820	2820	60	154	218	180	44	136	49.56	4.									

Daily Tests on Modified Deponox-BNRRAS External Nitrification System

Day No	1998			Anaerobic Mass			Anoxic 1 Mass			Anoxic 2 Mass			Aerobic Mass			Waste Mass			DSVI	COD/VSS	TKN/VSS	TKN/COD
	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS				
1	24-Feb	Tuesday	1250	1064	186	1802	1472	330	3180	2658	322	1396	1194	232	NO	NO	NO	NO	107	1.61	0.11	0.05
2	25-Feb	Wednesday	1370	1218	242	1570	1210	360	3788	3204	294	1468	1234	214	NO	NO	NO	NO	136	1.68	0.10	0.04
3	26-Feb	Thursday	1370	1166	204	1620	1362	258	2038	2450	528	1520	1274	346	NO	NO	NO	NO	132	1.45	0.11	0.06
End of Batch 1			1587	1186	211	1644	1381	283	2445	2204	441	1461	1231	231	0	0	0	0	125	1.58	0.11	0.05
4	27-Feb	Friday	1148	966	182	1576	1298	278	2934	2398	536	1380	1132	248	NO	NO	NO	NO	152	1.40	0.10	0.08
5	28-Feb	Saturday	1136	976	160	1442	1234	208	2512	2092	430	1282	1118	164	NO	NO	NO	NO	140	2.23	0.12	0.07
6	01-Mar	Sunday	738	626	132	1212	966	246	1968	1560	468	1768	1396	372	NO	NO	NO	NO	107	1.57	0.10	0.08
7	02-Mar	Monday	908	766	142	1392	1160	232	2112	1734	378	1800	1456	344	NO	NO	NO	NO	111	1.42	0.09	0.07
8	03-Mar	Tuesday	856	716	170	1316	1080	236	2298	1874	424	1734	1406	328	NO	NO	NO	NO	104	1.16	0.07	0.08
9	04-Mar	Wednesday	886	620	266	1292	1038	234	1990	1618	372	1102	386	316	NO	NO	NO	NO	163	2.32	0.21	0.09
10	05-Mar	Thursday	952	738	214	1390	1148	242	2050	1694	306	2940	2378	362	NO	NO	NO	NO	95	1.78	0.08	0.09
11	06-Mar	Friday	970	818	152	1218	1060	198	2828	2310	318	2230	1786	444	NO	NO	NO	NO	94	1.42	0.10	0.09
12	07-Mar	Saturday	924	784	130	1228	1010	218	2670	2164	506	2376	1914	462	NO	NO	NO	NO	84	1.25	0.09	0.10
13	08-Mar	Sunday	1102	918	184	1358	1110	248	2894	2362	532	2426	1956	470	NO	NO	NO	NO	93	1.37	0.09	0.09
14	09-Mar	Monday	884	740	144	1206	1002	204	2030	1664	366	2420	1944	476	NO	NO	NO	NO	107	1.48	0.09	0.09
15	10-Mar	Tuesday	946	804	142	1290	1074	216	2086	1726	360	2506	2026	480	NO	NO	NO	NO	92	1.32	0.08	0.08
16	11-Mar	Wednesday	880	718	152	1188	982	206	2624	2132	492	2014	1636	378	NO	NO	NO	NO	109	1.44	0.10	0.09
17	12-Mar	Thursday	840	716	124	1110	946	164	2036	1684	352	2446	1998	448	NO	NO	NO	NO	90	1.37	0.08	0.07
End of Batch 2			945	780	165	1304	1091	224	2357	1930	427	2030	1624	407	0	0	0	0	110	1.54	0.10	0.08
18	13-Mar	Friday	868	736	132	1200	1006	194	2878	2314	564	1608	1308	300	NO	NO	NO	NO	124	2.75	0.17	0.07
19	14-Mar	Saturday	1126	964	162	1512	1264	248	1758	1314	264	1990	1634	366	NO	NO	NO	NO	109	2.27	0.09	0.06
20	15-Mar	Sunday	1224	1074	150	1392	1248	144	2240	1910	330	2238	1916	322	NO	NO	NO	NO	71	1.78	0.09	0.07
21	16-Mar	Monday	1190	1044	146	1424	1252	172	2538	2178	360	2064	1764	300	NO	NO	NO	NO	97	0.00	0.06	ERR
End of Batch 3			1073	925	148	1368	1173	195	2232	1846	386	1945	1616	329	0	0	0	0	99	2.27	0.12	0.07
23	18-Mar	Wednesday	1428	1234	194	1600	1380	220	4034	3490	384	2234	2002	232	NO	NO	NO	NO	98	0.00	0.00	0.00
24	19-Mar	Thursday	1706	1492	214	1846	1566	280	4546	3844	702	2420	2026	394	NO	NO	NO	NO	103	0.00	0.00	0.00
25	20-Mar	Friday	1686	1440	246	1840	1346	294	4426	3626	600	2746	2296	450	NO	NO	NO	NO	97	1.58	0.10	0.08
26	21-Mar	Saturday	1776	1528	248	1718	1490	238	4784	4038	726	2262	1978	384	NO	NO	NO	NO	119	1.71	0.10	0.07
27	22-Mar	Sunday	1492	1380	118	1566	1332	234	4038	3444	614	3004	2504	500	NO	NO	NO	NO	80	1.82	0.10	0.07
End of Batch 4			1619	1415	294	1716	1463	253	4370	3724	645	2553	2161	392	0	0	0	0	94	1.62	0.06	0.07
31	26-Mar	Thursday	1260	1096	164	1642	1436	206	3626	3094	532	1684	1442	242	1328	1364	-36	93	1.60	0.13	0.06	
32	27-Mar	Friday	1444	1210	234	1406	1200	206	3514	2908	608	1822	1750	72	1480	1240	168	181	1.50	0.10	0.06	
34	29-Mar	Sunday	1624	1428	196	1630	1408	242	4034	3424	630	3438	2894	544	1638	1450	188	52	0.93	0.05	0.05	
35	30-Mar	Monday																				
36	31-Mar	Tuesday																				
37	01-Apr	Wednesday																				
38	02-Apr	Thursday																				
End of Batch 5			1443	1245	198	1566	1348	218	3731	3141	590	2315	2029	286	1458	1351	107	109	1.35	0.09	0.06	
39	03-Apr	Friday																				
40	04-Apr	Saturday																				
41	05-Apr	Sunday																				
42	06-Apr	Monday	1478	1280	198	1618	1374	244	3480	3148	532	3808	3428	380	1676	1662	14	53	0.81	0.09	0.10	
43	07-Apr	Tuesday	1216	1040	176	1442	1216	226	3376	3010	366	3204	2664	540	1624	1614	10	66	1.62	0.12	0.10	
44	08-Apr	Wednesday	1306	1160	146	1500	1278	222	4066	3482	384	2236	1966	370	1742	1714	28	94	1.81	0.17	0.10	
45	09-Apr	Thursday	1420	1218	212	1506	1242	264	4142	3484	658	3704	3074	620	2586	2176	410	76	1.60	0.10	0.08	
End of Batch 6			1358	1174	183	1517	1277	239	3816	3331	485	3262	2793	480	1907	1792	114	72	1.44	0.12	0.09	
46	10-Apr	Friday	1476	1282	194	1616	1366	250	5388	4598	790	3448	2886	562	2186	1728	458	107	0.83	0.10	0.11	
47	11-Apr	Saturday	1504	846	838	2032	1774	278	1682	1466	216	3606	3004	602	2112	1740	372	107	0.81	0.10	0.11	
48	12-Apr	Sunday																				
49	13-Apr	Monday																				
50	14-Apr	Tuesday																				
51	15-Apr	Wednesday	2198	1938	260	1364	1390	174	2318	2050	258	3994	3424	570	2188	1952	236	73	0.55	0.09	0.11	
52	16-Apr	Thursday	1934	1738	216	2030	1882	168	6200	3366	2834	3440	2972	468	2898	2330	548	70	0.85	0.09	0.10	
End of Batch 7			1783	1491	382	1870	1653	217	3897	2873	1024	3422	3471	551	2346	1943	403	72	0.76	0.08	0.11	
53	17-Apr	Friday	1970	1734	216	2190	1830	340	5394	4450	944	3318	2782	536	1180	1906	-726	60	1.68	0.14	0.09	
54	18-Apr	Saturday																				
55	19-Apr	Sunday	2006	1706	300	2410	2028	382	6826	5740	1086	2400	2154	346	3826	2954	872	83	2.03	0.13	0.07	
56	20-Apr	Monday	2082	1756	306	2626	2212	414	5722	4798	926	3192	2642	530	3136	2484	672	72	1.57	0.10	0.07	
57	21-Apr	Tuesday	2296	1978	318	2632	2230	412	7132	5918	1174	3260	2702	558	2822	2218	604	64	1.44	0.10	0.07	
58	22-Apr	Wednesday	2024	1762	262	2334	1992	362	5740	4820	920	2964	2464	500	2734	2240	494	74	1.45	0.09	0.08	
59	23-Apr	Thursday	2276	1918	318	2724	2274	450	7312	6030	1262	2990	2442	548	3310	2680	630	67	1.47	0.09	0.07	
60																						

Daily Tests on Modified Deplexon BTRAS External Nitritation System

Day No	1999	Aerobic Mass			ANOXIC 1 Mass			ANOXIC 2 Mass			Aerobic Mass			Waste Mass			DSVI	COD/VSS	TKN/VSS	TKN/COD	
		VSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS					
120	23-Jun	Tuesday																			
121	24-Jun	Wednesday	2524	2284	340	2942	2542	400	14550	1894	8656	2942	2496	446	3114	2658	456	75	1.40	0.10	0.11
122	25-Jun	Thursday																			
123	26-Jun	Friday	2392	2070	322	2636	2288	348	6760	5740	960	3780	3130	630	3128	2588	540		1.47	0.11	0.09
124	27-Jun	Saturday																			
125	28-Jun	Sunday																			
End of Batch 6			2938	2177	331	2789	2415	374	10625	9817	4908	3061	2813	548	3121	2623	498	79	1.44	0.12	0.10
126	29-Jun	Monday	2630	2468	362	2738	2394	344	3422	2942	480	1524	2980	544	3400	3002	398	68	1.32	0.09	0.09
127	30-Jun	Tuesday																			
128	01-Jul	Wednesday	2272	1998	314	2694	2264	380	7232	6120	1112	2992	2528	464	2692	2296	396	74	1.31	0.14	0.12
129	02-Jul	Thursday	2214	1904	310	2556	2182	374	6838	5770	1058	3194	2674	520	2734	2318	416	69	1.13	0.13	0.12
130	03-Jul	Friday																			
131	04-Jul	Saturday																			
132	05-Jul	Sunday																			
133	06-Jul	Monday	2324	1830	494	2568	2210	338	6938	6490	448	3014	2562	452	2704	1802	502	73	1.42	0.06	0.06
134	07-Jul	Tuesday																			
End of Batch 7			2410	2040	370	2627	2262	364	6108	5531	777	3181	2686	496	2880	2386	528	71	1.30	0.11	0.10
135	08-Jul	Wednesday																			
136	09-Jul	Thursday	2178	1698	480	2424	1910	514	7204	4022	3182	3106	2878	228	2564	2342	222	71	1.33	0.04	0.10
137	10-Jul	Friday	2060	1978	82	2456	2090	366	4840	3854	986	2662	2238	424	2620	2202	418	83	0.00	0.12	
138	11-Jul	Saturday																			
139	12-Jul	Sunday																			
140	13-Jul	Monday																			
141	14-Jul	Tuesday																			
142	15-Jul	Wednesday																			
143	16-Jul	Thursday																			
144	17-Jul	Friday																			
145	18-Jul	Saturday																			
146	19-Jul	Sunday																			
147	20-Jul	Monday																			
End of Batch 18			2119	1858	281	2440	2000	440	6022	3638	2084	2894	2598	326	2892	2272	320	77	0.67	0.08	0.10
148	21-Jul	Tuesday																			
149	22-Jul	Wednesday																			
End of Batch 19																					
150	23-Jul	Thursday	2578	2088	490	2542	2256	306	6498	6084	414	3250	2848	402	2972	2232	740	62	0.00	0.00	
151	24-Jul	Friday	2338	1980	358	2390	2074	316	6128	3118	1010	3822	2390	432	2716	2330	486	71	1.52	0.11	0.09
152	25-Jul	Saturday	2554	2210	344	2614	2240	374	6938	5846	1092	3218	2656	562	2806	2366	440	71	1.11	0.12	0.10
153	26-Jul	Sunday																			
154	27-Jul	Monday	2526	2178	348	2666	2274	392	6372	5342	1030	2894	2412	482	3278	2694	594	93	1.42	0.10	0.10
End of Batch 20			2699	2314	385	2628	2211	347	6484	3998	886	3046	2576	470	2940	2378	565	72	1.01	0.08	0.09
155	28-Jul	Tuesday																			
156	29-Jul	Wednesday																			
157	30-Jul	Thursday																			
158	31-Jul	Friday																			
159	01-Aug	Saturday																			
160	02-Aug	Sunday																			
161	03-Aug	Monday																			
162	04-Aug	Tuesday																			
163	05-Aug	Wednesday																			
164	06-Aug	Thursday																			
165	07-Aug	Friday																			
166	08-Aug	Saturday																			
167	09-Aug	Sunday																			
168	10-Aug	Monday																			
169	11-Aug	Tuesday	3494	2934	560	3902	3140	762	10288	8426	1643	3738	3084	654	3784	3072	712	70	1.32	0.04	0.12
170	12-Aug	Wednesday	3720	3170	530	3520	2958	562	8736	7312	1424	3802	3122	680	3706	2992	714	84	1.33	0.05	0.12
171	13-Aug	Thursday																			
172	14-Aug	Friday																			
173	15-Aug	Saturday																			
174	16-Aug	Sunday																			
175	17-Aug	Monday																			
End of Batch 22			3697	3052	595	3711	3049	662	9512	7899	1643	3770	3163	667	3746	3032	713	77	1.32	0.04	0.12
176	18-Aug	Tuesday	2796	2362	434	3064	2562	502	7862	6464	1398	3218	2674	544	3454	2748	706	87	1.31	0.08	0.07
177	19-Aug	Wednesday	2610	2212	398	2868	2403	468	7330	6188	1342	2868	2382	486	3042	2500	542	105	1.34	0.09	0.05
178	20-Aug	Thursday	2668	2192	416	2312	1982	330	7920	6614	1306	2458	2046	412	2724	2296	418	122	1.20	0.12	0.06
179	21-Aug	Friday																			
180	22-Aug	Saturday	2718	2426	292	3112	2656	456	8026	6770	1256	3142	2736	406	2988	2388	400	95	1.35	0.09	0.06
181	23-Aug	Sunday																			
182	24-Aug	Monday	2930	2462	446	2950	2500	450	7876	6536	1340	3134	2582	552	2876	2312	526	96	1.37	0.10	0.06
183	25-Aug	Tuesday	2592	2260	372	2872	2436	456	10086	8506	1580	3942	3232	710	4566	3770	796	66	1.15	0.08	0.06
184	26-Aug	Wednesday																			
185	27-Aug	Thursday																			
186	28-Aug	Friday																			
187	29-Aug	Saturday																			
188	30-Aug	Sunday																			
End of Batch 23			3718	3222	397	3863	3403	440	8217	6946	1370	3177	2639	518	3284	2789	575	95	1.29	0.09	0.08
189	31-Aug	Monday	1814	1570	244	2292	1872	420	5296	4282	1014	2320									

Daily Tests on Modified Dephosph BNRAS External Nitrification System

Dry No	1998			Amesbury Mass			Amesbury 1 Mass			Amesbury 2 Mass			Aerobic Mass			Waste Mass			DSVI	COD/VSS	TKN/VSS	TKN/COD
	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS	TSS	VSS	ISS				
235	05-Nov	Thursday	2670	1648	1022	1974	1344	230	3602	2990	672	2138	1738	380					108	1.51	0.08	0.05
236	06-Nov	Friday	936	412	324	934	800	134	4152	3748	404	2064	1666	398					82	1.57	0.08	0.03
237	07-Nov	Saturday	1028	896	132	1350	1132	218	2266	1886	380	1983	1503	480					101		0.09	
238	08-Nov	Sunday																				
239	09-Nov	Monday																				
240	10-Nov	Tuesday	900	826	74	1106	300	806	3816	3132	684	1838	912	926					87	2.25	0.15	0.06
241	11-Nov	Wednesday	2510	2488	22	1246	1062	184	5818	5490	328	1710	1432	278					99	1.31	0.09	0.06
242	12-Nov	Thursday	940	760	180	1292	992	300	3648	3052	396	1982	1648	334					101	1.39	0.10	0.07
243	13-Nov	Friday	1140	1020	120	1726	1332	394	3920	3244	676	3290	1652	638					96		0.08	
End of Batch 29			1446	1150	294	1318	995	324	3897	3363	534	2881	1510	491					96	1.66	0.10	0.06
244	14-Nov	Saturday																				
245	15-Nov	Sunday																				
246	16-Nov	Monday	1062	706	356	1446	1258	188	3044	2592	452	2102	1730	372					103	1.53	0.10	0.07
247	17-Nov	Tuesday	634	478	156	868	688	180	2000	1436	544	1092	786	306					201	3.57	0.18	0.05
248	18-Nov	Wednesday	1012	804	208	964	738	236	2890	2304	586	1230	878	352					179	2.63	0.15	0.08
249	19-Nov	Thursday	1264	1150	144	1900	1344	246	3872	3324	548	2010	1726	284					109	1.54	0.07	0.05
250	20-Nov	Friday	1792	1296	496	1376	1244	132	3322	2886	536	1918	1586	332					113	1.41	0.09	0.07
251	21-Nov	Saturday	1444	1154	290	1446	1134	312	3416	2818	598	1730	1392	338					127		0.10	
252	22-Nov	Sunday																				
253	23-Nov	Monday																				
254	24-Nov	Tuesday	1640	420	1220	1954	1630	304	5130	4300	830	2058	1710	328					108	1.57	0.08	0.03
255	25-Nov	Wednesday	1898	1620	278	1478	1318	160	9142	7586	1556	1790	1480	310								
256	26-Nov	Thursday																				
End of Batch 30			1347	953	394	1388	1168	220	4127	3421	706	1739	1411	328					133	2.03	0.11	0.06
257	27-Nov	Friday																				
258	28-Nov	Saturday																				
259	29-Nov	Sunday																				
260	30-Nov	Monday	1868	1526	342	2040	1662	378	3628	4620	1008	2308	1910	398								
261	01-Dec	Tuesday																				
262	02-Dec	Wednesday	1788	1540	248	2092	1750	342	5344	4292	1032	2574	1940	634					101	1.44	0.09	0.06
263	03-Dec	Thursday	1936	1666	290	2326	1632	694	5868	4958	910	2886	2306	580					83		0.07	
264	04-Dec	Friday																				
265	05-Dec	Saturday																				
266	06-Dec	Sunday																				
End of Batch 31			1872	1603	249	2209	1691	538	5606	4625	981	2730	2123	607					92	1.44	0.08	0.06
267	07-Dec	Monday																				
268	08-Dec	Tuesday																				
269	09-Dec	Wednesday																				
270	10-Dec	Thursday																				
271	11-Dec	Friday																				
272	12-Dec	Saturday																				
273	13-Dec	Sunday																				
274	14-Dec	Monday																				
275	15-Dec	Tuesday	1996	1628	368	2340	2070	470	3890	4628	1262	2086	1600	486					86	2.08	0.12	0.05
276	16-Dec	Wednesday	2020	1712	308	4394	5480	1114	6834	4622	2232	2304	2274	30	2822	2520	302		74	1.46	0.12	0.08
277	17-Dec	Thursday	2498	2038	440	3130	2530	380	7178	5718	1460	4026	3066	960					43	1.14	0.06	0.06
278	18-Dec	Friday	2198	1860	338	7314	2662	4632	10064	8338	1726	3238	2616	622					49		0.11	
279	19-Dec	Saturday																				
280	20-Dec	Sunday																				
281	21-Dec	Monday																				
282	22-Dec	Tuesday																				
283	23-Dec	Wednesday																				
284	24-Dec	Thursday																				
285	25-Dec	Friday																				
286	26-Dec	Saturday																				
287	27-Dec	Sunday																				
End of Batch 32			2178	1815	363	5145	2440	1784	7497	5827	1670	2913	2389	525	2822	2620	302		64	1.56	0.10	0.07
303	23-Dec	Wednesday																				
304	24-Dec	Thursday	2026	1674	362	2726	1886	840	6984	5486	1498	3168	2632	536					51	1.39	0.21	0.13
305	25-Dec	Friday	2564	2030	264	2620	2120	300	7190	5722	1468	3014	2396	118					64	1.50	0.06	0.03
306	26-Dec	Saturday	1934	1634	300	2022	1712	310	5194	4340	834	2028	1686	342					99		0.17	
307	27-Dec	Sunday																				
308	28-Dec	Monday	1798	1622	176	1708	1418	280	5980	4992	988	2518	578	1940					93	7.82	0.37	0.07
309	29-Dec	Tuesday	2030	1424	606	1706	1432	274	4610	3884	726	2246	1832	394					116	1.53	0.19	0.12
310	30-Dec	Wednesday	2012	1648	364	2114	1634	480	5882	4616	1266	2072	1590	482	3994	3342	652		145		0.20	
311	31-Dec	Thursday																				
312	01-Jan	Friday																				
313	02-Jan	Saturday																				
314	03-Jan	Sunday																				
315	04-Jan	Monday	1762	1440	322	2450	1868	582				2606	2064	542								0.14
End of Batch 33			2919	1947	218	3393	1897	298	3238	2640	618	1559	1163	396	3994	3342	652		86	3.16	0.22	0.09
316	05-Jan	Tuesday	2082	1670	412	2000	1934	546	7118	5590	1628	3078	2448	630	4218	3610	608		84		0.08	

Daily Tests on Modified Deponox BNRAS External Nitrification System

Day No	1998		Measured Nitrate Values mgNO <sub>3</sub> -N/l							Measured Nitrite Values mgNO <sub>2</sub> -N/l							
			Anoxic	Man_Ano	Pre_Ano	Aerobic	Final	IntSet	ExtN	Anoxic	Man_Ano	Pre_Ano	Aerobic	Final	IntSet	ExtN	
							Filtered EM	Filtered EM	Filtered EM					Filtered EM	Filtered EM	Filtered EM	
1	24-Feb	Tuesday	0.36	8.32	1.19	7.13	11.88	0.59	21.86								
2	25-Feb	Wednesday	0.20	7.43	0.93	6.30	6.30	0.27	23.05								
3	26-Feb	Thursday	0.23	9.98	0.83	9.86	7.72	0.14	22.81								
End of Batch 1			0.27	8.57	0.99	7.76	8.63	0.24	22.57								
4	27-Feb	Friday	0.21	11.29	0.49	13.33	12.48	0.15	22.57								
5	28-Feb	Saturday	0.21	13.13	1.06	19.96	20.44	0.15	23.05								
6	01-Mar	Sunday	0.36	10.69	1.51	24.83	25.19	0.24	25.43								
7	02-Mar	Monday	0.42	11.64	2.22	26.85	26.73	0.27	26.14								
8	03-Mar	Tuesday	0.77	10.36	2.11	13.78	17.13	0.26	20.09								
9	04-Mar	Wednesday	0.66	11.40	1.78	14.42	15.46	0.26	20.33								
10	05-Mar	Thursday	0.44	13.14	2.06	13.46	16.74	0.27	21.64								
11	06-Mar	Friday	0.26	10.36	1.98	13.07	16.36	0.30	24.21								
12	07-Mar	Saturday	0.32	12.11	2.32	18.16	15.97	0.26	24.47								
13	08-Mar	Sunday	0.44	9.72	1.37	13.07	14.42	0.21	23.70								
14	09-Mar	Monday	0.41	9.47	1.52	12.36	13.07	0.17	18.03								
15	10-Mar	Tuesday	0.40	10.88	2.00	14.04	16.36	0.17	21.89								
16	11-Mar	Wednesday	0.55	11.08	2.09	17.39	16.61	0.27	24.99								
17	12-Mar	Thursday	0.45	14.17	2.38	15.46	17.64	0.35	20.86								
End of Batch 2			0.42	11.42	1.83	17.01	17.61	0.24	22.67								
18	13-Mar	Friday	0.44	10.63	1.75	13.78	11.98	0.22	19.83								
19	14-Mar	Saturday	0.38	11.02	1.97	18.10	14.73	0.30	24.96								
20	15-Mar	Sunday	0.31	8.32	1.90	12.82	11.47	0.23	20.23								
21	16-Mar	Monday	0.34	7.98	1.46	10.79	11.35	0.22	23.41								
22	17-Mar	Tuesday															
End of Batch 3			0.37	9.49	1.77	13.87	12.38	0.25	24.86								
23	18-Mar	Wednesday															
24	19-Mar	Thursday															
25	20-Mar	Friday															
26	21-Mar	Saturday															
27	22-Mar	Sunday	0.22	0.56	0.09	2.36	2.14	0.49	16.19								
28	23-Mar	Monday	0.39	0.56	0.07	2.47	2.36	0.24	16.19								
29	24-Mar	Tuesday	0.19	0.28	0.04	2.47	2.23	0.28	18.21								
30	25-Mar	Wednesday	0.19	0.34	0.04	1.33	1.24	0.13	19.34								
End of Batch 4			0.25	0.44	0.06	2.16	2.00	0.29	17.48								
31	26-Mar	Thursday															
32	27-Mar	Friday	0.21	1.03	0.16	1.41	1.74	0.18	13.01								
33	28-Mar	Saturday	0.24	0.65	0.20	0.76	1.52	0.24	10.19								
34	29-Mar	Sunday	0.26	0.49	0.08	0.43	2.60	0.14	13.85								
35	30-Mar	Monday	0.23	0.49	0.10	0.65	2.06	0.16	13.88								
36	31-Mar	Tuesday															
37	01-Apr	Wednesday															
38	02-Apr	Thursday															
End of Batch 5			0.23	0.64	0.13	0.81	1.98	0.18	13.23								
39	03-Apr	Friday															
40	04-Apr	Saturday															
41	05-Apr	Sunday															
42	06-Apr	Monday	0.39	0.92	0.16	3.36	1.74	0.16	13.88								
43	07-Apr	Tuesday	0.15	0.38	0.04	0.87	1.93	0.16	11.06								
44	08-Apr	Wednesday	0.20	0.49	0.13	0.65	1.74	0.29	14.73								
45	09-Apr	Thursday															
End of Batch 6			0.25	0.68	0.18	1.43	1.81	0.21	13.23								
46	10-Apr	Friday	0.37	0.77	0.35	2.12	2.12	0.23	11.59								
47	11-Apr	Saturday	0.22	0.87	0.18	1.74	1.74	0.25	18.15								
48	12-Apr	Sunday															
49	13-Apr	Monday															
50	14-Apr	Tuesday															
51	15-Apr	Wednesday	0.19	1.26	0.30	1.74	1.16	0.23	29.16								
52	16-Apr	Thursday	0.25	0.77	0.29	1.64	1.45	0.24	31.28								
End of Batch 7			0.24	0.92	0.31	1.81	1.62	0.24	22.55								
53	17-Apr	Friday	0.22	1.09	0.24	5.94	5.74	0.29	19.79								
54	18-Apr	Saturday															
55	19-Apr	Sunday	0.25	0.94	0.36	6.33	5.74	0.31	19.39								
56	20-Apr	Monday	0.22	1.58	0.38	6.23	5.74	0.33	16.22								
57	21-Apr	Tuesday	0.29	1.34	0.38	5.94	6.23	0.33	16.62								
58	22-Apr	Wednesday	0.33	1.24	0.39	6.23	5.94	0.36	18.22								
59	23-Apr	Thursday	0.23	1.09	0.32	6.33	6.33	0.32	13.85								
60	24-Apr	Friday															
61	25-Apr	Saturday	0.28	0.99	0.28	6.63	5.94	0.37	18.99								
62	26-Apr	Sunday	0.23	0.74	0.38	1.48	2.57	0.42	22.93								
63	27-Apr	Monday															
64	28-Apr	Tuesday	0.26	0.69	0.28	1.98	2.57	0.36	19.39								
65	29-Apr	Wednesday															
End of Batch 8			0.25	1.08	0.33	5.27	5.20	0.34	18.18								
66	30-Apr	Thursday	0.28	0.08	0.25	1.42	3.60	0.50	23.93								
67	01-May	Friday	0.27	0.82	0.33	1.64	2.73	0.24	23.53								
68	02-May	Saturday	0.28	1.04	0.41	2.07	2.18	0.28	27.64								
End of Batch 9			0.28	0.65	0.33	1.71	2.83	0.34	25.51								
69	03-May	Sunday															
70	04-May	Monday															
71	05-May	Tuesday															
72	06-May	Wednesday															
73	07-May	Thursday															
74	08-May	Friday															
End of Batch 10																	
75	09-May	Saturday	0.31	0.09	0.27	1.55	3.93	0.55	28.32								
76	10-May	Sunday	0.30	0.89	0.36	1.78	2.97	0.26	23.70								
77	11-May	Monday	0.31	1.13	0.43	2.26	2.38	0.31	29.31								
78	12-May	Tuesday	0.40	1.44	0.30	12.14	6.19	0.38	20.70								
79	13-May	Wednesday	0.31	0.63	0.31	1.31	1.78	0.37	25.70								
80	14-May	Thursday															
81	15-May	Friday	1.56	0.93	0.26	1.78	1.07	0.37	21.42								
82	16-May	Saturday															
83	17-May	Sunday	0.73	0.48	0.31	1.67	1.07	0.32	43.08								
84	18-May	Monday	0.39	0.48	0.30	1.31	1.55	0.51	49.26								
85	19-May	Tuesday	0.43	0.42	0.30	1.67	1.31	0.29	36.64								
End of Batch 11			0.54	1.39	0.32	2.83	2.47	0.37	33.27								
86	20-May	Wednesday	0.24	0.47	0.24	0.79	0.47	0.35	25.50								
87	21-May	Thursday															
88	22-May	Friday	0.99	0.87	0.30	1.10	0.79	0.30	23.93								
89	23-May	Saturday	0.98	0.47	0.47	1.10	0.63	0.44	20.78								
90	24-May	Sunday	0.63	0.47	0.43	0.79	0.79	0.36	23.30								
91	25-May	Monday	0.71	0.53	0.38	0.63	0.31	0.41	25.19								
92	26-May	Tuesday															
93	27-May	Wednesday															
94	28-May	Thursday	0.80	0.79	0.24	0.31	0.47	0.30	24.56								
95	29-May	Friday	0.33	0.47	0.49	0.31	0.47	0.35	21.41								
96	30-May	Saturday	1.18	0.31	0.31	0.79	0.63	0.39	22.67								
97	31-May	Sunday	0.38	0.47	0.25	0.31	0.79	0.16	19.21								
98	01-Jun	Monday	0.55	1.34	0.17	2.05	2.05	0.24	20.46								
99	02-Jun	Tuesday															
100	03-Jun	Wednesday															
101	04-Jun	Thursday															
102	05-Jun	Friday															

Daily Tests on Modified Dephosphorization (ENTRAS External) Nitrate/Ammonia System																		
Day No	1998			Measured Nitrate Values mg/(O <sub>2</sub> -N)				Measured Nitrate Values mg/(O <sub>2</sub> -N)										
				Anaerobic	Man_Ano	Pre_Ano	Aerobic	Fnl Filtered Eff	InSet Filtered Eff	ExtNI Filtered Eff	Anaerobic	Man_Ano	Pre_Ano	Aerobic	Fnl Filtered Eff	InSet Filtered Eff	ExtNI Filtered Eff	
120	23-Jun	Tuesday		0.76	0.53	0.73	2.24	1.45	0.24	3.52								
121	24-Jun	Wednesday																
122	25-Jun	Thursday																
123	26-Jun	Friday		0.34	0.66	0.28	1.72	1.38	0.29	7.36								
124	27-Jun	Saturday																
125	28-Jun	Sunday																
End of Batch 6				0.55	0.39	0.30	1.78	1.51	0.26	6.44								
126	29-Jun	Monday		0.30	0.53	0.46	1.84	1.71	0.26	8.94								
127	30-Jun	Tuesday																
128	01-Jul	Wednesday		0.32	0.59	0.36	2.37	2.24	0.32	6.31								
129	02-Jul	Thursday		0.29	0.66	0.29	1.84	1.84	0.24	7.63								
130	03-Jul	Friday																
131	04-Jul	Saturday																
132	05-Jul	Sunday																
133	06-Jul	Monday		0.39	0.46	0.28	1.97	1.71	0.34	14.47								
134	07-Jul	Tuesday																
End of Batch 7				0.52	0.56	0.35	2.01	1.87	0.29	9.34								
135	08-Jul	Wednesday																
136	09-Jul	Thursday		0.41	1.05	0.79	1.97	1.97	0.17	7.36								
137	10-Jul	Friday		0.39	1.05	0.07	2.24	2.24	0.25	6.05								
138	11-Jul	Saturday		0.38	1.94	0.05	1.97	1.97	0.24	5.79								
139	12-Jul	Sunday																
140	13-Jul	Monday																
141	14-Jul	Tuesday																
142	15-Jul	Wednesday																
143	16-Jul	Thursday																
144	17-Jul	Friday																
145	18-Jul	Saturday																
146	19-Jul	Sunday																
147	20-Jul	Monday																
End of Batch 18				0.59	1.32	0.30	2.08	2.08	0.22	6.40								
148	21-Jul	Tuesday																
149	22-Jul	Wednesday																
End of Batch 19				0.80	1.78	0.21	6.31	5.13	0.29	22.62								
150	23-Jul	Thursday		0.50	2.63	0.21	4.21	4.87	0.24	17.36								
151	24-Jul	Friday		0.69	4.27	0.18	6.18	4.47	0.25	22.88								
152	25-Jul	Saturday																
153	26-Jul	Sunday																
154	27-Jul	Monday		0.57	1.97	0.21	4.60	3.55	0.25	23.67								
End of Batch 20				0.64	1.66	0.20	5.33	4.50	0.26	21.63								
155	28-Jul	Tuesday																
156	29-Jul	Wednesday																
157	30-Jul	Thursday																
158	31-Jul	Friday																
159	01-Aug	Saturday																
160	02-Aug	Sunday																
161	03-Aug	Monday																
162	04-Aug	Tuesday																
163	05-Aug	Wednesday																
164	06-Aug	Thursday																
165	07-Aug	Friday																
166	08-Aug	Saturday																
167	09-Aug	Sunday																
168	10-Aug	Monday																
169	11-Aug	Tuesday		0.43	3.31	1.61	7.83	8.65	0.86	12.15								
170	12-Aug	Wednesday		0.51	3.87	1.66	9.94	9.85	1.20	19.73								
171	13-Aug	Thursday																
172	14-Aug	Friday																
173	15-Aug	Saturday																
174	16-Aug	Sunday																
175	17-Aug	Monday																
End of Batch 22				0.48	3.39	1.63	8.88	9.25	1.03	15.74								
176	18-Aug	Tuesday		0.73	3.87	2.03	14.45	15.93	1.09	21.91								
177	19-Aug	Wednesday		0.78	3.13	1.43	15.28	16.29	0.66	14.36								
178	20-Aug	Thursday		0.89	2.58	1.43	12.61	16.11	0.74	10.68								
179	21-Aug	Friday																
180	22-Aug	Saturday		0.06	0.14	0.31	4.23	3.59	0.23	0.37								
181	23-Aug	Sunday		0.06	0.18	0.03	2.21	1.93	0.36	0.74								
182	24-Aug	Monday		0.07	0.18	0.03	1.37	1.57	0.12	0.55								
183	25-Aug	Tuesday		0.04	0.14	0.04	1.20	1.10	0.07	1.10								
184	26-Aug	Wednesday																
185	27-Aug	Thursday																
186	28-Aug	Friday																
187	29-Aug	Saturday																
188	30-Aug	Sunday																
End of Batch 23				0.51	1.46	0.75	7.36	8.06	0.46	7.10								
189	31-Aug	Monday		0.17	0.18	0.33	6.15	6.44	0.48	4.92								
190	01-Sep	Tuesday		0.41	0.36	0.18	4.34	5.43	0.41	4.63								
191	02-Sep	Wednesday		0.19	0.47	0.10	5.29	0.72	0.18	3.62								
192	03-Sep	Thursday		0.21	0.47	0.11	5.14	4.63	1.04	7.48								
193	04-Sep	Friday																
194	05-Sep	Saturday		0.33	0.33	0.09	5.65	6.30	0.62	3.73								
195	06-Sep	Sunday		0.17	0.43	0.13	5.21	5.86	0.73	3.33								
196	07-Sep	Monday																
End of Batch 24				0.25	0.37	0.16	5.30	4.50	0.38	3.89								
197	08-Sep	Tuesday																
198	09-Sep	Wednesday																
199	10-Sep	Thursday		0.81	1.48	0.14	8.98	10.64	0.32	2.61								
200	11-Sep	Friday		0.18	1.45	0.13	11.58	11.29	1.47	5.07								
201	12-Sep	Saturday		0.19	1.38	0.09	11.95	11.29	1.25	5.79								
202	13-Sep	Sunday		0.22	0.00	0.24	13.18	11.73	1.81	5.50								
203	14-Sep	Monday																
204	15-Sep	Tuesday																
205	16-Sep	Wednesday																
End of Batch 25				0.35	1.08	0.15	11.42	11.34	1.21	4.74								
206	17-Sep	Thursday																
207	18-Sep	Friday																
208	19-Sep	Saturday																
209	20-Sep	Sunday		0.77	9.54	3.42	7.78	8.30	1.05	17.39	0.17	0.35	0.45	0.36	0.36	0.15	3.22	
210	21-Sep	Monday		0.11	9.58	2.07	7.56	6.71	0.32	10.77	0.09	0.10	0.40	2.95	2.14	0.10	3.04	
211	22-Sep	Tuesday		0.54	16.10	1.00	6.34	6.66	1.10	12.98	0.29	0.38	0.49	3.04	3.13	0.74	2.68	
212	23-Sep	Wednesday		0.27	1.77	4.30	5.49	7.86	0.15	11.80	0.14	0.38	0.49	4.97	4.91	0.13	3.04	
213	24-Sep	Thursday																
214	25-Sep	Friday		0.35	3.74	0.99	4.55	3.88	0.25	3.01	0.20	0.07	0.40	4.89	3.13	0.29	4.47	
215	26-Sep	Saturday		0.38	6.76	0.51	6.45	4.46	0.91	4.78	0.13	0.24	2.99	2.41	0.89	0.70	4.29	
216	27-Sep	Sunday																
217	28-Sep	Monday																
218	29-Sep	Tuesday																
219	30-Sep	Wednesday																
End of Batch 26				0.23	7.85	2.05	6.36	6.31	0.63	10.45	0.17	0.34	0.87	3.43	2.43	0.33	3.46	
220	01-Oct	Thursday																
221	02-Oct	Friday			4.98	1.89	12.36	11.33	0.12	25.57	1.13	0.89	0.42			1.05	1.83	
222	03-Oct	Saturday			2.68	0.48	4.33	3.19	0.28	25.65	1.05	0.71	0.05			0.32	1.75	
223	04-Oct	Sunday			1.83	1.11	6.49	4.41	0.19	26.00	0.79	0.54	0.08			0.20	1.81	
224	05-Oct	Monday		0.31	3.19	1.10	7.73	5.16	0.15	29.30	0.00							

Daily Tests on Modified Deponox BNRAS External Nitrification System

Day No	1998		Measured Nitrate Values mgNO <sub>3</sub> -N/l						Measured Nitrate Values mgNO <sub>2</sub> -N/l							
			Anaerobic	Main_Ano	Pre_Ano	Aerobic	Final Filtered Eff	InSet Filtered Eff	ExNit Filtered Eff	Anaerobic	Main_Ano	Pre_Ano	Aerobic	Final Filtered Eff	InSet Filtered Eff	ExNit Filtered Eff
253	05-Nov	Thursday	0.49	0.42	0.34	7.94	10.13	0.47	6.53	0.24	0.02	0.10	0.43	0.43	0.29	0.27
256	06-Nov	Friday	0.20	6.93	0.07	9.64	10.23	0.44	17.32	0.08	0.59	0.08	0.59	0.44	0.36	0.70
257	07-Nov	Saturday	0.08	5.64		13.96	12.73	0.43	16.77	0.07	0.48	1.07	0.82	0.55	0.43	0.72
258	08-Nov	Sunday	0.16	6.13	1.01	16.69	13.32	0.30	12.16	0.09	0.51	1.07	0.98	0.65	0.31	0.43
259	09-Nov	Monday														
260	10-Nov	Tuesday	0.15	4.13	0.39	14.09	15.11	0.65	19.46	0.10	0.34	0.23	0.79	0.72	0.74	0.66
261	11-Nov	Wednesday	0.08	1.94		13.02	16.48	0.54	18.46	0.07	0.16	1.07	0.62	0.66	0.55	0.79
262	12-Nov	Thursday	0.25	5.09	0.61	12.05	12.73	0.82	20.07	0.10	0.42	0.33	0.53	0.21	0.90	0.57
263	13-Nov	Friday	0.51	5.05	0.02	11.65	16.93	0.56	12.90	1.01	0.46	0.61	0.86	1.00	0.80	0.57
End of Batch 29			0.24	4.42	0.41	12.38	13.49	0.53	15.46	0.22	0.37	0.57	0.71	0.59	0.55	0.59
264	14-Nov	Saturday														
265	15-Nov	Sunday														
266	16-Nov	Monday	0.79	0.18	0.04	1.99	2.84	0.33	24.23	0.71	0.02	0.09	0.10	0.05	0.18	0.46
267	17-Nov	Tuesday	1.13	0.08	0.10	3.11	2.25	0.26	21.43	0.99	0.02	0.10	0.18	0.04	0.14	0.45
268	18-Nov	Wednesday	0.70	0.19	0.07	2.37	3.38	0.29	31.00	0.62	0.01	0.05	0.12	0.10	0.16	0.46
269	19-Nov	Thursday	0.44	0.09	0.06	7.11	4.39	0.32	28.69	0.08	0.01	0.64	0.56	0.19	0.19	0.38
270	20-Nov	Friday	0.37	0.47	0.06	8.84	7.96	0.41	15.68	0.19	0.03	0.94	0.71	0.41	0.37	0.25
271	21-Nov	Saturday	1.23	0.38	0.18	3.11	6.47	0.37	20.35	0.47	0.02	0.06	0.17	0.20	0.20	0.36
272	22-Nov	Sunday														
273	23-Nov	Monday														
274	24-Nov	Tuesday														
275	25-Nov	Wednesday	0.05	0.19	0.08	2.96	1.58	0.10	26.37	0.07	0.01	0.05	0.09	0.03	0.03	0.46
276	26-Nov	Thursday	0.22	2.53	0.09	3.32	1.87	0.14	24.33	0.17	0.21	0.03	0.24	0.06	0.10	0.47
End of Batch 30			0.64	0.49	0.08	4.15	5.87	0.28	24.01	0.41	0.04	0.06	0.27	0.14	0.17	0.41
277	27-Nov	Friday														
278	28-Nov	Saturday														
279	29-Nov	Sunday														
280	30-Nov	Monday	0.08	0.29	0.11	7.50	7.26	0.16	33.41	0.12	0.01	0.12	0.01	0.05	0.17	0.74
281	01-Dec	Tuesday														
282	02-Dec	Wednesday	0.05	1.39	0.10	6.90	6.43	0.24	35.92	0.04	0.13	0.03	0.42	0.28	0.12	0.66
283	03-Dec	Thursday	0.10	0.64	0.03	9.82	5.98	0.13	31.81	0.01	0.07	0.01	0.33	0.22	0.15	0.71
284	04-Dec	Friday														
285	05-Dec	Saturday														
286	06-Dec	Sunday														
End of Batch 31			0.08	0.78	0.09	8.07	6.56	0.18	33.71	0.06	0.07	0.05	0.26	0.18	0.18	0.70
287	07-Dec	Monday														
288	08-Dec	Tuesday														
289	09-Dec	Wednesday														
290	10-Dec	Thursday														
291	11-Dec	Friday														
292	12-Dec	Saturday														
293	13-Dec	Sunday														
294	14-Dec	Monday														
295	15-Dec	Tuesday	0.14	2.21	0.80	1.52	0.97	0.03	23.29	0.03	0.01	0.03	0.05	0.04		0.40
296	16-Dec	Wednesday	0.12	0.63	0.06	0.36	0.34	0.06	22.53		0.02		0.01	0.03		0.42
297	17-Dec	Thursday	0.14	0.64	0.06	1.06	0.82	0.08	20.36	0.01	0.01	0.01	0.05	0.02		0.37
298	18-Dec	Friday	0.09	0.36	0.07	0.80	0.43	0.01	16.36	0.01	0.01	0.01	0.03	0.01	0.02	0.30
299	19-Dec	Saturday														
300	20-Dec	Sunday														
301	21-Dec	Monday														
302	22-Dec	Tuesday														
End of Batch 32			0.12	0.96	0.24	0.94	0.84	0.05	29.64	0.02	0.01	0.02	0.04	0.03	0.02	0.37
303	23-Dec	Wednesday														
304	24-Dec	Thursday	0.12	1.23	0.08	7.17	5.52	0.23	8.33	0.03	0.07	0.03	0.51	0.31	0.37	0.18
305	25-Dec	Friday	0.37	1.51	0.08	5.53	7.91	1.04	26.89	1.06	0.06	0.09	0.35	0.42		0.31
306	26-Dec	Saturday	0.20	1.75	0.07	7.22	9.06	0.53	30.54	0.20	0.10	0.04	0.46	0.47		0.56
307	27-Dec	Sunday														
308	28-Dec	Monday	0.56	1.47	0.13	6.28	7.90	0.49	31.25	1.01	0.11	0.18	0.39	0.42		0.59
309	29-Dec	Tuesday	0.46	1.30	0.10	4.03	4.61	0.36	30.52	0.83	0.09	0.12	0.23	0.20		0.58
310	30-Dec	Wednesday	0.46	2.57	0.08	6.79	4.91	0.23	31.59	0.91	0.21	0.09	0.34	0.18		0.62
311	31-Dec	Thursday														
312	01-Jan	Friday														
313	02-Jan	Saturday														
314	03-Jan	Sunday														
315	04-Jan	Monday	1.43	0.56	0.20	7.50	11.08	0.48	23.95							
End of Batch 33			0.55	1.48	0.11	6.36	7.29	0.50	26.15	0.66	0.11	0.09	0.38	0.34	0.37	0.51
316	05-Jan	Tuesday	0.35	8.29	0.16	14.89	8.73	0.12	35.37							
317	06-Jan	Wednesday														
318	07-Jan	Thursday														
319	08-Jan	Friday														
320	09-Jan	Saturday														
321	10-Jan	Sunday														
322	11-Jan	Monday														
323	12-Jan	Tuesday														
324	13-Jan	Wednesday	0.18	12.98	1.84	21.27	20.82	1.70	28.88							
325	14-Jan	Thursday	1.67	12.98	2.44	21.49	20.26	0.20	23.30							
326	15-Jan	Friday														
327	16-Jan	Saturday														
328	17-Jan	Sunday														
329	18-Jan	Monday														
330	19-Jan	Tuesday														
331	20-Jan	Wednesday														
332	21-Jan	Thursday	0.31	1.68	0.20	10.07	12.98	0.83	18.80							
333	22-Jan	Friday														
334	23-Jan	Saturday														
335	24-Jan	Sunday														
336	25-Jan	Monday														
End of Batch 34			0.72	9.22	1.49	17.61	18.02	0.91	24.33							
337	26-Jan	Tuesday	0.20	3.13	0.09	13.43	12.54	0.81	21.27							
338	27-Jan	Wednesday	0.81	0.95	0.15	12.65	13.32	0.72	18.58							
339	28-Jan	Thursday	0.40	1.23	0.22	13.88	8.95	0.43	12.76							
340	29-Jan	Friday	0.17	1.01	0.10	14.44	10.07	0.43	8.73							
341	30-Jan	Saturday														
342	31-Jan	Sunday														
343	01-Feb	Monday														
344	02-Feb	Tuesday														
End of Batch 35			0.39	1.58	0.14	15.60	11.22	0.59	15.33							
345	03-Feb	Wednesday														
346	04-Feb	Thursday														
347	05-Feb	Friday														
348	06-Feb	Saturday														
349	07-Feb	Sunday	0.25	0.17	0.13	4.01	5.66	0.26	24.91	0.11	0.09	0.03	0.12	0.05	0.03	0.28
350	08-Feb	Monday														
351	09-Feb	Tuesday	0.07	0.18	0.05	3.38	2.54	0.10	24.82	0.02	0.34	0.07	0.12	0.04	0.04	0.19
352	10-Feb	Wednesday	0.03	0.26	0.06	2.89	3.09	0.10	24.66	0.11	0.41	0.04	0.14	0.04	0.03	0.17
353	11-Feb	Thursday	0.16	0.81	0.19	3.86	2.54	0.13	25.62	0.02	0.37	0.08	0.10	0.04	0.03	0.12
354	12-Feb	Friday														
355	13-Feb	Saturday	0.08	0.18	0.08	3.43	3.28	0.09	27.32	0.02	0.13	0.15	0.06	0.03		

Daily Tests on Modified Deponox BNRAS External Nitrification System

Day No	1998	Influent V/d	Recycle V/d	Nitrate Dosage mg/100V/d	Anaerobic Outflow	Flow into Ae & Anox	Flow to Ext Number (V/d)	Bypass to Mean Anox (mg/100V)	Direct Recy to Anox (mg/100V)	NO3 denit Mean Anox (mg/100V)	NO3 denit Pre-Anox (mg/100V)	NO3 denit Anaerobic (mg/100V)	NO3 denit Settle (mg/100V)	Total Denit (mg/100V)	N in W (mg/100V)	N in Eff (mg/100V)	TKN Sec (mg/100V)	Total TKN Leaving (mg/100V)	Inf TKN (mg/100V)	MB %	
1	24-Feb	Tuesday	20.00	20.00	500.00	40.00	30.00	10.00		829.11	213.86	9.50		1037.47	371.86	377.62		1701.95	2045.60	83.20	
2	25-Feb	Wednesday	20.00	20.00	500.00	40.00	30.00	10.00		897.19	106.93	10.93		1015.05	264.59	223.54		89.52	1598.70	1720.20	92.43
3	26-Feb	Thursday	20.00	20.00	500.00	40.00	30.00	10.00		786.37	137.82	6.65	85.54	1016.59	299.72	179.65	138.92	1034.80	1759.00	97.89	
End of Batch 1																					
4	27-Feb	Friday	20.00	20.00	500.00	40.00	30.00	10.00		837.62	152.87	9.83		999.52	278.91	262.27		1540.78	1844.93	83.51	
5	28-Feb	Saturday	20.00	20.00	500.00	40.00	30.00	10.00		727.29	239.76	1.19	114.00	1082.20	258.83	341.90	171.61	1854.66	1841.20	100.73	
6	01-Mar	Sunday	20.00	20.00	500.00	40.00	30.00	10.00		667.88	387.56	12.59		1068.04	297.32	495.51	94.35	1955.42	1816.00	107.68	
7	02-Mar	Monday	20.00	20.00	500.00	40.00	30.00	10.00		837.42	473.58	15.92		1326.93	324.06	559.76		2210.75	1788.00	123.64	
8	03-Mar	Tuesday	20.00	20.00	500.00	40.00	30.00	10.00		821.15	490.22	27.80	4.73	1343.92	323.30	583.05		2234.27	1760.00	128.08	
9	04-Mar	Wednesday	20.00	20.00	500.00	40.00	30.00	10.00		682.99	300.24	11.33		994.56	237.56	390.19	108.48	1730.79	1823.80	94.43	
10	05-Mar	Thursday	20.00	20.00	500.00	40.00	30.00	10.00		457.13	273.55	9.27		739.95	269.65	370.70	165.83	1746.16	1754.40	99.33	
11	06-Mar	Friday	20.00	20.00	500.00	40.00	30.00	10.00		626.31	293.65	23.70		943.69	389.31	376.86	115.00	1824.86	1874.80	97.34	
12	07-Mar	Saturday	20.00	20.00	500.00	40.00	30.00	10.00		806.91	287.46	20.36		1123.74	380.14	327.13	263.20	2094.21	1872.00	111.87	
13	08-Mar	Sunday	20.00	20.00	500.00	40.00	30.00	10.00		752.43	273.94	33.49	87.58	1146.34	397.52	333.01	155.61	2052.67	1883.20	109.00	
14	09-Mar	Monday	20.00	20.00	500.00	40.00	30.00	10.00		824.04	257.07	13.91	25.76	1120.78	396.94	310.89	236.05	2064.66	1905.60	106.33	
15	10-Mar	Tuesday	20.00	20.00	500.00	40.00	30.00	10.00		663.93	270.98	13.91		948.84	373.53	343.37	434.30	2104.04	1911.20	110.69	
16	11-Mar	Wednesday	20.00	20.00	500.00	40.00	30.00	10.00		723.20	287.21	23.96		1034.36	365.48	309.13	234.84	2000.17	1880.40	106.37	
17	12-Mar	Thursday	20.00	20.00	500.00	40.00	30.00	10.00		809.23	290.36	19.58	30.91	1150.27	377.77	367.28	104.84	2000.17	1880.40	106.37	
End of Batch 2																					
18	13-Mar	Friday	20.00	20.00	500.00	40.00	30.00	10.00		725.99	316.17	19.25		1041.32	366.92	397.48	161.37	1981.68	1848.80	107.20	
19	14-Mar	Saturday	20.00	20.00	500.00	40.00	30.00	10.00		672.20	304.51	17.52	72.12	996.36	273.56	282.95	274.63	1551.32	1808.80	81.30	
20	15-Mar	Sunday	20.00	20.00	500.00	40.00	30.00	10.00		811.07	255.20	24.06		1349.81	454.12	312.43	94.03	3108.83	3277.60	94.33	
21	16-Mar	Monday	20.00	20.00	500.00	40.00	30.00	10.00		1046.59	194.34	25.41	33.96	1317.30	330.83	302.14		1950.37	1799.20	108.40	
22	17-Mar	Tuesday	20.00	20.00	500.00	40.00	30.00	10.00		959.17	187.74	15.74		1158.79	368.78	320.89	69.83	1918.29	1844.00	104.03	
End of Batch 3																					
23	18-Mar	Wednesday								868.76	212.23	20.68	59.63	1161.30	407.63	312.03	111.20	1992.16	1878.20	104.06	
24	19-Mar	Thursday																			
25	20-Mar	Friday																			
26	21-Mar	Saturday																			
27	22-Mar	Sunday																			
28	23-Mar	Monday	40.00	20.00	550.00	60.00	50.00	10.00		1428.07	45.87		6.79	1480.86	608.18	954.03	168.37	3211.27	3192.40	100.59	
29	24-Mar	Tuesday	40.00	20.00	500.00	60.00	30.00	10.00		1386.56	44.07		13.49	1454.12	312.43	814.03	314.44	3108.83	3277.60	94.33	
30	25-Mar	Wednesday	40.00	20.00	500.00	60.00	30.00	10.00		1447.93	23.83		6.75	1478.51	636.87	721.47	82.92	2919.77	3143.20	92.89	
End of Batch 4																					
31	26-Mar	Thursday	40.00	20.00	500.00	60.00	50.00	10.00		1123.52	36.93		18.12	1449.59	346.91	833.02	213.59	2837.11	3284.00	88.54	
32	27-Mar	Friday	40.00	20.00	500.00	60.00	30.00	10.00		1090.74	31.45			1122.19	483.02	444.61	261.50	2311.33	2930.40	78.87	
33	28-Mar	Saturday	40.00	20.00	500.00	60.00	30.00	10.00		973.07	26.46			999.53	446.40	396.73	543.20	2387.87	2975.20	80.26	
34	29-Mar	Sunday																			
35	30-Mar	Monday	40.00	20.00	500.00	60.00	50.00	10.00		1166.44	39.26			1205.70	339.38	412.82	357.04	2314.94	2700.80	83.71	
36	31-Mar	Tuesday																			
37	01-Apr	Wednesday																			
38	02-Apr	Thursday	40.00	20.00	500.00	60.00	50.00	10.00		1123.52	36.93			1188.45	477.57	424.97	185.27	2448.27	2856.20	85.72	
End of Batch 5																					
39	03-Apr	Friday																			
40	04-Apr	Saturday																			
41	05-Apr	Sunday																			
42	06-Apr	Monday	40.00	20.00	500.00	60.00	50.00	10.00		1140.41	31.45		97.61	1269.47	739.91	826.61	294.04	3140.02	3638.40	83.83	
43	07-Apr	Tuesday	40.00	20.00	500.00	60.00	50.00	10.00		1031.96	38.18			1070.14	773.67	862.09	274.03	2981.92	3759.20	79.32	
44	08-Apr	Wednesday	40.00	20.00	500.00	60.00	50.00	10.00		1211.12	32.10			1243.23	820.63	831.01	572.16	3467.03	3781.60	91.68	
45	09-Apr	Thursday	40.00	20.00	500.00	60.00	50.00	10.00		500.00				500.00	778.73	750.40	1302.00	3331.13	3748.00	88.88	
End of Batch 6																					
46	10-Apr	Friday	40.00	20.00	500.00	60.00	45.00	15.00		978.54	37.46			1016.50	729.81	1714.57	1031.42	4511.80	3944.00	114.40	
47	11-Apr	Saturday	40.00	20.00	500.00	60.00	45.00	15.00		1268.50	31.09			1299.59	758.60	1687.92	945.82	4691.93	4442.40	105.62	
48	12-Apr	Sunday																			
49	13-Apr	Monday																			
50	14-Apr	Tuesday																			
51	15-Apr	Wednesday	40.00	20.00	500.00	60.00	45.00	15.00		1740.38	13.13		34.76	1788.27	746.33	2011.93	109.41	4653.97	4032.60	111.86	
52	16-Apr	Thursday	40.00	20.00	500.00	60.00	45.00	15.00		1863.08	23.17		11.59	1899.84	690.10	2306.33	1233.30	6129.58	6162.00	151.96	
End of Batch 7																					
53	17-Apr	Friday	40.00	20.00	500.00	60.00	45.00	15.00		1463.13	26.22		11.59	1500.93	733.74	1865.59	834.99	4935.15	4145.69	119.05	
54	18-Apr	Saturday	40.00	20.00	500.00	60.00	45.00	15.00		1451.24	973.64			1451.24	973.64	2228.71	1037.76	5691.55	4240.80	134.21	
55	19-Apr	Sunday	40.00	20.00	500.00	60.00	45.00	15.00		1320.76	107.63		35.61	1466.00	703.33	1259.91	86.26	3515.50	3231.60	109.12	
56	20-Apr	Monday	40.00	20.00	500.00	60.00	45.00	15.00		1140.02	107.24		29.68	1276.93	663.08	1181.51	84.70	3206.23	3130.80	102.74	
57	21-Apr	Tuesday	40.00	20.00	500.00	60.00	45.00	15.00		1181.56	117.13			1208.70	690.24	1086.50	190.29	3265.82	3176.80	102.80	
58	22-Apr	Wednesday	40.00	20.00	500.00	60.00	45.00	15.00		1181.24	111.00			1293.96							

Delw. Tare on Modified Deposition RWRS Journal Nitrogen System

Day No	1998	2nd Int Id	Recycle Id	House Dose mg/10Yd	Aerobic Outflow	Flow into As & Anox	Flow to Exit Nbr/10Yd	Bypass to Main Anox	Nitrate recy As to Anox (mg/10Yd)	NO3 denit Main Anox (mg/10Yd)	NO3 denit Pre-Anox (mg/10Yd)	NO3 denit Aerobic (mg/10Yd)	NO3 denit Settle (mg/10Yd)	Tot Denit (mg/10Yd)	N in W (mg/10Yd)	N in Eff (mg/10Yd)	TKN Sic (mg/10Yd)	Total TKN Leaving (mg/10Yd)	Eff TKN mg/10Yd	10B %	
120	23-Jun	Tuesday																			
121	24-Jun	Wednesday	40.00	20.00	250.00	60.00				495.97	22.34		47.34	566.67	649.59	3028.66	589.67	4834.59	4472.40	108.10	
122	25-Jun	Thursday								668.19	24.99			701.07	711.60	2005.98	1344.03	4762.58	3761.20	126.63	
123	26-Jun	Friday	40.00	20.00	250.00	60.00				533.27	37.61		7.89	578.77	894.42	1834.62	302.16	3401.97	4382.00	84.12	
124	27-Jun	Saturday								594.29	31.04			625.32	679.60	1809.64	225.46	3540.03	4506.00	78.56	
125	28-Jun	Sunday																			
End of Batch 6			40.00	20.00	250.00	60.00	90.00	10.00		339.32	34.30			15.78	579.29	746.37	1844.00	364.06	3434.71	3947.33	116.54
126	29-Jun	Monday																			
127	30-Jun	Tuesday	40.00	20.00	250.00	60.00				668.19	24.99			701.07	711.60	2005.98	1344.03	4762.58	3761.20	126.63	
128	01-Jul	Wednesday	40.00	20.00	250.00	60.00				533.27	37.61		7.89	578.77	894.42	1834.62	302.16	3401.97	4382.00	84.12	
129	02-Jul	Thursday	40.00	20.00	250.00	60.00				594.29	31.04			625.32	679.60	1809.64	225.46	3540.03	4506.00	78.56	
130	03-Jul	Friday																			
131	04-Jul	Saturday																			
132	05-Jul	Sunday																			
133	06-Jul	Monday	40.00	20.00	250.00	60.00				948.86	28.67		15.78	993.31	372.43	1065.18		2430.93	2243.60	108.35	
134	07-Jul	Tuesday																			
End of Batch 7			40.00	20.00	250.00	60.00	90.00	10.00		696.21	30.38			7.89	724.69	713.73	1338.48	233.61	3000.30	3008.56	100.73
135	08-Jul	Wednesday																			
136	09-Jul	Thursday	40.00	20.00	250.00	60.00				536.81	23.67			580.48	326.93	1596.50		2503.91	3039.80	82.40	
137	10-Jul	Friday	40.00	20.00	250.00	60.00				491.84	43.40			535.24	653.09	1467.02	256.03	2911.39	3386.00	85.98	
138	11-Jul	Saturday	40.00	20.00	250.00	60.00				431.22	38.60			469.62	4.93	1434.10	275.52	2194.17	3453.20	63.23	
139	12-Jul	Sunday																			
140	13-Jul	Monday																			
141	14-Jul	Tuesday																			
142	15-Jul	Wednesday																			
143	16-Jul	Thursday	40.00	20.00	250.00	60.00				536.81	23.67			580.48	326.93	1596.50		2503.91	3039.80	82.40	
144	17-Jul	Friday	40.00	20.00	250.00	60.00				491.84	43.40			535.24	653.09	1467.02	256.03	2911.39	3386.00	85.98	
145	18-Jul	Saturday	40.00	20.00	250.00	60.00				431.22	38.60			469.62	4.93	1434.10	275.52	2194.17	3453.20	63.23	
146	19-Jul	Sunday																			
147	20-Jul	Monday																			
End of Batch 8			40.00	20.00	250.00	60.00	90.00	10.00		695.29	35.16			0.00	528.44	518.29	1499.31	157.62	2703.57	3292.67	82.11
148	21-Jul	Tuesday																			
149	22-Jul	Wednesday																			
End of Batch 9																					
150	23-Jul	Thursday	30.00	15.00	500.00	45.00				940.21	69.83			1010.04	665.02	1313.57	34.49	3023.12	2600.00	116.27	
151	24-Jul	Friday	30.00	15.00	500.00	45.00				1043.15	64.31			1184.39	841.45	1310.14		3335.98	3177.60	106.32	
152	25-Jul	Saturday																			
153	26-Jul	Sunday																			
154	27-Jul	Monday	30.00	15.00	500.00	45.00				1171.96	50.10			1269.41	638.01	1198.52		3105.94	2707.60	104.39	
End of Batch 10			30.00	15.00	500.00	45.00	33.00	13.00		1095.75	64.50			36.99	1177.24	573.37	1296.32		3014.90	3002.40	103.88
155	28-Jul	Tuesday																			
156	29-Jul	Wednesday																			
157	30-Jul	Thursday																			
158	31-Jul	Friday																			
159	01-Aug	Saturday																			
160	02-Aug	Sunday																			
161	03-Aug	Monday																			
162	04-Aug	Tuesday																			
163	05-Aug	Wednesday																			
164	06-Aug	Thursday								750.85	105.64	4.70		861.18	310.06	1288.61		2459.85	2936.00	89.78	
165	07-Aug	Friday	30.00	15.00	500.00	45.00				1014.61	122.90	0.83	4.14	1142.48	302.68	1232.11	178.65	3855.93	3120.90	91.51	
166	08-Aug	Saturday																			
167	09-Aug	Sunday																			
168	10-Aug	Monday																			
169	11-Aug	Tuesday	30.00	15.00	500.00	45.00															
170	12-Aug	Wednesday	30.00	15.00	500.00	45.00															
171	13-Aug	Thursday																			
172	14-Aug	Friday																			
173	15-Aug	Saturday																			
174	16-Aug	Sunday																			
175	17-Aug	Monday																			
End of Batch 11			30.00	15.00	500.00	45.00	35.00	10.00		899.67	114.27	2.76		1016.70	275.22	1260.36	75.40	2627.59	3028.40	86.77	
176	18-Aug	Tuesday	30.00	15.00	500.00	45.00				1103.17	207.13			1310.35	444.71	773.22		2538.24	2280.90	110.65	
177	19-Aug	Wednesday	30.00	15.00	500.00	45.00				868.42	223.01	4.42		1095.85	472.96	1033.03		2271.85	2404.80	94.39	
178	20-Aug	Thursday	30.00	15.00	500.00	45.00				765.13	220.25			985.38	515.22	970.51		2471.12	2222.00	111.21	
179	21-Aug	Friday	30.00	15.00	500.00	45.00															
180	22-Aug	Saturday	30.00	15.00	500.00	45.00				508.98	49.16	3.04	29.00	590.17	498.67	594.91	245.07	1928.62	2222.00	86.80	
181	23-Aug	Sunday																			
182	24-Aug	Monday	30.00	15.00	500.00	45.00				512.34	23.06			535.30	509.93	410.25	215.16	1670.64	2440.40	68.46	
183	25-Aug	Tuesday	30.00	15.00	500.00	45.00				533.19	16.02		4.14	553.35	534.39	574.94	47.21	1709.90	2432.00	70.31	
184	26-Aug	Wednesday																			
185	27-Aug	Thursday																			
186	28-Aug	Friday																			
187	29-Aug	Saturday																			



Daily Tests on Modified Deponox BNRAS External Nitrification System														
Day No	1998		Influent COD mgCOD/d	Effluent COD mgCOD/d	Waste COD mgCOD/d	COD used In Ex/NR mgCOD/d	Nitrifying Check ! mgO/d	OUR <sup>24</sup> *V Measured mgO/d	MOn 4.57*N <sub>in</sub> mgO/d	MOc OUR-MO mgO/d	Dens On MO <sub>2</sub> mgO/d	MOR MO <sub>2</sub> +MO <sub>4</sub> mgO/d	COD Involving mgCOD/d	MR COD %
	Year	Day												
1	24-Feb	Tuesday	19089	1123	3751	3376	0	3240		3240	3010	6250	14503	76
2	25-Feb	Wednesday	16505	1250	4210	3376	0	1938		1938	2903	4861	13698	83
3	26-Feb	Thursday	13005	1260	3698	833	0	1872		1872	2907	4779	10591	81
End of Batch 1			16200	1212	3886	2535	0	2376	0	2376	2859	5235	12868	79
4	27-Feb	Friday	12192	328	3170	1707	162	2016	738	1278	3093	4373	9778	80
5	28-Feb	Saturday	12842	975	5039	2560	273	1512	1249	263	3053	3318	11893	93
6	01-Mar	Sunday	12842	1707	4389	1463	566	2304	2585		3793	3514	11074	86
7	02-Mar	Monday	12924	1097	4145	2073	608	2232	278		3644	3506	10611	82
8	03-Mar	Tuesday	10892	325	3251	1581	129	1426	389	837	2844	3681	8943	81
9	04-Mar	Wednesday	10810	732	2723	1341	121	1764	553	1211	2688	3899	8695	80
10	05-Mar	Thursday	11542	650	8453	1707	93	1224	424	800	2699	3499	14309	124
11	06-Mar	Friday	11948	833	5080	732	180	1541	824	717	3214	3931	10596	89
12	07-Mar	Saturday	11217	163	4796	1219	242	1800	1107	693	3279	3973	10130	90
13	08-Mar	Sunday	11867	732	5364	1219	214	1922	977	943	3203	4151	11466	97
14	09-Mar	Monday	12335	1097	3771	2682	116	1807	530	1277	2714	3991	13542	110
15	10-Mar	Tuesday	12408	993	5333	1241	126	1670	377	1094	2958	4052	11621	94
16	11-Mar	Wednesday	12409	910	4715	2109	232	1548	394	3290	3684	4418	11418	92
17	12-Mar	Thursday	15055	579	5460	1737	32	1591	32	1346	2467	3923	11699	78
End of Batch 2			12236	810	4835	1670	224	1656	1023	433	3035	3668	10983	90
18	13-Mar	Friday	14228	993	7238	1730	126	1512	577	933	2764	3699	14639	103
19	14-Mar	Saturday	13233	163	7197	1613	283	1728	1295	433	3504	3937	12913	98
20	15-Mar	Sunday	15386	163	7362	2482	180	1879	822	1037	3767	4825	14834	96
21	16-Mar	Monday	13566	331	6824	3226	112	2182	514	1668	3314	4982	15363	113
22	17-Mar	Tuesday												
End of Batch 3			14104	414	7155	2513	175	1800	802	998	3321	4319	14401	102
23	18-Mar	Wednesday												
24	19-Mar	Thursday												
25	20-Mar	Friday												
26	21-Mar	Saturday												
27	22-Mar	Sunday												
28	23-Mar	Monday	26327	2780	9096	6132	115	1879	524	1353	4235	5590	23598	90
29	24-Mar	Tuesday	26817	4252	8432	2248	132	3240	601	2639	4159	6798	21729	81
30	25-Mar	Wednesday	27798	5069	11395	7154	61	3089	277	2811	4229	7040	30658	110
End of Batch 4			26981	4033	9641	5178	104	2736	474	2262	4146	6408	25260	94
31	26-Mar	Thursday												
32	27-Mar	Friday	30415	2044	5774	5928	23	2203	104	2099	3209	5309	19034	63
33	28-Mar	Saturday	30088	3107	6541	4292	7	2491	30	2461	2839	5320	19260	64
34	29-Mar	Sunday												
35	30-Mar	Monday	27144	1799	6847	1633	10	2390	45	2346	3448	5794	16075	59
36	31-Mar	Tuesday												
37	01-Apr	Wednesday												
38	02-Apr	Thursday												
End of Batch 5			28861	2105	6298	4241	9	2342	41	2321	3319	5440	18284	63
39	03-Apr	Friday												
40	04-Apr	Saturday												
41	05-Apr	Sunday												
42	06-Apr	Monday	25312	2895	6928	4550	146	2376	669	1707	3631	5338	19710	78
43	07-Apr	Tuesday	24485	2151	10805	4136	29	2837	134	2703	3061	5764	22836	93
44	08-Apr	Wednesday	24816	2647	8892	3309	10	2326	45	2281	3556	5837	20685	83
45	09-Apr	Thursday	29423	4389	12294	6096		2513		2513	3450	3943	26722	91
End of Batch 6			24609	3821	9730	4523		2513		2513	3323	5833	23108	89
46	10-Apr	Friday	24685	2113	5941	4206	81	2232	371	1861	2906	4767	17081	63
47	11-Apr	Saturday	27310	2601	6096	4023		2808		2808	3717	6525	19245	70
48	12-Apr	Sunday												
49	13-Apr	Monday												
50	14-Apr	Tuesday												
51	15-Apr	Wednesday	28611	3251	4674	4938	29	4522	132	4389	5114	9504	22366	78
52	16-Apr	Thursday	28448	4470	6350	4938	52	3240	238	3002	5434	8435	24193	83
End of Batch 7			27838	3189	5779	4526	54	3298	245	4293	7248	20662	74	
53	17-Apr	Friday	30724	4877	11684	4938	291	2376	1329	1047	4151	5197	26696	87
54	18-Apr	Saturday												
55	19-Apr	Sunday	28731	2147	10939	3043	323	3032	1478	574	4187	4761	19890	69
56	20-Apr	Monday	28236	3043	10372	3016	279	2563	1275	1288	3652	4840	24290	86
57	21-Apr	Tuesday	26419	2559	9701	1486	276	1721	1261	459	3714	4174	17920	68
58	22-Apr	Wednesday	26089	2724	8927	3344	306	2045	1397	648	3706	4354	19349	74
59	23-Apr	Thursday	25263	2477	8978	2415	326	2041	1492	549	3417	3967	17837	71
60	24-Apr	Friday												
61	25-Apr	Saturday	25759	3468	11249	3786	338	2700	1546	1134	4163	5317	22820	89
62	26-Apr	Sunday	27080	3053	13158	3344	45	2714	203	2311	4400	6911	26467	98
63	27-Apr	Monday												
64	28-Apr	Tuesday	23117	2312	11868	743	77	1994	353	1642	3953	5595	20518	89
65	29-Apr	Wednesday												
End of Batch 8			26824	3965	10764	2902	251	2275	1148	1127	3889	5016	21746	81
66	30-Apr	Thursday	29376	1632	10608	4223	80	4968	366	4134	4969	9103	25565	97
67	01-May	Friday	28397	11118	3303	3303	49	4500	224	4276	4468	8746	27058	95
68	02-May	Saturday	27091	2122	10098	2020	62	3197	284	2913	4846	7758	21998	81
End of Batch 9			28288	2587	10608	3182	64	4066	291	3774	4761	8536	24882	88
69	03-May	Sunday												
70	04-May	Monday												
71	05-May	Tuesday												
72	06-May	Wednesday												
73	07-May	Thursday												
74	08-May	Friday												
End of Batch 10														
75	09-May	Saturday	29376	1632	10608	4223	87	4500	400	4100	5292	9392	25855	88
76	10-May	Sunday	28397	3917	11118	3303	54	4500	245	4255	4746	9001	27341	96
77	11-May	Monday	27091	2122	10098	2020	68	3197	310	2887	5138	8044	22284	82
78	12-May	Tuesday	28071	2955	4463	4617	282	1434	1289	166	4193	4358	16393	58
79	13-May	Wednesday	28564	3201	7932	739	39	1931	179	1772	4726	6498	18389	64
80	14-May	Thursday												
81	15-May	Friday	22326	2791	7233	3899	50	1980	228	1752	4509	6260	20183	90
82	16-May	Saturday												
83	17-May	Sunday	26594	3201	7131	6566	71	2368	326	1942	7663	9605	26503	100
84	18-May	Monday	26738	2544	8413	3899	80	2276	228	2148	8479	10627	25483	93
85	19-May	Tuesday	24952	3201	8362	410	75	2932	343	2609	9585	12195	24168	97
End of Batch 11			26983	2840	8375	3481	86	2732	394	2318	6158	8477	23174	86
86	20-May	Wednesday	23990	2122	7956	3468	19	2326	86	2239	4358	6597	20143	84
87	21-May	Thursday												
88	22-May	Friday	28723	2448	8160	2040	14	2520	63	2435	4079	6534	19182	67
89	23-May	Saturday	28234	1632	7242	3370	38	2390	173	2218	3708	5926	18370	63
90	24-May	Sunday	28227	3509	7089	2856	19	2232	86	2146	3997	6142	19596	82
91	25-May	Monday	27907	3754	4641	4896	5	2254	22	2232	4288	6320	19811	71
92	26-May	Tuesday												
93	27-May	Wednesday												
94	28-May	Thursday	24480	2611	7140	5406		1699		1699	4114	5813	20970	86
95	29-May	Friday	25949	3182	6426	5100		2678		2678	3703	6384	21092	81
96	30-May	Saturday	26928	3427	8568	7956	28	2254	129	2				



Daily Tests on Modified DePhanos BNRRS External Nitrification System

DwY No	1998	Influent COD mgCOD/d	Effluent COD mgCOD/d	Waste COD mgCOD/d	COD used in EXNR mgCOD/d	Nitrifying Check 1 mgO/d	OUR *24*V Measured mgO/d	MOOn 4.57*V/mg mgO/d	MOOn mgO/d	MOOn mgO/d	Dwell O <sub>2</sub> MCh mgO/d	MOOn-MCO mgO/d	COD leaving mgCOD/d	MB_COD %
253	05-Nov	Thursday	21787	1918	5304	2481	563	5458	2380	2877	1676	4533	14296	66
256	06-Nov	Friday	21542	2020	3222	3656	203	4824	928	3896	1344	5240	16137	75
257	07-Nov	Saturday	22032	1918	4937	1697	624	5098	2852	2346	2261	4597	13099	59
258	08-Nov	Sunday												
259	09-Nov	Monday												
260	10-Nov	Tuesday	15667	2203	4284	2611	747	5443	3414	2029	2797	4827	13923	89
261	11-Nov	Wednesday	15912	1346	4325	522	831	5283	3798	1487	3183	4672	10866	68
262	12-Nov	Thursday	24235	1714	4570	1938	322	5717	2385	3332	2320	5632	13893	57
263	13-Nov	Friday	16157	1530	4566	1044	495	5990	2203	3728	1843	5571	12511	77
End of Batch 29			19419	1819	4715	1994	597	5402	2730	2672	2053	4725	13255	68
264	14-Nov	Saturday												
265	15-Nov	Sunday												
266	16-Nov	Monday	21342	1918	5304	1828	133	5833	618	5214	2525	7738	16829	78
267	17-Nov	Tuesday	24235	1391	5304	2330	227	5702	1056	4667	2483	7149	14293	68
268	18-Nov	Wednesday	19217	1163	4610	2742	179	5330	816	4714	3218	7932	16447	86
269	19-Nov	Thursday	15667	1652	5304	3264	526	5242	2406	2836	3841	6676	16897	108
270	20-Nov	Friday	23214	1530	4488	3133	628	7819	2869	4950	2647	7597	16748	66
271	21-Nov	Saturday	22377	1469	4774	3003	205	8179	935	7244	2374	9618	18863	85
272	22-Nov	Sunday												
273	23-Nov	Monday												
274	24-Nov	Tuesday												
275	25-Nov	Wednesday	20038	1457	5384	1684	207	6003	947	3058	2917	7973	16500	82
276	26-Nov	Thursday	19916	1761	5303	239	80	5643	408	5237	2348	7583	14908	75
End of Batch 30			21813	1573	5059	2383	274	6244	1254	4999	2714	7704	16418	79
277	27-Nov	Friday												
278	28-Nov	Saturday												
279	29-Nov	Sunday												
280	30-Nov	Monday												
281	01-Dec	Tuesday												
282	02-Dec	Wednesday	24652	1397	5586	777	413	6062	1887	4176	3986	8162	15922	65
283	03-Dec	Thursday	24774	1943	6801	777	688	6723	3144	3581	4449	8030	17551	71
284	04-Dec	Friday												
285	05-Dec	Saturday												
286	06-Dec	Sunday												
End of Batch 31			24713	1670	6193	777	547	6394	2501	3893	4184	8079	16719	68
287	07-Dec	Monday												
288	08-Dec	Tuesday												
289	09-Dec	Wednesday												
290	10-Dec	Thursday												
291	11-Dec	Friday												
292	12-Dec	Saturday												
293	13-Dec	Sunday												
294	14-Dec	Monday												
295	15-Dec	Tuesday	17280	1440	6640	2560		3182		3182	1917	5099	15739	91
296	16-Dec	Wednesday	17520	1020	6640	2304		4003		4003	2008	6012	15976	91
297	17-Dec	Thursday	23760	1260	7000	3712	31	4234	144	4090	1921	6011	17983	76
298	18-Dec	Friday	23760	1320	7640	2176	33	5242	152	5090	1579	6669	17805	75
299	19-Dec	Saturday												
300	20-Dec	Sunday												
301	21-Dec	Monday												
302	22-Dec	Tuesday												
End of Batch 32			20580	1260	6980	2488		4165		4165	1853	6018	16946	82
303	23-Dec	Wednesday												
304	24-Dec	Thursday	22920	1620	7320	1920	446	4738	2028	2699	1622	4322	15182	66
305	25-Dec	Friday	23040	1440	9120	2560	301	4334	1377	2937	3033	5990	19110	83
306	26-Dec	Saturday	22360	1200	9280	2432	411	4910	1876	3034	2492	6327	19439	86
307	27-Dec	Sunday												
308	28-Dec	Monday	24000	1920	9040	2304	261	4666	1649	3016	3477	6494	19758	82
309	29-Dec	Tuesday	21120	2230	3680	1280	205	4550	935	3616	3104	6720	16200	77
310	30-Dec	Wednesday	20640	1800	5920	1280	317	5386	1447	3938	3421	7359	16359	79
311	31-Dec	Thursday												
312	01-Jan	Friday												
313	02-Jan	Saturday												
314	03-Jan	Sunday												
315	04-Jan	Monday	19920	720	6120	1152	520	5643	2379	3266	3200	6466	14458	73
End of Batch 33			22029	1403	7497	1847	364	4890	1672	3218	2995	6213	17168	78
316	05-Jan	Tuesday	27720	1560	6480	384	487	5141	2223	2916	3878	6794	15218	55
317	06-Jan	Wednesday												
318	07-Jan	Thursday												
319	08-Jan	Friday												
320	09-Jan	Saturday												
321	10-Jan	Sunday												
322	11-Jan	Monday												
323	12-Jan	Tuesday												
324	13-Jan	Wednesday	22680	2160	5440	2688	621	4522	2839	1683	2674	4358	14644	63
325	14-Jan	Thursday	24600	1800	5640	2048	638	5873	2916	2959	2304	5264	14752	60
326	15-Jan	Friday												
327	16-Jan	Saturday												
328	17-Jan	Sunday												
329	18-Jan	Monday												
330	19-Jan	Tuesday												
331	20-Jan	Wednesday												
332	21-Jan	Thursday	28903	1943	6193	259	630	4781	2877	1903	2804	4708	13103	45
333	22-Jan	Friday												
334	23-Jan	Saturday												
335	24-Jan	Sunday												
336	25-Jan	Monday												
End of Batch 34			25594	1968	5758	1665	630	5880	2877	2282	2504	4708	14094	56
337	26-Jan	Tuesday	23990	1588	6350	1756	772	4910	3530	1381	3186	4487	14181	59
338	27-Jan	Wednesday	20819	1235	6330	1503	877	4810	4039	801	3173	3974	13064	63
339	28-Jan	Thursday	18816	1823	7213	2007	949	9518	4335	5183	3119	8207	19545	103
340	29-Jan	Friday	18110	1529	5174	251	1007	7790	4604	3187	2827	6014	12968	72
341	30-Jan	Saturday												
342	31-Jan	Sunday												
343	01-Feb	Monday												
344	02-Feb	Tuesday												
End of Batch 35			20433	1544	6272	1380	901	4757	4119	2638	3035	5673	14868	73
345	03-Feb	Wednesday												
346	04-Feb	Thursday												
347	05-Feb	Friday												
348	06-Feb	Saturday												
349	07-Feb	Sunday	22044	1411	4861	2883	288	6048	1317	4731	2836	7567	16724	75
350	08-Feb	Monday												
351	09-Feb	Tuesday	21050	1705	6390	2634	240	4822	1096	3526	2697	6223	16913	80
352	10-Feb	Wednesday	20923	1176	5723	1631	197	5126	901	4223	2510	6736	15263	73
353	11-Feb	Thursday	21521	1352	6507	2383	228	6062	1043	3019	2673	7693	17926	83
354	12-Feb	Friday												
355	13-Feb	Saturday	23640	2400	6600	3712	244	5098	1114	3984	2893	6879	19591	83
356	14-Feb	Sunday												
357	15-Feb	Monday	17280	1440	6640	2560	309	5213	1410	3802	3144	6946	17586	102
358	16-Feb	Tuesday	18240	1380	6880	2304	328	4003	1497	2306	2825	5331	15895	87
End of Batch 36			21128	1581	6114	2634	259	5168	1182	3986	2809	6795	17124	81
359	17-Feb	Wednesday												
360	18-Feb	Thursday	18240	1740	6760	1792	184	3738	841	2917	2966	5883	16173	89
361	19-Feb	Friday	18560	1200	7520	1408	76	3713	346	3369	2466	3833	13963	67
362	20-Feb	Saturday												
363	21-Feb	Sunday												
364	22-Feb	Monday	20280	2820	6080	2432	902	4608	4121	487	3799	4286	15618	77
365	23-Feb	Tuesday	17320	1560	6160	1280	641	5990	2931	306				

Daily Tests on Modified DePhosox DNRAS External Nitrification System

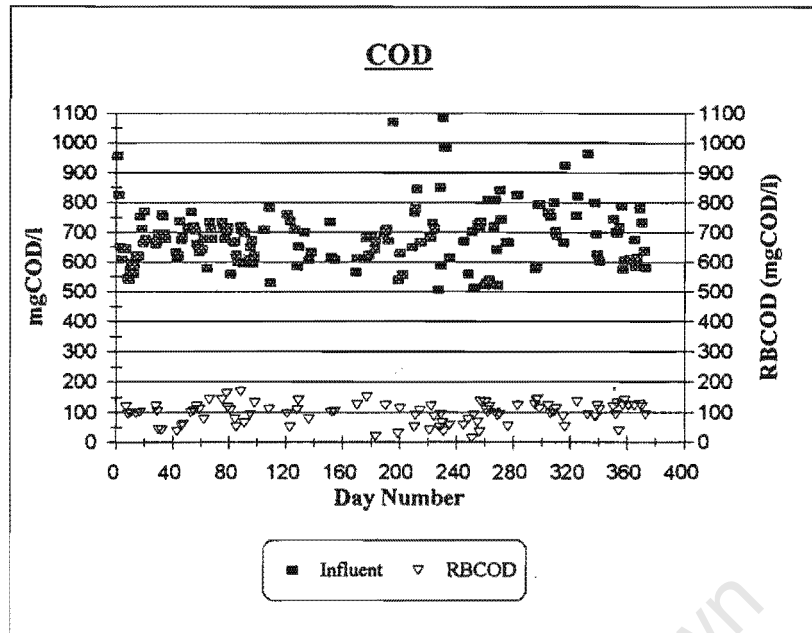
Day No	1998	Total Phosphates mg PO4-P/l										Phosphorus Mass Balance mg P/l d						P Removal	
		AN	Main_Anox	Pre_Anox	AZ	Final Filtered Eff	Inlet Filtered Eff	ExTR Filtered Eff	InDuct	Anaerobic	Main Anox	Pre-Anox	Aerobic	Final Filtered Eff	Inlet Filtered Eff	ExTR Filtered Eff	In-AE	In-PrePEE	
1	24-Feb	Tuesday	25.0	15.6	10.8	10.8	12.1	23.3	26.7	19.4	-19.4	20.1	1.4	9.7	-3.8	-0.7	-2.1	9.0	7.6
2	25-Feb	Wednesday	19.1	12.1	8.3	8.0	10.4	21.9	22.6	19.4	-10.4	19.8	2.1	8.3	-4.9	-5.6	-1.0	11.3	9.0
3	26-Feb	Thursday	17.0	11.1	4.9	6.6	7.3	20.1	22.9	15.3	-13.9	19.4	2.4	9.0	-1.4	-6.2	-4.2	8.7	8.0
End of Batch 1			26.4	18.0	8.9	8.4	9.9	22.4	24.1	18.3	-14.6	19.8	2.0	9.0	-3.0	-4.2	-2.4	9.7	8.2
4	27-Feb	Friday	18.1	11.0	4.6	7.1	6.4	19.9	24.2	20.3	-11.4	19.9	1.8	7.8	1.4	-3.6	-6.4	13.1	13.9
5	28-Feb	Saturday	15.3	12.1	6.4	8.9	7.5	18.8	23.5	16.3	-7.8	15.8	1.1	6.4	2.8	-7.1	-6.9	7.3	8.9
6	01-Mar	Sunday	16.7	14.6	8.3	11.4	8.5	22.7	18.3	17.4	-7.3	16.9	0.0	6.4	5.7	-12.1	-1.6	6.0	8.9
7	02-Mar	Monday	14.9	13.2	8.2	10.7	9.6	19.5	21.3	22.4	-0.7	13.0	1.4	3.7	2.1	-9.2	-2.7	11.7	12.8
8	03-Mar	Tuesday	15.3	12.8	8.9	10.3	9.6	16.7	18.5	17.4	-4.3	8.7	0.7	5.0	1.4	-2.8	-3.7	7.1	7.8
9	04-Mar	Wednesday	11.8	12.4	8.2	10.3	10.3	14.2	16.3	18.3	1.1	4.6	2.1	4.3	0.0	-2.8	-3.2	8.2	8.2
10	05-Mar	Thursday	15.1	12.1	9.2	11.7	10.7	15.6	15.6	17.8	0.7	7.1	1.4	0.7	2.1	-3.0	0.0	6.0	7.1
11	06-Mar	Friday	12.8	10.0	8.2	10.3	9.2	17.1	13.6	18.1	0.7	13.5	1.1	-0.7	2.1	-8.5	2.1	7.8	8.9
12	07-Mar	Saturday	12.1	10.7	9.2	10.3	9.2	16.7	17.1	18.5	3.6	12.3	0.0	0.7	2.1	-9.2	-0.5	8.2	9.2
13	08-Mar	Sunday	14.6	12.1	8.9	10.3	9.6	16.7	18.3	18.1	-2.1	10.1	0.7	3.6	1.4	-4.3	-2.7	7.8	8.3
14	09-Mar	Monday	13.9	10.7	8.2	10.0	10.0	14.6	14.9	19.2	-0.4	8.0	1.8	1.4	0.0	-1.4	-0.3	9.2	9.4
15	10-Mar	Tuesday	14.2	10.3	9.2	10.7	11.4	14.9	17.4	18.3	-0.7	10.5	2.1	-0.7	-1.4	-1.4	-3.7	7.8	7.1
16	11-Mar	Wednesday	13.1	11.7	10.0	11.0	10.7	13.9	14.9	19.3	3.2	4.8	0.7	1.4	0.7	-1.4	-1.6	8.3	8.9
17	12-Mar	Thursday	11.7	11.4	10.0	11.0	10.3	13.1	13.9	18.5	5.0	3.9	0.4	0.7	1.4	-2.8	-1.1	7.5	8.2
End of Batch 2			14.2	11.8	8.4	10.3	9.5	16.8	18.3	18.6	-1.4	10.4	1.1	3.0	1.4	-5.1	-2.2	8.3	9.1
18	13-Mar	Friday	18.9	13.4	10.3	11.7	11.4	19.3	20.0	15.8	-11.7	12.1	1.0	3.4	0.7	-0.7	-1.0	4.1	4.3
19	14-Mar	Saturday	35.8	20.7	17.6	14.6	15.2	35.5	34.1	22.4	-21.7	28.9	-2.4	4.1	6.9	0.7	-2.1	13.4	17.3
20	15-Mar	Sunday	24.9	19.6	15.8	17.6	18.6	39.4	35.1	22.9	-12.7	28.4	2.8	4.1	-2.1	-10.3	-2.6	10.3	9.3
21	16-Mar	Monday	35.5	20.3	14.1	16.9	16.3	35.8	34.8	28.2	-28.6	30.5	2.4	6.9	0.7	-0.7	1.5	11.4	11.7
End of Batch 3			29.6	18.5	14.5	16.2	15.4	31.0	31.0	26.1	-19.7	25.0	0.9	4.6	1.5	-2.8	8.8	9.9	10.7
23	18-Mar	Wednesday																	
24	19-Mar	Thursday																	
25	20-Mar	Friday																	
26	21-Mar	Saturday																	
27	22-Mar	Sunday	40.8	22.8	25.6	16.0	18.0	51.7	45.2	30.8	-17.6	41.6	-3.8	10.2	-3.0	-16.2	8.6	14.8	12.8
28	23-Mar	Monday	41.4	23.6	29.2	17.6	17.2	44.0	46.0	37.2	-11.8	31.1	-6.0	9.0	0.8	-2.4	-2.5	19.6	20.0
29	24-Mar	Tuesday	31.7	24.0	34.0	19.2	18.0	46.9	48.5	31.2	-37.2	34.6	-10.0	7.2	1.8	7.3	-1.0	12.0	13.2
30	25-Mar	Wednesday	46.4	24.8	33.6	19.2	20.0	48.2	46.0	21.2	-21.6	34.8	-6.8	8.4	-1.2	-3.0	3.0	12.0	11.2
End of Batch 4			45.3	23.8	31.6	19.0	18.3	47.8	44.4	32.4	-19.6	35.6	-6.7	8.7	-0.5	-3.6	1.6	14.0	14.3
31	26-Mar	Thursday																	
32	27-Mar	Friday	20.0	7.2	11.7	4.8	7.2	20.3	18.9	15.8	-8.3	19.3	-2.2	3.6	-3.6	-0.5	1.7	11.0	8.6
33	28-Mar	Saturday	20.7	9.6	17.3	5.5	5.5	23.4	23.8	15.8	-6.5	20.8	-5.9	6.2	0.0	-4.1	-0.4	10.3	10.3
34	29-Mar	Sunday	22.7	11.0	21.0	6.8	7.6	22.4	23.1	15.5	-8.1	17.2	-6.7	9.3	-4.1	0.5	-0.9	10.7	7.9
35	30-Mar	Monday	22.7	14.1	17.6	5.3	8.3	23.1	23.8	15.5	-9.8	13.6	-4.6	12.9	-4.1	-0.5	-0.9	10.0	7.2
36	31-Mar	Tuesday	23.4	13.8	18.9	5.9	7.9	23.4	23.8	15.8	-8.3	14.6	-5.5	11.9	-3.1	-1.5	-0.4	10.0	7.9
37	01-Apr	Wednesday																	
38	02-Apr	Thursday																	
End of Batch 5			21.5	18.5	16.9	5.2	7.1	22.3	22.4	15.7	-8.2	17.7	-4.9	8.8	-3.8	-1.2	-0.1	10.5	8.5
39	03-Apr	Friday																	
40	04-Apr	Saturday																	
41	05-Apr	Sunday																	
42	06-Apr	Monday	21.7	14.8	16.2	7.9	7.9	18.3	22.0	14.5	-10.0	6.1	-4.1	10.3	0.0	5.1	-4.7	6.5	6.5
43	07-Apr	Tuesday	20.0	14.3	16.2	9.0	10.0	20.7	21.4	15.5	-6.4	9.5	-3.1	8.3	-1.5	-1.0	-0.9	6.5	5.5
44	08-Apr	Wednesday	23.4	13.8	15.5	5.9	10.0	21.4	25.8	15.2	-12.2	12.5	-2.8	11.9	-6.2	3.1	-3.6	9.3	5.2
45	09-Apr	Thursday	24.8	15.8	17.6	10.0	11.4	23.4	23.8	18.6	-9.8	11.5	-3.1	8.8	-2.1	2.1	-0.4	8.6	7.2
End of Batch 6			22.8	14.7	16.4	8.2	9.8	24.9	23.2	18.9	-9.6	9.9	-3.3	9.8	-2.8	2.3	-2.9	7.7	6.1
46	10-Apr	Friday	23.4	16.2	20.3	11.4	12.1	24.5	25.5	18.9	-6.0	12.7	-4.1	7.2	-1.0	-1.3	-1.3	7.6	6.9
47	11-Apr	Saturday	23.8	16.9	18.3	11.7	12.1	24.1	26.9	18.6	-7.9	11.5	-3.1	7.7	-0.5	-0.5	-0.4	6.9	6.5
48	12-Apr	Sunday																	
49	13-Apr	Monday																	
50	14-Apr	Tuesday																	
51	15-Apr	Wednesday	19.6	16.2	14.1	6.5	17.2	20.0	24.1	18.9	-3.4	6.7	1.5	14.3	-16.0	-0.5	-5.2	12.4	1.7
52	16-Apr	Thursday	23.8	22.4	22.4	10.0	11.4	23.4	26.9	22.4	-1.5	1.0	-6.0	18.6	-2.1	3.1	-5.2	12.4	11.0
End of Batch 7			22.6	17.9	19.0	8.9	13.2	22.7	25.7	19.7	-6.7	8.8	-3.9	12.8	-4.9	-8.1	-3.8	9.8	6.5
53	17-Apr	Friday	21.4	14.8	22.0	10.0	11.7	23.1	26.3	15.5	-5.5	15.8	-3.2	7.3	-2.6	-5.7	-1.7	5.3	3.8
54	18-Apr	Saturday																	
55	19-Apr	Sunday	25.1	16.5	17.6	5.3	10.7	24.8	23.4	16.9	-12.1	12.1	-3.4	16.5	-7.7	0.5	1.7	11.4	6.2
56	20-Apr	Monday	26.3	14.5	21.7	8.3	10.3	28.2	30.0	16.9	-12.1	21.1	-5.7	9.3	-3.1	2.6	-2.2	8.6	6.5
57	21-Apr	Tuesday	30.3	16.9	24.3	8.3	9.6	30.3	31.3	16.9	-14.4	20.4	-7.4	12.9	-2.1	0.0	-1.3	8.6	7.2
58	22-Apr	Wednesday	30.3	18.6	18.6	11.7	11.7	31.3	18.6	17.6	-18.6	19.7	-3.4	10.3	0.0	-1.5	-3.0	5.9	5.9
59	23-Apr	Thursday	30.0	18.3	20.7	9.6	11.0	30.3	30.7	16.9	-17.7	18.2	-4.8	12.9	-2.1	-0.5	-0.4	7.2	5.9
60	24-Apr	Friday																	
61	25-Apr	Saturday	29.6	20.3	19.6	12.4	13.8	30.3	32.4	18.9	-15.7	15.5	-2.9	11.9	-2.1	-1.0	-2.6	6.5	5.2
62	26-Apr	Sunday																	
63	27-Apr	Monday	22.0	27.2	10.3	8.3	12.1	18.6	19.6	23.4	-4.3	-12.7	0.9	28.4	-5.7	3.2	-1.3	15.2	11.4

Daily Tests on Modified Deponox BNRAS External Nitrification System

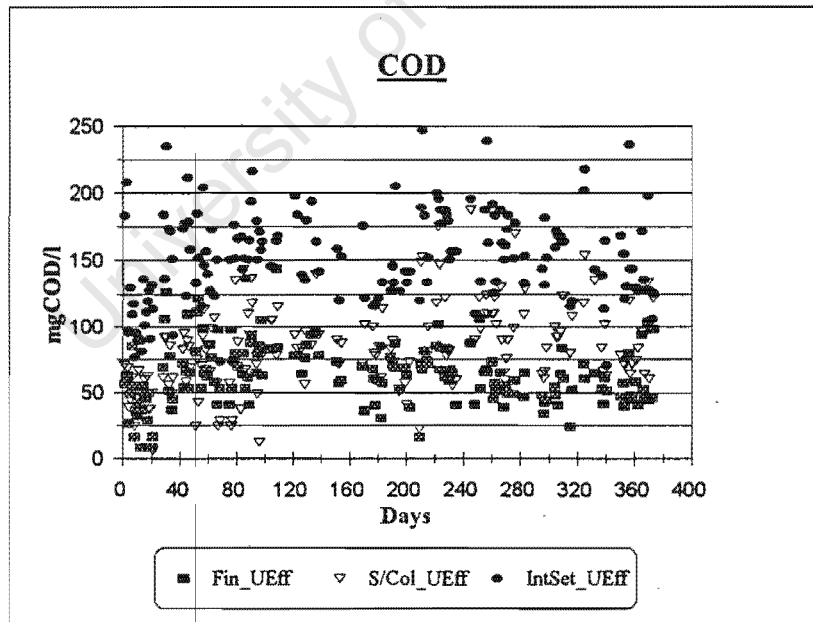
Day No	1998	Total Phosphates mg P04-P/l							Phosphorus Mass Balance mg P/l Inf							P Removal			
		AN	Main_Anox	Pre_Anox	AE	Final Filtered Eff	IntSet Filtered Eff	ExtNit Filtered Eff	Influent	Anaerobic	Main Anox	Pre-Anox	Aerobic	Final Filtered Eff	IntSet Filtered Eff	ExtNit Filtered Eff	In-AE	In-Fin/FEff	
120	23-Jun	Tuesday																	
121	24-Jun	Wednesday	28.6	25.5	23.8	11.0	13.1	28.9	29.3	23.1	-7.9	5.3	-5.3	21.7	-3.1	-0.5	-0.4	12.1	10.0
122	25-Jun	Thursday																	
123	26-Jun	Friday	28.2	26.5	25.5	14.5	14.8	27.6	27.2	12.7	-6.9	1.5	-5.3	18.1	-0.5	1.0	0.4	8.3	7.9
124	27-Jun	Saturday																	
125	28-Jun	Sunday																	
End of Batch 16			28.4	26.0	24.6	12.7	13.9	28.2	28.2	22.9	-7.4	3.4	-5.3	19.9	-1.8	0.3	0.0	10.2	9.0
126	29-Jun	Monday	27.6	22.4	17.9	10.0	13.4	26.5	26.9	23.4	-9.0	6.3	-2.2	18.6	-5.2	1.5	-0.4	13.4	10.0
127	30-Jun	Tuesday																	
128	01-Jul	Wednesday	25.8	23.1	21.0	13.1	14.8	25.5	26.2	22.0	-6.2	3.8	-3.1	15.0	-2.6	0.5	-0.9	9.0	7.2
129	02-Jul	Thursday	24.1	19.6	19.6	16.9	14.5	23.8	25.1	21.4	-5.0	9.1	-2.6	4.1	3.6	-2.6	0.9	4.3	6.9
130	03-Jul	Friday	24.8	21.7	20.0	14.1	15.2	25.1	25.5	22.4	-4.8	5.3	-2.4	11.4	-1.5	-0.3	-0.4	8.3	7.2
131	04-Jul	Saturday																	
132	05-Jul	Sunday																	
133	06-Jul	Monday	24.5	26.9	24.5	17.2	17.2	24.8	28.6	22.4	-2.1	-2.2	-3.6	14.5	0.0	-0.5	-4.7	5.2	5.2
134	07-Jul	Tuesday																	
End of Batch 17			25.3	22.7	20.6	14.3	15.0	25.6	26.5	22.3	-5.4	4.5	-2.8	12.7	-1.1	-0.3	-1.1	8.1	7.3
135	08-Jul	Wednesday																	
136	09-Jul	Thursday	23.8	20.7	18.6	13.4	13.4	23.1	24.5	23.1	-3.3	4.0	-2.6	10.8	0.0	1.0	-1.7	9.6	9.6
137	10-Jul	Friday	25.1	21.0	18.9	15.2	14.1	24.5	25.8	24.1	-4.1	5.5	-2.4	8.8	1.5	1.0	-1.7	9.0	10.0
138	11-Jul	Saturday	25.9	21.0	19.3	16.5	15.8	24.8	23.8	27.2	-1.9	5.4	-1.7	6.7	1.0	1.3	10.7	11.4	
139	12-Jul	Sunday																	
140	13-Jul	Monday																	
141	14-Jul	Tuesday																	
142	15-Jul	Wednesday																	
143	16-Jul	Thursday																	
144	17-Jul	Friday																	
145	18-Jul	Saturday	30.0	22.7	20.3	16.5	15.5	29.6	34.1	26.5	-8.3	11.5	-2.4	9.3	1.5	0.5	-5.6	10.0	11.0
146	19-Jul	Sunday	28.9	23.4	21.4	13.1	16.9	26.9	32.0	28.6	-4.1	6.5	-2.2	15.5	-0.7	3.1	-6.5	15.5	11.7
147	20-Jul	Monday																	
End of Batch 18			24.9	20.9	18.9	15.8	14.8	24.1	24.7	24.8	-5.1	5.0	-2.3	8.8	0.9	1.2	-0.7	9.8	10.3
148	21-Jul	Tuesday	18.9	14.1	12.1	9.0	10.7	17.9	23.8	19.6	-2.8	7.1	-0.7	7.7	-2.6	1.5	-7.3	10.7	9.0
149	22-Jul	Wednesday																	
End of Batch 19																			
150	23-Jul	Thursday	30.7	25.1	19.9	17.2	14.5	32.4	29.6	27.9	-8.1	9.9	-2.7	11.9	4.1	-2.9	3.2	10.7	13.4
151	24-Jul	Friday	31.7	27.2	18.3	17.9	18.9	37.5	33.4	24.5	-13.9	14.1	0.3	13.9	-1.5	-0.8	4.8	6.5	5.5
152	25-Jul	Saturday	31.7	25.1	20.0	15.2	16.9	35.1	31.7	26.5	-11.0	13.8	-1.5	15.0	-2.6	-5.7	4.0	11.4	9.6
153	26-Jul	Sunday																	
154	27-Jul	Monday	32.0	25.8	18.9	15.5	17.6	34.8	35.5	23.1	-15.5	13.7	-0.7	15.5	-3.1	-4.6	-0.8	7.6	5.5
End of Batch 20			31.5	25.8	19.3	16.3	17.0	35.0	32.5	25.5	-12.2	12.9	-1.1	14.1	-4.8	-5.7	2.8	9.0	8.5
155	28-Jul	Tuesday																	
156	29-Jul	Wednesday																	
157	30-Jul	Thursday																	
158	31-Jul	Friday																	
159	01-Aug	Saturday																	
160	02-Aug	Sunday																	
161	03-Aug	Monday																	
162	04-Aug	Tuesday																	
163	05-Aug	Wednesday																	
164	06-Aug	Thursday																	
165	07-Aug	Friday																	
166	08-Aug	Saturday																	
167	09-Aug	Sunday																	
168	10-Aug	Monday																	
169	11-Aug	Tuesday	34.4	25.8	12.4	10.3	10.3	39.6	39.6	23.8	-21.7	10.7	-1.0	23.2	0.0	-4.6	0.0	13.4	13.4
170	12-Aug	Wednesday	31.3	33.1	11.4	12.1	13.8	39.3	39.6	21.0	-20.3	9.4	1.2	31.5	-2.6	-13.2	-0.4	9.0	7.2
171	13-Aug	Thursday																	
172	14-Aug	Friday																	
173	15-Aug	Saturday																	
174	16-Aug	Sunday																	
175	17-Aug	Monday																	
End of Batch 21			32.9	29.4	11.9	11.2	12.1	39.4	39.6	22.4	-21.0	15.0	0.1	27.4	-1.3	-10.9	-0.1	11.2	10.3
176	18-Aug	Tuesday	28.0	19.4	4.3	10.3	11.0	30.7	31.7	17.4	-23.5	17.4	3.3	13.5	-1.0	-4.4	-1.2	7.0	6.1
177	19-Aug	Wednesday	31.7	23.7	3.7	9.3	10.3	33.4	34.4	16.0	-29.7	14.8	3.3	21.5	-1.5	-2.8	-1.2	6.7	5.7
178	20-Aug	Thursday	30.0	28.0	11.3	14.7	13.7	33.7	34.4	16.0	-23.4	8.7	1.2	20.0	1.5	-6.1	-0.8	1.3	2.3
179	21-Aug	Friday																	
180	22-Aug	Saturday	31.0	29.0	7.7	4.7	3.7	29.0	30.0	22.0	-20.7	0.3	-2.0	36.5	1.5	3.3	-1.2	17.4	18.4
181	23-Aug	Sunday																	
182	24-Aug	Monday	32.4	32.4	9.7	11.1	7.7	32.0	35.4	23.7	-20.0	0.6	-1.0	31.5	5.5	0.6	-3.9	12.3	16.0
183	25-Aug	Tuesday	35.7	38.0	18.7	11.7	9.7	35.4	48.4	21.7	-22.5	0.3	-4.5	39.5	3.0	0.6	-13.2	10.0	12.0
184	26-Aug	Wednesday																	
185	27-Aug	Thursday																	
186	28-Aug	Friday																	
187	29-Aug	Saturday																	
188	30-Aug	Sunday																	
End of Batch 22			31.5	28.4	9.2	10.3	9.3	32.4	38.7	19.8	-23.1	7.0	0.1	27.1	1.5	-1.8	-3.9	9.1	10.1
189	31-Aug	Monday	43.9	25.7	11.1	14.3	13.6	43.0	45.7	27.9	-32.5	27.5	1.2	17.1	1.1	0.6	-2.5	13.6	14.3
190	01-Sep	Tuesday	46.4	27.5	11.1	14.6	12.9	45.7	48.9	22.9	-41.3	28.4	0.9	19.3	2.7	1.2	-3.8	8.2	10.0
191	02-Sep	Wednesday	48.9	25.0	11.8	13.6	13.6	50.7	50.4	24.6	-42.9	38.5	0.9	17.1	0.0	-3.0	4.0	11.1	11.1
192	03-Sep	Thursday	47.5	30.0	15.4	17.1	14.6	45.4	50.7	25.0	-38.6	24.8	-0.4	19.3	3.8	3.6	-6.2	7.9	10.4
193	04-Sep	Friday																	
194	05-Sep	Saturday	43.6	23.9	9.3	8.9	11.1	44.6	43.9	26.8	-33.9	30.8	0.9	22.5	-3.2	-1.8	0.8	17.9	15.7
195	06-Sep	Sunday	40.7	29.7	9.6	11.8	10.7	43.2	45.4	32.5	-23.8	17.0	0.5	20.9	1.6	-4.2	-2.5	20.7	21.8
196	07-Sep	Monday																	
End of Batch 23			45.1	26.3	11.4	13.4	12.7	45.5	47.5	26.6	-35.6	29.5	0.7	19.4	1.0	-0.6	-3.3	13.2	13.9
197	08-Sep	Tuesday																	
198	09-Sep	Wednesday																	
199	10-Sep	Thursday	32.5	15.4	2.5	7.5	6.8	32.1	30.4	27.5	-20.0	24.6	2.1	11.8	1.1	0.6	2.1	20.0	20.7
200	11-Sep	Friday																	
201	12-Sep	Saturday	34.3	20.7	7.5	12.1	11.1	39.3	31.6	28.2	-19.5	26.0	1.8	12.9	1.6	-8.3	6.7	16.1	17.1
202	13-Sep	Sunday	33.2	16.4	6.1	11.1	12.5	37.1	32.9	31.1	-15.7	29.6	3.2	8.0	-2.1	-6.5	5.0	20.0	18.6
203	14-Sep	Monday																	
204	15-Sep	Tuesday																	
205	16-Sep	Wednesday																	

Daily Tests on Modified Dephnox BNRAS External Nitrification System

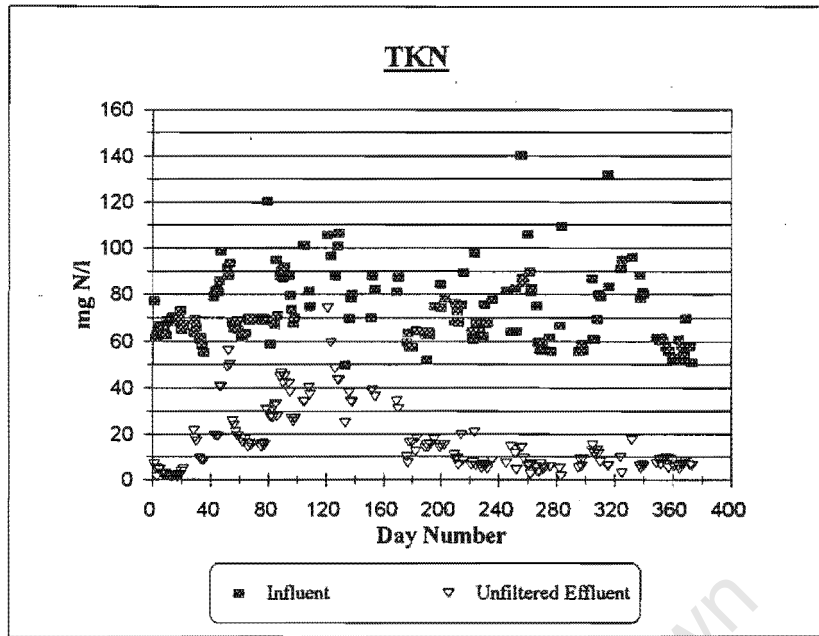
Day No	1998	Total Phosphates mg PO4-P/l										Phosphorus Mass Balance mg P/l Inf								P Removal	
		AN	Main_Anox	Pre_Anox	AE	Final Filtered Eff	IntSet Filtered Eff	ExtNit Filtered Eff	Influent	Anaerobic	Main Anox	Pre-Anox	Aerobic	Final Filtered Eff	IntSet Filtered Eff	ExtNit Filtered Eff	In-AE	In-Fin/Eff	P Removal		
																			In-AE	In-Fin/Eff	
255	05/Nov	Thursday	26.207	13.103	14.828	13.793	11.724	27.241	26.552	20.000	-12.414	21.161	-1.552	3.103	-1.552	0.736	6.207	8.28			
256	06/Nov	Friday	24.483	17.931	17.931	16.207	12.414	20.690	26.552	20.345	-8.276	8.667	-2.759	5.690	5.690	-6.253	4.138	7.93			
257	07/Nov	Saturday	26.207	15.862	13.448	12.759	13.103	26.207	24.828	21.054	-11.897	10.943	-0.172	7.759	-0.517	1.471	8.274	7.93			
258	08/Nov	Sunday	21.034	13.103	8.966	10.345	13.103	21.379	18.276	22.069	-4.310	6.345	6.897	-4.138	-0.517	3.310	11.724	8.93			
259	09/Nov	Monday																			
260	10/Nov	Tuesday	20.690	16.897	12.759	7.586	10.690	22.759	24.828	19.655	-7.586	1.690	-1.034	23.276	-4.655	-3.103	-2.207	12.069	8.97		
261	11/Nov	Wednesday	24.483	19.655	17.241	14.483	13.793	25.862	28.621	18.021	-10.862	7.080	-1.724	12.931	1.034	-2.069	-2.943	4.138	4.83		
262	12/Nov	Thursday	23.759	19.655	17.241	16.897	14.483	24.138	31.724	21.724	-3.966	12.057	-1.379	6.897	3.621	-2.069	-8.092	4.828	7.24		
263	13/Nov	Friday	24.483	19.310	18.966	19.310	18.966	35.172	27.241	17.931	-9.138	11.000		0.517	-1.034	-2.207	-1.379	-1.03			
AVG BATCH No 29			23.793	16.940	15.172	13.922	13.534	24.181	26.078	20.172	-8.556	11.036	-0.936	10.345	0.582	-0.665	-2.023	6.250	6.637931		
264	14/Nov	Saturday																			
265	15/Nov	Sunday																			
266	16/Nov	Monday	20.756	15.221	18.680	12.453	13.145	20.410	20.756	20.410	-4.497	5.385	-2.767	6.919	-1.038	0.519	-0.369	7.956	7.26		
267	17/Nov	Tuesday	24.561	20.410	20.756	12.799	9.806	24.907	24.215	33.555	3.113	-5.535	19.026	4.670	-0.519	0.738	20.756	23.87			
268	18/Nov	Wednesday	24.215	19.026	20.064	10.724	12.107	24.561	24.561	19.026	-11.934	-3.978	20.756	-2.076	-0.519		8.302	9.62			
269	19/Nov	Thursday	22.831	21.011	15.567	12.799	11.761	23.177	24.907	22.139	-5.708	-1.903	20.756	1.537	-0.519	-1.845	9.340	10.38			
270	20/Nov	Friday	22.485	25.599	15.221	14.529	12.453	21.793	21.869	19.372	-7.071	-1.384	27.674	3.113	1.038	-2.214	4.843	6.92			
271	21/Nov	Saturday	24.215	15.221	15.913	8.648	11.761	24.561	25.253	27.328	-4.670	8.175	-2.076	16.431	-4.670	-0.519	-0.738	18.680	15.37		
272	22/Nov	Sunday																			
273	23/Nov	Monday																			
274	24/Nov	Tuesday																			
275	25/Nov	Wednesday																			
276	26/Nov	Thursday	30.856	16.831	15.428	10.870	8.415	30.155	31.558	21.740	-19.110	15.522	-3.506	14.902	3.682	1.052	-1.496	10.870	13.32		
AVG BATCH No Jb			24.274	19.058	17.375	11.832	11.333	24.223	25.047	23.367	-7.128	9.694	-3.021	18.066	0.748	0.076	-0.987	11.535	12.03		
277	27/Nov	Friday	23.493	15.779	11.558	10.519	9.818	30.688	30.856	22.090	-7.889	12.950	-10.870	13.149	1.052	4.208	-10.846	11.571	12.27		
278	28/Nov	Saturday																			
279	29/Nov	Sunday																			
280	30/Nov	Monday																			
281	01/Dec	Tuesday	40.324	27.350	41.025	29.804	19.636	41.025	42.428	23.493	-22.090	24.463	-10.695	15.253	-1.052	-1.496	-6.312	3.86			
282	02/Dec	Wednesday																			
283	03/Dec	Thursday	19.622	18.935	14.376	12.623	9.117	39.973	42.077	28.051	-23.071	27.490	-2.630	15.779	5.260	-0.526	-2.244	15.428	18.93		
284	04/Dec	Friday	42.778	21.038	19.285	12.623	9.818	41.376	43.479	27.550	-30.506	24.334	-4.734	21.038	4.208	2.104	-2.244	14.727	17.53		
285	05/Dec	Saturday	43.129	22.090	25.947	13.324	12.272	39.973	41.726	23.493	-34.538	19.928	-6.837	21.915	1.578	4.734	-1.870	10.619	11.22		
286	06/Dec	Sunday	40.674	22.090	21.038	9.117	10.169	40.324	37.869	19.636	-36.817	11.758	-5.435	32.434	-1.578	0.526	2.618	10.519	9.47		
AVG BATCH No J1			38.337	21.214	25.538	14.668	11.805	37.226	39.739	24.019	-26.152	20.154	-6.867	20.863	4.195	1.666	-2.680	9.350	12.214		
287	07/Dec	Monday																			
288	08/Dec	Tuesday																			
289	09/Dec	Wednesday																			
290	10/Dec	Thursday																			
291	11/Dec	Friday																			
292	12/Dec	Saturday																			
293	13/Dec	Sunday																			
294	14/Dec	Monday																			
295	15/Dec	Tuesday																			
296	16/Dec	Wednesday																			
297	17/Dec	Thursday	43.526	26.927	28.403	4.795	5.533	45.002	49.059	26.558	-36.333	9.308	-11.435	55.330	-1.107	-2.213	-4.328	21.763	21.03		
298	18/Dec	Friday	19.100	30.247	26.189	5.902	7.377	48.690	34.961	19.919	-35.780	10.009	-9.406	60.863	-2.213	-14.386	-6.689	14.017	12.54		
299	19/Dec	Saturday	40.944	29.509	28.771	4.058	5.164	46.108	53.485	19.181	-40.206	7.316	-11.804	63.629	-1.660	-7.746	-7.869	15.123	14.02		
300	20/Dec	Sunday	45.002	28.771	25.083	6.271	2.951	47.215	50.903	19.181	-45.186	9.099	-11.066	56.252	-4.980	-3.320	-3.935	12.910	16.23		
301	21/Dec	Monday																			
302	22/Dec	Tuesday																			
AVG BATCH No J2			42.143	28.864	27.112	5.256	5.256	46.754	52.102	21.210	-39.376	8.933	-10.928	59.018	-0.000	-6.916	-5.705	15.953	15.953		
303	23/Dec	Wednesday																			
304	24/Dec	Thursday																			
305	25/Dec	Friday																			
306	26/Dec	Saturday																			
307	27/Dec	Sunday	15.780	15.861	10.697	2.213	2.213	35.780	26.558	18.443	-34.120	6.394	-4.242	34.120	-6.086	2.766	-1.017	25.083	21.03		
308	28/Dec	Monday	40.944	21.763	15.492	7.377	11.435	39.100	49.428	32.460	-25.267	22.636	-2.029	35.964	-0.738	-9.959	-10.513	-9.836	19.181	12.54	
309	29/Dec	Tuesday	47.215	29.509	19.919	14.755	21.394	54.223	63.445	33.936	-29.509	32.153	0.738	36.886	-9.959	-10.513	-9.836	19.181	12.54		
310	30/Dec	Wednesday																			
311	31/Dec	Thursday	51.641	29.878	24.714	20.288	21.394	48.690	64.551	24.345	-42.973	35.546	-1.660	23.976	-1.660	4.426	-16.919	4.058	2.95		
312	01/Jan	Friday	58.650	37.255	37.255	25.083	21.394	57.174	64.182	34.673	-40.760	25.181	-7.931	30.431	5.533	2.213	-7.476	9.590	13.28		
313	02/Jan	Saturday	63.638	38.731	29.140	40.575	25.821	66.765	70.453	33.198	-45.002	47.829	-1.660	22.132	-1.660	-3.935	-7.377	7.38			
314	03/Jan	Sunday																			
315	04/Jan	Monday																			
AVG BATCH No J3			52.821	31.427	25.304	21.615	20.288	53.199													



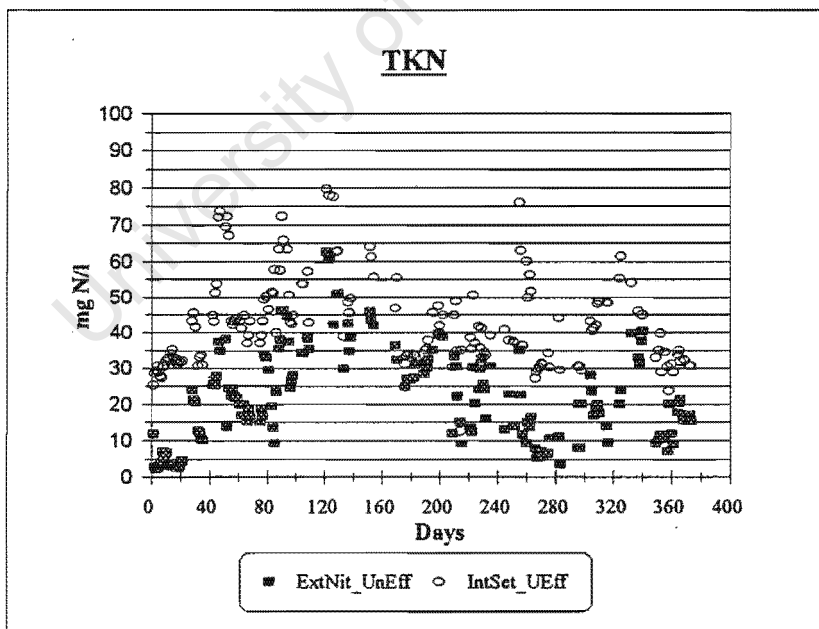
**Figure A1:** Daily unfiltered influent and RBCOD concentrations in BNRAS External Nitrification system.



**Figure A2:** Daily unfiltered external nitrifier, internal settler and final effluent COD concentrations in BNRAS External Nitrification system.



**Figure A3:** Daily unfiltered influent and effluent TKN concentrations in BNRAS External Nitrification system.



**Figure A4:** Daily unfiltered external nitrifier and internal settler effluent TKN concentrations in BNRAS External Nitrification system.

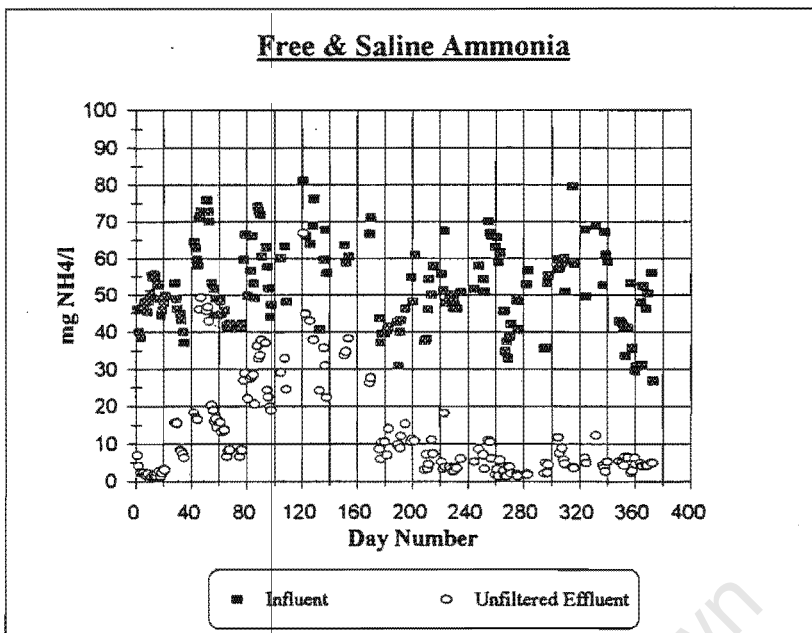


Figure A5: Daily unfiltered influent and effluent Ammonia concentrations in BNRAS External Nitrification system.

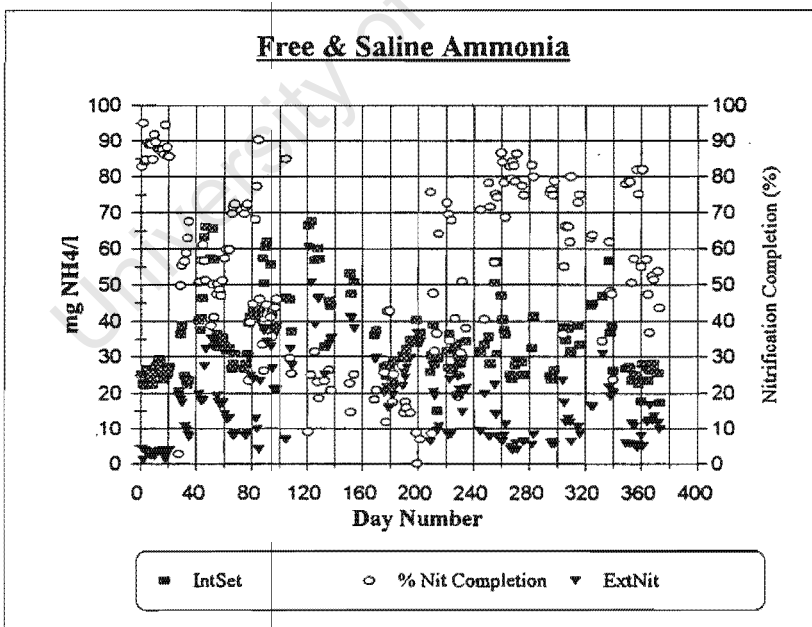
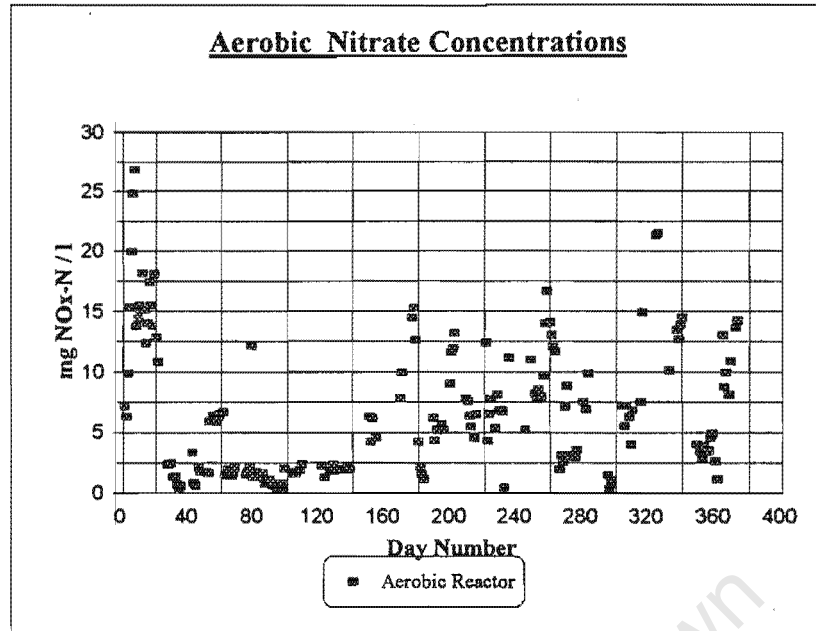
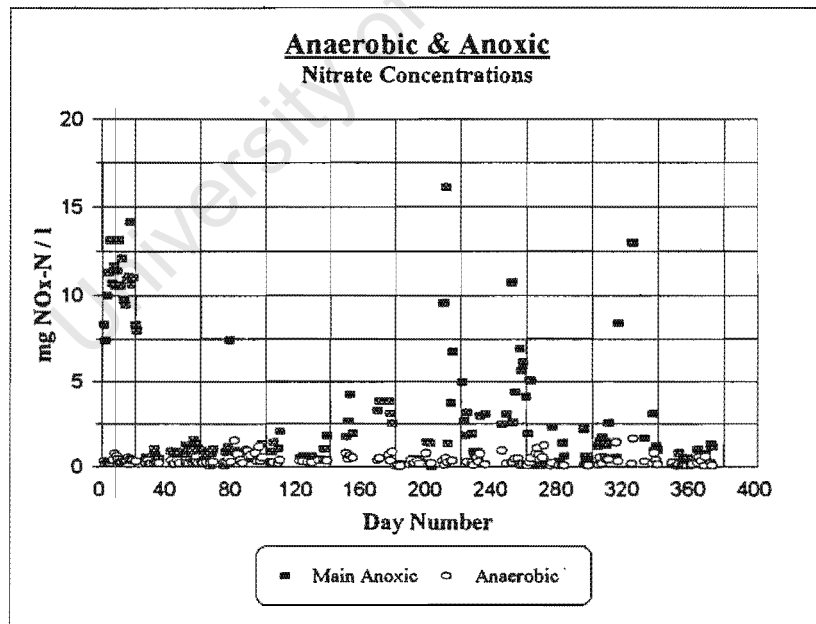


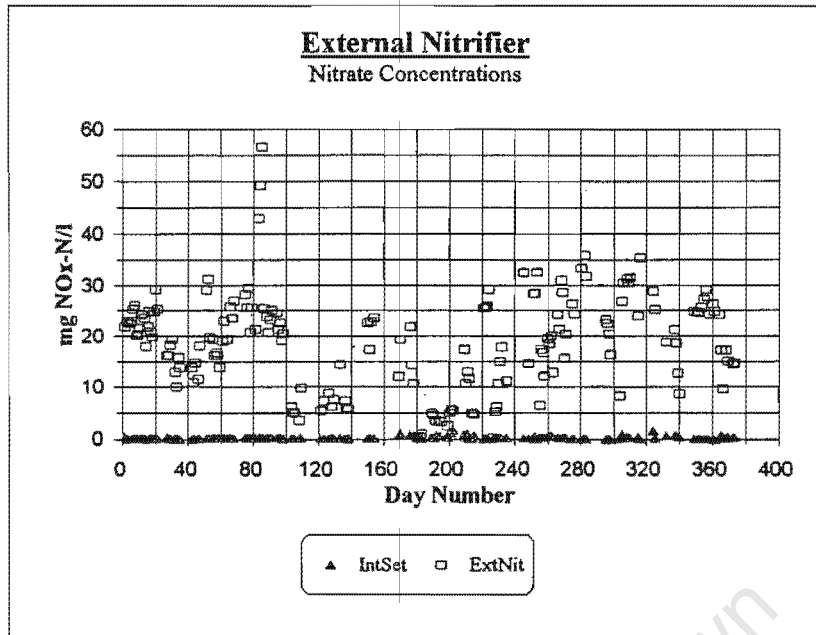
Figure A6: Daily unfiltered internal settler and external nitrifier effluent Ammonia concentrations in BNRAS External Nitrification system.



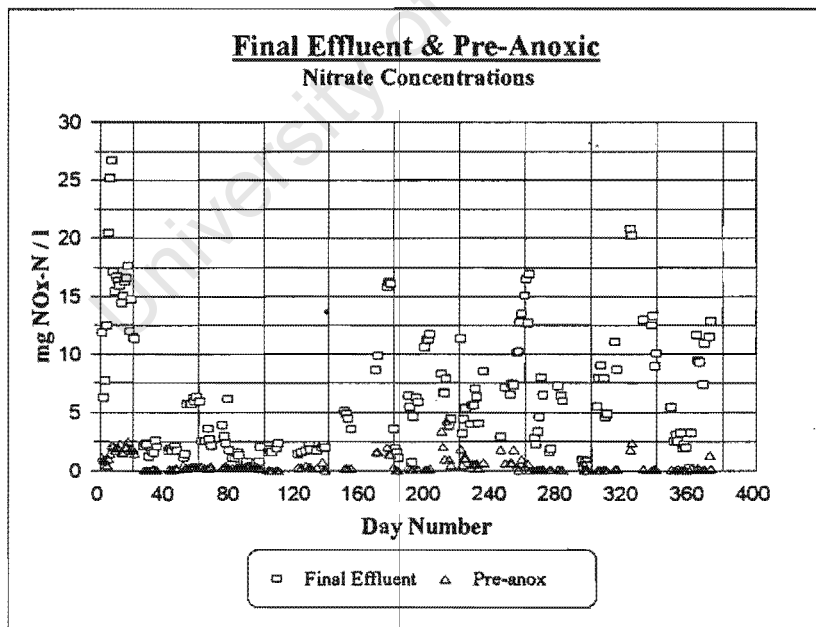
**Figure A7:** Daily filtered aerobic reactor nitrate concentration in BNRAS External Nitrification system.



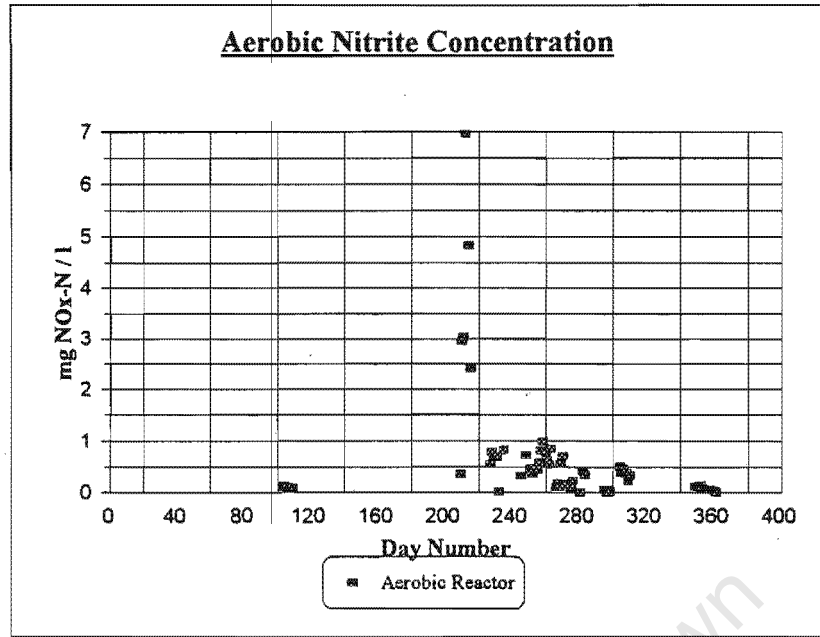
**Figure A8:** Daily filtered anaerobic and main anoxic reactor nitrate plus nitrite concentration in BNRAS External Nitrification system.



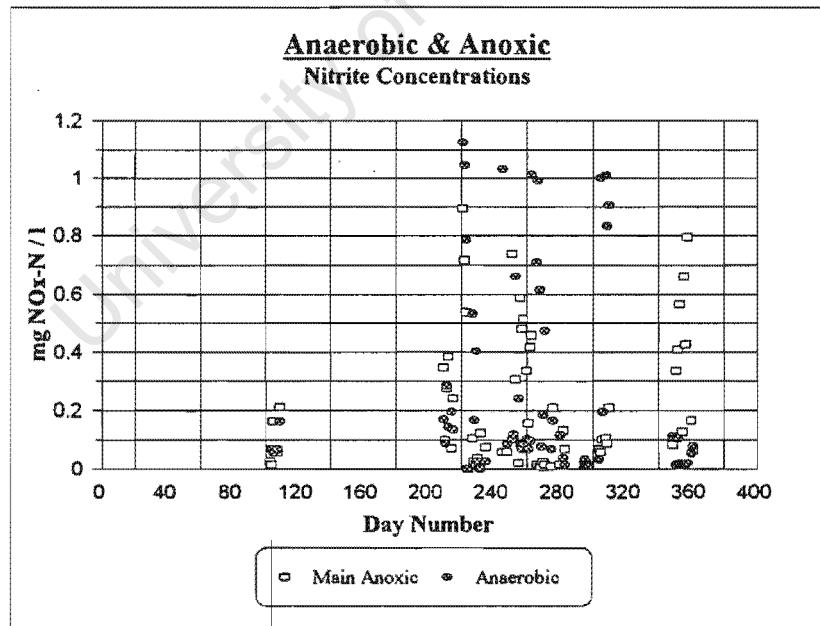
**Figure A9:** Daily filtered external nitrifier and internal settler nitrate concentrations in BNRAS External Nitrification system.



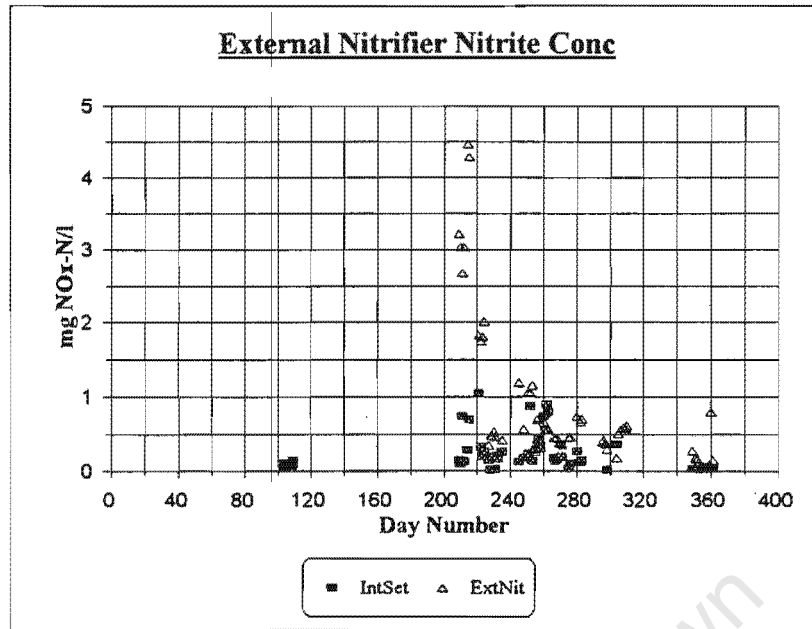
**Figure A10:** Daily filtered pre-anoxic and final effluent nitrate concentrations in BNRAS External Nitrification system.



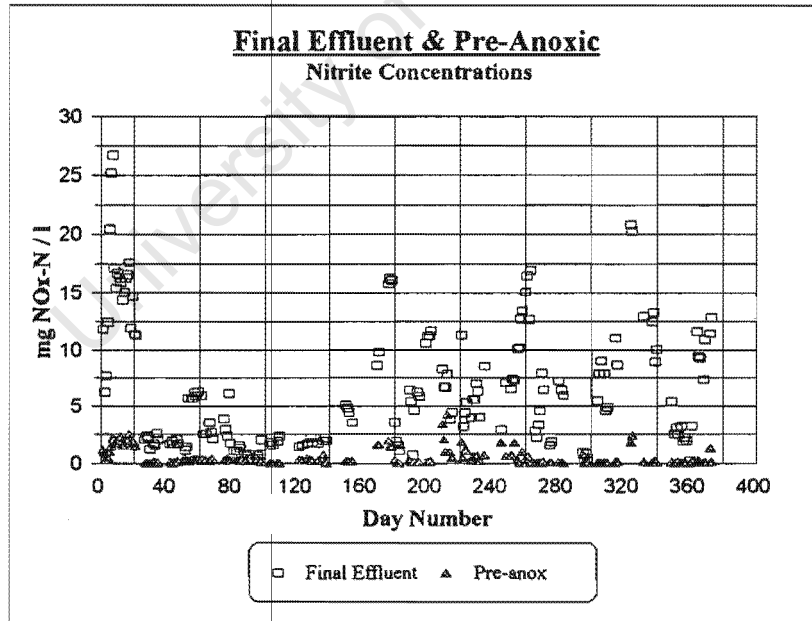
**Figure A11:** Daily filtered aerobic reactor nitrite concentration in BNRAS External Nitrification system.



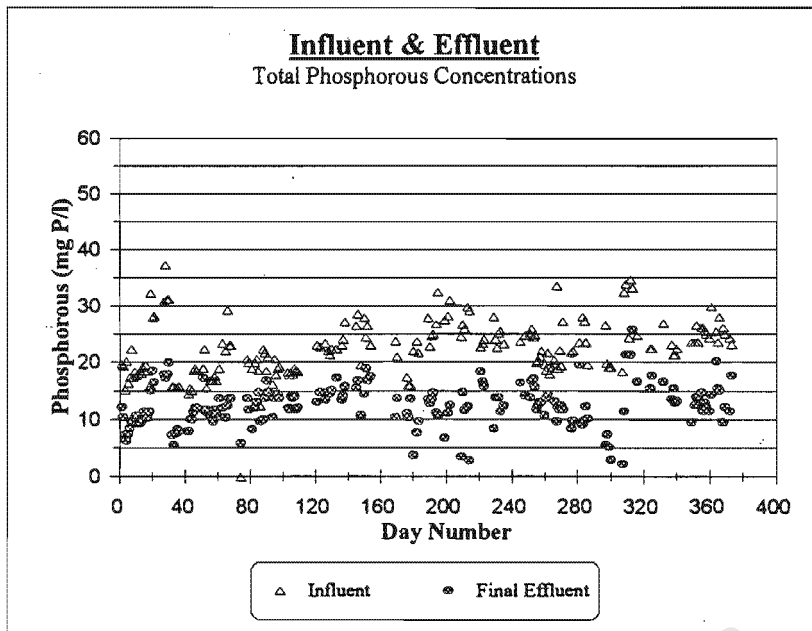
**Figure A12:** Daily filtered anaerobic and main anoxic reactor nitrite concentrations in BNRAS External Nitrification system.



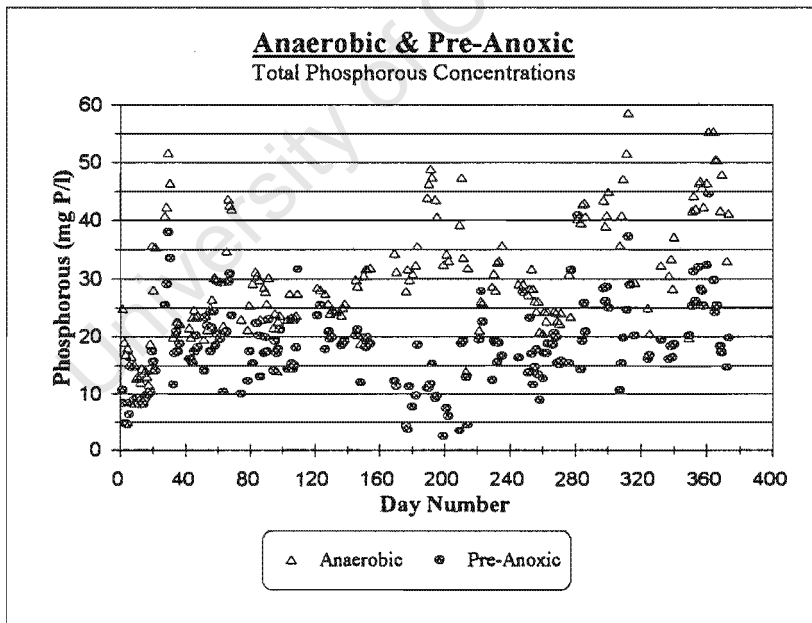
**Figure A13:** Daily filtered external nitrifier and internal settler nitrite concentrations in BNRAS External Nitrification system.



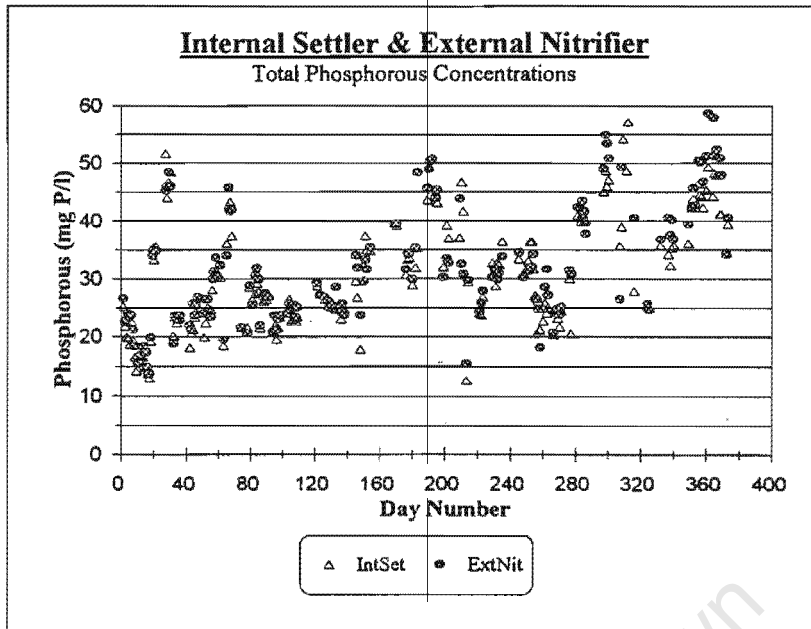
**Figure A14:** Daily filtered pre-anoxic and final effluent nitrite concentrations in BNRAS External Nitrification system.



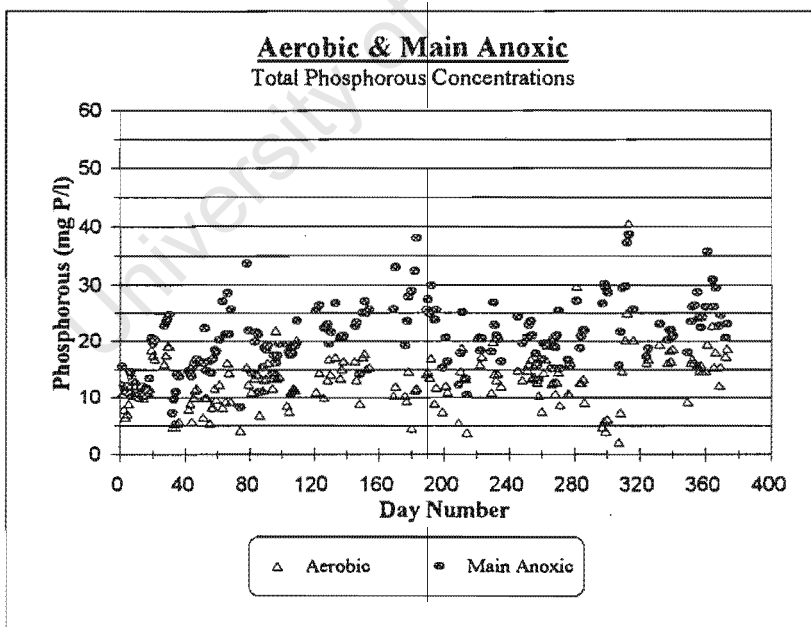
**Figure A15:** Daily unfiltered influent and final unfiltered effluent Total P concentration in BNRAS External Nitrification system.



**Figure A16:** Daily filtered anaerobic and pre-anoxic Total P concentrations in BNRAS External Nitrification system.



**Figure A17:** Daily filtered internal settler and external nitrifier Total P concentrations in BNRAS External Nitrification system.



**Figure A18:** Daily filtered aerobic and main anoxic Total P concentrations in BNRAS External Nitrification system.

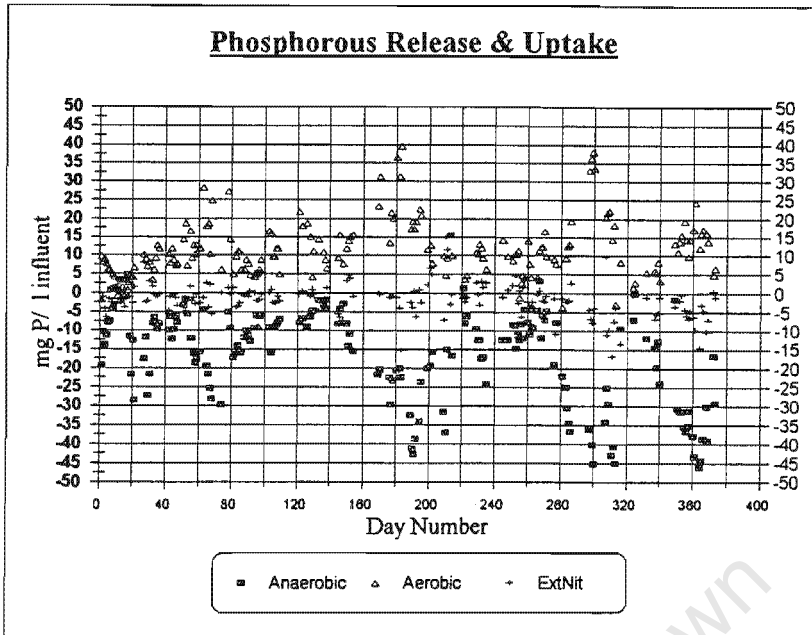


Figure A19: Daily filtered anaerobic, aerobic and external nitrifier Total P mass balance in BNRAS External Nitrification system.

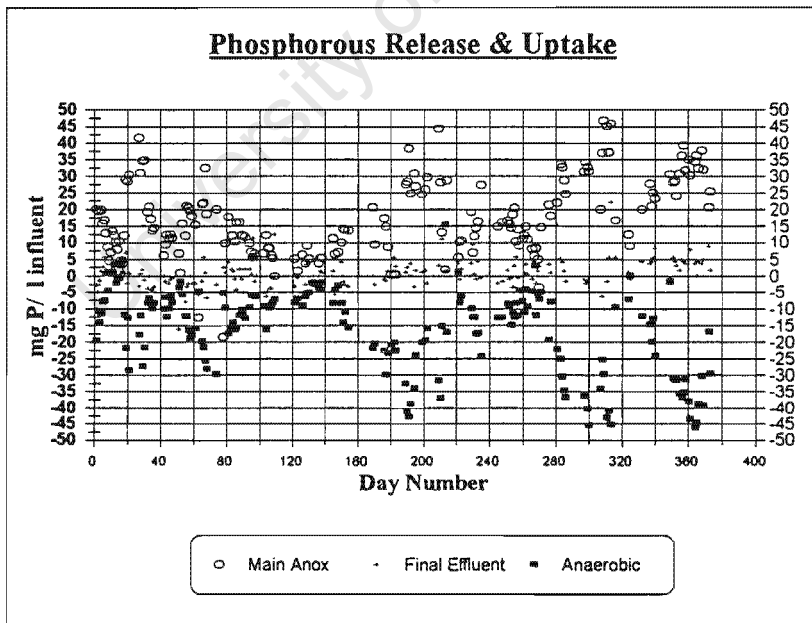


Figure A20: Daily filtered anaerobic, main anoxic and final effluent Total P mass balance in BNRAS External Nitrification system.

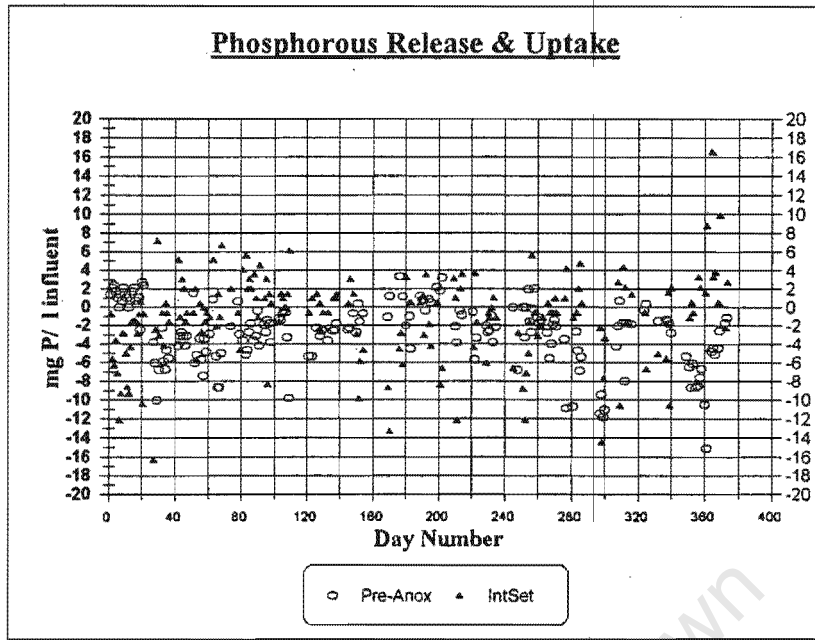


Figure A21: Daily filtered anaerobic, main anoxic and final effluent Total P mass balance in BNRAS External Nitrification system.

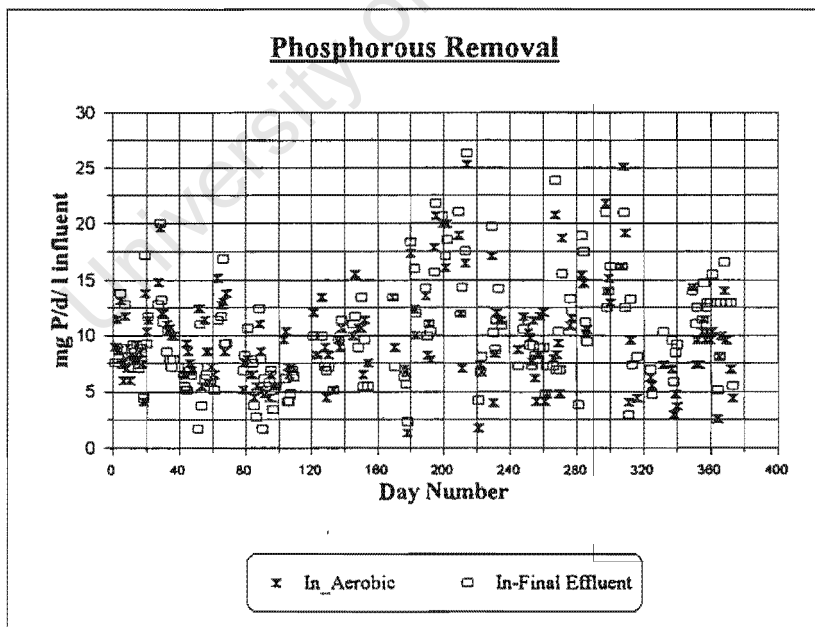


Figure A22: Daily Total P removal in BNRAS External Nitrification system.

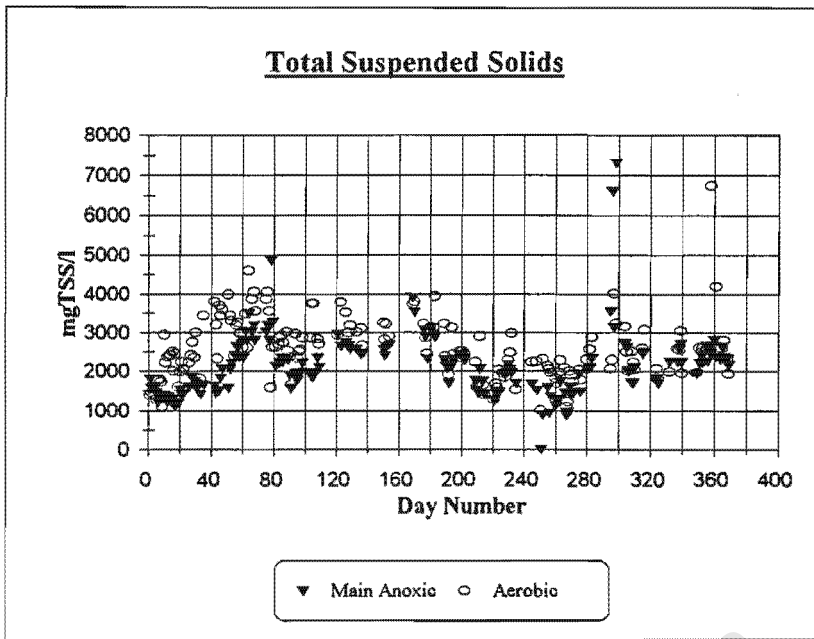


Figure A23: Daily aerobic and main anoxic Total Suspended Solids concentrations in BNRAS External Nitrification system.

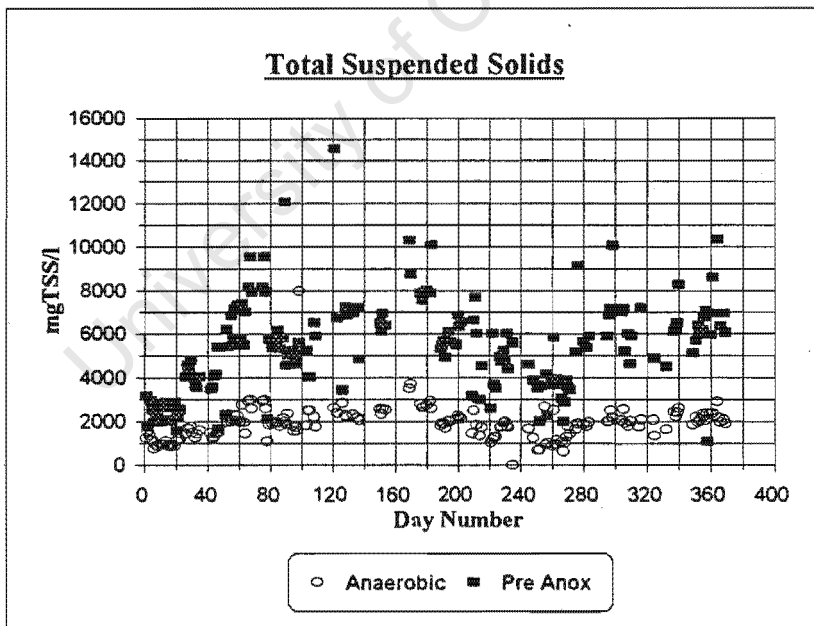
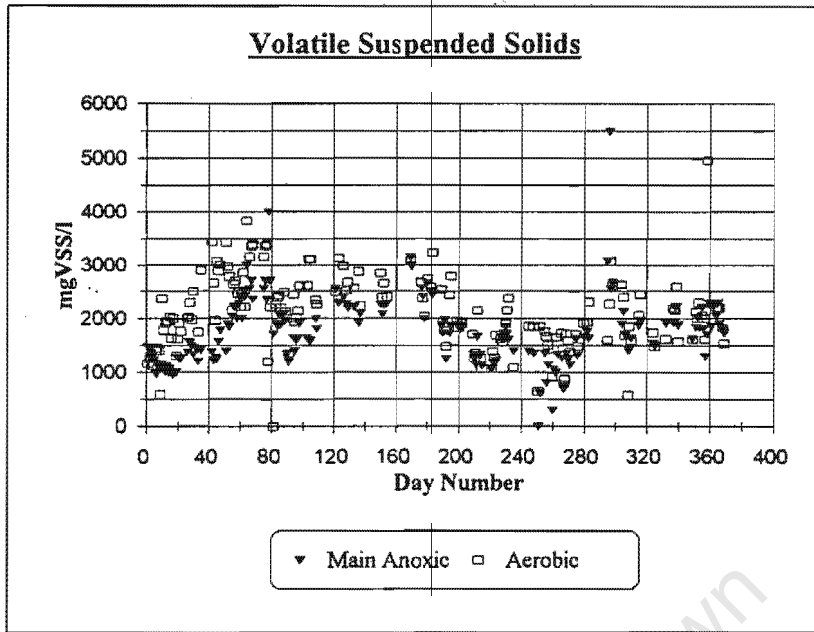
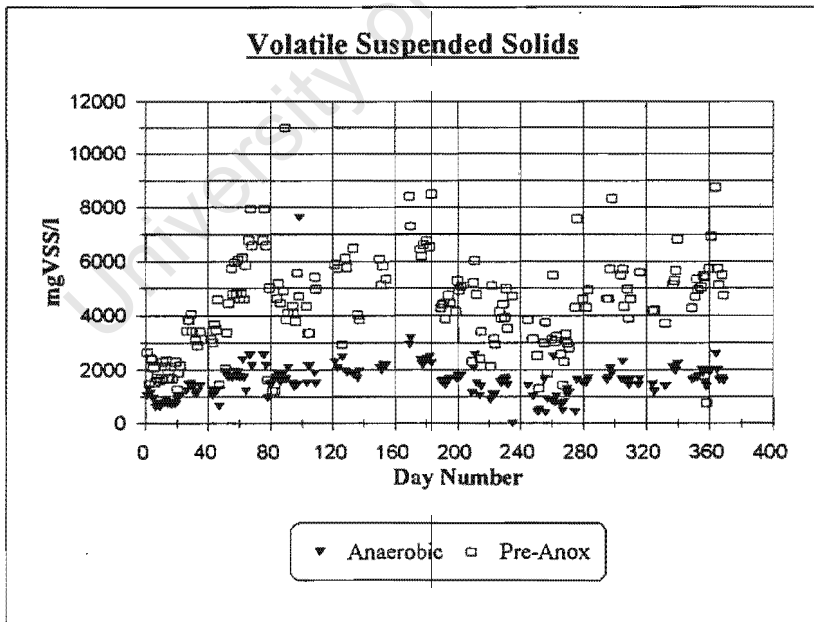


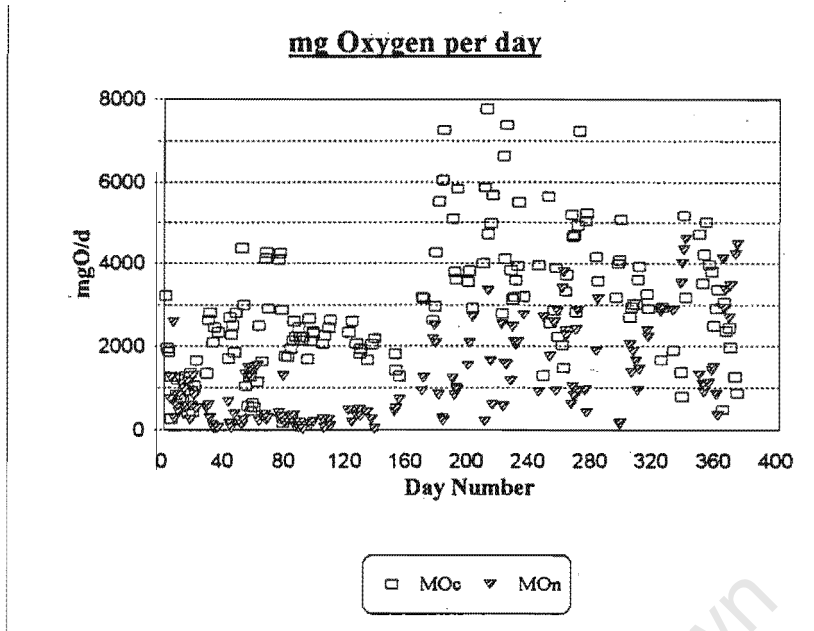
Figure A24: Daily anaerobic and pre-anoxic Total Suspended Solids concentrations in BNRAS External Nitrification system.



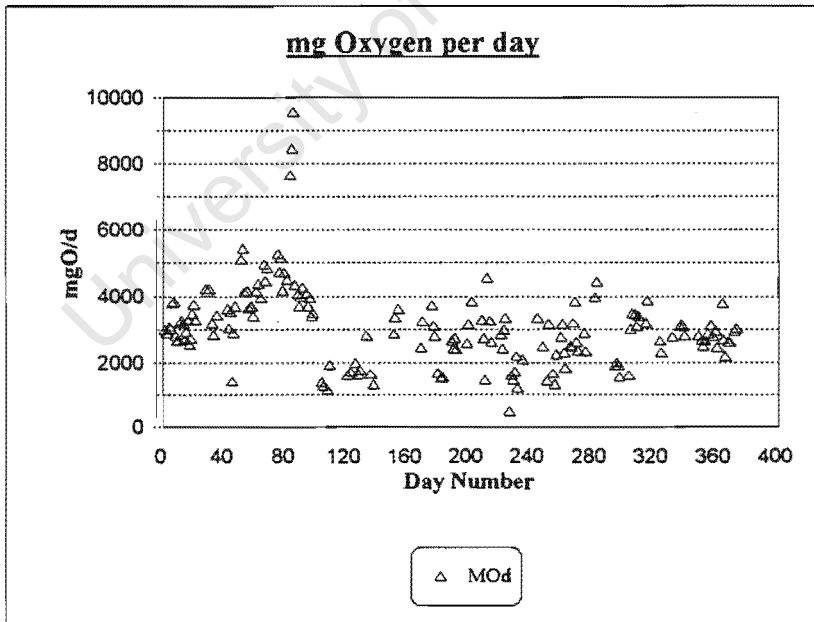
**Figure A25:** Daily aerobic and main anoxic Volatile Suspended Solids concentrations in BNRAS External Nitrification system.



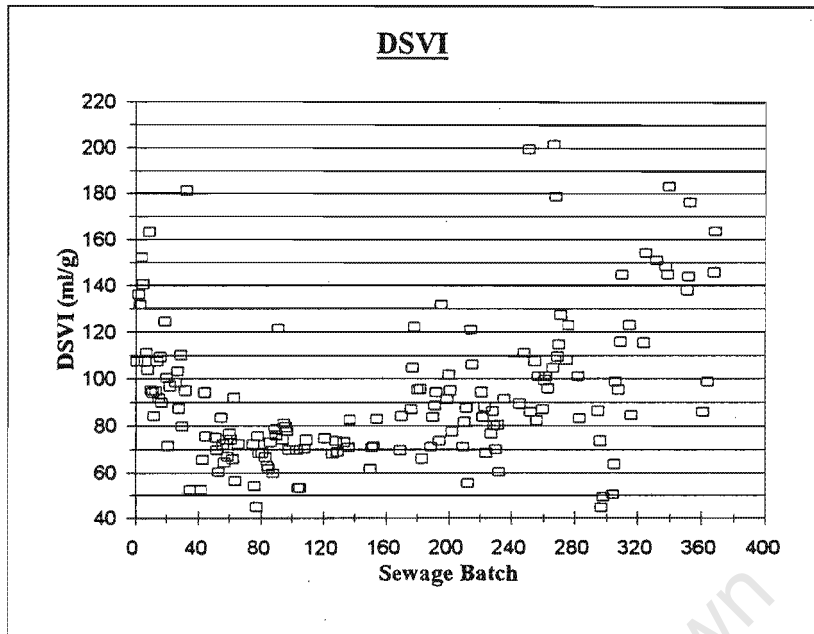
**Figure A26:** Daily anaerobic and pre-anoxic Volatile Suspended Solids concentrations in BNRAS External Nitrification system.



**Figure A27:** Daily carbonaceous and nitrification oxygen demand in BNRAS External Nitrification system.



**Figure A28:** Daily denitrification oxygen recovery in BNRAS External Nitrification system.



**Figure A29:** Daily aerobic reactor Diluted Sludge Volume Index in BNRAS External Nitrification system.

## **APPENDIX B**

- Nitrogen Mass Balance.
- COD Mass Balance.

University of Cape Town

**APPENDIX B**  
**NITROGEN AND COD MASS BALANCES**

In order to test the accuracy of the measured system response data, nitrogen and COD mass balances were performed on the system. These are discussed in detail and illustrated by an example using the data of sewage batch 32 of the external nitrification BNRAS system (see Table B1 and B2 below).

### 1. NITROGEN MASS BALANCE

The daily mass of nitrogen that enters the laboratory system in the form of the influent TKN and nitrate dose should be accounted for as follows:

- i) Nitrogen that is denitrified.
- ii) Nitrogen in the waste sludge.
- iii) Nitrogen utilized in the external nitrification system.
- iv) Nitrogen in the effluent i.e. TKN plus nitrate and nitrite.

#### 1.1 Mass of Nitrate Denitrified

In the external nitrification BNRAS system configuration (see figure 3.1) the mass of the nitrogen denitrified is calculated by carrying out a mass balance around the pre-anoxic, anaerobic and main anoxic reactors. If significant amounts of nitrite were generated it would have been necessary to split the nitrate and nitrite in order to produce an accurate calculation particularly for the COD mass balance. However, as there were no large amounts of nitrite produced during this investigation, the nitrate and nitrite can be added together and is indicated by the symbol  $\text{NO}_x$ .

The mass of nitrate and nitrite denitrified in the pre-anoxic, anaerobic, main anoxic reactors and final settler was calculated in the following way:

Mass of  $\text{NO}_x$  denitrified in the pre-anoxic reactor:

$$M_{\text{NO}_x \text{d pre-anox}} = s \cdot Q \cdot (\text{NO}_2 + \text{NO}_3)_{\text{eff}} - (s) \cdot Q \cdot (\text{NO}_2 + \text{NO}_3)_{\text{pre-anox}} \quad (\text{mg NO}_x\text{-N/d})$$

Mass of  $\text{NO}_x$  denitrified in the anaerobic reactor:

## B.2

$$MNO_{xd \text{ anaer}} = s.Q.(NO_2 + NO_3)_{\text{pre-anox}} - (1+s).Q.(NO_2 + NO_3)_{\text{anaer}} \quad (\text{mg } NO_x\text{-N/d})$$

Mass of  $NO_x$  denitrified in the main anoxic reactor:

$$MNO_{xd \text{ anox}} = q.Q.(NO_2 + NO_3)_{\text{Ext}} + n.Q.(NO_3)_{\text{dose}} + a.Q.(NO_2 + NO_3)_{\text{acr}} - (1+s-q).(NO_2 + NO_3)_{\text{IntSet}} - (1+s+n+a).Q.(NO_2 + NO_3)_{\text{anox}} \quad (\text{mg } NO_x\text{-N/d})$$

And mass of  $NO_x$  denitrified in the final settler

$$MNO_{xd \text{ Set}} = (1+s).Q.(NO_2+NO_3)_{\text{aer}} - Q.(NO_2+NO_3)_{\text{eff}} - s.Q.(NO_2+NO_3)_{\text{eff}} \quad (\text{mg } NO_x\text{-N/d})$$

- where:  $MNO_{xd}$  = mass of nitrite and nitrate denitrified in the pre-anoxic, anaerobic, or main anoxic reactor respectively per day (mg  $NO_x$ -N/d)
- pre-anox = indicates  $NO_x$  concentration in pre-anoxic reactor
- anaer = indicates  $NO_x$  concentration in pre-anoxic reactor
- anox = indicates  $NO_x$  concentration in main anoxic reactor
- aer = indicates  $NO_x$  concentration in aerobic reactor
- eff = indicates  $NO_x$  concentration in effluent
- Ext = indicates  $NO_x$  concentration in external nitrifier
- IntSet = indicates  $NO_x$  concentration in internal settling tank
- a,s = recycle ratios equal to 2 and 1 respectively
- q,n = flow ratios of external nitrifier and nitrate dose respectively

Substituting the appropriate average values for steady state 36 of the external nitrification BNRAS system you get

$$MNO_{xd \text{ pre-anox}} = 0.5*30.(0.03 + 2.89) - 0.5*30.(0.05 + 0.08)$$

$$= 42 \quad \text{mgNO}_x\text{-N/d}$$

$$MNO_{xd \text{ anaer}} = 0.5*30.(0.05 + 0.08) - (1+0.5).30.(0.04 + 0.10)$$

$$= -0.3 \quad (\text{here set to zero}) \quad \text{mgNO}_x\text{-N/d}$$

$$MNO_{xd \text{ anox}} = 1.07*30.(0.13 + 26.05) + 0 + 1*30(0.09 + 3.82) + (1+0.5-1.07).30.(0.03 + 0.13) - (1+0.5+0+1).30.(0.43 + 0.37)$$

### B.3

$$\begin{aligned}
 &= 896 \quad \text{mgNO}_x\text{-N/d} \\
 \text{MNO}_{\text{xd Set}} &= (1+0.5).30.(0.09 + 3.82) - 30.(0.03 + 2.89) - 0.5*30.(0.03 + 2.89) \\
 &= 45 \quad \text{mgNO}_x\text{-N/d}
 \end{aligned}$$

Therefore the total mass of nitrate and nitrite ( $\text{NO}_x$ ) denitrified

$$\begin{aligned}
 \text{MNO}_{\text{xd}} &= \text{MNO}_{\text{xd pre-anox}} + \text{MNO}_{\text{xd anear}} + \text{MNO}_{\text{xd Set}} + \text{MNO}_{\text{xd anox}} \\
 &= 42 + 0 + 45 + 896 \\
 &= 983 \quad \text{mgNO}_x\text{-N/d}
 \end{aligned}$$

#### 1.2 Nitrogen in Waste Sludge

The mass of N in the waste sludge is given by the product of the TKN/VSS ratio ( $f_n$ ) and the mass of VSS wasted per day.

$$\begin{aligned}
 \text{MX}_n &= f_n \cdot \text{MX}_v + Q_{\text{ws}} \cdot (\text{NO}_2 + \text{NO}_3)_{\text{aer}} \\
 \text{where: } f_n &= (215.4)/(2332.75) = 0.09 \quad \text{and} \quad Q_{\text{ws}} = 20/10 = 2 \text{ l/d}
 \end{aligned}$$

Substituting the appropriate values gives

$$\begin{aligned}
 \text{MX}_n &= 0.09 \cdot (2.2332.75) + 2 \cdot (0.09 + 3.82) \\
 &= 438 \quad (\text{mg N/d})
 \end{aligned}$$

#### 1.3 Mass of Nitrogen Utilized in External Nitrifier

The mass of nitrogen utilized in the external nitrifier is the product of the flow to the external nitrifier and the difference in the nitrate, nitrite and TKN concentrations entering and leaving the external nitrifier:

$$\begin{aligned}
 \text{MN}_{\text{Ext}} &= q \cdot Q [(\text{NO}_2 + \text{NO}_3 + \text{TKN})_{\text{IntSet}} - (\text{NO}_2 + \text{NO}_3 + \text{TKN})_{\text{Ext}}] \\
 &= 1.07 \cdot 30 [(0.03 + 0.13 + 32.19) - (0.13 + 26.05 + 11.57)] \\
 &= -172.8 \text{ (here set to zero)} \quad (\text{mg N/d})
 \end{aligned}$$

#### 1.4 Mass of Nitrogen in Effluent

The mass of N in the effluent is the product of the daily flow rate and the sum of the effluent TKN, nitrate and nitrite concentrations:

$$\begin{aligned}
 \text{MN}_{\text{eff}} &= Q \cdot (\text{N}_{\text{te}} + \text{NO}_{2 \text{ eff}} + \text{NO}_{3 \text{ eff}}) \\
 &= 30 \cdot (7.98 + 0.03 + 2.89)
 \end{aligned}$$

$$= 327 \quad (\text{mg N/d})$$

### 1.5 Nitrogen Mass Balance

The % N mass balance is then given by:

$$\% \text{ N Balance} = 100 \cdot (MNO_{xd} + MX_n + MN_{Ext} + MN_{eff}) / (MN_{in})$$

where:  $MN_{in}$  is the mass of TKN in the influent given by the product of the influent TKN concentration and the daily flow rate ( $MN_{in} = N_{in} \cdot Q$ )

Substituting the values calculated above:

$$\begin{aligned} \% \text{ N Balance} &= 100 \cdot (983 + 438 + 0 + 327) / (59.06 \cdot 30) \\ &= 99 \% \end{aligned}$$

## 2. **COD MASS BALANCE**

The daily mass of COD ( $MS_d$ ) that enters the system should be accounted by:

- i) The mass oxygen demand required per day for degradation of carbonaceous material in the aerobic reactor.
- ii) The equivalent mass oxygen demand per day by denitrification of nitrate and nitrite.
- iii) The COD utilized in the external nitrifier.
- iv) The COD mass in the waste sludge.
- v) The COD mass in the effluent.

### 2.1 Carbonaceous Oxygen Demand

The total amount of oxygen utilized in the aerobic reactor is made up of the nitrification oxygen demand and the carbonaceous oxygen demand. Since nitrification, if any, does not consume any of the influent COD, the oxygen demand due to nitrification must be subtracted from the total measured oxygen demand. Stoichiometrically, the oxygen requirements for nitrification of ammonia to nitrite (by *nitrosomonas*) and to nitrate (by both *nitrosomonas* and *nitrobacter*) is different with the former being slightly less (i.e. 3.43 mgO/mgN and 4.57 mgO/mgN generated from ammonia). As already stated however, there was never excessive nitrite build up in the system which meant that the nitrite

## B.5

could be added to the nitrate and called  $\text{NO}_x$ . The calculation for the carbonaceous oxygen demand is as follows:

Provided that the nitrogen mass balance is acceptable, the mass of nitrogen generated in the systems  $\text{MS}_{\text{no}}$  is found by calculating the mass balance of  $\text{NO}_x$  around the aerobic reactor.

$$\begin{aligned}\text{MS}_{\text{no}} &= \text{MNO}_{x \text{ aer}} \\ &= (1 + s + n + a) \cdot Q \cdot [(\text{NO}_2 + \text{NO}_3)_{\text{acr}} - (\text{NO}_2 + \text{NO}_3)_{\text{anox}}]\end{aligned}$$

Substituting the appropriate values for sewage batch 29 of the external nitrification BNRAS system:

$$\begin{aligned}&= (1 + 0.5 + 0 + 1) \cdot 30[(0.09 + 3.82) - (0.43 + 0.37)] \\ &= 259 \quad \text{mgN/d}\end{aligned}$$

From the mass of nitrate generated, the nitrification oxygen demand ( $\text{MO}_n$ ) is given by:

$$\begin{aligned}\text{MO}_n &= 4.57 \cdot (\text{MS}_{\text{no}}) \\ &= 4.57 \cdot (259) \\ &= 1182 \quad \text{mgO/d}\end{aligned}$$

where: 4.57 is the mass of oxygen utilized per mg  $\text{NH}_4\text{-N}$  nitrified.

From the measured OUR (mgO/l/h) the mass carbonaceous oxygen demand is given by:

$$\begin{aligned}\text{MO}_c &= (\text{OUR}) \cdot V_a \cdot (24) - \text{MO}_n \\ \text{where } &V_a \text{ is the volume of the aerobic reactor (l)} \\ &= 35.89 \cdot 24 \cdot 6 - 1182 \\ &= 3986 \quad \text{mgO/d}\end{aligned}$$

### 2.2 Equivalent Oxygen Demand for Denitrification

The equivalent oxygen demand for denitrification  $\text{MO}_d$  is given by:

$$\begin{aligned}\text{MO}_d &= 2.86(\text{MNO}_{x \text{ d}}) \\ &= 2.86 \cdot (983) \\ &= 2810 \quad \text{mgO/d}\end{aligned}$$

## B.6

### 2.3 Mass of COD Utilized in the External Nitrifier

The COD utilized in the external nitrifier  $MS_{Ext}$  is given by the product of the flow to the external nitrifier and the difference in the COD concentrations entering and leaving the external nitrifier:

$$\begin{aligned}MS_{Ext} &= q \cdot Q(\text{COD}_{IntSet} - \text{COD}_{Ext}) \\ &= 1.07 \cdot 30(159.37 - 77.05) \\ &= 2634 \quad \text{mgCOD/d}\end{aligned}$$

### 2.4 Mass of COD in Waste Sludge

The COD of the waste sludge mass is given by the COD/VSS ratio times the mass of VSS wasted per day i.e.

$$\begin{aligned}MS_{ws} &= f_{cv} \cdot (MX_v) \\ \text{where: } f_{cv} &= (3056.8)/(2332.75) = 1.31 \\ MS_{ws} &= 1.31 \cdot (2.2332.75) \\ &= 6113.6 \quad \text{mgCOD/d}\end{aligned}$$

### 2.5 Mass of COD in Effluent

The mass of COD in the effluent  $MS_{te}$  is given by:

$$\begin{aligned}MS_{te} &= Q \cdot S_{te} \\ &= 30 \cdot (52.69) \\ &= 1580.8 \quad \text{mgCOD/d}\end{aligned}$$

### 2.6 COD Mass Balance

The % COD mass balance is then given by:

$$\% \text{ COD Balance} = 100(MO_c + MO_d + MS_{Ext} + MS_{ws} + MS_{te})/MS_{ti}$$

where:  $MS_{ti}$  is the total COD mass fed to the system.

Substituting the values calculated above:

$$\begin{aligned}\% \text{ COD Balance} &= 100(3986 + 2810 + 2634 + 6114 + 1581)/(704 \cdot 30) \\ &= 81 \%\end{aligned}$$

Average of Sewage Batch	Nitrogen Mass Balance										Carbonaceous Mass Balance																
	NO3 Dosage mg/NO3/d	Nitrate recy mg/d	NO3 denitr <sub>max</sub> mg/d	NO3 denitr <sub>min</sub> mg/d	NO3 denitr <sub>avg</sub> mg/d	NO3 denitr <sub>std</sub> mg/d	Tot Denitr (mg/d)	N in Waste (mg/d)	N in Eff (mg/d)	TKN <sub>Leak</sub> (mg/d)	Tot TKN <sub>Leak</sub> (mg/d)	Inf TKN (mg/d)	MB % (mg/d)	Influent mgCOD	Effluent mgCOD	Waste mgCOD	ExtNit mgCOD/d	Oxygen mg/d	MOJ Recov mg/d	MOC mg/d	MOJ mg/d	MOC mg/d	COD leavin mgCOD	MBCOD %	OUR mg/d		
1	500		838	153	9		1000	279	262		1541	1845	84	16200	1212	3886	2535	2376	2859	2376	0	5235	12868	79	33		
2	500		726	316	19		1061	361	397	162	1982	1849	107	12236	810	4835	1670	1656	3035	633	1023	3668	10983	96	23		
3	500		869	212	21	60	1161	408	312	111	1992	1878	106	14104	414	7155	2513	1800	3321	998	802	4319	14401	102	25		
4	550		1401	39		10	1450	341	833	214	2837	3204	89	26981	4033	9641	5178	2736	4146	2262	474	6408	25260	94	38		
5	500		1124	37			1160	478	425	385	2448	2856	86	28861	2105	6298	4241	2362	3319	2321	41	3640	18284	63	31		
6	500		1128	34			1162	821	838	448	3268	3737	87	26009	3021	9730	4523	2513	3323	2313		5835	23108	89	35		
7	500		1463	26		12	1501	734	1865	835	4935	4146	119	27838	3109	5779	4526	3200	4293		245	7248	20662	74	44		
8	500		1239	97		4	1360	642	1050	182	3233	2961	109	26824	3063	10764	2902	2275	3889	1127	1148	5016	21746	81	32		
9	500		1615	50			1665	572	714		2951	3281	90	28288	2557	10608	3182	4066	4761	3774	291	8535	24882	88	56		
10																											
11	500		2089	43		21	2153	458	1108		3720	3558	105	26903	2840	8375	3481	2712	6158	2318	394	8477	23174	86	38		
12	250		1351	8		5	1364	533	1465		3362	3481	97	25861	2940	7190	4339	2324	3901	2270	54	6171	20640	80	32		
13	250		470	39			510	644	1538	536	3228	3834	84	27285	3942	9541	2760	2513	1458	2356	156	3814	26056	74	35		
14																											
15																											
16	250		539	24		16	579	746	1844	265	3435	2947	117	29920	3120	10125	5100	2804	1657	2480	325	4137	22482	75	39		
17	250		686	31		8	725	714	1358	234	3031	3009	101	26440	3200	8706	4100	2282	2073	1886	397	3958	19958	75	32		
18	250		493	35		0	528	518	1499	158	2704	3293	82	24800	3480	8750	1800	2232	1511	2028	204	3539	17569	71	31		
19																											
20	500		1076	65		37	1177	557	1280		3015	2902	104	19584	1897	8330	1958	2074	3367	1343	730	4710	16896	86	29		
21																											
22	500		900	114		3	1017	275	1260	75	2628	3028	87	17640	1590	8220	2170	4248	2908	3159	1089	6067	18047	102	30		
23	500		687	110			797	502	641		1940	2334	83	19557	1572	6697	1011	6192	2280	4978	1214	7257	16537	83	43		
24	500	159	773	71		18	862	325	604		1888	2398	79	23079	2145	6475	2502	5616	2464	4604	1012	7068	18190	79	39		
25	500	343	940	166		8	1114	325	778	70		2867	80	17238	1704	6003	2887	5616	3187	3489	2127	6676	17269	100	39		
26	500	265	883	113		44	1042	266	518		1825	2429	75	21838	1913	4429	2360	6469	2980	5958	511	8938	17640	81	45		
27	500	196	579	80		42	701	335	410		1446	2091	69	23403	2227	5088	2180	6028	2005	4502	1526	6507	16002	68	42		
28	500	259	688	88		105	882	323	482		1686	2221	76	18360	1971	5173	940	4962	2053	3512	1450	6033	14117	77	14		
29	500	353	521	196			718	303	677	75.4	2452	2876	85	19619	1819	4713	1996	5402	2522	2672	2730	4725	13255	68	38		
30	500	175	872	58		19	949	297	272		1518	1817	84	21013	1573	5059	2283	6244	2714	4990	1254	7704	16618	79	43		
31	500	251	1293	99		72	1464	362	300		2126	2640	81	24713	1670	6193	777	6394	4186	3893	2501	8079	16719	68	44		
32	500	28	628	6		14	648	478	239		1365	1699	80	20580	1260	6980	2688	4165	1853	4165	0	6018	16946	82	29		
33	500	191	916	111			1047	665	561		2273	2438	93	22029	1603	7497	1847	4890	2995	3218	1672	6213	17160	78	34		
34	500	528	627	248			875	763	838	180	2657	2821	94	25394	1968	5758	1665	5080	2504	2202	2877	4706	14096	56	35		
35	500	408	788	166		107	1061	467	514		2042	2462	83	20433	1544	6272	1380	6757	3035	2638	4119	5671	14868	73	47		
36	500	116	896	42		44	982	439	327		1748	1772	99	21128	1381	6114	2634	5168	2809	3986	1182	6795	17124	81	36		
37	500	336	889	122		28	1039	450	453		1942	1729	112	19665	1815	6700	1888	5027	2972	2089		5061	15464	79	35		
Average 1	500		811	227	16	20	1074	349	324	91	1838	1857	99	14180	812	5292	2239	1944	3072	1336	608	4408	12751	90	27		
Averages above are for sewage batches 1 to 3 i.e. Configuration 1																											
Average 2	400		1135	39			1180	600	1212	271	3263	3359	97	27168	3118	8792	3844	2668	3374	2303	339	5731	21485	79	37		
Averages above are for sewage batches 4 to 19 i.e. Configuration 2																											
Average 3	500	251	825	113	3	9	947	357	821	61	2185	2657	82	19379	1753	6849	2142	5418	2710	4057	1361	6767	17511	91	38		
Averages above are for sewage batches 22 to 25 i.e. Configuration 3																											
Average 4	500	255	800	111		40	951	429	466	78	1923	2250	86	21516	1745	5831	1887	5549	2719	3652	1897	6371	15834	74	39		
Averages above are for sewage batches 26 to 37 i.e. Configuration 4																											
Average 5	443	254	938	94	3	22	1055	481	802	147	2484	2700	91	22620	2178	7096	2688	4006	3270	2927	1112	5943	17907	80	36		
Averages above are for sewage batch 1 to 37 i.e. average over entire investigation																											

B7

## APPENDIX C

- Average Sewage Batch Results of External Nitrification System.
- $f_{S,up}$  and  $f_{XBG,P}$  Calculations for each Sewage Batch

University of Cape Town

Average of Sewage Batch	Carbonaceous Oxygen Demand						BRCOD Flow			COD		Free & Soluble Ammonia					Total Kjeldahl Nitrogen					Nitrogen				Measured Nitrite Values mgNO <sub>2</sub> -N/L				Measured Nitrate Values mgNO <sub>3</sub> -N/L					
	Sys. Inf mgCOD	Reactor 3 mgCOD	Fin. UEff mgCOD	Est. FEff mgCOD	InSet FEff mgCOD	Fin. FEff mgCOD	Flow. Inf. mgCOD	Flow. Eff. mgCOD	BRCOD mgCOD	Removal %	Influent mgN/L	Fin. UEff mgN/L	EstN <sub>2</sub> UE mgN/L	InSet UE mgN/L	Influent mgN/L	Reactor 3 mgN/L	Fin. UEff mgN/L	EstN <sub>2</sub> UE mgN/L	InSet UE mgN/L	Removal %	Anaerobic	Main_Aoo	Pre_Aoo	Acrobie	Fin. FEff	InSet FEff	EstN <sub>2</sub> FE	Anaerobic	Main_Aoo	Pre_Aoo	Acrobie	Fin. FEff	InSet FEff	EstN <sub>2</sub> FE	
1	810	1940	41	79	163			92	93	42	3	3	23	67	132	6	6	28	24	0.27	0.57	0.99	7.76	8.63	0.34										
2	612	2418	41	46	107		142	40	103	93	31	2	26	67	133	1	4	31	78	0.42	11.42	1.81	17.01	17.61	0.24										
3	703	1378	33	33	116			92	97	47	3	3	26	69	188	3	4	32	63	0.37	9.49	1.77	13.87	12.38	0.21										
4	475	3836	101	82	185		148	59	89	85	49	16	18	32	66	234	19	22	42	74	0.23	0.44	0.06	2.14	2.00	0.29									
5	722	1519	53	63	146	38		141	100	41	93	41	7	9	24	59	171	9	11	32	83	0.23	0.66	0.13	0.81	1.96	0.18								
6	630	1892	76	81	172	73		64	27	37	88	61	17	18	41	81	210	19	26	48	78	0.25	0.60	0.11	1.62	1.81	0.21								
7	696	2211	78	64	164	73		77	20	57	89	73	47	32	63	91	391	47	21	72	53	0.26	0.92	0.21	1.81	1.62	0.24								
8	671	4206	77	83	149	59		141	39	102	89	50	19	18	36	68	216	20	22	46	63	0.23	1.06	0.33	3.27	3.20	0.34								
9	707	4242	64	37	107			167	24	143	91	42	8	29	70	227	15	17	40	78	0.28	0.63	0.23	1.71	2.83	0.34									
10																																			
11	673	3530	71	73	142	33		154	44	110	89	53	21	14	37	76	191	25	21	47	69	0.54	1.39	0.32	2.83	2.47	0.37								
12	647	2876	74	82	169	48		160	43	92	89	59	28	29	48	81	211	37	25	54	17	0.68	0.43	0.33	0.82	0.74	0.33								
13	682	3816	99	101	156	53		162	53	109	86	58	29	18	44	90	254	26	26	52	60	0.30	1.37	0.03	1.94	1.94	0.26								
14																																			
15																																			
16	748	4030	78	89	191		117	64	72	90	74	36	53	67	101	228	67	62	79	26	0.23	0.39	0.30	1.78	1.31	0.26									
17	661	3488	80	80	163	62		163	39	92	88	62	26	39	32	86	282	40	43	61	15	0.22	0.36	0.31	2.01	1.87	0.29								
18	620	3508	87	117	153	64		136	58	78	86	61	30	35	43	76	223	35	39	48	14	0.39	1.21	0.30	2.06	2.06	0.22								
19																																			
20	653	3233	63	83	144	57		136	34	102	90	61	36	40	50	80	281	38	44	60	26	0.64	1.66	0.20	3.73	4.50	0.26								
21																																			
22	588	4110	53	87	169	50		134	28	63	91	69	27	30	37	84	129	33	24	51	28	0.48	3.39	1.62	8.88	9.25	1.02								
23	632	3249	32	86	113	42		122	37	86	92	40	9	19	27	61	240	19	27	32	73	0.31	1.46	0.73	7.26	8.06	0.46								
24	769	2227	72	72	148	52		124	91	41	11	26	31	63	182	15	31	38	53	0.25	0.27	0.16	3.26	4.90	0.38										
25	575	3001	17	57	129	47		108	38	71	90	55	11	35	37	70	199	15	39	45	72	0.23	1.08	0.15	11.42	11.24	1.21								
26	729	2214	64	97	171	41		121	38	82	91	41	5	13	24	64	124	9	18	30	78	0.23	7.85	2.05	6.26	6.31	0.63								
27	780	2344	74	110	178	54		125	44	70	90	51	5	18	30	70	160	8	23	28	80	0.39	2.07	0.75	6.33	5.69	0.73								
28	612	2387	66	111	141		102	43	58	89	53	6	13	32	74	152	9	19	29	78	0.27	4.41	0.92	8.64	6.11	0.74									
29	634	2358	61	113	175		135	26	100	91	65	6	11	42	96	139	8	18	36	76	0.24	4.42	0.41	12.38	13.49	0.53									
30	700	2329	52	97	169	39		119	33	84	93	40	2	3	26	41	144	3	7	30	83	0.64	0.49	0.08	4.13	3.87	0.28								
31	824	2097	56	119	144	26		160	36	122	93	55	2	7	37	88	173	7	7	37	89	0.08	0.78	0.09	8.27	6.36	0.18								
32	686	3480	42	69	153		159	29	121	94	45	3	6	23	57	228	7	14	20	86	0.13	0.94	0.24	0.94	0.64	0.03									
33	734	2749	52	101	159	56		143	39	104	93	60	8	12	26	81	328	11	20	43	77	0.55	1.46	0.11	6.26	7.39	0.50								
34	846	2879	66	134	188	59		162	47	113	92	62	8	21	45	94	364	10	28	37	70	0.72	9.22	1.49	17.61	18.02	0.91								
35	681	3126	51	79	122		133	31	101	92	60	4	20	40	82	220	6	26	44	79	0.39	1.38	0.14	13.60	11.22	0.59									
36	704	3037	53	77	159	73		127	31	102	93	41	3	7	23	59	213	8	12	32	82	0.10	0.77	0.08	3.82	2.89	0.12								
37	656	3350	60	82	141	62		124	48	124	91	44	5	12	23	58	216	7	18	27	74	0.26	0.37	0.28	9.14	8.32	0.33								
Average 1	789	3446	41	53	128		143	48	94	94	46	3	3	25	68	158	4	4	36	81	0.35	9.82	1.52	11.88	12.88	0.27									
Average 2	679	3517	78	79	158		134	46	85	89	57	24	15	43	79	252	31	38	52	64	0.24	0.85	0.24	1.87	2.17	0.28									
Average 3	628	3721	58	85	147		145	31	82	81	65	31	35	44	82	285	35	39	54	57	0.54	3.13	0.92	7.18	6.88	0.64									
Average 4	787	2972	59	94	151		134	28	92	92	50	8	15	32	72	266	9	21	39	78	0.34	2.47	0.52	8.15	7.48	0.47									
Average 5	621	2192	61	84	152		132	41	91	91	53	15	19	36	75	219	18	24	44	72	0.34	3.59	0.53	6.23	6.05	0.38									
Averages above are for sewage batches 1 to 37 i.e. Configuration 1.																																			
Averages above are for sewage batches 4 to 19 i.e. Configuration 2.																																			
Averages above are for sewage batches 22 to 25 i.e. Configuration 3.																																			
Averages above are for sewage batches 26 to 37 i.e. Configuration 4.																																			
Averages above are for sewage batches 1 to 37 i.e. average over entire investigation.																																			

C.1.





External Nitrification BNRAS system  $f_{NO_3}$  calculation with  $f_{O_2}$  fraction using the model of Wetzel et al. (1990)

Sewage Batch	Q (l/d)	a ratio	NO <sub>3</sub> -N mgN/l	S <sub>bi</sub> mgCOD/l	f <sub>NO3</sub> SP/mgAVS	f <sub>NO3</sub> fraction	f <sub>O2</sub> fraction	S <sub>org</sub> mgCOD/l	S <sub>bi</sub> mgCOD/l	S <sub>sol</sub> mgCOD/l	S <sub>va</sub> mgCOD/l	INPUT		9th Iteration		MS <sub>org</sub> mgCOD/l	MS <sub>20,21</sub> mgCOD/l	MX <sub>2,C</sub> mgVSS/d	MX <sub>2,G</sub> mgVSS/d	O <sub>2</sub> mgP/l Inf	MX <sub>2,N</sub> mgVSS/d	MX <sub>2,21</sub> mgVSS/d	O <sub>Pr</sub> mgP/l Inf	MX <sub>1</sub> mgAVSS/d	O <sub>Pr</sub> mgP/l Inf	K <sub>d</sub>	NXXV <sub>(1-4)</sub> mgVSS	O <sub>Pr</sub> (calc) mgP/l Inf	MXXV <sub>(1-4)</sub> mgVSS	O <sub>Pr</sub> (nom) mgP/l Inf	fav_OHO	fav_PAO					
												S <sub>va</sub> mgCOD/l	S <sub>va</sub> mgCOD/l	MX <sub>2,Q</sub> mgVSS/d	MX <sub>2,21</sub> mgVSS/d																						
1st	1	1	500.00	0.78	0.07	0.13	61.00	400.00	96.00	87.40	0.00	323.38	12.99	61.42	328.58	307.10	61.42	3.93	525.38	304.37	1.54	878.38	1.32	20	2276.65	8.79	43261.49	10.40									
1	20	1	0.99	683.22	0.175	0.07	0.13	88.82	546.59	92.00	83.49	0.00	641.36	10.74	1240.05	9691.67	7985.86	398.59	3.55	12827.21	6137.06	2.85	12092.72	1.80	10	33371.44	8.20	21336.67	8.21	0.36	0.11						
2	20	1	1.81	326.31	0.287	0.07	0.13	68.58	424.73	102.77	87.24	0.00	483.06	17.74	1195.03	7299.64	3841.16	384.12	5.37	9661.38	4637.42	2.14	9281.04	1.79	10	27803.01	9.11	28413.00	9.11	0.35	0.14						
3	20	1	1.77	579.56	0.569	0.09	0.13	73.34	486.81	92.00	76.78	0.00	371.18	10.73	1105.46	6631.10	3353.23	335.33	6.61	11423.32	3483.29	2.34	10181.41	1.33	10	30996.79	10.67	28280.00	10.68	0.37	0.11						
4	40	0.3	0.06	343.07	0.475	0.09	0.13	70.86	426.86	89.23	88.99	0.00	446.38	16.13	2391.83	14882.32	7066.62	565.49	3.88	22350.34	8526.38	2.32	13720.79	1.44	8	47666.45	14.30	35927.00	14.32	0.37	0.15						
5	40	0.5	0.13	615.50	0.361	0.05	0.13	80.01	502.79	40.88	40.31	0.00	581.26	5.99	1233.06	18838.61	7413.42	273.39	3.08	22350.34	8526.38	3.02	17300.53	1.62	8	33169.81	8.32	37192.72	8.32	0.44	0.06						
6	40	0.5	0.11	537.17	0.743	0.11	0.13	69.83	406.71	37.22	36.74	0.00	468.02	6.43	1083.75	13184.56	2955.68	236.45	2.27	18720.69	7188.74	2.43	15098.69	1.42	8	44200.26	6.11	51021.67	6.11	0.42	0.07						
7	40	0.5	0.31	583.80	0.151	0.05	0.13	75.76	479.81	56.90	55.58	0.00	579.21	8.75	1094.20	17494.31	4671.46	730.52	2.22	21568.32	8282.24	2.80	16381.49	1.54	8	51231.03	6.55	36310.83	6.54	0.42	0.09						
8	40	0.5	0.33	598.06	0.891	0.09	0.13	77.75	467.39	102.47	101.05	0.00	483.59	17.27	3006.02	13689.72	8198.24	653.86	2.39	19340.48	7427.90	2.51	16810.41	1.58	8	32433.89	6.48	47970.00	6.50	0.37	0.16						
9	40	0.5	0.37	627.64	0.283	0.07	0.13	81.59	524.32	142.80	141.58	0.00	314.73	23.05	4271.94	16700.89	11650.76	932.06	7.48	20590.14	7906.61	2.67	17641.77	1.65	8	58721.34	11.80	60324.44	11.82	0.35	0.20						
10							0.13																														
11	40	0.5	0.32	583.54	0.124	0.05	0.13	76.12	480.84	109.88	108.62	0.00	492.73	18.70	3246.64	13986.98	8834.48	708.36	3.41	19709.97	7568.61	2.56	16438.55	1.54	8	53300.00	7.51	41580.00	7.52	0.37	0.17						
12	40	0.5	0.33	538.07	0.885	0.07	0.13	69.95	428.00	92.00	90.59	0.00	446.33	16.42	2628.47	11481.42	7195.82	575.67	1.97	17833.81	6853.86	2.32	15124.02	1.42	8	47605.18	5.70	39162.93	5.72	0.38	0.13						
13	40	0.5	0.05	613.14	0.844	0.08	0.13	79.71	485.83	108.97	108.76	0.00	498.47	18.17	3260.30	16172.71	8891.72	711.34	1.21	19938.95	7636.56	2.59	17234.26	1.62	8	54432.83	5.41	49665.00	5.42	0.37	0.16						
14							0.13																														
15							0.13																														
16	40	0.5	0.30	620.50	0.235	0.06	0.13	80.67	503.34	73.00	71.70	0.00	552.64	11.08	2203.45	17929.95	6009.40	480.75	4.46	22105.42	8488.48	2.87	17441.08	1.64	8	54523.14	8.96	51571.67	8.95	0.44	0.11						
17	40	0.5	0.35	558.50	0.151	0.09	0.13	72.61	473.51	92.00	90.52	0.00	452.89	16.23	2646.64	14693.73	7218.11	577.43	3.46	18115.36	6956.37	2.31	13698.38	1.47	8	48265.87	7.28	49243.33	7.30	0.37	0.15						
18	40	0.5	0.30	575.00	0.351	0.10	0.13	74.73	440.90	78.00	76.70	0.00	507.13	12.65	2309.10	15726.70	7422.11	742.21	6.37	20285.34	9736.97	2.25	20202.70	1.52	10	58389.34	10.34	46896.67	10.33	0.35	0.13						
19							0.13																														
20	70	0.5	0.20	587.32	0.189	0.09	0.13	76.38	459.73	102.00	101.12	0.00	507.71	16.66	3283.93	11508.08	7341.27	734.13	4.70	19231.29	7311.02	2.25	15481.93	1.55	10	60999.64	8.50	47233.83	8.52	0.33	0.16						
21							0.13																														
22	30	0.5	1.63	515.67	0.495	0.05	0.13	67.04	424.07	63.00	55.97	0.00	503.36	9.25	1262.88	11459.36	4059.25	405.93	6.74	15166.79	7280.06	2.24	13688.51	1.36	10	40300.34	10.34	36688.33	10.33	0.37	0.10						
23	30	0.5	0.75	618.22	0.285	0.06	0.13	80.37	498.19	86.16	82.91	0.00	374.32	12.43	1927.93	13017.88	6195.93	619.59	5.95	17229.55	8270.19	2.55	16590.97	1.63	10	48607.33	10.13	47825.36	10.12	0.35	0.12						
24	30	0.5	0.16	685.89	0.589	0.07	0.13	89.17	550.54	121.95	123.27	0.00	600.92	17.84	2859.19	13621.04	9705.97	970.60	9.27	18027.85	8653.77	2.67	18074.05	1.81	10	34991.87	13.84	39520.56	13.87	0.33	0.17						
25	30	0.5	0.15	478.34	0.855	0.08	0.13	62.19	377.36	70.98	70.33	0.00	432.26	13.05	1522.85	9797.93	4694.89	489.45	15.63	12967.85	6234.57	1.92	12605.03	1.26	10	37162.82	18.81	54989.17	18.81	0.32	0.19						
26	30	0.5	2.03	649.92	0.748	0.08	0.13	84.49	510.59	82.25	73.45	0.00	599.77	10.65	1724.29	13593.46	5342.35	154.24	12.87	17991.34	6353.85	2.66	17126.34	1.71	10	49850.12	18.23	26970.17	18.25	0.36	0.11						
27	30	0.5	0.75	707.42	0.284	0.07	0.13	91.96	566.12	70.23	67.01	0.00	678.09	8.81	1613.64	15730.01	5186.69	518.67	5.00	20342.66	9764.48	3.01	18641.41	1.86	10	34433.91	9.87	30534.33	9.88	0.37	0.10						
28	30	0.5	0.92	580.67	0.431	0.07	0.13	75.49	464.15	58.34	54.38	0.00	558.87	8.23	1216.54	12667.82	4028.87	402.89	5.84	16766.24	8047.79	2.48	13501.32	1.57	10	44518.11	9.83	36766.67	9.83	0.36	0.09						
29	30	0.5	0.41	587.44	0.111	0.05	0.13	76.37	479.14	99.67	97.91	0.00	533.33	15.50	2240.04	12124.07	7200.14	720.01	2.74	16059.80	7708.71	2.38	14379.90	1.55	10	47168.56	6.66	27683.33	6.64	0.24	0.15						
30	30	0.5	0.08	624.33	0.371	0.06	0.13	81.17	508.23	83.54	83.18	0.00	386.92	12.26	1943.29	13303.36	6246.62	624.66	7.79	17607.68	8451.69	2.61	16432.41	1.63	10	49383.06	12.04	23683.33	12.03	0.26	0.13						
31	30	0.5	0.09	797.86	0.413	0.03	0.13	103.72	668.65	123.46	123.10	0.00	751.63	14.69	3022.66	17036.96	9715.74	971.57	13.47	22548.91	10823.48	3.34	21024.71	2.10	10	65084.42	18.91	38921.67	18.93	0.35	0.15						
32	30	0.5	0.24	396.40	0.405	0.04	0.13	77.53	494.09	130.50	129.45	0.00	323.96	20.83	2946.27	18764.43	9470.14	947.01	12.88	13718.83	7343.04	2.33	15723.93	1.5													

## **APPENDIX D**

- Design and Operating Parameters of UCT Control System.
- Daily Results of UCT Control System
- Figures D1 to D18 : Graphs of Daily Results.

University of Cape Town

Table D1: Design and operating parameters of the laboratory scale UCT system.

Parameter	Value	Units
<b>System:</b>		
Sludge age	8	days
Temperature	20	°C
pH of anaerobic reactor	7.2 - 8.2	
ph of aerobic reactor	7.2 - 8.2	
DO in aerobic eactor	2.0 - 5.0	mg/l
<b>Influent: Mitchells Plain (Raw) unsettled wastewater</b>		
Flow	20	l/d
COD concentration	755	mgCOD/l
TKN/VSS ratio	0.10	mgN/mgVSS
Total P removal/l influent COD	0.020	mgP/mgCOD
<b>Reactor Volumes (l) and Mass Fractions:</b>		
Anaerobic	3*	15%
Anoxic	7	35%
Aerobic	10	50%
Unaerated mass fraction	10	50%
<b>Recycles:</b>		
Anoxic to anaerobic (r-recycle)	1:1	
Aerobic to anoxic (a-recycle)	2:1	
Underflow (s-recycle)	1:1	
* actual volume is 6l, but with $r = 1:1$ the VSS concentration in the anaerobic reactor is half that in the remainder of the system; therefore equivalent volume at system VSS concentration is 3l.		

Daily Tests on Control System (System 2)

Day No.	1998	OUR	COD				FSA			TKN			OSVI mg/l	TSS mg/l	VSS mg/l	COD/VSS	TKN/VSS		
			Sys Inf. mgCOD/l	Reactor mgCOD/l	mgCOD/l	FE mgCOD/l	Influent mgN/l	UE mgN/l	FE mgN/l	Influent mgN/l	Reactor mgN/l	UE mgN/l						FE mgN/l	
1	Thursday	26 February	49,000	654	152	102	47.2	14.8	12.2	72.7	20.9	18.9	95	2314	2022	1.48	0.10		
2	Friday	27 February	32,500	715	110	69	48.2	8.5	6.6	72.2	12.9	10.1	84	2262	1984	1.48	0.10		
3	Saturday	28 February	29,900	867	93	85	55.0	3.1	2.1	68.2	6.9	4.1	110	2178	1888	1.48	0.10		
4	Sunday	01 March	34,500	732	73	47	54.7	3.5	2.7	88.3	6.9	5.9	120	2154	1884	1.48	0.10		
5	Monday	02 March	35,850	959	106	91	53.3	2.1	1.7	70.3	2.9	1.8	119	2178	1834	1.48	0.10		
6	Tuesday	03 March	44,200	850	81	71	53.1	1.7	1.5	67.5	3.2	2.9	108	2400	1992	1.48	0.10		
7	Wednesday	04 March	42,500	682	71	35	52.8	1.8	1.0	88.9	4.5	3.8	119	2278	1878	1.48	0.10		
8	Thursday	05 March	39,300	642	2641.80	75	37	54.3	3.4	2.7	72.5	141.4	3.9	2.8	104	2396	1952	1.35	0.07
9	Friday	06 March	41,100	764	2804.16	71	71	59.9	2.9	2.4	79.9	190.4	5.2	4.1	117	2398	1938	1.45	0.10
10	Saturday	07 March	40,200	744	2458.72	61	39	52.9	1.7	0.0	77.8	211.4	4.9	3.6	114	2372	1860	1.32	0.10
11	Sunday	08 March	42,500	711	2418.08	45	39	51.4	1.7	1.4	78.5	171.5	3.8	3.2	110	2354	1870	1.29	0.09
12	Monday	09 March	41,200	875	2397.76	45	39	55.7	1.8	1.5	74.9	201.6	3.4	2.9	118	2288	1830	1.31	0.11
13	Tuesday	10 March	41,800	740	1861.20	41	35	57.7	2.2	2.2	77.3	151.2	3.8	2.9	83	3024	2518	0.74	0.08
14	Wednesday	11 March	41,900	724	2460.92	52	39	56.7	2.7	2.4	76.4	183.4	4.8	3.9	128	2060	1952	1.26	0.09
15	Thursday	12 March	41,600	749	2460.92	70	41	56.7	1.7	1.4	78.3	188.7	3.4	2.7	124	2208	1800	1.37	0.09
End of Batch 2			39,863	719,191	2437.92	76,434	55,982	53,769	3,569	2,784	73,323	177,450	6,059	4,779	110	2325	1945	1.38	0.10
16	Friday	13 March	37,900	778	2647.04	56	39	49.1	2.9	2.8	70.6	176.4	3.5	3.2	128	2352	1852	1.43	0.10
17	Saturday	14 March	38,200	778	2440.24	54	41	49.0	2.2	2.0	73.4	161.0	4.1	3.2	123	2278	1804	1.35	0.09
18	Sunday	15 March	34,600	877	2419.56	50	25	54.0	1.7	1.4	74.8	171.5	3.1	2.4	130	2156	1708	1.42	0.10
19	Monday	16 March	35,500	860	2398.38	37	29	51.2	2.1	2.0	73.5	151.2	4.1	3.1	123	2114	1690	1.42	0.09
20	Tuesday	17 March	35,900	802	2502.28	70	29	50.7	4.1	2.1	78.6	184.8	5.9	2.2	133	2248	1832	1.37	0.10
End of Batch 3			38,020	818,931	2481.60	53,354	32,674	50,820	2,804	2,044	73,752	168,980	4,116	2,828	127	2230	1777	1.48	0.10
21	Wednesday	18 March	38,200	744	2584.32	52	31	51.2	1.7	1.7	71.5	176.4	4.5	3.6	123	2270	1832	1.40	0.10
22	Thursday	19 March	33,200	720	2274.80	58	37	50.0	1.7	1.7	68.7	165.9	2.8	2.0	130	2156	1718	1.32	0.10
23	Friday	20 March	33,300	756	2168.64	59	43	51.1	1.5	1.5	68.0	149.8	2.9	2.2	130	2008	1580	1.37	0.09
24	Saturday	21 March	33,800	809	2248.40	49	37	51.4	2.1	1.7	74.3	152.6	3.1	2.2	130	2002	1850	1.22	0.08
25	Sunday	22 March	33,200	719	2125.76	41	27	53.2	1.7	1.4	71.4	141.4	2.9	2.2	135	1920	1516	1.40	0.09
26	Monday	23 March	33,500	777	2289.28	65	35	48.4	1.5	1.4	73.4	144.2	3.8	2.8	137	1872	1520	1.51	0.09
27	Tuesday	24 March	34,300	801	2371.04	78	53	48.4	1.8	1.4	75.6	134.4	3.8	2.2	144	1944	1498	1.58	0.09
28	Wednesday	25 March	34,100	711	2207.52	70	53	50.1	2.0	1.1	72.5	145.8	3.2	2.8	138	1984	1540	1.43	0.09
End of Batch 4			33,850	754,826	2280.97	58,925	39,441	50,488	1,750	1,490	71,943	151,288	3,343	2,520	133	2020	1632	1.40	0.09
29	Thursday	26 March	33,400	870	2105.32	53	29	63.8	4.2	2.9	73.6	161.0	4.5	3.5	144	1942	1500	1.40	0.11
30	Friday	27 March	32,100	732	2555.00	87	49	35.4	2.1	2.1	49.8	144.2	3.8	2.4	140	2284	1808	1.41	0.08
31	Saturday	28 March	28,000	852	2378.20	82	37	41.4	1.3	1.0	59.8	138.6	2.1	1.8	138	2102	1692	1.41	0.08
32	Sunday	29 March	29,000	728	2130.04	41	31	38.9	1.5	1.1	54.2	151.2	2.1	1.4	143	2032	1892	1.26	0.09
33	Monday	30 March	28,200	789	2440.24	60	50	36.1	2.4	1.8	59.1	131.6	2.7	2.0	149	1880	1600	1.53	0.08
34	Tuesday	31 March	29,500	753	2212.78	50	35	36.8	1.7	1.3	56.0	144.9	2.4	1.5	149	1878	1434	1.54	0.10
35	Wednesday	01 April	41,300	790	2543.64	60	52	39.5	1.7	1.7	57.3	154.0	2.2	2.0	155	2066	1782	1.43	0.09
36	Thursday	02 April	42,800	728	2584.32	58	37	38.5	2.0	1.7	51.7	147.0	2.9	2.4	142	2118	1670	1.54	0.09
End of Batch 5			33,013	752,764	2368.19	56,433	39,954	41,283	2,100	1,998	57,883	148,563	2,818	2,118	145	2038	1647	1.44	0.09
37	Friday	03 April	41,900	740	2522.96	52	27	35.4	2.2	1.4	55.2	171.5	2.4	1.8	153	2096	1612	1.57	0.11
38	Saturday	04 April																	
39	Sunday	05 April		720	2522.98	58	37	34.3	0.7	0.6	58.2	154.7	2.4	2.4	155	2064	1596	1.58	0.10
40	Monday	06 April	43,400	790	2398.88	46	37	37.2	1.0	0.0	58.2	150.5	2.9	1.8	157	2032	1614	1.49	0.09
41	Tuesday	07 April	39,600	877	2254.12	33	25	37.0	2.2	0.7	58.5	160.3	2.5	1.0	150	2000	1572	1.43	0.10
42	Wednesday	08 April																	
43	Thursday	09 April	39,500	881	2479.04	45	37	67.3	1.7	1.3	99.3	187.6	6.3	2.4	140	2290	1766	1.40	0.11
End of Batch 6			41,100	801,548	2435.59	46,166	32,540	42,252	1,568	0,784	86,080	154,920	3,304	1,876	151	1747	1632	1.07	0.07
44	Friday	10 April	54,500	740	2397.76	37	28	73.3	2.0	2.2	102.7	157.5	2.3	3.1	157	2292	1814	1.32	0.09
45	Saturday	11 April	80,570	780	2580.64	41	20	88.2	2.1	1.7	81.1	170.8	2.7	2.5	153	2224	1732	1.49	0.10
46	Sunday	12 April																	
47	Monday	13 April	52,500	902	2298.18	81	20	59.2	3.4	1.8	91.4	173.6	5.3	3.8	156	2052	1650	1.39	0.11
48	Tuesday	14 April	56,900	732	2338.80	37	28	83.2	2.2	0.8	101.6	185.2	3.1	1.3	151	2126	1666	1.40	0.10
49	Wednesday	15 April	54,600	727	2275.84	35	14	74.5	1.8	1.8	102.5	174.3	2.9	2.9	155	2084	1674	1.36	0.11
50	Thursday	16 April	48,800	740	2259.52	53	13	75.8	3.8	2.4	100.4	195.9	4.8	3.2	174	2008	1578	1.43	0.11
End of Batch 7			54,645	788,743	2357.12	43,688	24,045	71,983	2,520	1,797	96,610	187,883	3,502	2,777	158	1823	1686	1.40	0.10
51	Friday	17 April	44,800	744	2133.60	53	33	57.3	3.8	1.8	78.5	188.3	4.1	2.2	140	2142	1606	1.33	0.12
52	Saturday	18 April																	
53	Sunday	19 April	38,000	788	1971.04	81	37	48.8	2.0	1.8	77.7	141.4	3.2	2.4	191	1574	1238	1.59	0.11
54	Monday	20 April	42,500	780	2332.32	70	64	57.7	3.2	2.2	79.2	168.6	3.5	3.5	161	1866	1562	1.49	0.11
55	Tuesday	21 April	40,700	813	2518.08	54	50	47.7	1.4	0.8	75.7	127.4	2.4	1.7	143	1952	1580	1.81	0.08
56	Wednesday	22 April	32,800	751	2148.56	50	41	53.9	2.7	2.2	55.0	131.8	3.1	2.9	143	1954	1538	1.40	0.09
57	Thursday	23 April	34,100	751	1857.60	40	41	84.3	4.1	1.4	74.2	166.6	4.5	1.7	137	1			

Daily Tests on Control System (System 2)

Day No.	1998	OUR	COD				FSA			TKN				DSVI	TSS	VSS	COD/VSS	TKN/VSS	
			Sys Inf. mgCOD/l	Reactor mgCOD/l	UE mgCOD/l	FE mgCOD/l	Influent mgNI	UE mgNI	FE mgNI	Influent mgNI	Reactor mgNI	UE mgNI	FE mgNI						
84	Wednesday	20 May	34.800	812	2040.00	35	8	58.0	2.2	1.8	74.5	154.0	4.8	3.5	131	1808	1280	1.59	0.12
85	Thursday	21 May	36.000	763	1530.00	2	0	83.3			80.4	144.2	2.9	2.8	95	2214	1780	0.86	0.08
86	Friday	22 May	37.000	840	1838.00	41	33	78.1	2.2	2.1	105.4	182.4	4.1	3.8	122	1644	1312	1.40	0.12
87	Saturday	23 May	39.000	829	2570.40	49	41	73.2	6.7	2.8	103.7	112.0	8.3	2.9	128	1566	1208	2.13	0.09
88	Sunday	24 May														1842	1440		
89	Monday	25 May	30.200	783	2529.60	65	37	84.0	12.7	10.1	103.0	175.0	5.3	3.4	114				
90	Tuesday	26 May	43.200	824	2407.20	61	37	89.2	2.2	2.0	73.8	193.2	2.9	2.7					
91	Wednesday	27 May																	
92	Thursday	28 May	47.200	710	2284.80	57	24	66.1	1.8	2.9	70.0	194.6	3.2	3.4	113	1952	1584	1.44	0.12
93	Friday	29 May	36.000	840	2488.80	37	33	57.1	1.5	2.1	85.7	177.8	3.2	3.2	97	2070	1844	1.35	0.10
94	Saturday	30 May	42.300	690	3100.80	53	37	48.9	2.0	2.2	68.0	156.2	2.9	2.8	122	2124	1704	1.82	0.09
95	Sunday	31 May	38.500	738		69	41	44.4	1.1	2.9	66.8	119.0	2.2	4.5	122	1806	1378		0.09
96	Monday	01 June	43.800	892	1862.08	28	28	47.3	3.4	2.0	70.1	130.1	4.3	4.1	115	1748	1330	1.40	0.10
97	Tuesday	02 June	54.800	700	2550.24	45	28	57.0	4.3	4.1	74.9	177.8	5.8	5.0	124	1862	1544	1.65	0.12
98	Wednesday	03 June																	
99	Thursday	04 June																	
100	Friday	05 June	33.500	575	2671.58	53	24	48.2	1.4	1.7	67.3	189.2	1.7	2.0	114	2110	1668	1.60	0.11
	End of Batch 12		42.300	706.533	2483.07	48.767	30.799	52.700	2.220	2.558	71.820	163.391	3.320	3.560	115	1519	1579	1.32	0.10
101	Saturday	08 June	32.800	745	2307.36	38	32	53.5	2.4	2.1	73.2	152.8	4.3	3.5	122	1984	1528	1.31	0.10
102	Sunday	09 June	30.700	680	1902.56	49	40	48.4	2.0	1.5	76.6	150.0	4.9	2.9	126	1746	1378	1.38	0.11
103	Monday	08 June	30.900	888	2024.18	53	53	56.0	1.5	1.4	72.0	216.4	2.2	1.7	149	1608	1238	1.64	0.17
104	Tuesday	09 June	37.600	692	2165.88	34	34	54.9	1.8	1.4	78.8	180.8	2.4	2.2	107	2238	1728	1.25	0.10
105	Wednesday	10 June	45.700	747	2580.00	60	56	60.1	6.9	3.4	79.8	156.8	6.9	5.8	133	1810	1454	1.77	0.11
106	Thursday	11 June	43.200	747	1857.60	78	29	59.4	4.3	2.8	82.9	148.4	5.6	3.4	131	1674	1320	1.41	0.11
107	Friday	12 June	45.100	654	1803.88	58	37	58.8	1.4	1.2	77.6	113.4	3.5	3.4	150	1400	1096	1.46	0.10
	End of Batch 13		38.000	707.830	2063.01	52.514	40.219	55.880	2.900	1.974	77.260	159.629	4.220	3.240	131	1777	1391	1.49	0.12
108	Saturday	13 June	19.900	724	2184.96	58	37	61.3	2.1	1.7	93.5	159.6	11.3	4.5	128	1740	1400	1.70	0.11
109	Sunday	14 June																	
110	Monday	15 June																	
111	Tuesday	16 June																	
112	Wednesday	17 June																	
	End of Batch 14		19.900	724	2184.96	58	37	61.320	2.100	1.880	93.520	159.600	11.340	4.480	126	1740	1400	1.70	0.11
113	Thursday	18 June	36.300	831	1809.28	56	41	104.7	28.6	27.4	133.0	137.2	32.2	29.7	82	1464	1236	1.46	0.11
114	Friday	19 June	45.400																
115	Saturday	20 June																	
116	Sunday	21 June	49.600	775	2407.20	128	106	95.5	38.9	37.9	135.0	215.6	44.8	44.2	259	1874	1582	1.54	0.14
117	Monday	22 June	48.300	783	2325.60	88	81	85.1	28.9	25.6	155.1	183.4	40.9	40.0	130	1770	1524	1.53	0.12
	End of Batch 15		45.400	798.393	2180.89	92.560	69.467	95.107	31.453	30.333	141.027	178.733	39.299	37.987	157	1703	1441	1.51	0.12
118	Tuesday	23 June	48.700	685	1917.80	78	65	55.0	24.8	19.2	85.1	155.4	25.9	23.1	134	1790	1508	1.27	0.10
119	Wednesday	24 June	41.850	787	2040.00	73	65	67.3	4.2	4.2	93.8	135.8	7.1	6.4	172	1512	1302	1.57	0.10
120	Thursday	25 June	38.500	808	2244.00	90	57	57.4	7.0	6.3	94.1	154.0	6.1	7.8	138	1468	1312	1.71	0.12
121	Friday	26 June																	
122	Saturday	27 June																	
123	Sunday	28 June																	
	End of Batch 16		43.017	753.440	2067.20	80.240	62.560	58.920	11.947	9.893	91.000	148.400	13.720	12.367	147	1590	1374	1.52	0.11
124	Monday	29 June	34.800	877	1378.80	94	38	63.8	3.8	2.4	66.8	120.4	4.8	3.8	173	1560			
125	Tuesday	30 June	36.800	702	2058.32	45	48	75.0	1.4	1.4	96.3	147.0	4.5	3.8	158	1540	1310	1.57	0.11
126	Wednesday	01 July	34.800	722	1854.72	59	56	58.7	1.8	1.5	80.9	135.8	4.1	2.9	161	1368	1168	1.59	0.12
127	Thursday	02 July																	
128	Friday	03 July																	
129	Saturday	04 July																	
130	Sunday	05 July																	
131	Monday	08 July	30.600	778	1814.40	89	52	66.9	6.8	5.3	100.1	126.0	7.7	7.3	198	1324	1192	1.52	0.11
132	Tuesday	07 July	29.000	879	2479.68	83	83	74.2	4.2	6.8	95.8	173.8	6.6	7.3	164	1708	1500	1.85	0.12
	End of Batch 17		33.160	751.548	2016.38	79.550	61.188	67.676	3.528	3.444	91.880	140.560	5.488	4.956	170	1500	1292	1.27	0.09
133	Wednesday	08 July	31.000	698	2262.08	50	46	62.1	2.7	2.7	68.3	169.4	5.2	3.9	187	1608	1430	1.65	0.12
134	Thursday	09 July	39.800	729	2942.24	54	41	44.0	0.0	0.0	88.3	145.0	0.0	0.0	187	1920	1692	1.74	0.09
135	Friday	10 July	36.800	800	2859.40	82	62	53.2	1.4	1.4	74.5	155.4	2.2	1.7	182	1762	1562	1.33	0.03
136	Saturday	11 July	32.800	804	2589.30	50	25	53.8	1.8	1.7	73.4	158.8	3.9	2.8	160	1748	1528	1.88	0.10
137	Sunday	12 July	31.300	750	1899.00	37	29	53.2	2.8	1.7	76.2	134.4	3.9	2.2	178	1480	1282	1.35	0.11
138	Monday	13 July	34.300	787	1878.30	52	39	56.3	6.7	1.4	77.0	99.4	9.9	1.7	166	1148	898	1.87	0.11
139	Tuesday	14 July																	
140	Wednesday	15 July																	
141	Thursday	18 July	41.800	895	2154.90	79	68	80.1	4.8	5.7	79.0	133.0	8.1	6.3	200	1190	1102	1.96	0.12
142	Friday	17 July	36.700	751	1591.20	57	45	43.7	4.2	2.0	75.2	120.4	4.8	3.9					
143	Saturday	18 July	39.200																
144	Sunday	19 July	39.200																
145	Monday	20 July	39.200																
	End of Batch 18		35.488	773.974	2232.05	55.048	44.203	52.033	3.045	2.085	73.975	139.300	4.760	2.917	177	1548	1353	1.73	0.11
146																			

## Nitrate (NO3) and Nitrite (NO2) Concentrations

Day No.	1996		Nitrates (mg/l NO3-N)				Phosphorous (mg/l PO4-P)				
			Anaerobic	Anoxic	Aerobic	Filtered Effluent	Influent	Anaerobic	Anoxic	Aerobic	Filtered Effluent
1	Thursday	26 February	0.36	0.36	8.60	5.80	19.2	18.9	10.2	0.0	0.0
2	Friday	27 February	0.65	0.66	13.20	10.10	19.2	20.0	8.3	0.0	0.0
3	Saturday	28 February	0.46	0.15	10.00	11.30	19.2	23.3	23.4	11.7	1.3
4	Sunday	01 March	0.58	0.31	12.70	12.50	20.8	23.8	10.6	0.0	0.0
5	Monday	02 March	0.77	1.01	13.60	12.00	21.9	26.0	12.1	0.8	0.8
6	Tuesday	03 March	0.34	0.50	13.20	13.00	20.0	27.5	11.7	0.8	0.4
7	Wednesday	04 March	0.13	0.65	13.40	16.00	19.5	27.9	12.3	2.2	1.1
8	Thursday	05 March	0.26	0.60	15.20	15.20	22.1	31.5	14.5	4.3	3.3
9	Friday	06 March	0.31	0.65	16.10	16.00	22.4	34.0	16.6	5.1	4.3
10	Saturday	07 March	0.47	0.74	16.20	16.20	23.5	36.2	17.4	5.1	4.7
11	Sunday	08 March	0.48	0.59	16.00	16.00	24.2	37.3	18.5	5.8	5.4
12	Monday	09 March	0.45	0.44	15.20	16.20	24.2	38.0	18.5	6.5	6.2
13	Tuesday	10 March	0.21	1.86	16.20	15.20	24.6	38.3	23.5	8.3	5.8
14	Wednesday	11 March	0.11	1.27	16.60	21.00	24.0	35.3	16.6	5.7	5.7
15	Thursday	12 March	0.22	2.29	16.20	18.40	23.0	34.3	16.6	7.8	6.4
End of Batch 2			0.387	0.805	14.160	14.327	21.862	30.143	15.374	4.258	3.013
16	Friday	13 March	0.23	0.56	15.20	16.60	23.0	37.8	20.5	8.1	7.8
17	Saturday	14 March	0.23	0.86	16.00	14.40	22.6	35.7	18.4	6.7	6.4
18	Sunday	15 March	0.26	0.75	15.40	16.60	23.3	36.0	20.9	7.4	7.4
19	Monday	16 March	0.28	0.60	13.60	13.00	25.4	36.4	20.1	7.8	7.4
20	Tuesday	17 March	0.20	0.45	13.00	14.20	23.0	33.0	1.9	5.5	5.5
End of Batch 3			0.240	0.644	14.640	14.960	23.474	35.786	16.344	7.106	6.894
21	Wednesday	18 March	0.11	0.62	13.00	13.40	19.6	33.0	17.2	4.8	4.5
22	Thursday	19 March	0.20	0.70	14.20	12.60	21.7	31.3	14.8	4.1	3.8
23	Friday	20 March	0.15	1.23	15.60	15.00	20.6	31.3	14.1	3.4	3.4
24	Saturday	21 March	0.28	0.72	13.80	17.80	22.7	31.6	15.5	4.1	2.8
25	Sunday	22 March	0.25	0.65	14.40	15.60	22.4	32.4	17.2	5.5	4.8
26	Monday	23 March	0.15	0.45	13.00	13.80	23.7	33.7	18.6	5.8	5.8
27	Tuesday	24 March	0.19	0.69	12.70	13.60	22.2	35.1	19.0	7.2	5.7
28	Wednesday	25 March	0.15	0.69	13.70	11.70	22.2	35.1	17.2	5.4	4.7
End of Batch 4			0.185	0.719	13.800	14.188	21.881	32.933	16.681	5.048	4.434
29	Thursday	26 March	0.12	0.78	13.50	13.00	23.3	35.8	16.5	4.3	3.6
30	Friday	27 March	0.25	0.56	9.60	10.00	24.4	34.7	15.9	5.0	5.0
31	Saturday	28 March	0.14	0.46	8.60	8.50	24.7	34.4	17.2	5.7	4.7
32	Sunday	29 March	0.10	0.46	8.50	8.00	23.6	34.4	16.5	4.3	4.3
33	Monday	30 March	0.07	0.42	8.00	7.70	22.2	33.7	17.9	6.8	6.8
34	Tuesday	31 March	0.20	0.41	7.90	8.10	19.4	32.8	18.0	7.8	5.3
35	Wednesday	01 April	0.13	0.36	8.10	8.80	18.7	32.1	13.4	2.1	2.1
36	Thursday	02 April	0.21	0.50	8.10	9.00	19.0	32.8	13.7	2.5	2.1
End of Batch 5			0.152	0.494	9.038	9.138	21.904	33.815	16.131	4.809	4.230
37	Friday	03 April	0.15	0.40	8.50	8.40	20.4	33.5	13.7	2.5	2.5
38	Saturday	04 April									
39	Sunday	05 April	0.25	0.50	7.40	8.30	19.4	34.5	11.3	2.1	1.8
40	Monday	06 April	0.28	0.34	8.10	7.50	19.0	34.5	14.1	2.8	2.8
41	Tuesday	07 April	0.21	0.45	8.10	7.00	19.7	33.8	12.7	2.1	2.1
42	Wednesday	08 April									
43	Thursday	09 April	0.25	1.16	14.70	14.80	21.8	40.9	19.7	6.7	5.3
End of Batch 6			0.228	0.570	9.360	9.200	20.080	35.440	14.302	3.240	2.888
44	Friday	10 April	0.40	4.10	17.20	17.50	22.0	39.8	18.8	4.9	4.5
45	Saturday	11 April	0.52	6.80	20.70	20.70	22.0	39.8	18.5	5.9	5.6
46	Sunday	12 April									
47	Monday	13 April	0.48	9.00	25.10	25.00	22.0	41.2	17.1	5.9	5.2
48	Tuesday	14 April	0.41	8.00	24.60	23.50	22.3	37.7	16.8	9.1	9.1
49	Wednesday	15 April	0.37	7.75	24.00	24.00	21.6	37.3	18.8	8.7	7.7
50	Thursday	16 April	0.33	6.50	23.50	21.60	22.7	34.5	17.8	12.5	11.2
End of Batch 7			0.418	7.025	22.517	22.050	22.097	38.382	17.970	7.850	7.212
51	Friday	17 April	0.45	0.53	15.10	19.70	23.7	36.5	21.5	10.9	11.3
52	Saturday	18 April									
53	Sunday	19 April	0.18	0.75	11.80	13.50	26.4	33.9	17.7	7.5	7.5
54	Monday	20 April	0.35	0.80	11.00	12.70	24.9	38.4	20.0	7.2	7.2
55	Tuesday	21 April	0.23	0.85	13.10	12.50	27.8	40.3	20.3	6.4	6.4
56	Wednesday	22 April	0.21	0.95	12.20	13.10	25.2	42.2	21.5	7.5	7.5
57	Thursday	23 April	0.22	2.04	13.20	13.50	26.0	39.6	22.7	11.4	10.3
58	Friday	24 April	0.29	2.46	12.30	14.80	26.0	39.6	23.1	11.0	9.9
59	Saturday	25 April	0.22	1.69	12.70	16.20	26.0	42.5	23.8	10.3	10.3
60	Sunday	26 April	0.11	0.95	11.10	14.00	36.3	46.2	26.7	13.9	12.1
61	Monday	27 April									
62	Tuesday	28 April	0.63	2.43	14.90	15.30	29.3	41.0	27.1	20.5	16.5
63	Wednesday	29 April	0.11	0.45	6.70	11.00	24.9	42.1	27.1	14.3	17.6
End of Batch 8			0.273	1.264	12.373	14.209	26.955	40.198	22.860	16.987	10.588
64	Thursday	30 April	0.10	0.00	10.90	10.50	24.7	40.6	20.9	7.1	6.7
65	Friday	01 May	0.24	0.34	6.20	10.90	22.3	39.2	19.8	6.7	6.0
66	Saturday	02 May	0.22	0.65	9.20	11.60	21.9	35.3	18.0	6.7	5.3
End of Batch 9			0.187	0.330	8.767	11.000	22.967	38.393	19.553	6.830	6.007
67	Sunday	03 May	0.12	0.56	12.50	10.50	20.5	37.8	19.4	6.0	6.0
68	Monday	04 May	0.00	0.16	15.00	10.50	23.7	38.5	20.5	6.7	6.4
69	Tuesday	05 May	0.35	0.82	11.50	13.10	24.0	36.8	18.7	5.3	5.3
70	Wednesday	06 May	0.17	0.65	12.80	12.60	23.3	40.3	21.2	8.1	7.2
71	Thursday	07 May	0.39	1.29	12.60	12.40	23.3	41.0	21.2	8.8	8.5
72	Friday	08 May	0.88	2.55	19.70	15.50	22.1	38.0	22.5	10.0	9.2
End of Batch 10			0.318	1.005	14.017	12.433	22.827	38.722	20.588	7.490	7.093
73	Saturday	09 May									
74	Sunday	10 May	0.28	2.11	14.30	14.10	21.4	36.2	14.4	5.9	5.5
75	Monday	11 May	0.65	2.55	16.10	17.50	24.0	31.0	17.7	5.2	4.4
76	Tuesday	12 May	0.82	2.55	15.20	16.30	19.9	35.0	18.4	6.3	5.2
77	Wednesday	13 May	0.31	1.68	12.90	15.00	21.4	34.3	19.9	10.0	7.4
78	Thursday	14 May	0.96	1.58	19.60	18.50	21.8	32.6	18.9	7.4	7.0
79	Friday	15 May	0.63	1.38	20.70	18.70	22.2	32.6	18.5	6.3	5.6
80	Saturday	16 May	0.46	2.75	20.20	19.60	22.6	32.2	18.1	7.4	6.7
81	Sunday	17 May	0.44	2.75	18.30	20.60	25.2	34.0	20.2	9.6	8.9
82	Monday	18 May	0.33	2.75	16.40	19.20	17.0	32.9	19.6	10.7	10.0
83	Tuesday	19 May	0.55	1.13	20.10	20.00	21.5	36.6	19.6	11.8	10.7
End of Batch 11			0.543	2.123	17.380	17.950	21.687	33.733	18.532	8.056	7.134

D.5

Nitrate (NO3) and Nitrite (NO2) Concentrations

Day No.	1996				Nitrates (mg/l NO3-N)				Phosphorous (mg/l PO4-P)				
					Anaerobic	Anoxic	Aerobic	Filtered Effluent	Influent	Anaerobic	Anoxic	Aerobic	Filtered Effluent
84	Wednesday	20 May	0.62	1.38	22.10	24.30	19.9	33.1	21.3	12.1	11.8		
85	Thursday	21 May	0.64	1.26	25.00	26.30	25.3	36.3	21.7	12.1	11.8		
86	Friday	22 May	0.40	0.52	21.60	23.90	27.1	35.6	22.1	10.7	10.7		
87	Saturday	23 May	0.50	0.25	20.90	22.00	21.9	34.2	21.7	11.0	10.3		
88	Sunday	24 May											
89	Monday	25 May	0.22	0.16	18.60	17.60	23.5	37.4	19.6	9.3	9.3		
90	Tuesday	26 May					24.2	36.7	21.0	7.1	5.7		
91	Wednesday	27 May											
92	Thursday	28 May	0.30	0.90	19.40	12.60	25.7	40.7	20.8	7.1	7.1		
93	Friday	29 May	0.24	2.01	12.60	12.60	24.9	42.3	19.9	5.4	5.4		
94	Saturday	30 May	0.28	1.09	13.80	12.60	25.3	42.3	20.3	6.6	6.6		
95	Sunday	31 May	0.25	1.42	12.00	12.80	28.6	44.4	22.8	7.9	3.7		
96	Monday	01 June	0.24	1.18	11.00	11.60	24.5	43.2	24.9	7.9	7.5		
97	Tuesday	02 June	0.20	0.14	11.00	8.80	25.7	43.6	30.3	8.3	8.7		
98	Wednesday	03 June											
99	Thursday	04 June											
100	Friday	05 June	0.44	1.41	14.40	14.40	24.9	44.0	21.2	5.4	4.2		
	End of Batch 12				0.279	1.164	13.457	12.200	25.678	42.931	22.877	6.940	6.169
101	Saturday	06 June	0.42	0.81	18.40	19.00	25.5	37.5	20.2	3.7	3.4		
102	Sunday	07 June	0.32	3.85	18.20	14.60	21.3	41.9	21.0	3.7	2.3		
103	Monday	08 June	0.50	3.44	15.00	17.00	22.8	47.8	21.3	3.7	3.0		
104	Tuesday	09 June	0.37	2.55	18.20	18.00	22.5	38.2	21.3	3.0	2.6		
105	Wednesday	10 June	0.20	1.88	18.80	18.80	22.5	32.6	25.5	6.0	6.0		
106	Thursday	11 June	0.81	0.91	19.20	29.80	22.5	34.1	25.8	9.7	6.7		
107	Friday	12 June	0.89	0.92	22.40	31.00	19.5	31.4	25.3	12.3	9.4		
	End of Batch 13				0.501	2.051	18.600	21.171	22.363	37.839	22.920	6.031	4.784
108	Saturday	13 June	0.31	0.59	27.40	30.00	23.8	31.8	21.7	4.3	3.3		
109	Sunday	14 June											
110	Monday	15 June											
111	Tuesday	16 June											
112	Wednesday	17 June											
	End of Batch 14				0.310	0.590	27.400	30.000	23.820	31.760	21.660	4.330	3.250
113	Thursday	18 June	0.30	1.07	32.40	33.00	24.5	30.0	20.9	10.8	11.2		
114	Friday	19 June	0.47	0.64	40.00	33.60							
115	Saturday	20 June					21.7	30.0	21.7	12.6	11.9		
116	Sunday	21 June					23.5	29.2	22.0	11.9	11.9		
117	Monday	22 June	0.24	0.80	44.40	36.80							
	End of Batch 15				0.337	0.837	38.933	34.467	23.220	29.720	21.540	11.790	11.670
118	Tuesday	23 June	0.18	1.46	43.40	44.00	21.7	28.6	22.0	14.4	12.6		
119	Wednesday	24 June	0.18	0.90	40.00	31.60	23.5	28.2	24.5	17.3	16.2		
120	Thursday	25 June	0.55	0.85	20.60	19.00	23.8	29.5	25.9	19.4	18.0		
121	Friday	26 June											
122	Saturday	27 June											
123	Sunday	28 June											
	End of Batch 16				0.303	1.070	34.667	31.533	22.962	28.750	24.154	17.070	15.823
124	Monday	29 June	0.42	0.89	21.50	19.00	24.5	22.3	16.2	7.6	7.2		
125	Tuesday	30 June	0.15	0.31	20.30	20.00	22.0	25.2	18.0	9.0	7.6		
126	Wednesday	01 July	0.13	0.37	20.30	20.90	23.4	26.3	22.0	15.1	11.5		
127	Thursday	02 July											
128	Friday	03 July											
129	Saturday	04 July											
130	Sunday	05 July											
131	Monday	06 July	0.38	0.34	19.00	18.60	24.5	23.0	21.6	18.0	17.6		
132	Tuesday	07 July	0.12	0.17	17.20	20.20	28.8	30.6	19.8	14.8	16.6		
	End of Batch 17				0.240	0.416	19.660	19.740	24.824	25.488	19.512	12.888	12.096
133	Wednesday	08 July	0.12	0.10	14.80	15.00	24.1	23.0	22.0	16.9	15.8		
134	Thursday	09 July	0.15	0.53	13.40	12.80	26.0	21.4	20.4	15.8	16.4		
135	Friday	10 July	0.12	0.12	15.60	13.10	23.7	24.7	22.7	18.0	16.7		
136	Saturday	11 July	0.13	0.53	16.50	15.00	26.4	22.4	22.4	19.4	18.7		
137	Sunday	12 July	0.21	0.85	18.10	15.70	24.7	22.7	21.7	18.7	18.7		
138	Monday	13 July	0.15	0.32	16.10	13.00	24.7	25.4	23.7	21.4	20.0		
139	Tuesday	14 July											
140	Wednesday	15 July											
141	Thursday	16 July	0.13	0.12	15.40	14.60	26.0	19.4	18.0	15.7	16.0		
142	Friday	17 July	0.17	0.79	17.50	15.10	24.5	19.9	18.1	14.5	12.1		
143	Saturday	18 July											
144	Sunday	19 July											
145	Monday	20 July											
	End of Batch 18				0.148	0.420	15.925	14.289	25.004	47.583	21.100	17.539	16.794
146	Tuesday	21 July	0.23	0.76	13.00	17.10	25.5	15.2	12.4	10.4	7.8		
147	Wednesday	22 July											
	End of Batch 19				0.230	0.760	13.000	17.100	25.520	15.240	12.410	10.370	7.800
148	Thursday	23 July	0.27	0.61	15.10	14.00	20.2	21.3	22.0	17.4	16.0		
149	Friday	24 July	0.23	1.64	14.00	12.00	18.8	21.3	21.3	16.7	16.7		
150	Saturday	25 July	0.22	0.72	15.00	13.20	20.2	37.6	19.9	14.5	14.2		
151	Sunday	26 July	0.16	0.58	17.70	17.10	21.6	22.3	19.5	13.1	14.2		
152	Monday	27 July											
	End of Batch 20				0.220	0.888	15.450	14.075	20.208	25.813	20.650	15.420	15.243
153	Tuesday	28 July	0.38	0.35	16.40	14.40	22.7	24.5	19.9	13.5	13.5		
154	Wednesday	29 July					26.1	22.6	17.4	13.2	13.2		
155	Thursday	30 July					21.6	24.0	20.5	14.9	14.6		
156	Friday	31 July					23.6	24.3	19.8	14.6	13.9		
157	Saturday	01 August											
158	Sunday	02 August											
159	Monday	03 August											
	End of Batch 21				0.380	0.350	16.400	14.400	23.488	23.833	19.388	14.033	13.783
160	Tuesday	04 August					22.6	24.3	19.8	13.6	13.2		
161	Wednesday	05 August					21.6	23.3	17.7	15.0	14.3		
162	Thursday	06 August											
163	Friday	07 August					21.2	21.6	15.6	13.6	13.6		
164	Saturday	08 August											
165	Sunday	09 August											
166	Monday	10 August											
167	Tuesday	11 August											
168	Wednesday	12 August					20.7	20.0	14.4	12.3	11.9		
169	Thursday	13 August					20.4	14.0	16.8	14.4	11.9		
170	Friday	14 August											
171	Saturday	15 August					19.7	21.4	17.19	14.4	14.0		
172	Sunday	16 August											
173	Monday	17 August											
	End of Batch 22				ERR	ERR	ERR	ERR	21.007	20.788	14.088	13.855	13.153
174	Tuesday	18 August					19.7	23.9	17.9	11.2	10.9		
175	Wednesday	19 August					20.4	22.5	21.1	14.7	9.8		
176	Thursday	20 August					20.4	26.7	22.1	13.0	10.9		
	End of Batch 23				ERR	ERR	ERR	ERR	20.117	24.330	20.353	12.980	10.530

## Mass Balance for Phosphorous

Day No.	1998	Anaerobic			Anoxic			Aerobic			Settler			Sum Diff.	
		Mass In mgP/l	Mass Out mgP/l	Diff	Mass In mgP/l	Mass Out mgP/l	Diff	Mass In mgP/l	Mass Out mgP/l	Diff	Mass In mgP/l	Mass Out mgP/l	Diff		
1	Thursday	26 February	29.4	37.7	8.3	37.7	51.0	13.2	40.8		-40.8	0.0	0.0	-19.2	
2	Friday	27 February	27.5	40.0	12.5	40.0	41.5	1.5	33.2		-33.2	0.0	0.0	-19.2	
3	Saturday	28 February	42.5	46.6	3.9	70.0	117.0	47.0	93.6	46.8	-46.8	23.4	2.6	-20.8	
4	Sunday	01 March	31.3	47.5	16.2	47.5	52.8	5.3	42.2		-42.2	0.0	0.0	-20.8	
5	Monday	02 March	34.0	52.1	18.1	53.6	60.4	6.8	48.3	3.0	-45.3	1.5	1.5	0.0	
6	Tuesday	03 March	31.7	55.1	23.4	56.6	58.5	1.9	46.8	3.0	-43.8	1.5	0.8	-0.7	
7	Wednesday	04 March	31.8	55.7	23.9	60.0	61.5	1.5	49.2	8.7	-40.5	4.3	2.2	-2.2	
8	Thursday	05 March	36.5	62.9	26.4	71.6	72.4	0.7	57.9	17.4	-40.5	8.7	6.5	-2.2	
9	Friday	06 March	39.1	68.0	28.9	78.1	83.2	5.1	66.6	20.2	-46.3	10.1	8.7	-1.4	
10	Saturday	07 March	40.9	72.3	31.5	82.5	86.8	4.3	69.4	20.2	-49.2	10.1	9.4	-0.7	
11	Sunday	08 March	42.7	74.5	31.8	86.1	92.3	6.2	73.8	23.2	-50.6	11.6	10.9	-0.7	
12	Monday	09 March	42.7	76.0	33.3	89.0	92.3	3.3	73.8	26.0	-47.8	13.0	12.3	-0.7	
13	Tuesday	10 March	48.1	76.7	28.6	93.3	117.6	24.2	94.0	33.3	-60.8	16.6	11.6	-5.1	
14	Wednesday	11 March	40.6	70.7	30.0	82.0	83.1	1.1	56.4	22.6	-43.8	11.3	11.3	0.0	
15	Thursday	12 March	39.6	68.5	29.0	84.1	83.1	-1.0	66.4	31.1	-35.4	15.5	12.7	-2.8	
End of Batch 2			37.238	60.285	23.049	68.801	76.870	8.069	61.496	17.032	-44.464	8.516	8.026	-2.490	-15.836
16	Friday	13 March	43.5	75.6	32.2	91.9	102.5	10.6	82.0	32.5	-49.4	16.3	15.6	-0.7	-7.4
17	Saturday	14 March	41.0	71.4	30.4	84.8	91.9	7.1	73.5	26.8	-46.6	13.4	12.7	-0.7	-9.9
18	Sunday	15 March	44.2	72.1	27.9	86.9	104.3	17.3	83.4	29.7	-53.7	14.8	14.8	0.0	-8.5
19	Monday	16 March	45.5	72.8	27.2	88.3	100.7	12.4	80.6	31.1	-49.5	15.5	14.8	-0.7	-10.6
20	Tuesday	17 March	24.9	66.0	41.1	77.0	9.4	-67.7	7.5	22.0	14.5	11.0	11.0	0.0	-12.0
End of Batch 3			39.818	71.572	31.754	85.784	81.720	-4.064	66.376	28.424	-36.952	14.212	13.788	-0.424	-9.686
21	Wednesday	18 March	36.8	66.0	29.2	75.6	86.0	10.3	68.8	19.2	-49.5	9.6	8.9	-0.7	-10.7
22	Thursday	19 March	36.4	62.6	26.1	70.8	73.9	3.1	59.1	16.5	-42.6	8.3	7.6	-0.7	-14.1
23	Friday	20 March	34.7	62.6	27.9	69.5	70.5	1.0	56.4	13.8	-42.6	6.9	6.9	0.0	-13.7
24	Saturday	21 March	38.2	63.3	25.1	71.5	77.4	5.8	61.9	16.5	-45.4	8.3	5.5	-2.8	-17.2
25	Sunday	22 March	39.5	64.8	25.2	75.8	86.0	10.2	68.8	22.0	-46.8	11.0	9.6	-1.4	-12.7
26	Monday	23 March	42.3	67.4	25.1	79.1	92.8	13.7	74.2	23.4	-50.9	11.7	11.7	0.0	-12.0
27	Tuesday	24 March	41.2	70.2	29.0	84.5	94.9	10.4	75.9	28.6	-47.3	14.3	11.5	-2.9	-10.7
28	Wednesday	25 March	39.4	70.2	30.8	80.9	85.9	5.0	68.7	21.5	-47.2	10.7	9.3	-1.4	-12.9
End of Batch 4			38.582	65.865	27.303	75.960	83.404	7.444	66.724	20.190	-46.534	10.095	8.868	-1.228	-10.014
29	Thursday	26 March	39.7	71.8	31.9	80.2	82.4	2.1	65.9	17.2	-48.7	8.6	7.2	-1.4	-16.1
30	Friday	27 March	40.3	69.5	29.2	79.5	79.6	0.1	63.7	20.0	-43.6	10.0	10.0	0.0	-14.3
31	Saturday	28 March	41.9	68.7	26.8	80.2	86.0	5.8	68.8	22.9	-45.8	11.5	9.3	-2.2	-15.4
32	Sunday	29 March	40.1	68.7	28.6	77.3	82.4	5.0	65.9	17.2	-48.7	8.6	8.6	0.0	-15.0
33	Monday	30 March	40.1	67.3	27.2	80.9	89.5	8.6	71.6	27.2	-44.4	13.6	13.6	0.0	-8.6
34	Tuesday	31 March	37.4	65.5	28.2	81.0	89.9	8.8	71.9	31.0	-40.9	15.5	10.6	-4.9	-8.8
35	Wednesday	01 April	32.1	64.1	32.1	68.3	67.0	-1.4	53.6	8.4	-45.1	4.2	4.2	0.0	-14.5
36	Thursday	02 April	32.8	65.5	32.8	70.5	68.7	-1.8	55.0	9.9	-45.1	4.9	4.2	-0.7	-14.8
End of Batch 5			38.035	67.630	29.595	77.248	80.656	3.409	64.525	19.235	-45.290	9.618	8.460	-1.158	-13.444
37	Friday	03 April	34.2	66.9	32.8	71.9	68.7	-3.2	55.0	9.9	-45.1	4.9	4.9	0.0	-15.5
38	Saturday	04 April	30.7	69.0	38.4	73.3	56.4	-16.9	45.1	8.4	-36.6	4.2	3.5	-0.7	-15.9
39	Sunday	05 April	33.1	69.0	35.9	74.7	70.5	-4.2	56.4	11.3	-45.1	5.6	5.6	0.0	-13.4
40	Monday	06 April	32.4	67.6	35.2	71.9	63.4	-8.5	50.7	8.4	-42.3	4.2	4.2	0.0	-15.5
41	Tuesday	07 April	41.6	81.7	40.2	95.1	98.7	3.5	78.9	26.8	-52.2	13.4	10.6	-2.8	-11.3
42	Wednesday	08 April	34.382	70.880	36.498	77.360	71.510	-5.850	57.208	12.960	-44.248	6.480	5.776	-0.704	-14.304
43	Thursday	09 April	40.8	79.6	38.7	89.3	94.2	4.9	75.4	19.5	-55.8	9.8	9.1	-0.7	-12.9
44	Friday	10 April	40.5	79.6	39.1	91.4	92.5	1.0	74.0	23.7	-50.2	11.9	11.2	-0.7	-10.8
45	Saturday	11 April	39.1	82.3	43.3	94.2	85.5	-8.7	68.4	23.7	-44.7	11.9	10.5	-1.4	-11.5
46	Sunday	12 April	39.1	75.4	36.3	93.5	83.8	-9.8	67.0	36.3	-30.7	18.1	18.1	0.0	-4.2
47	Monday	13 April	40.5	74.7	34.2	92.1	94.2	2.1	75.4	34.9	-40.5	17.4	15.4	-2.1	-6.3
48	Tuesday	14 April	40.5	69.1	28.6	94.2	89.0	-5.2	71.2	50.2	-21.0	25.1	22.3	-2.8	-0.3
49	Wednesday	15 April	40.067	76.783	36.697	92.463	89.850	-2.613	71.880	31.400	-40.480	15.700	14.423	-1.277	-7.873
50	Thursday	16 April	45.2	73.0	27.9	94.9	107.3	12.4	85.8	43.7	-42.2	21.8	22.5	0.8	-1.1
51	Friday	17 April	44.1	67.8	23.7	82.8	88.5	5.7	70.8	30.1	-40.7	15.1	15.1	0.0	-11.3
52	Saturday	18 April	44.8	76.8	32.0	91.1	99.8	8.7	79.8	28.6	-51.2	14.3	14.3	0.0	-10.5
53	Sunday	19 April	48.2	80.6	32.4	93.4	101.7	8.3	81.3	25.6	-55.7	12.8	12.8	0.0	-15.0
54	Monday	20 April	46.7	84.3	37.7	99.4	107.3	7.9	85.8	30.1	-55.7	15.1	15.1	0.0	-10.2
55	Tuesday	21 April	48.7	79.1	30.4	101.8	113.6	11.7	90.8	45.4	-45.4	22.7	20.5	-2.2	-5.5
56	Wednesday	22 April	49.1	79.1	30.0	101.1	115.4	14.3	92.3	44.0	-48.4	22.0	19.8	-2.2	-6.2
57	Thursday	23 April	49.8	85.0	35.2	105.5	119.1	13.5	95.2	41.0	-54.2	20.5	20.5	0.0	-5.5
58	Friday	24 April	63.0	92.3	29.3	120.1	133.7	13.6	107.0	55.7	-51.3	27.8	24.2	-3.7	-12.1
59	Saturday	25 April	56.4	82.1	25.7	123.1	135.6	12.5	108.4	82.0	-26.4	41.0	33.0	-8.1	3.7
60	Sunday	26 April	52.0	84.2	32.2	112.8	135.6	22.7	108.4	57.2	-51.3	28.6	35.2	6.6	10.3
61	Monday	27 April	49.815	80.398	30.582	102.371	114.300	11.929	91.440	43.949	-47.491	21.975	21.177	-0.798	-5.778
62	Tuesday	28 April	45.6	81.3	35.7	95.4	104.3	8.8	83.4	28.3	-55.1	14.1	13.4	-0.7	-11.3
63	Wednesday	29 April	42.1	78.4	36.4	91.9	99.0	7.1	79.2	26.8	-52.3	13.4	12.0	-1.4	-10.2
64	Thursday	30 April	39.9	70.7	30.7	84.1	90.1	6.0	72.1	26.8	-45.2	13.4	10.6	-2.8	-11.3
End of Batch 8			42.520	76.787	34.267	90.447	97.787	7.320	78.213	27.320	-50.893	13.860	12.913	-1.647	-10.953
65	Friday	03 May	39.9	75.6	35.7	87.6	97.2	9.5	77.7	24.0	-53.7	12.0	12.0	0.0	-8.5
66	Saturday	04 May	44.2	77.0	32.9	90.4	102.5	12.0	82.0	26.8	-55.1	13.4	12.7	-0.7	-11.0
67	Sunday	05 May	42.8	73.5	30.7	84.1	93.7	9.6	74.9	21.2	-53.7	10.6	10.6	0.0	-13.4
68	Monday	06 May	44.5	80.6	36.1	96.8	106.0	9.1	84.8	32.5	-52.2	16.3	14.4	-1.9	-8.9
69	Tuesday	07 May	44.5	82.0	37.5	99.6	106.0	5.3	84.8	35.3	-49.4	17.7	17.0	-0.7	-6.4
70	Wednesday	08 May	44.6	76.0	31.4	95.9	112.5	16.6	90.0	39.8	-50.2	19.9	18.4	-1.5	-3.7
End of Batch 10			43.415	77.443	34.028	92.423	102.942	10.518	82.353	29.960	-52.393	14.980	14.187	-0.793	-8.640
71	Thursday	09 May	35.8	72.3	36.5	84.1	72.0	-12.1	57.6	23.6	-34.0	11.8	11.1	-0.7	-10.3
72	Friday	10 May	41.7	62.0	20.3	72.3	88.6	16.3	70.8	20.6	-50.2	10.3	8.9	-1.5	-15.1
73	Saturday	11 May	38.4	70.1	31.7	82.6	92.2	9.6	73.8	25.1	-48.7	12.5	10.3	-2.2	-9.6
74	Sunday	12 May	41.3	68.6	27.3	88.5	99.6	11.1	79.7	39.8	-39.9	19.9	14.8	-5.1	-6.6
75	Monday	13 May	40.7	65.1	24.4	79.9	94.3	14.4	75.4	29.6	-45.8	14.8	14.1	-0.7	-7.8
76	Tuesday	14 May	40.7	65.1	24.4	77.7	92.5	14.8	74.0	25.2	-48.8	12.6	11.1	-1.5	-11.1
77	Wednesday	15 May	40.7	64.4	23.7	79.2	90.7	11.5	72.5	29.6	-42.9	14.8	13.3	-1.5	-9.2
78	Thursday	16 May	45.3	68.1	22.7	87.3	100.9	13.6	80.7	38.5	-42.2	19.2	17.8	-1.5	-7.4
79	Friday	17 May	36.6	65.8	29.2	87.3	98.0	10.7	78.4	42.9	-35.5	21.5	20.0	-1.5	3.0
80	Saturday	18 May	41.1												

## Mass Balance for Phosphorous

Day No.	1998	Anaerobic			Anoxic			Aerobic			Settler			Sum Diff.	
		Mass In mgP/l infl	Mass Out mgP/l infl	Diff	Mass In mgP/l infl	Mass Out mgP/l infl	Diff	Mass In mgP/l infl	Mass Out mgP/l infl	Diff	Mass In mgP/l infl	Mass Out mgP/l infl	Diff		
84	Wednesday	20 May	41.2	66.2	25.0	90.4	106.4	15.9	85.1	48.4	-36.6	24.2	23.5	-0.7	3.6
85	Thursday	21 May	47.0	72.6	25.6	96.9	108.6	11.7	86.9	48.4	-38.4	24.2	23.5	-0.7	-1.8
86	Friday	22 May	49.1	71.2	22.1	92.6	110.4	17.8	88.3	42.7	-45.6	21.4	21.4	0.0	-5.7
87	Saturday	23 May	43.6	68.4	24.7	90.4	108.6	18.2	86.9	44.2	-42.7	22.1	20.7	-1.4	-1.3
88	Sunday	24 May													
89	Monday	25 May	43.1	74.8	31.7	93.3	97.9	4.6	78.3	37.0	-41.3	18.5	18.5	0.0	-5.0
90	Tuesday	26 May	45.2	73.3	28.1	87.6	105.1	17.5	84.0	28.5	-55.6	14.2	11.4	-2.8	-12.8
91	Wednesday	27 May													
92	Thursday	28 May	46.5	81.4	34.9	95.5	103.8	8.3	83.0	28.2	-54.8	14.1	14.1	0.0	-11.6
93	Friday	29 May	44.8	34.7	39.9	95.5	99.3	3.8	79.4	21.6	-57.8	10.8	10.8	0.0	-14.1
94	Saturday	30 May	45.7	84.7	39.0	98.0	101.7	3.7	81.4	26.6	-54.8	13.3	13.3	0.0	-12.0
95	Sunday	31 May	51.5	88.8	37.4	104.6	114.2	9.5	91.3	31.6	-59.8	15.8	7.5	-8.3	-21.2
96	Monday	01 June	49.4	86.3	37.0	102.1	124.5	22.4	99.6	31.6	-68.0	15.3	14.9	-0.8	-9.5
97	Tuesday	02 June	56.0	87.2	31.1	103.8	151.5	47.7	121.2	33.2	-88.0	16.6	17.4	0.8	-8.3
98	Wednesday	03 June													
99	Thursday	04 June													
100	Friday	05 June	46.1	88.0	41.9	98.8	105.9	7.1	84.7	21.6	-63.1	10.8	8.3	-2.5	-16.6
	End of Batch 12		48.553	85.863	37.310	98.743	114.386	14.643	91.509	27.760	-63.749	13.880	12.337	-1.543	-13.339
101	Saturday	06 June	45.7	74.9	29.2	82.4	101.1	18.7	80.9	15.0	-65.9	7.5	6.7	-0.7	-18.7
102	Sunday	07 June	42.3	83.9	41.6	91.4	104.9	13.5	83.9	15.0	-68.9	7.5	4.5	-3.0	-16.8
103	Monday	08 June	44.2	95.6	51.5	103.1	106.7	3.6	85.4	15.0	-70.4	7.5	6.0	-1.5	-16.8
104	Tuesday	09 June	43.8	76.4	32.6	82.4	106.7	24.3	85.4	12.0	-73.4	6.0	5.2	-0.8	-17.2
105	Wednesday	10 June	47.9	65.2	17.2	77.1	127.3	50.2	101.8	24.0	-77.9	12.0	12.0	0.0	-10.5
106	Thursday	11 June	48.3	88.2	19.8	87.6	129.2	41.6	103.4	39.0	-64.4	19.5	13.5	-6.0	-9.0
107	Friday	12 June	44.8	62.8	18.0	87.3	126.4	39.0	101.1	49.1	-52.0	24.5	18.8	-5.8	-0.7
	End of Batch 13		45.283	75.277	29.994	87.340	114.600	27.260	91.680	24.126	-67.554	12.063	9.529	-2.534	-12.834
108	Saturday	13 June	45.5	63.5	18.0	72.2	108.3	36.1	86.6	17.3	-69.3	8.7	6.5	-2.2	-17.3
109	Sunday	14 June													
110	Monday	15 June													
111	Tuesday	16 June													
112	Wednesday	17 June													
	End of Batch 14		45.480	83.520	18.040	72.180	108.300	36.120	86.640	17.320	-69.320	9.660	6.500	-2.160	-17.320
113	Thursday	18 June	45.5	59.9	14.4	81.6	104.7	23.1	83.8	43.3	-40.4	21.7	22.4	0.7	-2.2
114	Friday	19 June													
115	Saturday	20 June													
116	Sunday	21 June	43.3	59.9	16.6	85.2	108.3	23.1	86.6	50.5	-36.1	25.3	23.8	-1.4	2.2
117	Monday	22 June	45.5	58.5	13.0	82.3	110.1	27.8	88.1	47.6	-40.4	23.8	23.8	0.0	0.4
	End of Batch 15		44.760	59.440	14.680	83.020	107.700	24.680	88.180	47.160	-39.000	23.580	23.340	-0.240	0.120
118	Tuesday	23 June	43.7	57.2	13.5	86.0	110.0	24.0	88.0	57.8	-30.2	28.9	25.3	-3.6	3.6
119	Wednesday	24 June	48.0	56.3	8.3	91.0	122.7	31.7	98.2	69.3	-28.8	34.7	32.5	-2.2	9.0
120	Thursday	25 June	49.7	59.0	9.4	97.9	129.6	31.7	103.7	77.8	-25.9	38.9	36.0	-2.9	12.2
121	Friday	26 June													
122	Saturday	27 June													
123	Sunday	28 June													
	End of Batch 16		47.116	57.500	10.384	91.640	120.770	29.130	96.616	68.280	-28.336	34.140	31.247	-2.893	8.285
124	Monday	29 June	40.7	44.6	4.0	59.8	81.0	21.2	64.8	30.2	-34.6	15.1	14.4	-0.7	-10.1
125	Tuesday	30 June	40.0	50.4	10.4	68.4	90.0	21.6	72.0	36.0	-36.0	18.0	15.1	-2.9	-6.8
126	Wednesday	01 July	45.4	52.6	7.2	82.8	109.8	27.0	87.8	60.5	-27.4	30.2	23.0	-7.2	-0.4
127	Thursday	02 July													
128	Friday	03 July													
129	Saturday	04 July													
130	Sunday	05 July													
131	Monday	06 July	46.1	46.1	0.0	82.1	108.0	25.9	86.4	72.0	-14.4	36.0	35.3	-0.7	
132	Tuesday	07 July	48.6	61.2	12.6	90.7	99.0	8.3	79.2	59.0	-20.2	29.5	33.1	3.6	4.3
	End of Batch 17		44.136	50.976	6.840	76.752	97.560	20.808	78.048	51.552	-26.496	25.776	24.192	-1.584	-2.592
133	Wednesday	08 July	46.1	46.1	0.0	79.9	109.8	29.9	87.8	67.7	-20.2	33.8	31.7	-2.2	
134	Thursday	09 July	46.4	42.7	-3.7	74.3	101.8	27.5	81.4	63.2	-18.2	31.6	32.7	1.1	6.7
135	Friday	10 July	46.4	49.4	3.0	85.4	113.4	28.0	90.7	72.0	-18.7	36.0	33.4	-2.7	9.7
136	Saturday	11 July	48.7	448.7	400.0	487.4	111.8	-375.7	89.4	77.4	-12.0	38.7	37.4	-1.3	11.0
137	Sunday	12 July	46.4	45.4	-1.0	82.7	108.4	25.7	86.7	74.7	-12.0	37.4	37.4	0.0	12.7
138	Monday	13 July	48.4	50.7	2.3	93.4	118.5	25.1	94.8	85.4	-9.4	42.7	40.0	-2.7	15.4
139	Tuesday	14 July													
140	Wednesday	15 July													
141	Thursday	16 July	44.0	38.7	-5.3	70.1	90.1	20.0	72.0	62.7	-9.3	31.4	32.0	0.7	6.0
142	Friday	17 July	42.5	39.7	-2.8	68.8	90.4	21.6	72.3	58.1	-14.2	29.1	24.2	-4.9	-0.3
143	Saturday	18 July													
144	Sunday	19 July													
145	Monday	20 July													
	End of Batch 18		46.104	95.165	49.061	130.243	105.500	-24.742	84.400	70.155	-14.245	35.078	33.588	-1.490	7.639
146	Tuesday	21 July	37.9	30.5	-7.5	51.2	62.1	10.8	49.6	41.5	-8.2	20.7	15.6	-5.1	-9.9
147	Wednesday	22 July													
	End of Batch 19		37.930	30.480	-7.450	51.220	62.050	10.830	49.640	41.480	-8.160	20.740	15.600	-5.140	-9.920
148	Thursday	23 July	42.2	42.5	0.4	77.3	109.9	32.6	87.9	69.5	-18.4	34.7	31.9	-2.8	11.7
149	Friday	24 July	40.1	42.5	2.5	75.9	106.4	30.5	85.1	66.6	-18.4	33.3	33.3	0.0	14.5
150	Saturday	25 July	40.1	75.2	35.1	104.2	99.3	-5.0	79.4	58.1	-21.3	29.1	28.4	-0.7	8.1
151	Sunday	26 July	41.1	44.7	3.5	70.9	97.5	26.6	78.0	52.5	-25.5	26.2	28.4	2.1	6.7
152	Monday	27 July													
	End of Batch 20		40.858	51.225	10.367	82.065	103.250	21.185	82.600	61.680	-20.920	30.840	30.485	-0.355	10.277
153	Tuesday	28 July	42.5	48.9	6.4	75.9	99.3	23.4	79.4	53.9	-25.5	26.9	26.9	0.0	4.2
154	Wednesday	29 July	43.5	45.2	1.7	71.6	86.9	15.3	69.5	52.8	-16.7	26.4	26.4	0.0	0.4
155	Thursday	30 July	42.1	47.9	5.8	77.6	102.8	25.0	82.0	59.4	-22.6	29.7	29.1	-0.6	7.6
156	Friday	31 July	43.5	48.7	5.2	77.9	99.1	21.2	79.2	58.4	-20.8	29.2	27.8	-1.4	4.2
157	Saturday	01 August													
158	Sunday	02 August													
159	Monday	03 August													
	End of Batch 21		42.875	47.665	4.790	75.730	96.938	21.208	77.550	58.130	-21.420	28.065	27.565	-0.500	4.078
160	Tuesday	04 August	42.4	48.7	6.3	75.8	99.1	23.3	79.2	54.2	-25.0	27.1	26.4	-0.7	3.8
161	Wednesday	05 August	39.3	46.6	7.3	76.5	88.7	12.2	70.9	59.8	-11.1	29.9	28.5	-1.4	7.0
162	Thursday	06 August													
163	Friday	07 August	36.8	43.1	6.3	70.2	78.2	8.0	62.6	54.2	-8.3	27.1	27.1	0.0	5.9
164	Saturday	08 August													
165	Sunday	09 August													
166	Monday	10 August													
167	Tuesday	11 August													
168	Wednesday	12 August	35.1	40.0	4.9	64.6	72.0	7.4	57.6	49.1	-8.4	24.6	23.9	-0.7	3.2
169	Thursday	13 August	37.2	28.1	-9.1	56.9	84.2	27.3	67.4	57.6	-9.8	28.8	23.9	-4.9	3.5
170	Friday	14 August													
171	Saturday	15 August	19.7	42.8	23.2	71.6	0.0	0.0	57.6			28.8	28.1	-0.7	

## Mass Balance for Nitrogen

Day No.	1998	NO <sub>3</sub> denit mgN/d	Den in AN	Sum	N in Wast mgN/d	TKN in Eff mgN/d	NO <sub>3</sub> in Eff mgN/d	MB mgN/d
1	Thursday 26 February	438.4	0.0	438.4	404.4	417.2	116.0	94.7
2	Friday 27 February	690.0	0.0	690.0	396.8	258.0	202.0	107.1
3	Saturday 28 February	629.4	0.0	629.4	377.6	137.2	226.0	100.5
4	Sunday 01 March	750.2	0.0	750.2	372.8	137.2	250.0	110.5
5	Monday 02 March	713.8	0.0	713.8	366.8	58.8	240.0	98.1
6	Tuesday 03 March	751.6	0.0	751.6	398.4	64.4	260.0	109.2
7	Wednesday 04 March	796.2	7.8	804.0	375.2	89.6	320.0	118.7
8	Thursday 05 March	862.4	1.6	864.0	282.8	78.4	304.0	105.4
9	Friday 06 March	911.4	0.6	912.0	380.8	103.6	320.0	107.4
10	Saturday 07 March	916.8	0.0	916.8	422.8	98.0	324.0	113.2
11	Sunday 08 March	920.2	0.0	920.2	343.0	72.8	320.0	105.4
12	Monday 09 March	906.0	0.0	906.0	403.2	67.2	324.0	113.5
13	Tuesday 10 March	774.4	28.8	803.2	302.4	72.8	304.0	95.9
14	Wednesday 11 March	961.4	21.0	982.4	366.8	95.2	420.0	122.0
15	Thursday 12 March	795.8	37.0	832.8	337.4	67.2	368.0	105.2
	<b>End of Batch 2</b>	<b>787.9</b>	<b>6.5</b>	<b>794.3</b>	<b>368.7</b>	<b>121.2</b>	<b>286.5</b>	<b>107.1</b>
16	Friday 13 March	893.2	2.0	895.2	352.8	70.0	332.0	116.9
17	Saturday 14 March	851.2	8.0	859.2	322.0	81.2	288.0	105.7
18	Sunday 15 March	883.2	4.6	887.8	343.0	61.6	332.0	108.6
19	Monday 16 March	755.2	0.8	756.0	302.4	81.2	260.0	95.2
20	Tuesday 17 March	767.0	1.0	768.0	369.6	117.6	284.0	100.5
	<b>End of Batch 3</b>	<b>830.0</b>	<b>3.3</b>	<b>833.2</b>	<b>338.0</b>	<b>82.3</b>	<b>299.2</b>	<b>105.4</b>
21	Wednesday 18 March	730.4	8.0	738.4	352.8	89.6	268.0	101.3
22	Thursday 19 March	758.0	6.0	764.0	331.8	56.0	252.0	102.1
23	Friday 20 March	807.0	18.6	825.6	299.6	58.8	300.0	109.1
24	Saturday 21 March	847.2	3.2	850.4	305.2	61.6	356.0	105.8
25	Sunday 22 March	833.0	3.0	836.0	282.8	58.8	312.0	104.3
26	Monday 23 March	757.0	3.0	760.0	288.4	72.8	276.0	95.2
27	Tuesday 24 March	718.6	6.2	724.8	268.8	72.8	272.0	88.5
28	Wednesday 25 March	719.0	7.8	726.8	291.2	64.4	234.0	90.8
	<b>End of Batch 4</b>	<b>771.3</b>	<b>7.0</b>	<b>778.3</b>	<b>302.6</b>	<b>66.9</b>	<b>283.8</b>	<b>99.6</b>
29	Thursday 26 March	726.8	10.8	737.6	322.0	89.6	260.0	95.7
30	Friday 27 March	538.0	1.2	539.2	288.4	72.8	200.0	110.4
31	Saturday 28 March	473.6	3.6	477.2	277.2	42.0	170.0	81.0
32	Sunday 29 March	458.0	5.2	463.2	302.4	42.0	160.0	89.3
33	Monday 30 March	434.8	5.6	440.4	263.2	53.2	154.0	77.1
34	Tuesday 31 March	445.0	0.2	445.2	289.8	47.6	162.0	84.3
35	Wednesday 01 April	469.2	2.0	471.2	308.0	44.8	176.0	87.3
36	Thursday 02 April	462.4	1.6	464.0	294.0	58.8	180.0	96.5
	<b>End of Batch 5</b>	<b>501.0</b>	<b>3.8</b>	<b>504.8</b>	<b>293.1</b>	<b>56.4</b>	<b>182.8</b>	<b>90.2</b>
37	Friday 03 April	474.0	2.0	476.0	343.0	47.6	168.0	93.8
38	Saturday 04 April							
39	Sunday 05 April	422.0	0.0	422.0	309.4	47.6	166.0	81.1
40	Monday 06 April	451.2	0.0	451.2	301.0	58.8	150.0	81.1
41	Tuesday 07 April	427.4	0.6	428.0	320.6	50.4	140.0	80.2
42	Wednesday 08 April							
43	Thursday 09 April	778.0	13.2	791.2	375.2	126.0	296.0	80.0
	<b>End of Batch 6</b>	<b>510.5</b>	<b>3.2</b>	<b>513.7</b>	<b>329.8</b>	<b>66.1</b>	<b>184.0</b>	<b>83.3</b>
44	Friday 10 April	644.0	66.0	710.0	315.0	45.0	350.0	69.2
45	Saturday 11 April	582.8	115.2	698.0	341.6	53.2	414.0	92.9
46	Sunday 12 April							
47	Monday 13 April	623.2	160.8	784.0	347.2	106.4	500.0	95.0
48	Tuesday 14 April	670.4	143.6	814.0	330.4	61.6	470.0	82.4
49	Wednesday 15 April	679.8	140.2	820.0	348.6	58.8	480.0	83.3
50	Thursday 16 April	735.2	116.8	852.0	331.8	95.2	432.0	85.2
	<b>End of Batch 7</b>	<b>655.9</b>	<b>123.8</b>	<b>779.7</b>	<b>335.8</b>	<b>70.0</b>	<b>441.0</b>	<b>84.7</b>
51	Friday 17 April	963.0	0.0	963.0	376.6	81.2	394.0	115.5
52	Saturday 18 April							
53	Sunday 19 April	674.2	7.8	682.0	282.8	64.4	270.0	83.6
54	Monday 20 April	628.0	2.0	630.0	333.2	70.0	254.0	81.2
55	Tuesday 21 April	698.2	7.8	706.0	254.8	47.6	250.0	83.1
56	Wednesday 22 April	663.4	10.6	674.0	263.2	61.6	262.0	97.0
57	Thursday 23 April	602.8	32.0	634.8	333.2	89.7	270.0	89.5
58	Friday 24 April	553.6	37.6	591.2	260.4	81.2	296.0	77.5
59	Saturday 25 April	671.8	25.0	696.8	294.0	95.2	324.0	108.8
60	Sunday 26 April	633.4	14.6	648.0	288.4	78.4	280.0	87.3
61	Monday 27 April							
62	Tuesday 28 April	684.2	23.4	707.6	352.8	98.0	306.0	107.4
63	Wednesday 29 April	527.4	4.6	532.0	266.0	56.0	220.0	79.7
	<b>End of Batch 8</b>	<b>663.6</b>	<b>15.0</b>	<b>678.7</b>	<b>300.5</b>	<b>74.8</b>	<b>284.2</b>	<b>91.9</b>
64	Thursday 30 April	650.0	0.0	650.0	322.0	61.6	210.0	90.3
65	Friday 01 May	441.6	0.0	441.6	302.4	56.0	218.0	77.7
66	Saturday 02 May	543.8	4.2	548.0	254.8	72.8	232.0	87.1
	<b>End of Batch 9</b>	<b>545.1</b>	<b>1.4</b>	<b>546.5</b>	<b>293.1</b>	<b>63.5</b>	<b>220.0</b>	<b>85.0</b>
67	Sunday 03 May	658.8	6.4	665.2	296.8	67.2	210.0	92.6
68	Monday 04 May	794.0	3.2	797.2	322.0	64.4	210.0	110.1
69	Tuesday 05 May	654.0	2.4	656.4	271.6	72.8	262.0	91.1
70	Wednesday 06 May	705.8	6.2	712.0	238.0	0.0	252.0	95.0
71	Thursday 07 May	638.6	10.2	648.8	0.0	28.0	248.0	72.6
72	Friday 08 May	878.2	15.8	894.0	327.6	86.8	310.0	120.2
	<b>End of Batch 10</b>	<b>721.6</b>	<b>7.4</b>	<b>728.9</b>	<b>242.7</b>	<b>53.2</b>	<b>248.7</b>	<b>96.9</b>
73	Saturday 09 May							
74	Sunday 10 May	654.2	31.0	685.2	257.6	98.0	282.0	130.5
75	Monday 11 May	765.0	25.0	790.0	266.0	123.2	350.0	116.2
76	Tuesday 12 May	711.8	18.2	730.0	196.0	53.2	326.0	86.6
77	Wednesday 13 May	660.4	21.2	681.6	0.0	126.0	300.0	71.4
78	Thursday 14 May	1034.4	0.0	1034.4	316.4	170.8	370.0	118.3
79	Friday 15 May	1089.2	2.4	1091.6	277.2	100.8	374.0	111.4
80	Saturday 16 May	943.4	36.6	980.0	313.6	70.0	392.0	112.8
81	Sunday 17 May	886.6	37.4	924.0	352.8	61.6	412.0	99.2
82	Monday 18 May	778.2	41.8	820.0	252.0	78.4	384.0	94.8
83	Tuesday 19 May	1113.0	0.6	1113.6	257.6	7.3	400.0	118.5
	<b>End of Batch 11</b>	<b>863.6</b>	<b>21.4</b>	<b>885.0</b>	<b>248.9</b>	<b>88.9</b>	<b>359.0</b>	<b>106.0</b>

D.9

Mass Balance for Nitrogen

Day No.	1998	NO3 denit mgN/d	Den in A	Sum	N in Wast mgN/d	TKN in Eff mgN/d	NO3 in Eff mgN/d	MB mgN/d
84	Wednesday 20 May	1258.8	2.8	1259.6	308.0	95.2	486.0	144.3
85	Thursday 21 May	1425.6	0.0	1425.6	288.4	58.8	526.0	143.0
86	Friday 22 May	1306.0	0.0	1306.0	324.8	81.2	478.0	103.9
87	Saturday 23 May	1271.0	0.0	1271.0	224.0	185.2	440.0	101.2
88	Sunday 24 May							
89	Monday 25 May	1088.8	0.0	1088.8	0.0	106.4	352.0	75.1
90	Tuesday 26 May							
91	Wednesday 27 May							
92	Thursday 28 May	950.0	6.0	956.0	389.2	64.4	252.0	118.7
93	Friday 29 May	564.6	30.6	595.2	355.6	64.4	252.0	73.9
94	Saturday 30 May	706.2	10.6	716.8	316.4	58.8	252.0	98.8
95	Sunday 31 May	604.0	18.4	622.4	238.0	44.8	256.0	87.1
96	Monday 01 June	583.6	14.0	577.6	260.3	86.8	232.0	82.5
97	Tuesday 02 June	610.0	0.0	610.0	355.6	112.0	176.0	83.7
98	Wednesday 03 June							
99	Thursday 04 June							
100	Friday 05 June	740.8	10.6	751.2	372.4	33.6	288.0	107.3
End of Batch 12		677.0	12.9	689.9	326.8	66.4	244.0	93.1
101	Saturday 06 June	1051.8	0.0	1051.8	305.2	86.8	380.0	124.5
102	Sunday 07 June	647.8	64.2	712.0	300.0	98.0	292.0	91.5
103	Monday 08 June	616.0	48.8	664.8	431.2	44.8	340.0	102.9
104	Tuesday 09 June	847.8	36.2	884.0	361.2	47.6	360.0	104.8
105	Wednesday 10 June	948.0	29.6	977.6	313.6	131.6	376.0	112.7
106	Thursday 11 June	1305.4	0.0	1305.4	296.8	112.0	596.0	139.4
107	Friday 12 June	1459.6	0.0	1459.6	226.8	70.0	620.0	153.2
End of Batch 13		982.3	25.5	1007.9	319.3	84.4	423.4	118.4
108	Saturday 13 June	1649.4	0.0	1649.4	319.2	226.8	800.0	149.5
109	Sunday 14 June							
110	Monday 15 June							
111	Tuesday 16 June							
112	Wednesday 17 June							
End of Batch 14		1649.4	0.0	1649.4	319.2	226.8	600.0	149.5
113	Thursday 18 June	1861.0	9.4	1870.4	274.4	644.0	860.0	129.7
114	Friday 19 June							
115	Saturday 20 June							
116	Sunday 21 June							
117	Monday 22 June	2441.6	6.4	2448.0	366.8	818.0	736.0	140.8
End of Batch 15		2151.3	7.9	2159.2	320.6	731.0	698.0	135.2
118	Tuesday 23 June	2477.2	22.0	2499.2	310.8	518.0	880.0	247.2
119	Wednesday 24 June	2149.2	10.8	2160.0	271.6	142.8	632.0	170.9
120	Thursday 25 June	1141.0	0.0	1141.0	308.0	162.4	380.0	105.8
121	Friday 26 June							
122	Saturday 27 June							
123	Sunday 28 June							
End of Batch 16		1922.5	10.9	1933.4	296.8	274.4	630.7	174.6
124	Monday 29 June	1167.8	1.0	1168.8	0.0	92.4	300.0	94.5
125	Tuesday 30 June	1187.0	0.2	1187.2	294.0	89.6	400.0	102.3
126	Wednesday 01 July	1198.2	2.2	1200.4	271.6	81.2	418.0	121.8
127	Thursday 02 July							
128	Friday 03 July							
129	Saturday 04 July							
130	Sunday 05 July							
131	Monday 06 July	1113.2	0.0	1113.2	252.0	154.0	372.0	94.5
132	Tuesday 07 July	1079.8	0.0	1079.8	347.2	131.6	404.0	102.5
End of Batch 17		1149.2	0.7	1149.9	233.0	109.8	394.8	103.1
133	Wednesday 08 July	866.8	0.0	866.8	338.8	103.6	300.0	119.2
134	Thursday 09 July	745.0	4.6	749.6	291.2	0.0	256.0	94.9
135	Friday 10 July	878.8	0.0	878.8	310.8	44.8	262.0	100.4
136	Saturday 11 July	912.2	5.4	917.6	313.6	78.4	300.0	109.7
137	Sunday 12 July	961.4	8.6	970.0	268.8	78.4	314.0	107.1
138	Monday 13 July	878.0	0.4	878.4	198.8	198.8	260.0	99.7
139	Tuesday 14 July							
140	Wednesday 15 July							
141	Thursday 16 July	901.2	0.0	901.2	266.0	162.4	292.0	102.7
142	Friday 17 July	929.8	9.0	938.8	0.0	95.2	302.0	88.9
143	Saturday 18 July							
144	Sunday 19 July							
145	Monday 20 July							
End of Batch 18		886.7	3.5	890.2	248.5	95.2	285.8	102.8
146	Tuesday 21 July	795.2	6.0	801.2	277.2	33.6	342.0	141.9
147	Wednesday 22 July							
End of Batch 19		795.2	6.0	801.2	277.2	33.6	342.0	141.9
148	Thursday 23 July	833.8	1.4	835.2	296.8	120.4	280.0	91.2
149	Friday 24 July	645.2	23.6	668.8	285.6	126.0	240.0	85.0
150	Saturday 25 July	800.8	5.6	806.4	249.2	84.0	264.0	100.3
151	Sunday 26 July	998.4	5.2	1003.6	310.8	120.4	342.0	121.1
152	Monday 27 July							
End of Batch 20		819.6	8.3	828.5	285.6	112.7	281.5	94.4
153	Tuesday 28 July	924.2	0.0	924.2	313.6	134.4	288.0	120.8
154	Wednesday 29 July							
155	Thursday 30 July							
156	Friday 31 July							
157	Saturday 01 August							
158	Sunday 02 August							
159	Monday 03 August							
End of Batch 21		924.2	0.0	924.2	313.6	134.4	288.0	120.8
160	Tuesday 04 August							
161	Wednesday 05 August							
162	Thursday 06 August							
163	Friday 07 August							
164	Saturday 08 August							
165	Sunday 09 August							
166	Monday 10 August							
167	Tuesday 11 August							
168	Wednesday 12 August							
169	Thursday 13 August							
170	Friday 14 August							
171	Saturday 15 August							
172	Sunday 16 August							
173	Monday 17 August							
End of Batch 22		ERR	ERR	ERR	ERR	ERR	ERR	ERR

## COD Mass Balance

Day No.	1998	Sum den MSnod	MSnoe	MSno	MO n mgO/d	MO c mgO/d	MO d mgO/d	COD in W mgO/d	COD in E MStE	MB
1	Thursday 26 February	438.4	116.0	554.4	2533.6	9226.4	1253.8	5985.1	3042.6	149.1
2	Friday 27 February	690.0	202.0	892.0	4076.4	3723.6	1973.4	5872.6	2194.6	96.2
3	Saturday 28 February	629.4	226.0	855.4	3909.2	3266.8	1800.1	5588.5	1869.4	94.0
4	Sunday 01 March	750.2	250.0	1000.2	4570.9	3709.1	2145.6	5517.4	1463.0	87.7
5	Monday 02 March	713.8	240.0	953.8	4358.9	4197.1	2041.5	5428.6	2112.0	71.8
6	Tuesday 03 March	751.6	260.0	1011.6	4623.0	5985.0	2149.6	5896.3	1625.6	120.4
7	Wednesday 04 March	804.0	320.0	1124.0	5136.7	5063.3	2299.4	5553.0	1422.4	108.2
8	Thursday 05 March	864.0	304.0	1168.0	5337.8	4094.2	2471.0	5283.2	1503.6	104.0
9	Friday 06 March	912.0	320.0	1232.0	5630.2	4233.8	2608.3	5608.3	1422.4	90.8
10	Saturday 07 March	916.8	324.0	1240.8	5670.5	3977.5	2622.0	4917.4	1219.2	85.6
11	Sunday 08 March	920.2	320.0	1240.2	5867.7	4556.3	2631.8	4836.2	894.0	90.8
12	Monday 09 March	906.0	324.0	1230.0	5621.1	4266.9	2591.2	4795.5	894.0	93.0
13	Tuesday 10 March	803.2	304.0	1107.2	5059.9	4972.1	2297.2	3722.4	827.2	79.8
14	Wednesday 11 March	982.4	420.0	1402.4	6409.0	3647.0	2809.7	4921.8	1034.0	85.7
15	Thursday 12 March	832.8	368.0	1200.8	5487.7	4496.3	2381.8	4921.8	1406.2	88.2
End of Batch 2		794.3	286.5	1080.9	4939.5	4627.7	2271.8	5256.6	1528.7	96.4
16	Friday 13 March	895.2	332.0	1227.2	5608.3	3487.7	2580.3	5294.1	1116.8	80.1
17	Saturday 14 March	859.2	288.0	1147.2	5242.7	3445.3	2457.3	4880.5	1075.4	76.3
18	Sunday 15 March	887.8	332.0	1219.8	5574.7	2729.3	2539.2	4839.1	992.6	63.3
19	Monday 16 March	756.0	260.0	1016.0	4643.1	3876.9	2162.2	4797.8	744.4	67.3
20	Tuesday 17 March	768.0	284.0	1052.0	4807.6	3808.4	2196.5	5004.6	1406.2	77.4
End of Batch 3		833.2	299.2	1132.4	5175.3	3469.5	2383.1	4963.2	1067.1	72.9
21	Wednesday 18 March	738.4	268.0	1006.4	4599.2	4088.8	2111.8	5128.6	1034.0	83.0
22	Thursday 19 March	764.0	252.0	1016.0	4643.1	3324.9	2185.0	4549.6	1158.0	77.9
23	Friday 20 March	825.6	300.0	1125.6	5144.0	2848.0	2361.2	4333.3	1185.6	70.9
24	Saturday 21 March	850.4	356.0	1206.4	5513.2	2598.8	2432.1	4496.8	981.2	64.9
25	Sunday 22 March	836.0	312.0	1148.0	5246.4	2721.6	2391.0	4251.5	817.6	70.8
26	Monday 23 March	760.0	276.0	1036.0	4734.5	3305.5	2173.6	4578.6	1308.2	73.2
27	Tuesday 24 March	724.8	272.0	996.8	4555.4	3676.6	2072.9	4742.1	1553.4	75.2
28	Wednesday 25 March	726.8	234.0	960.8	4390.9	3793.1	2078.6	4415.0	1390.0	82.1
End of Batch 4		778.3	283.8	1062.0	4853.3	3294.7	2225.8	4561.9	1178.5	74.7
29	Thursday 26 March	737.6	260.0	997.6	4559.0	3457.0	2109.5	4210.6	1062.8	80.8
30	Friday 27 March	539.2	200.0	739.2	3378.1	4325.9	1542.1	5110.0	1349.0	84.2
31	Saturday 28 March	477.2	170.0	647.2	2957.7	3762.3	1364.8	4756.4	1240.8	65.3
32	Sunday 29 March	463.2	160.0	623.2	2848.0	4112.0	1324.8	4260.1	827.2	72.3
33	Monday 30 March	440.4	154.0	594.4	2716.4	4051.6	1259.5	4880.5	1199.4	74.0
34	Tuesday 31 March	445.2	162.0	607.2	2774.9	4305.1	1273.3	4425.5	992.6	73.0
35	Wednesday 01 April	471.2	176.0	647.2	2957.7	6954.3	1347.6	5087.3	1199.4	92.3
36	Thursday 02 April	464.0	180.0	644.0	2943.1	7280.9	1327.0	5128.6	1158.0	102.3
End of Batch 5		504.8	182.8	687.5	3141.9	4781.1	1443.6	4732.4	1128.7	80.5
37	Friday 03 April	476.0	168.0	644.0	2943.1	7112.9	1361.4	5128.6	1034.0	98.9
38	Saturday 04 April									
39	Sunday 05 April	422.0	166.0	588.0	2687.2		1206.9	5045.9	1116.8	
40	Monday 06 April	451.2	150.0	601.2	2747.5	7668.5	1290.4	4797.8	910.0	92.8
41	Tuesday 07 April	428.0	140.0	568.0	2595.8	6908.2	1224.1	4508.2	661.8	75.9
42	Wednesday 08 April									
43	Thursday 09 April	791.2	296.0	1087.2	4968.5	4511.5	2262.8	4958.1	894.0	71.7
End of Batch 6		513.7	184.0	697.7	3188.4	5240.2	1469.1	4887.7	923.3	67.8
44	Friday 10 April	710.0	350.0	1060.0	4844.2	8235.8	2030.6	4795.5	731.6	106.8
45	Saturday 11 April	698.0	414.0	1112.0	5081.8	9455.0	1996.3	5161.3	812.8	114.6
46	Sunday 12 April									
47	Monday 13 April	784.0	500.0	1284.0	5867.9	6732.1	2242.2	4592.3	1219.2	81.9
48	Tuesday 14 April	814.0	470.0	1284.0	5867.9	7788.1	2328.0	4673.6	731.6	106.1
49	Wednesday 15 April	820.0	480.0	1300.0	5941.0	7163.0	2345.2	4551.7	690.8	101.4
50	Thursday 16 April	852.0	432.0	1284.0	5867.9	5844.1	2436.7	4511.0	1056.6	93.6
End of Batch 7		779.7	441.0	1220.7	5578.4	7536.4	2229.8	4714.2	873.8	100.7
51	Friday 17 April	963.0	394.0	1357.0	6201.5	4502.5	2754.2	4267.2	1056.6	84.6
52	Saturday 18 April									
53	Sunday 19 April	682.0	270.0	952.0	4350.6	4769.4	1950.5	3942.1	1219.2	75.3
54	Monday 20 April	630.0	254.0	884.0	4039.9	6160.1	1801.8	4664.6	1403.6	89.9
55	Tuesday 21 April	706.0	250.0	956.0	4368.9	5399.1	2019.2	5036.2	1073.2	83.2
56	Wednesday 22 April	674.0	262.0	936.0	4277.5	3594.5	1927.6	4293.1	990.8	71.9
57	Thursday 23 April	634.8	270.0	904.8	4134.9	4049.1	1815.5	3715.2	990.8	70.3
58	Friday 24 April	591.2	296.0	887.2	4054.5	3649.5	1690.8	4994.9	866.8	76.7
59	Saturday 25 April	696.8	324.0	1020.8	4665.1	2750.9	1992.8	4540.8	990.8	69.9
60	Sunday 26 April	648.0	280.0	928.0	4241.0	5383.0	1853.3	4210.8	908.2	75.6
61	Monday 27 April									
62	Tuesday 28 April	707.6	306.0	1013.6	4632.2	5543.8	2023.7	5449.0	743.0	95.8
63	Wednesday 29 April	532.0	220.0	752.0	3436.6	4555.4	1521.5	5366.4	908.2	91.8
End of Batch 8		678.7	284.2	962.9	4400.2	4577.9	1941.0	4589.1	1013.7	80.5
64	Thursday 30 April	650.0	210.0	860.0	3930.2	4973.8	1859.0	5280.0	1200.0	78.1
65	Friday 01 May	441.6	218.0	659.6	3014.4	7281.6	1263.0	3920.0	720.0	82.8
66	Saturday 02 May	548.0	232.0	780.0	3564.6	5819.4	1567.3	4480.0	880.0	80.5
End of Batch 9		546.5	220.0	766.5	3503.1	6024.9	1563.1	4560.0	933.3	80.5
67	Sunday 03 May	665.2	210.0	875.2	3999.7	5888.3	1902.5	5280.0	880.0	93.8
68	Monday 04 May	797.2	210.0	1007.2	4602.9	4757.1	2280.0	3920.0	960.0	77.6
69	Tuesday 05 May	656.4	262.0	918.4	4197.1	5210.9	1877.3	3680.0	960.0	75.6
70	Wednesday 06 May	712.0	252.0	964.0	4405.5	5338.5	2036.3	3560.0	840.0	68.5
71	Thursday 07 May	648.8	248.0	896.8	4098.4	5093.6	1855.6	4080.0	1440.0	85.6
72	Friday 08 May	894.0	310.0	1204.0	5502.3	3593.7	2556.8	3840.0	1680.0	89.0
End of Batch 10		728.9	248.7	977.6	4467.8	4980.4	2084.7	4060.0	1126.7	81.7
73	Saturday 09 May									
74	Sunday 10 May	685.2	282.0	967.2	4420.1	3211.9	1959.7	4960.0	800.0	74.0
75	Monday 11 May	790.0	350.0	1140.0	5209.8	2662.2	2259.4	4760.6	1149.2	68.7
76	Tuesday 12 May	730.0	326.0	1056.0	4825.9	3238.1	2087.8	3899.8	1231.2	81.1
77	Wednesday 13 May	681.6	300.0	981.6	4485.9	3626.1	1949.4	4589.8	1231.2	72.3
78	Thursday 14 May	1034.4	370.0	1404.4	6418.1		2958.4	4432.3	1477.4	
79	Friday 15 May	1091.6	374.0	1465.6	6697.8	2230.2	3122.0	4514.4	1641.6	78.4
80	Saturday 16 May	980.0	392.0	1372.0	6270.0	2226.0	2802.8	4350.2	1477.4	75.2
81	Sunday 17 May	924.0	412.0	1336.0	6105.5	3278.5	2642.6	4924.8	1477.4	92.7
82	Monday 18 May	820.0	384.0	1204.0	5502.3	3185.7	2345.2	4324.8	897.6	89.0
83	Tuesday 19 May	1113.6	400.0	1513.6	6917.2	1386.8	3184.9	5140.8	1632.0	84.3
End of Batch 11		885.0	359.0	1244.0	5685.3	2504.5	2531.2	4589.8	1301.5	79.5



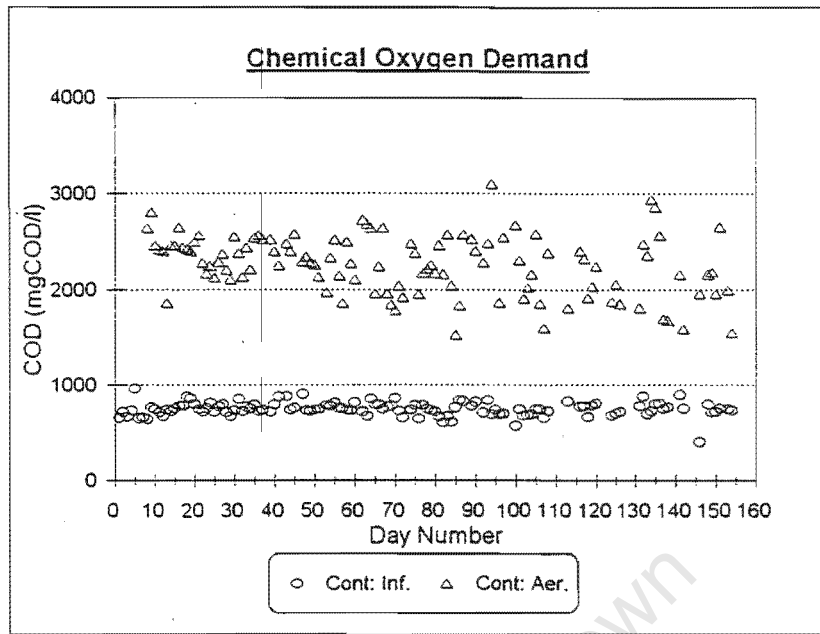


Figure D1: Daily influent and aerobic reactor COD concentrations in UCT system.

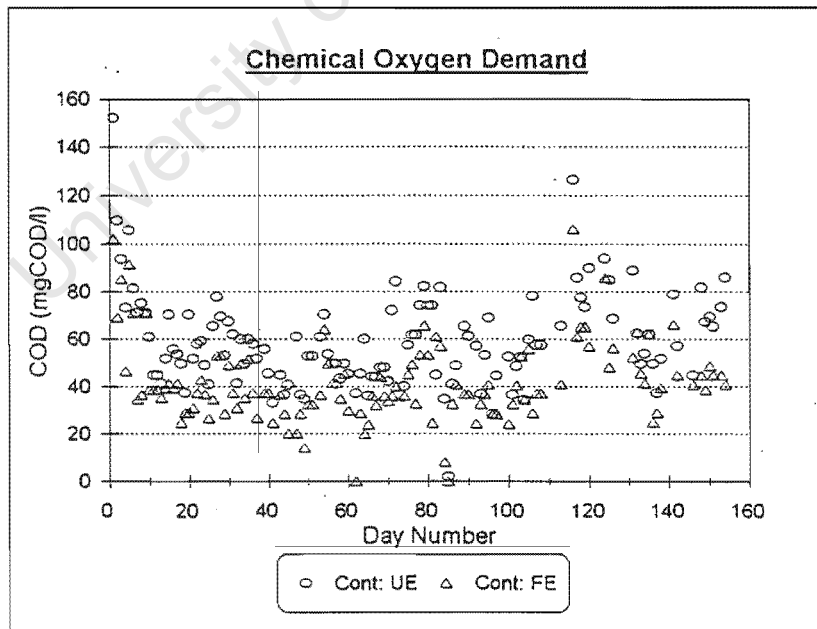


Figure D2: Daily Unfiltered and filtered COD concentrations in UCT system.

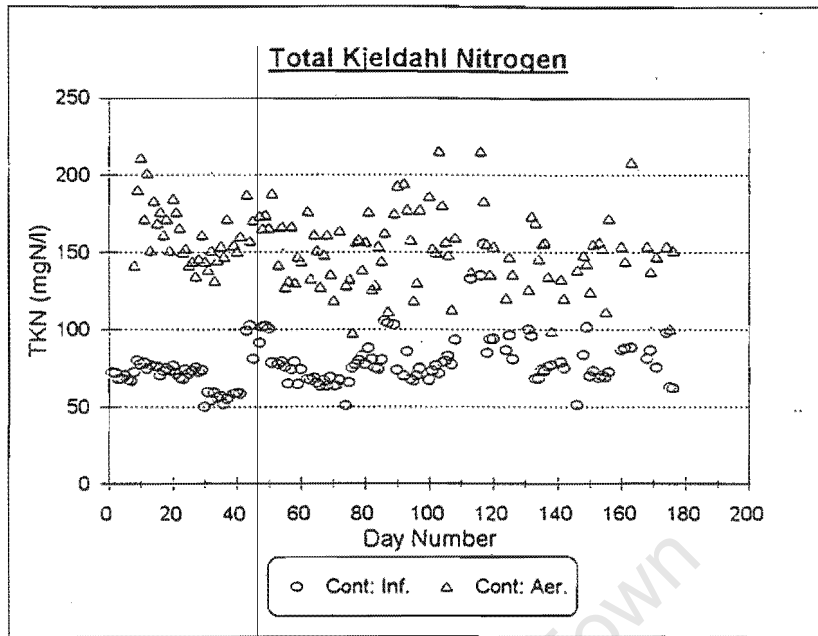


Figure D3: Daily influent and aerobic reactor TKN concentrations in UCT system.

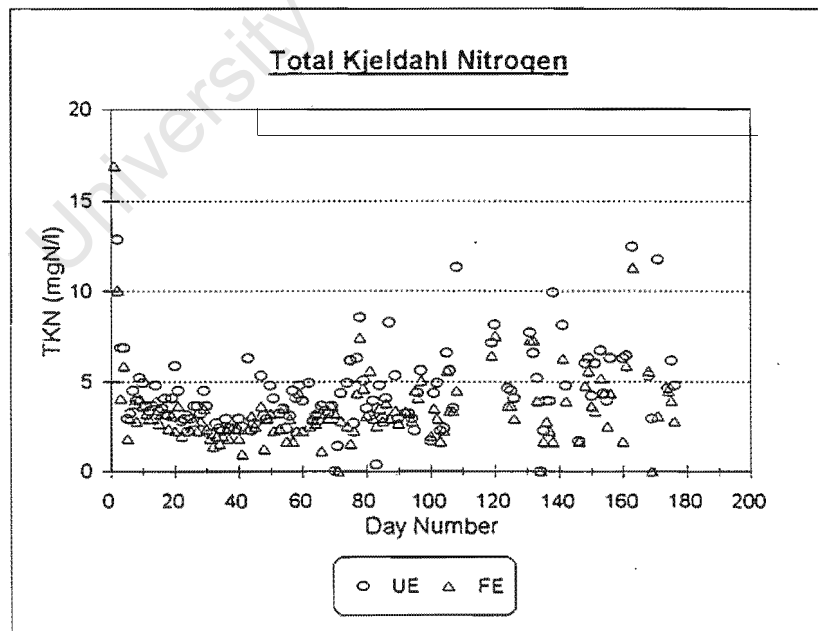


Figure D4: Daily Unfiltered and filtered effluent TKN concentrations in UCT system.

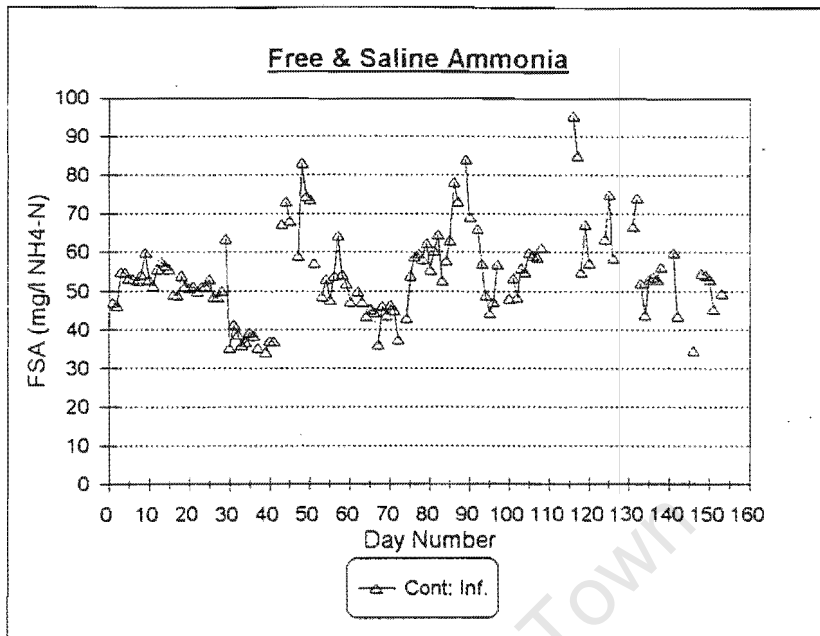


Figure D5: Daily influent Ammonia concentration in UCT system.



Figure D6: Daily Unfiltered and filtered Ammonia concentrations in UCT system.

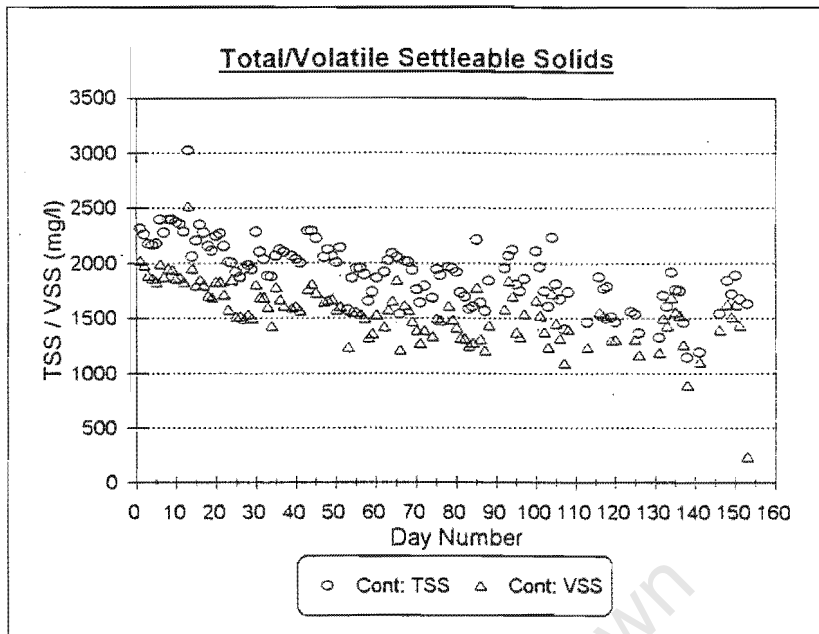


Figure D7: Daily aerobic reactor mixed liquor Total and Volatile Suspended Solids concentrations

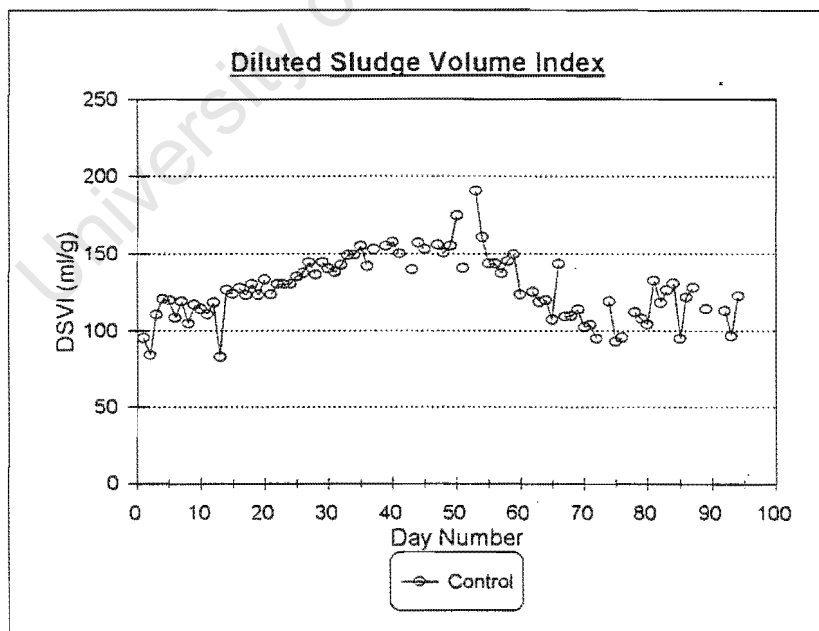


Figure D8: Daily aerobic reactor Diluted Sludge Volume Index in UCT system

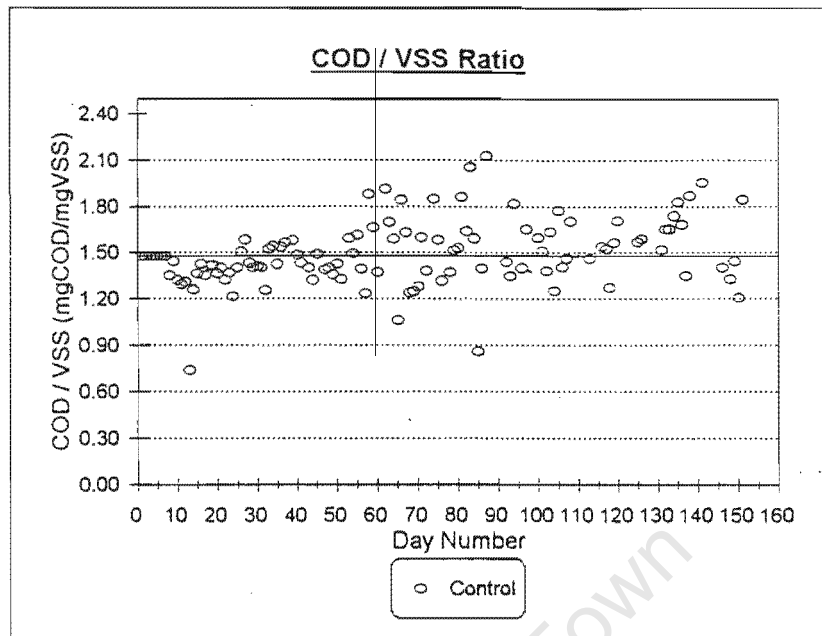


Figure D9: Daily COD/VSS ratio in UCT system

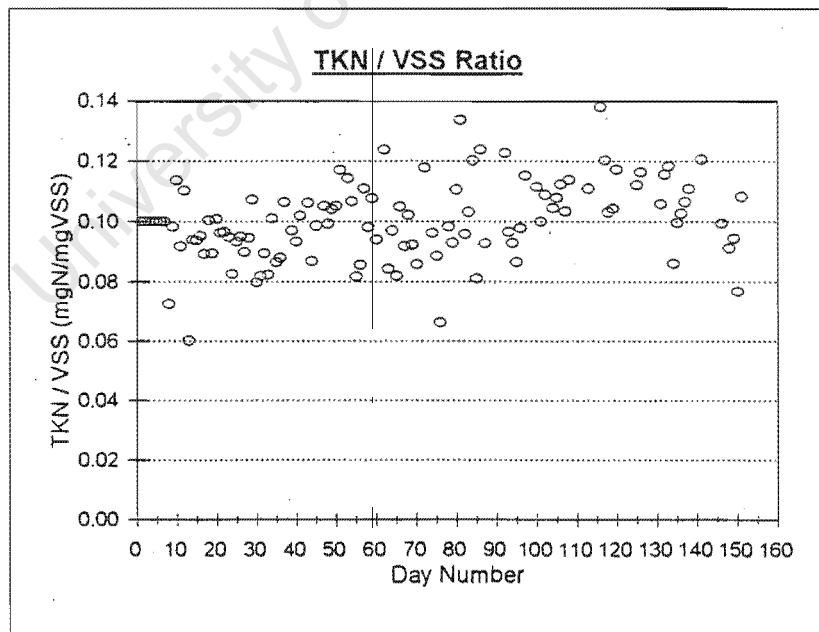


Figure D10: Daily TKN/VSS ratio in UCT system

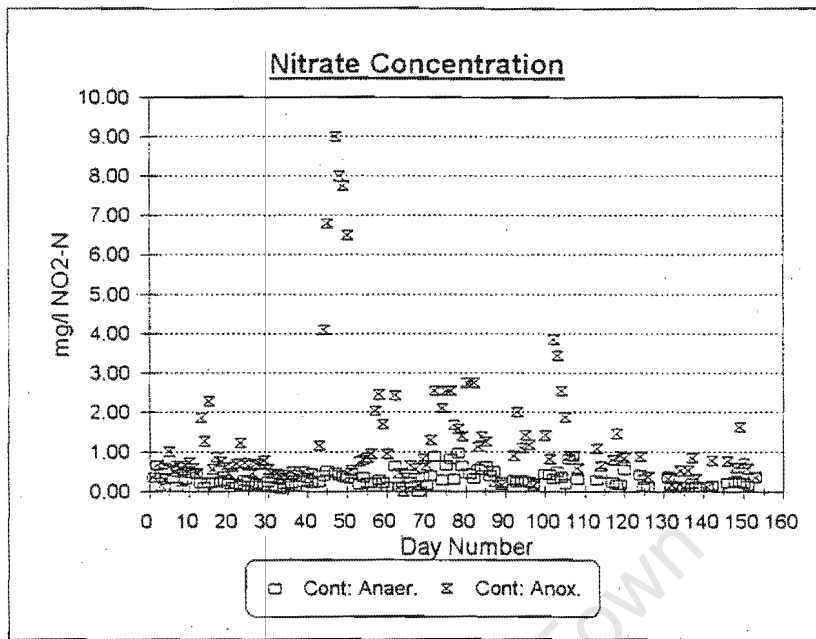


Figure D11: Daily anaerobic and anoxic reactor nitrate concentrations in UCT system.

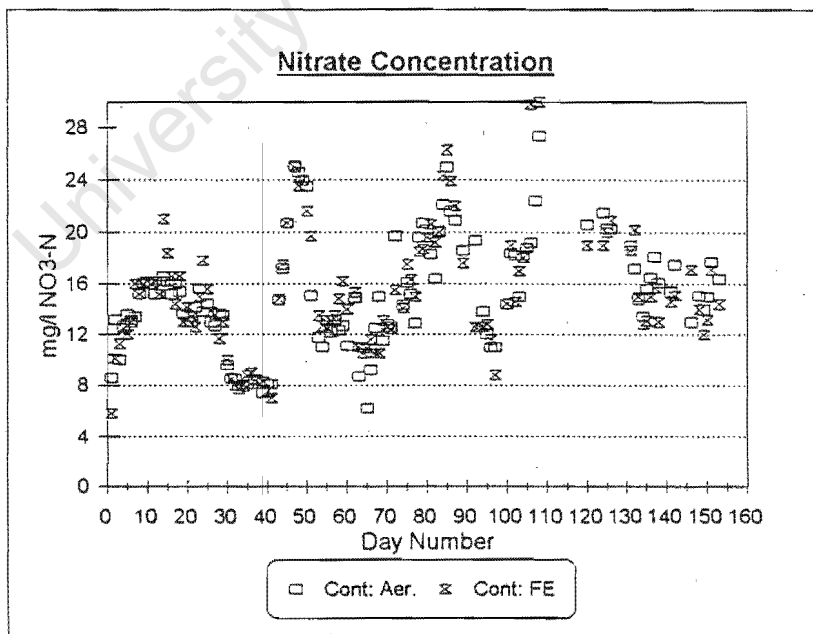


Figure D12: Daily aerobic and effluent reactor nitrate concentrations in UCT system.

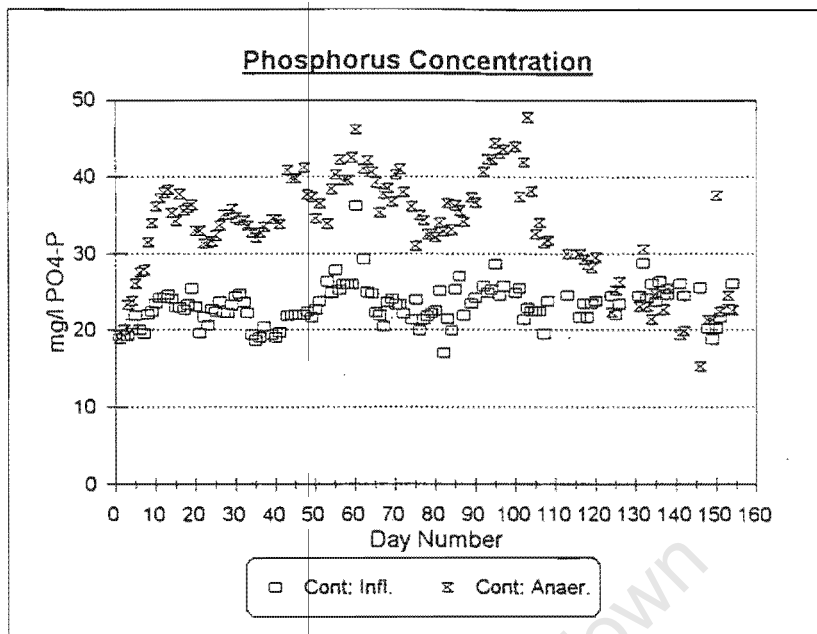


Figure D13: Daily influent and filtered anaerobic Total P concentrations in UCT system.

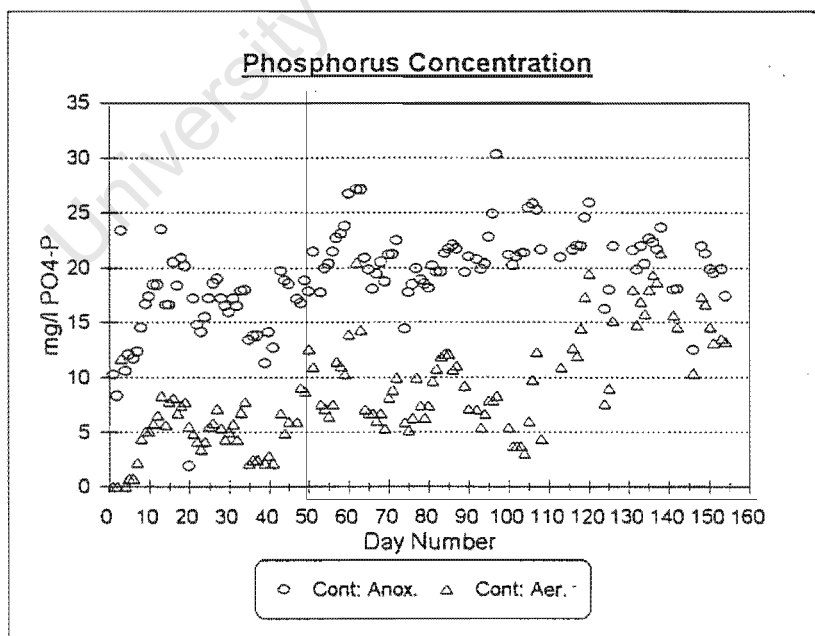


Figure D14: Daily filtered anoxic and aerobic Total P concentrations in UCT system.

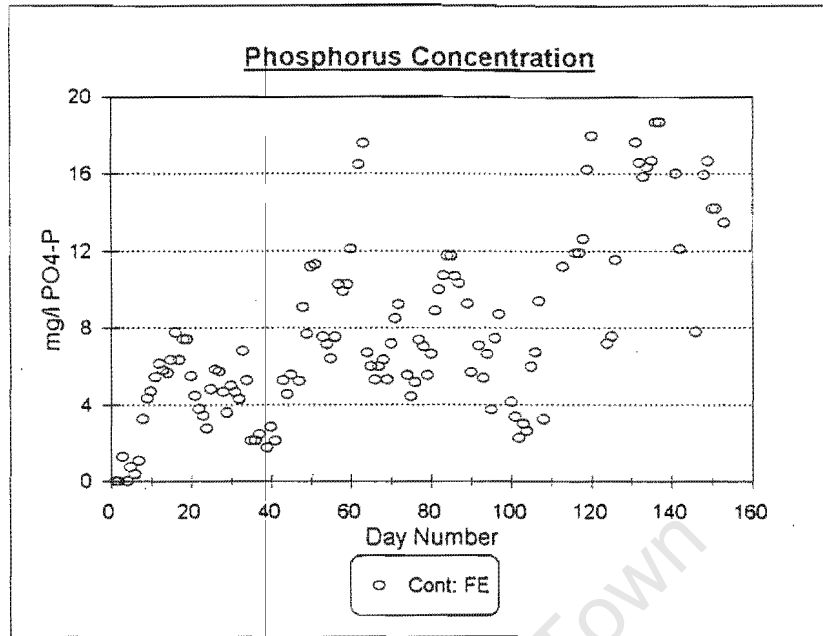


Figure D15: Daily filtered effluent Total P concentrations in UCT system.

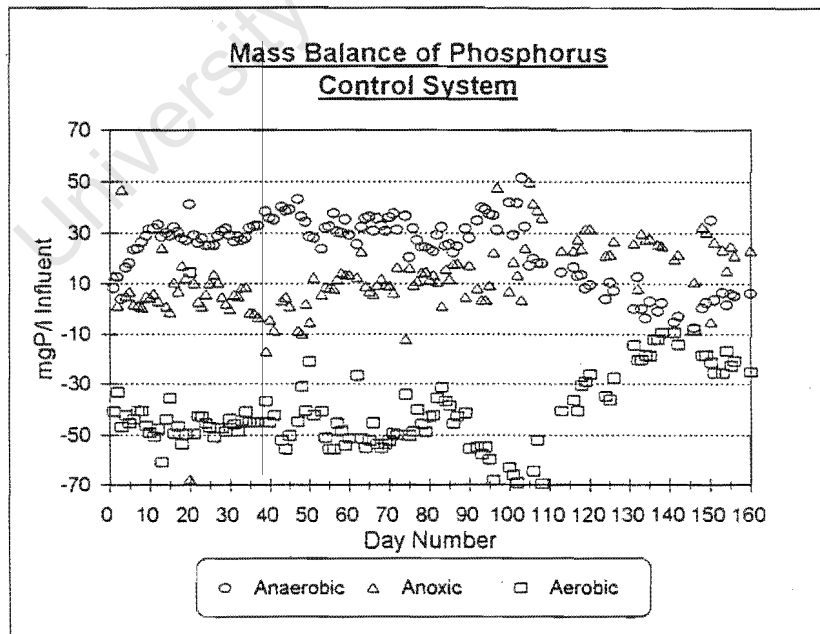


Figure D16: Daily Mass Balance of Total P UCT system.

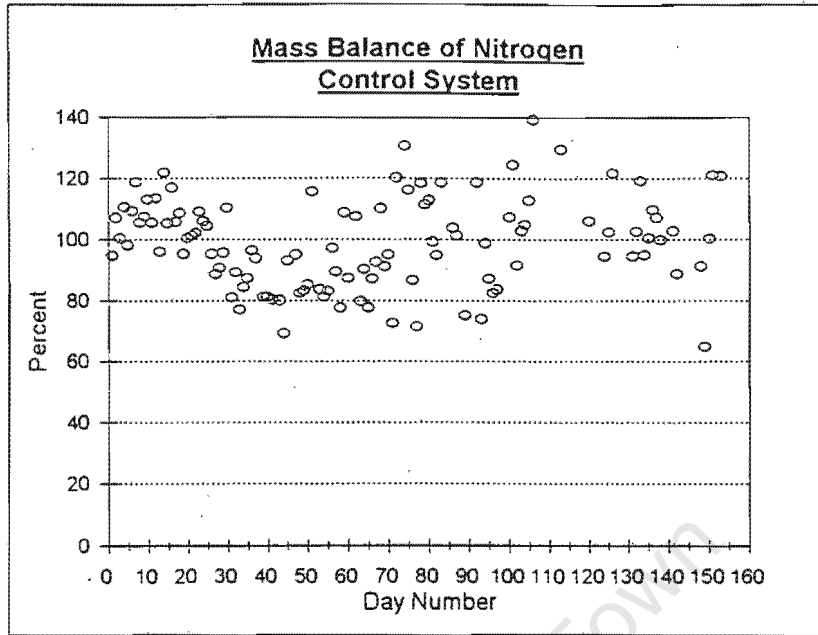


Figure D17: Daily Nitrogen Mass Balance of UCT system

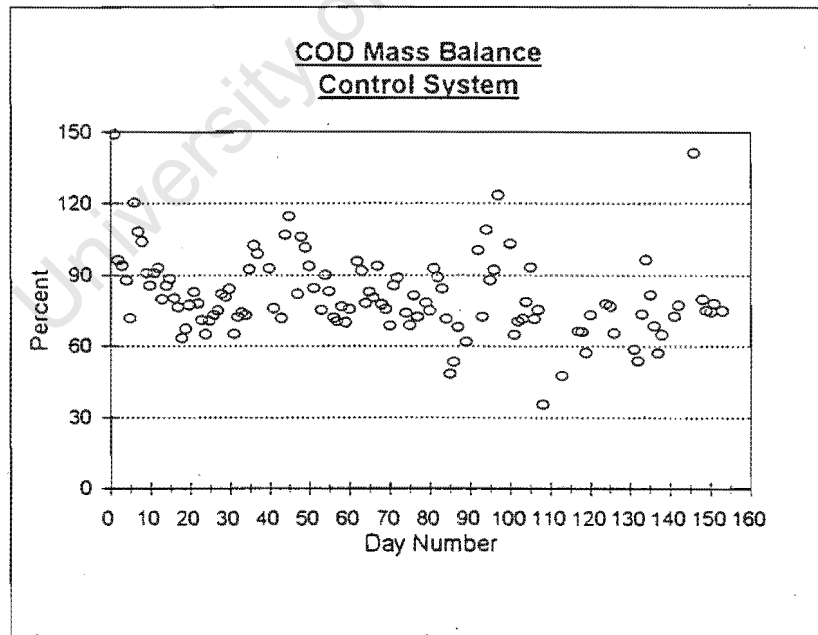


Figure D18: Daily COD Mass Balance of UCT system

## **APPENDIX E**

- Average Sewage Batch Results of UCT Control System.
- Figures E1 to E14 : Graphs of Average Sewage Batch Results.



Average sewage batch results for UCT control system.

Sewage Batch	DSVI	TSS	VSS	COD/VSS	TKN/VSS	FSA			TKN			COD				Nitrate (mg NO <sub>3</sub> -N/l)			Phosphorous (mg PO <sub>4</sub> -P/l)				Phosphorous Mass Balance				N MB	COD MB				
						Influent mgN/l	UE mgN/l	FE mgN/l	Influent mgN/l	Reactor mgN/l	UE mgN/l	FE mgN/l	Influent mgCOD/l	Reactor mgCOD/l	UE mgCOD/l	FE mgCOD/l	Anaerobic	Anoxic	Aerobic	Filtered Effluent	Influent	Anaerobic	Anoxic	Aerobic	Filtered Effluent	Anaerobic mgP/l infl			Anoxic mgP/l infl	Aerobic mgP/l infl	Settler mgP/l infl	Removal mgP/l infl
2	110	2325	1943	1.36	0.10	53.769	3.569	2.784	73.323	177.430	6.059	4.779	719.191	1950.336	76.434	55.982	0.387	0.803	14.160	14.327	21.862	30.143	13.734	4.238	3.013	23.049	8.059	-44.464	-2.490	18.8	107.1	96.4
3	127	2230	1777	1.40	0.10	50.820	2.604	2.044	73.752	168.980	4.116	2.828	818.931	2481.600	53.354	32.674	0.240	0.644	14.640	14.960	23.474	35.786	16.344	7.106	6.894	31.734	-4.064	-36.952	-0.424	16.6	105.4	72.9
4	133	2020	1632	1.40	0.09	50.488	1.750	1.490	71.943	151.288	3.343	2.320	754.826	2280.970	58.925	39.441	0.183	0.719	13.800	14.188	21.881	32.933	16.681	5.048	4.434	27.303	7.444	-46.334	-1.238	17.4	99.6	74.7
5	145	2038	1647	1.44	0.09	41.283	2.100	1.698	57.663	146.563	2.818	2.118	752.764	2366.190	56.433	39.934	0.152	0.494	9.038	9.138	21.904	33.815	16.131	4.809	4.230	29.595	3.409	-45.290	-1.158	17.7	90.2	80.5
6	151	1747	1632	1.07	0.07	42.252	1.568	0.784	66.080	164.920	3.304	1.876	801.548	2475.592	46.166	32.540	0.228	0.570	9.360	9.200	20.080	35.440	14.302	3.240	2.888	36.498	-5.850	-44.248	-0.704	17.2	83.3	67.8
7	158	1823	1686	1.40	0.10	71.983	2.520	1.797	96.610	167.883	3.502	2.777	766.743	2357.120	43.688	24.045	0.418	7.023	22.517	22.050	22.097	38.382	17.970	7.850	7.212	36.697	-2.613	-40.480	-1.277	14.9	84.7	100.7
8	143	1716	1475	1.32	0.09	52.335	2.890	2.075	73.105	150.245	3.742	2.609	754.732	2294.555	50.667	36.770	0.273	1.264	12.733	14.209	26.953	40.198	22.860	10.987	10.588	30.582	11.929	-47.491	-0.798	16.4	91.9	80.5
9	123	1893	1573	1.50	0.09	44.473	2.753	2.053	65.987	146.533	3.173	2.427	813.333	2280.000	46.667	26.667	0.187	0.330	8.767	11.029	22.967	38.390	19.553	6.800	6.007	34.267	7.320	-50.893	-1.647	17.0	85.0	80.5
10	105	1859	1454	1.40	0.08	42.360	1.913	1.400	65.637	145.600	2.660	1.637	755.333	2030.000	56.333	37.000	0.318	1.005	14.017	12.433	22.827	38.722	20.388	7.490	7.093	34.028	10.518	-52.393	-0.799	15.7	96.9	81.7
11	112	1817	1414	1.47	0.09	57.008	2.892	2.968	75.404	140.140	4.446	3.682	710.012	2282.904	65.075	47.852	0.543	1.123	17.380	17.950	21.687	33.733	18.532	8.056	7.134	27.247	9.082	-41.904	-1.844	14.6	106.0	79.5
12	115	1519	1579	1.32	0.10	52.700	2.220	2.558	71.820	163.391	3.320	3.360	706.533	2493.067	48.767	30.799	0.279	1.164	13.457	12.700	25.676	42.931	22.877	6.940	6.169	37.310	16.643	-63.749	-1.543	19.5	93.1	98.3
13	131	1777	1391	1.49	0.12	55.860	2.900	1.974	77.260	159.629	4.120	3.240	707.630	2063.006	52.514	40.219	0.501	2.051	18.600	21.171	22.363	37.639	22.920	6.031	4.764	29.994	27.260	-67.554	-2.334	17.6	118.4	75.1
14	126	1740	1400	1.70	0.11	61.320	2.100	1.680	93.520	159.600	11.340	4.480	724	2385	58	37	0.310	0.390	27.400	30.000	23.820	31.760	21.560	4.370	3.250	18.040	36.120	-69.320	-2.160	20.6	149.5	35.5
15	157	1703	1441	1.51	0.12	95.107	31.453	30.333	141.027	178.733	39.299	37.987	796.393	2180.693	92.650	69.467	0.337	0.837	38.933	34.467	23.220	29.720	21.340	11.790	11.670	14.680	24.680	-39.000	-0.240	11.5	135.2	57.0
16	147	1590	1374	1.52	0.11	59.920	11.947	9.893	91.000	148.400	13.720	12.367	753.440	2067.200	80.240	62.560	0.303	1.070	34.667	31.667	22.962	25.580	24.154	17.070	15.623	16.384	29.130	-28.336	-2.893	7.3	174.6	65.6
17	170	1500	1292	1.27	0.09	67.676	3.328	3.444	91.980	140.560	5.488	4.956	751.548	2016.384	79.650	61.186	0.240	0.416	19.660	19.740	24.624	28.458	19.512	12.888	12.096	6.840	20.808	-26.496	-1.584	12.5	103.1	66.6
18	177	1548	1353	1.73	0.11	52.033	3.045	2.065	73.975	139.300	4.760	2.817	773.974	2232.053	53.480	44.203	0.148	0.420	13.925	14.288	25.004	47.583	21.100	17.339	16.794	49.061	-24.742	-14.245	-1.490	8.2	102.8	74.0
19	130	1544	1394	1.40	0.10	34.580	1.160	0.800	51.240	138.600	1.680	1.880	399.800	1958.400	44.000	40.800	0.230	0.760	13.500	15.250	15.250	12.410	10.770	7.800	-7.430	10.830	-8.160	-5.140	17.7	141.9	74.9	
20	152	1781	1350	1.46	0.09	51.870	3.333	2.450	66.500	142.800	5.635	4.340	746.100	2238.900	70.900	44.360	0.220	0.888	15.450	14.075	20.208	25.613	20.650	15.420	15.243	10.367	21.183	-29.920	-0.355	5.0	94.4	76.8
21	164	1632	1098	3.21	0.24	49.945	8.470	7.297	70.210	148.400	5.318	4.095	740.350	2073.775	82.360	59.970	0.380	0.350	16.400	14.400	23.488	23.833	19.388	14.033	13.783	4.790	21.208	-21.480	-0.500	9.7	120.8	74.9
22	145	1685	1261	2.73	0.20	58.917	4.867	2.427	84.513	157.500	7.537	4.597	757.033	2091.667	72.783	52.550	ERR	ERR	ERR	ERR	21.007	20.768	14.068	13.855	13.133	6.642	13.025	-10.447	-1.403	7.9	74.8	74.8
23	153	1391	1304	0.02	0.12	48.253	6.653	6.653	78.299	153.333	5.160	3.733	791.067	1491.253	87.633	74.133	ERR	ERR	ERR	ERR	20.117	20.360	20.368	18.590	23.147	-29.493	-4.960	9.6				

Average 139 1824 1531 1.51 0.10 52 3.02 2.12 73.28 153.36 4.12 3.28 754.60 2242.28 58.94 48.85 0.29 1.27 14.71 14.71 22.94 35.04 19.05 8.66 8.82 28.09 7.85 -41.56 -1.27 14.92 99.00 80.10

Averages above are from start to end of study excluding sewage batches 14, 15, 16 and 19 as these were periods when the influent wastewater was septic and many operational problems were encountered.

ES<sub>up</sub> and DBGP calculation for the UCT system using Wenzel et al. (1999) model

Sewage Batch	R <sub>a</sub>	INPUT ES <sub>up</sub>	INPUT ES <sub>up</sub>	ES <sub>up</sub>	NO <sub>3x</sub>	S <sub>bi</sub> mgCOD/l	S <sub>sp</sub> mgCOD/l	S <sub>bi</sub> mgCOD/l	S <sub>sp</sub> mgCOD/l	INPUT S <sub>sp</sub> mgCOD/l	MX <sub>h</sub> Y <sub>Q</sub> 9h retention	S <sub>sp</sub>	MS <sub>sp</sub> mgCOD/d	MS <sub>sp</sub> mgCOD/d	MX <sub>h</sub> c mgAESS	MX <sub>h</sub> c mgAESS	δPc mgP/l infl	MX <sub>h</sub> mgAESS	MX <sub>h</sub> mgAESS	δP <sub>h</sub> mgP/l infl	MX <sub>i</sub> mgAESS	δP <sub>i</sub> mgP/l infl	δP <sub>h</sub> (annex) mgP/l infl	δP <sub>i</sub> (annex) mgP/l infl	MX <sub>h</sub> (annex) mgVSS	MX <sub>i</sub> (annex) mgVSS	ES <sub>up</sub> ES <sub>up</sub>	ES <sub>up</sub> ES <sub>up</sub>	Known Parameters	
																														K
2	10	0.848	6.612	0.08	0.81	719.19	49.62	614.30	102.80	97.27	714.84	11.13	1483.58	10788.11	4768.65	476.87	14.66	14278.78	6833.62	3.17	6608.78	0.99	18.85	18.82	33070.67	33083.49	0.43	0.14	K	0.86
3	10	-7.865	0.563	0.04	0.64	818.93	784.26	92.00	82.00	950.72	7.94	1258.77	14366.38	4367.48	436.75	12.58	19044.32	9136.87	4.22	2448.09	0.46	17.45	17.45	27735.50	27782.18	0.56	0.13	Q	20/d	
4	8	0.03	0.563	0.04	0.72	754.83	21.89	692.74	89.25	86.76	771.03	9.70	1347.26	12322.66	3674.35	293.95	12.98	15478.87	5938.53	4.01	2448.09	0.46	17.45	17.45	27735.50	27782.18	0.56	0.13	r	1
5	8	0.063	1.297	0.04	0.49	757.76	40.65	672.91	40.31	36.78	794.19	4.62	574.60	12868.62	1567.08	125.37	12.73	15865.42	6092.32	4.12	4313.13	0.81	17.67	17.65	28083.25	28144.70	0.57	0.06	Y <sub>h</sub> c	0.45
6	8	0.831	7.875	0.04	0.57	801.55	25.65	734.16	37.22	0.00	905.13	0.00	0.00	14467.11	0.00	0.00	18082.74	6943.77	4.69	2686.27	0.59	17.19	5.20	27744.00	27799.43	0.65	0.03	f <sub>h</sub>	0.13	
7	8	0.443	8.775	0.03	7.03	766.74	32.20	709.73	36.90	47.48	828.84	5.02	749.08	13468.82	2042.95	163.44	9.93	16593.52	6372.68	4.31	3564.32	0.67	14.88	14.90	28656.33	28656.03	0.59	0.07	f <sub>sp</sub> c	0.23
8	8	-7.851	0.455	0.05	1.26	754.73	717.96	102.47	100.95	0.00	788.08	11.10	1574.83	12784.40	4395.00	343.60	12.28	15761.59	6052.45	4.09	0.00	0.00	16.37	16.37	25082.73	26452.64	0.60	0.16	bc	0.04
9	8	-7.875	0.34	0.02	0.33	813.33	786.67	142.80	137.24	0.00	836.19	14.41	2168.46	13564.87	5913.98	473.12	12.66	16723.82	6421.95	4.34	0.00	0.00	16.96	17.00	26746.67	29532.86	0.57	0.20	f <sub>sp</sub> bc	0.2
10	8	-7.847	0.595	0.05	1.81	753.33	718.33	92.00	71.74	0.00	816.10	7.68	1127.76	12318.91	3075.70	246.06	11.48	16221.94	6267.63	4.24	0.00	0.00	15.73	15.72	24712.33	25911.33	0.63	0.12	ES <sub>up</sub>	0.03
11	8	-7.837	0.405	0.07	2.12	710.01	662.16	109.98	101.83	0.00	720.42	12.00	1556.46	11686.74	4244.89	339.1														

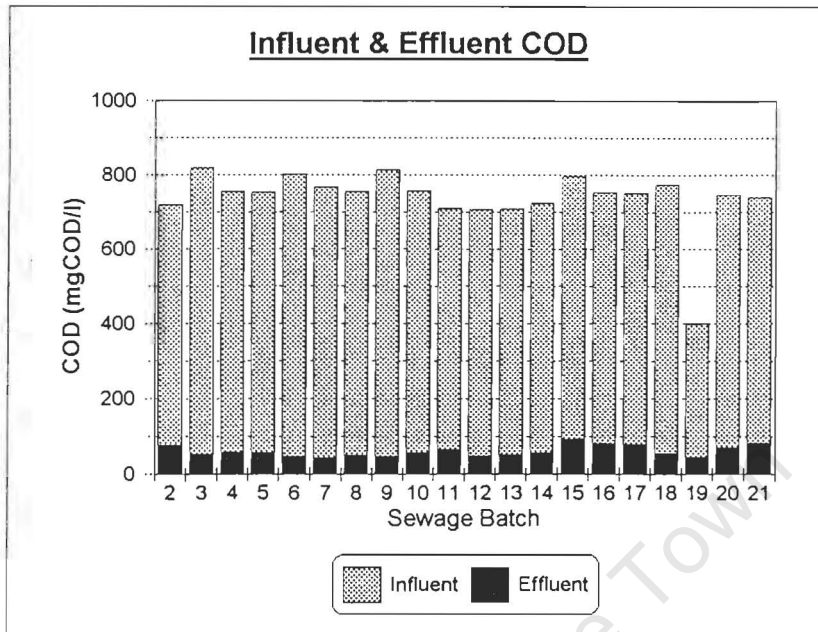


Figure E1: Average sewage batch influent and effluent COD concentrations in UCT system.

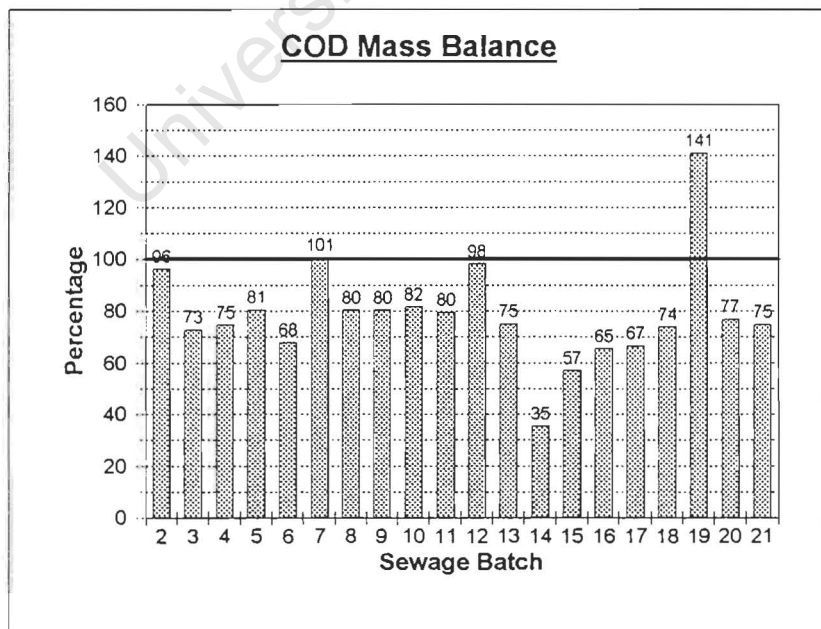


Figure E2: Average sewage batch COD Mass Balance in UCT system.

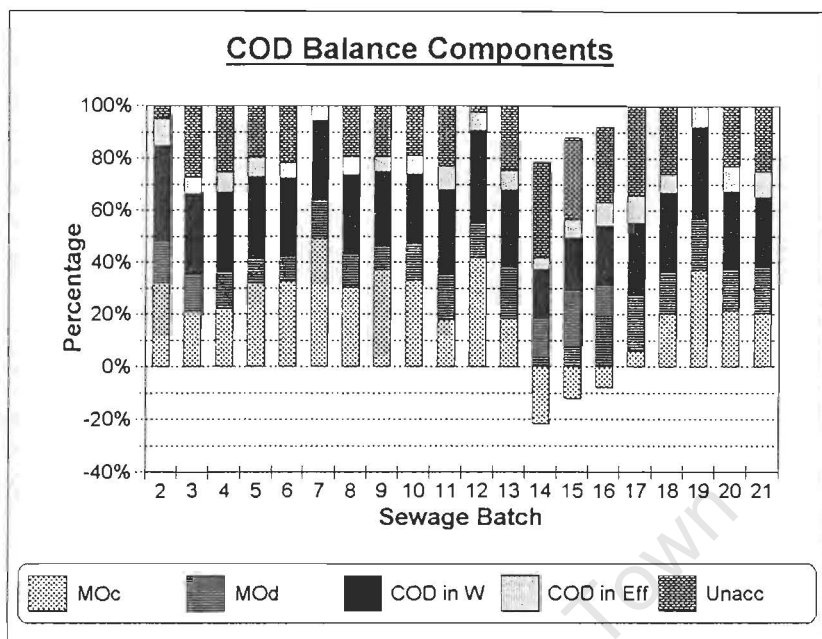


Figure E3: Average sewage batch COD Mass Balance Components in UCT system.

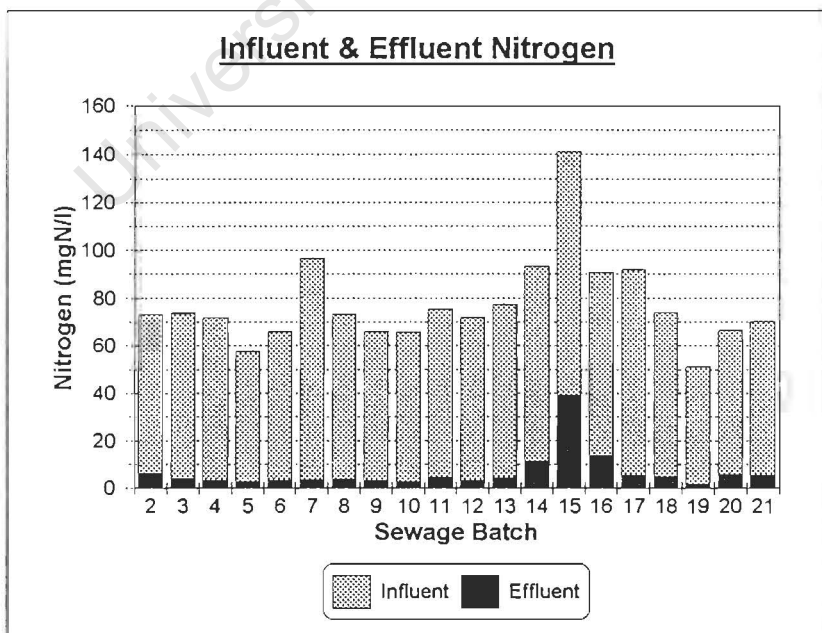
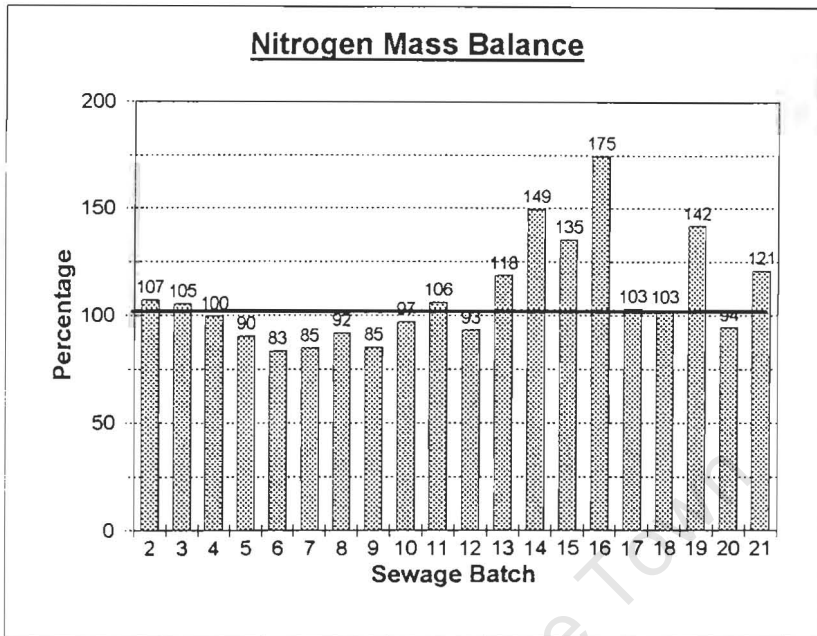
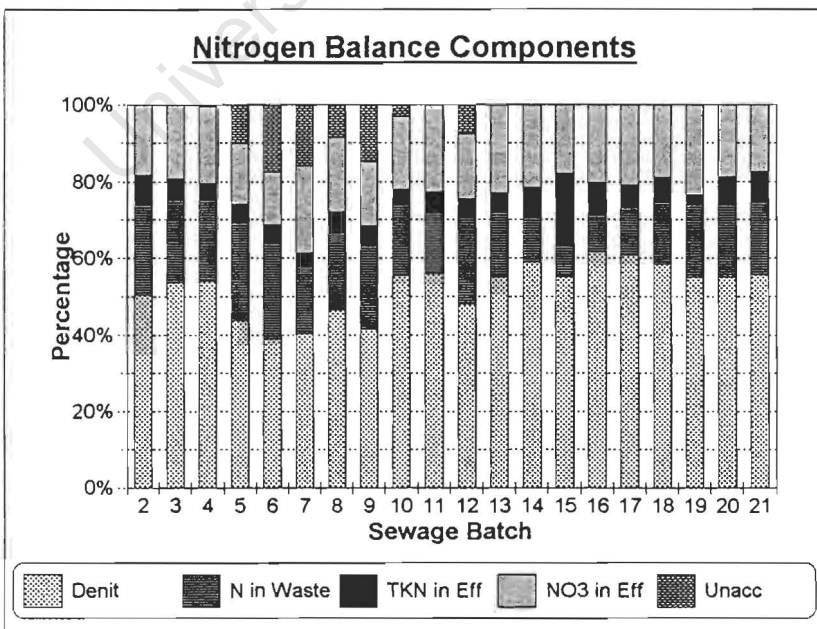


Figure E4: Average sewage batch influent and effluent Nitrogen concentrations in UCT system.



**Figure E5:** Average sewage batch Nitrogen Mass Balance in UCT system.



**Figure E6:** Average sewage batch Nitrogen Mass Balance Components in UCT system.

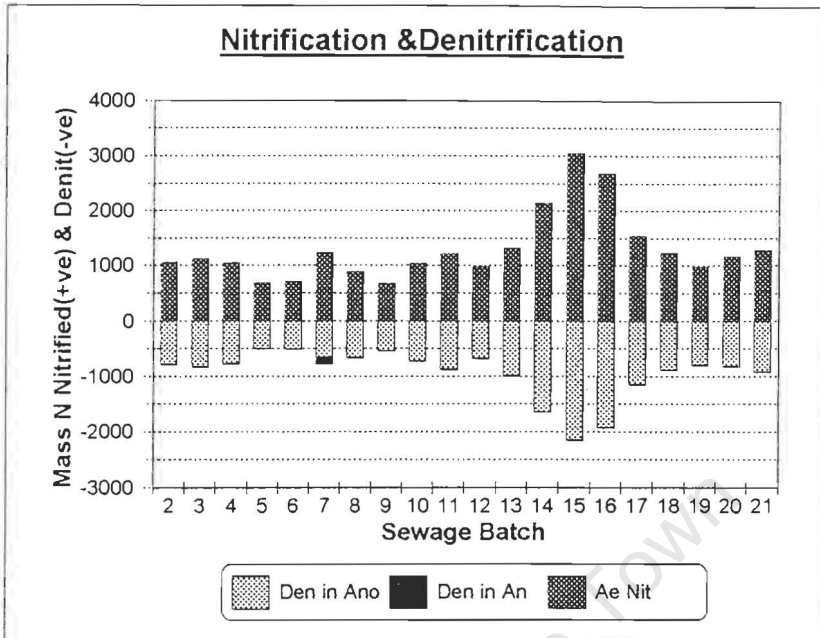


Figure E7: Average sewage batch Nitrification and Denitrification in UCT system.

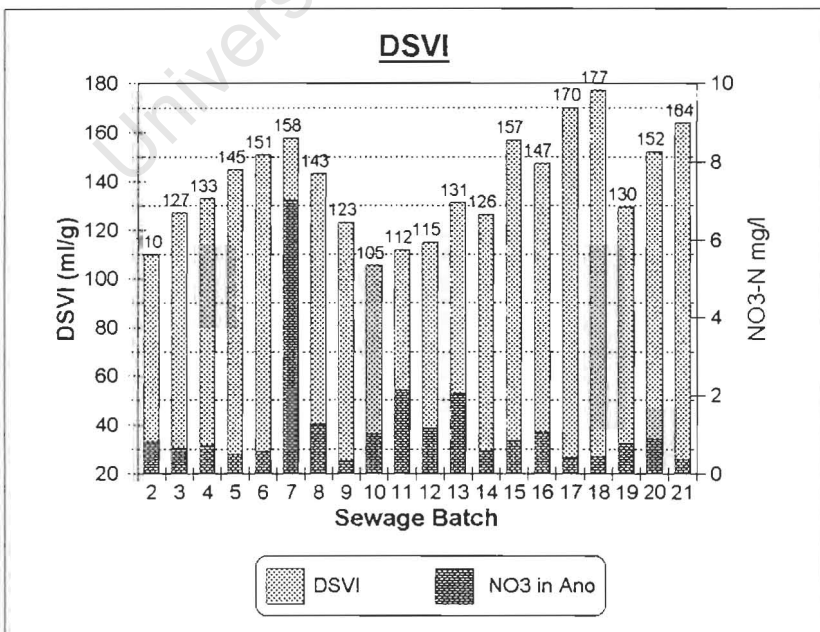


Figure E8: Average sewage batch Diluted Stirred Volume Index and Anoxic Nitrate concentration in UCT system

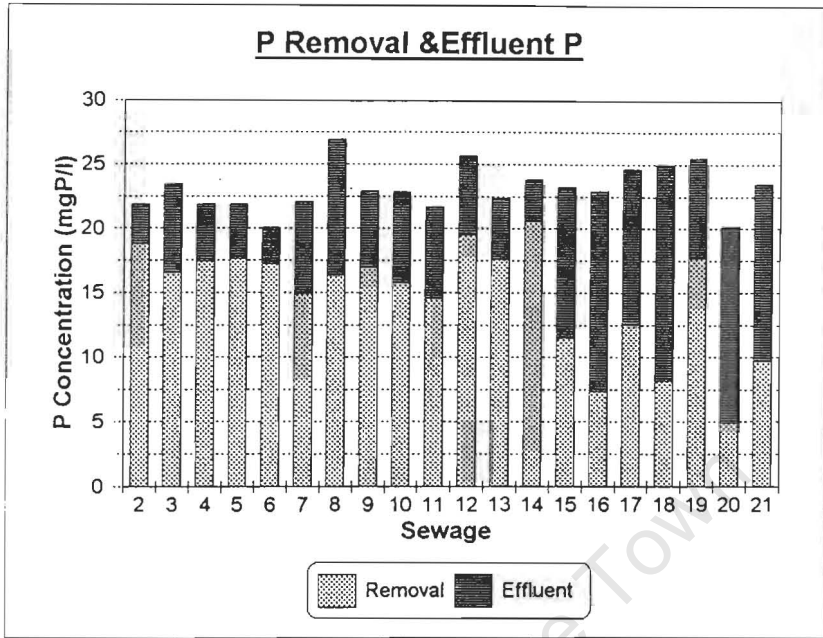


Figure E9: Average sewage batch P Removal and Effluent P in UCT system.

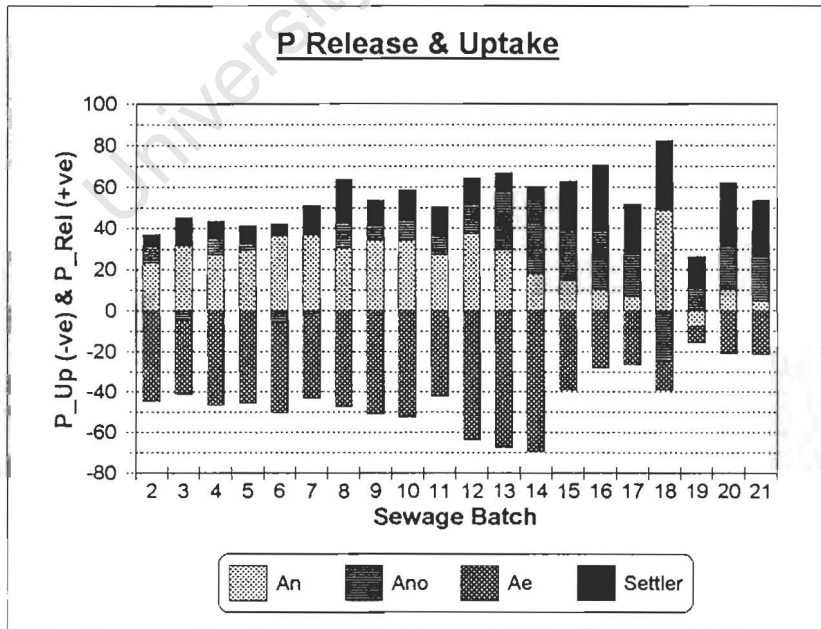


Figure E10: Average sewage batch P Release and Uptake in UCT system.

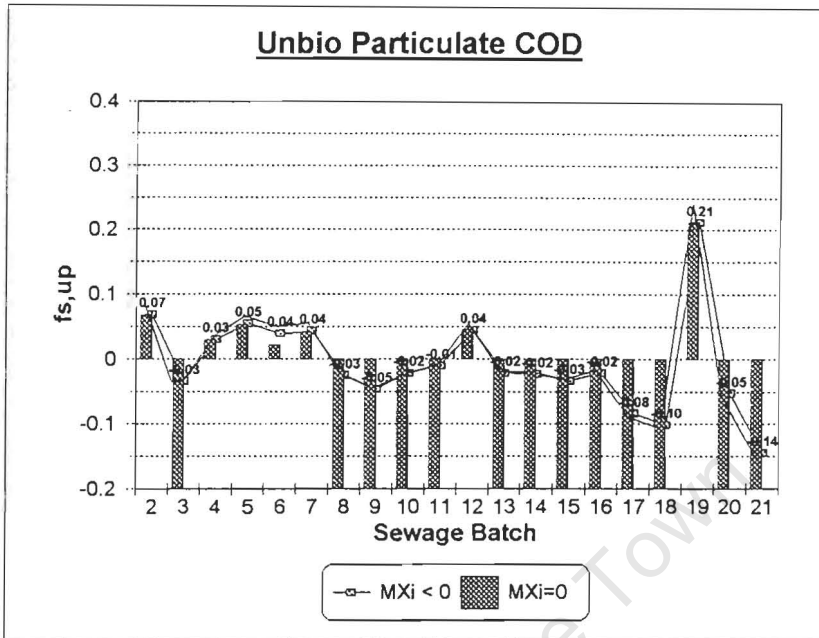


Figure E11: Average sewage batch unbiodegradable particulate fraction in UCT system.

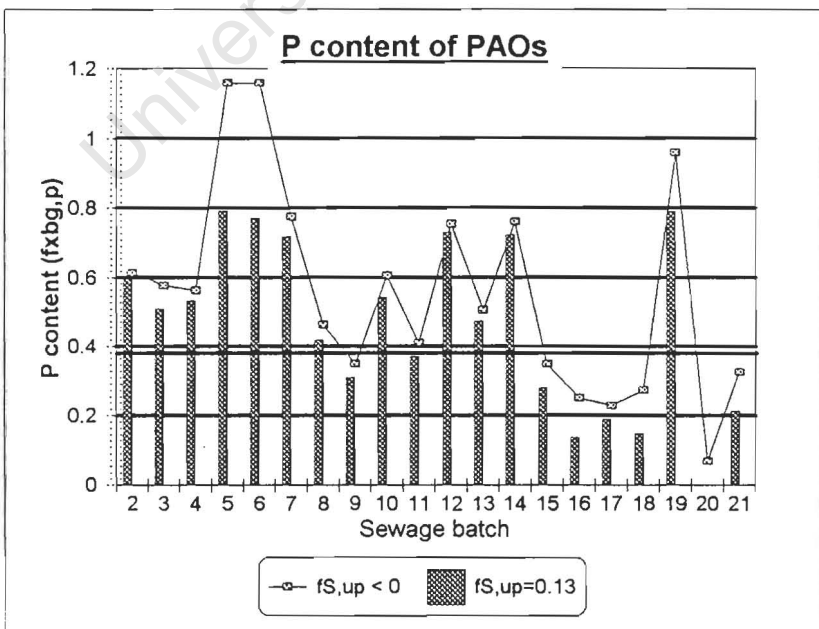


Figure E12: Average sewage batch P content of PAOs in UCT system.

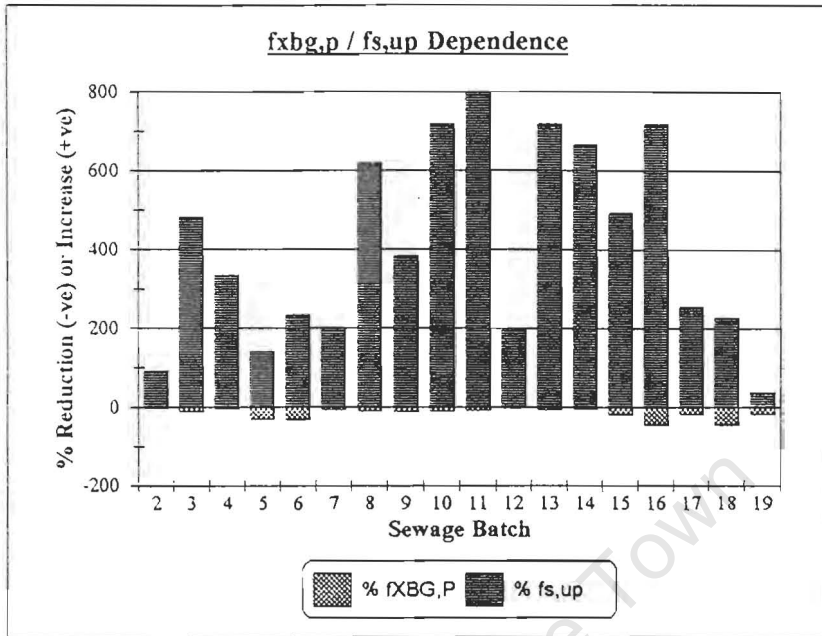


Figure E13: Average sewage batch fXBG,P and fs,up dependence on fs,up fraction equal to 0.13 in UCT system

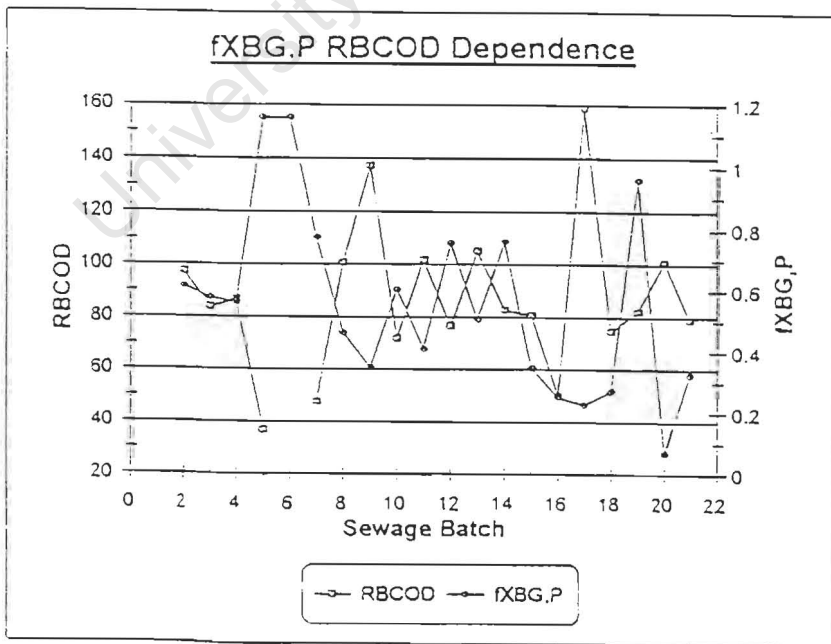


Figure E14: Average sewage batch fXBG,P dependence on influent RBCOD concentration.

## **APPENDIX F**

- Filament Identification in the External Nitrification and UCT Control Systems.

University of Cape Town

Table F 1: Filaments identified<sup>1</sup> in the external nitrification (EXT) and UCT Control (CTL) systems

Date & (Day)	Sewage Batch	DSVI		System	EXT System	CTL System
		EXT	CTL			
24/2/98 (1)	1	107	-	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary	type 1701	type 1701; type 0092
				Abundance	common; common	common; some; few
				Morphology	weak, irregular and	weak, irregular and
				Floc	100 - 150 $\mu\text{m}$	< 150 $\mu\text{m}$
23/03/98 (28)	3	87	137	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary	type 0092	type 0092; <i>Norcadia</i> sp; <i>H.hydroxsis</i>
				Abundance	some; few	common; some; few; few
				Morphology	weak, irregular and diffuse	weak, irregular and diffuse
				Floc Diameter	< 150 $\mu\text{m}$	< 150 $\mu\text{m}$
22/04/98 (58)	8	74	143	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary	type 021N; type 0092	type 021N
				Abundance	common; some; few	common; some
				Morphology	weak, irregular and diffuse	weak, irregular and diffuse
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$
20/05/98 (86)	12	73	131	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary	type 1851; <i>H.hydroxsis</i>	type 1851; type 0092; <i>H.hydroxsis</i>
				Abundance	some; few; few	common; some; few; few
				Morphology	weak, irregular and diffuse	firm
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$

<sup>1</sup>Filament identification according to Eikelboom and van Buisson (1981) and Jenkins *et al.* (1984).

## F.2

11/06/98 (108)	13	7	131	Dominant	<i>M.parvicella</i>	<i>M.parvicella; H.hydoisis</i>
				Secondary	type 1851	type 1851
				Abundance	common; common	common; few; some
				Morphology	weak, irregular and diffuse	firm, round and compact
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$
27/07/98 (154)	20	83	152'	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary		
				Abundance	some	few
				Morphology	weak, irregular and diffuse	firm, round and compact
				Floc Diameter	150 - 500 $\mu\text{m}$	> 500 $\mu\text{m}$
19/08/98 (177)	23	105	166	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary		
				Abundance	some	few
				Morphology	weak, irregular and diffuse	firm, round and compact
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$
Monitoring of UCT system, which was operated for a different project was stopped on day 188 after completing sewage batch 23. This system was kept operating for later use and filament identification was continued.						
15/09/98 (204)	25	91'	-	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary		
				Abundance	few	common
				Morphology	weak, irregular and diffuse	firm, round and compact
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$
20/10/98 (239)	28	115'	-	Dominant	<i>S Natans</i>	type 1701
				Secondary	<i>M.parvicella; type 1701</i>	<i>M.parvicella</i>
				Abundance	some; few; few	some; some

				Morphology	weak, irregular and diffuse	firm, round and compact
				Floc Diameter	< 150 $\mu\text{m}$	150 - 500 $\mu\text{m}$
24/11/98 (275)	29	108	-	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary	type 1851	type 1851
				Abundance	some; some	some; some
				Morphology	weak, irregular and diffuse	weak,irregular and diffuse
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$
20/12/98 (300)	31	64'	-	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary		
				Abundance	few	some
				Morphology	weak, round and compact	weak, round and compact
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$
18/01/99 (329)	34	140'	-	Dominant	<i>M.parvicella</i>	<i>M.parvicella</i>
				Secondary		Thiothrix sp
				Abundance	some	common; few
				Morphology	weak, irregular and diffuse	weak, round and compact
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$
22/02/99 (364)	37	99	-	Dominant	type 1851	<i>M.parvicella</i>
				Secondary	<i>M.parvicella</i>	type 1851
				Abundance	common; some	very common; common
				Morphology	weak and rounded	
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$
Monitoring of External nitrification system stopped on day 373 after completing sewage batch 37. The system was kept operating for later use and filament identifications were continued.						

EXT System				Aerobic Reactor	Nitrification Reactor	
24/03/99				Dominant	type 1851	Thiothrix
				Secondary		
				Abundance	some	excessive
				Morphology	weak, irregular and diffuse	irregular: not true floc but clumps sheered of sides of unit
				Floc Diameter	> 150 $\mu\text{m}$	> 500 $\mu\text{m}$
EXT System				Aerobic Reactor	Nitrification Reactor	
28/04/99				Dominant	type 1851	type 1851
				Secondary	<i>M.parvicella</i>	<i>M.parvicella</i> ; type 021N
				Abundance	common; common	some; few; few
				Morphology	weak; irregular and diffuse	firm, round and compact
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$
EXT System				Aerobic Reactor	Nitrification Reactor	
27/05/99				Dominant	type 1851	<i>N. limcola</i>
				Secondary	<i>M.parvicella</i>	
				Abundance	some; few	some
				Morphology	firm, round and compact	firm, round and compact
				Floc Diameter	150 - 500 $\mu\text{m}$	150 - 500 $\mu\text{m}$